

Thermal characterization of a biodiesel nitration: Bio-additive's synthesis by calorimetric methods

Adji Diop, Imed Ben Talouba, Laurent Balland, Nordine Mouhab

▶ To cite this version:

Adji Diop, Imed Ben Talouba, Laurent Balland, Nordine Mouhab. Thermal characterization of a biodiesel nitration: Bio-additive's synthesis by calorimetric methods. Thermochimica Acta, 2019, 673, pp.138-146. 10.1016/j.tca.2019.01.024 . hal-02138408

HAL Id: hal-02138408 https://hal.science/hal-02138408v1

Submitted on 21 Oct 2021

HAL is a multi-disciplinary open access archive for the deposit and dissemination of scientific research documents, whether they are published or not. The documents may come from teaching and research institutions in France or abroad, or from public or private research centers. L'archive ouverte pluridisciplinaire **HAL**, est destinée au dépôt et à la diffusion de documents scientifiques de niveau recherche, publiés ou non, émanant des établissements d'enseignement et de recherche français ou étrangers, des laboratoires publics ou privés.



Distributed under a Creative Commons Attribution - NonCommercial 4.0 International License

Thermal characterization of a biodiesel nitration:
 bio-additive's synthesis by calorimetric methods

3 DIOP Adji, BEN TALOUBA Imed ^{*1}, BALLAND Laurent, MOUHAB Nordine

4 Laboratoire de Sécurité des Procédés Chimiques (LSPC-EA4704), Normandie Univ, UNIROUEN, 76000
5 Rouen, France

6 Abstract

7 The aim of this study was to synthesize a substitute to the 2-Ethyl Hexyl Nitrate (EHN) by nitrating a biodiesel. EHN is commonly used to improve the auto-ignition properties of diesel 8 fuels. The biodiesel was obtained by trans-esterification of canola oil. The nitration reaction 9 was carried out in a reaction calorimetry RC1 with semi-batch mode to study its exothermic 10 behavior. Mixed sulfuric/nitric acid was used as nitrating agent. The impact of the synthesis 11 temperature on the thermal behavior and on the reaction medium composition was 12 investigated. The final product was analyzed by using several analytical techniques such as 13 14 iodine number, infrared spectrometry, GC-MS and mass spectrometry. This analytical study combined with the results of thermal stability study in DSC, allowed to highlight that 15 chemical transformations play an important role on the thermal reaction behavior and on the 16 17 Maximum Temperature of the Synthesis Reaction (MTSR). In addition to the mixed acid decomposition, the synthesis at high temperature involves the production of nitrated products: 18 methyl-8-nitro oleate, methyl-10-nitrate stearate, methyl-10-nitrate-9-nitrostearate. Also, the 19 Cooperative Fuel Research (CFR) engine was used to analyze the cetane number of diesel 20 fuel mixed with our additive according to the ASTM D613 standard. The results showed an 21 increase in cetane number of 3.2 points. 22

23

24 Keywords: methyl oleate, cetane number, reaction calorimeter, DSC, MTSR

25 **1** Introduction

The industrialization and motorization in recent years come along with a high demand for petroleum products and an increase in air pollution [1]. It has been established by the Interprofessional Center for Technical Studies of Atmospheric Pollution (CITEPA), in France, that the automotive sector (mainly diesel engines) plays a leading role in air pollution (CO_2, CO, NO_X, SO_2) .

31 To reduce the pollution related to diesel engines, several solutions have been tested including

- the setting up of catalytic oxidation pots, particles filters [2] and the use of additives, mainly
 cetane number improvers [3].
- 34 Cetane improver additives are commonly used to increase engine performances. According to
- Beatrice et *al* 1996 [4], an increase in the cetane number reduces NO_x and particle emissions.
- 36 There are a lot of cetane number improvers [5] [6] but the 2-EthylHexyl Nitrate (ENH) is the
- 37 main additive used for diesel. The EHN is an energy molecule obtained by nitration of iso-
- 38 octanol (fossil fuels) with mixed nitric/sulfuric acid (1:1.5 w/w).

^{*}imed.bentalouba@univ-rouen.fr

^{© 2019} published by Elsevier. This manuscript is made available under the CC BY NC user license https://creativecommons.org/licenses/by-nc/4.0/

39 Several studies showed that the iso-octanol nitration is a strongly exothermic reaction which

40 takes place in a heterogeneous liquid-liquid mixture [7] [8]. EHN additive is thermally

41 unstable and sensitive to heat. Its thermal instability is mainly due to energetic functional

42 groups like nitro (C–NO₂) and nitrate (C–O–NO₂). Those functional groups are composed of

43 easily broken C–N covalent bonds. In fact, according to Yang et al 2014 [9], several

44 industrial accidents in China are due to the loss of control during the EHN synthesis. The

- 45 thermal behavior of this reaction need to be carefully investigated to assess the associated
- 46 risks [10].

With the scarcity of fossil fuels, it is important to reduce the dependency on petroleum products. The goal of the work described in this article is to synthesize a substitute to the EHN by nitrating a trans-esterified vegetable oil (biodiesel). Many studies on the use of biodiesel as biofuels [11][12] or as bio-additive [13] have been realized over the years. The biodiesel's particularity is that it contains less carbon, less sulfide, less water and more oxygen atoms than fossil diesel. Therefore, it is less dangerous for humans [14] and its amount of oxygen atoms improves combustion [15].

54 In this article, the biodiesel obtained from canola oil was used. According to Abdullah et *al*

2010 [16], the presence of double bonds favors the nitration reaction. And the canola oil has a
lot of double bounds compared to the other vegetable oils. The classic mixed sulfuric/nitric

57 acid [17] (1.5:1 w/w) was used as the nitrating agent.

First, a study about the identification and the characterization of the chemical compounds that results from nitration by various analytical techniques (infrared spectrometer, GCMS, electro spray ionization mass spectrometer, and iodine index measurement) was conducted. Then, a complete study on the thermal stability of the reaction mixture (reagents and products) was realized. This study uses the thermal information given by a reaction calorimeter RC1 and a DSC type microcalorimeter. The quality of the synthesized bio-additive was determined by measuring its cetane number according to the ASTM standard D 613.

65 2 Materials and products

66 **2.1 Products**

The biodiesel (Diester®) used was obtained by trans-esterification of canola oil and was provided by Saipol company (Grand-Quevilly-France). Nitric (65%w/w), sulfuric (95% w/w) acids used as nitrating agent and solvents (potassium iodide 1% volumetric, sodium thiosulfate (Na₂S₂O₃) 0.1M, bicarbonate solution for analysis (>99.7%) and Wijs reactive 0.1 mol·L⁻¹) are provided by Fisher Chemical. The methyl nonadecanoate (> 98%) for GC analysis was supplied by Sigma Aldrich.

- 73 2.2 Materials
- 74 Calorimetric reactor RC1-*RTCal*

The nitration was carried out in a calorimetric reactor RC1-RTCal (Mettler®) operating in
 semi-batch mode. It is equipped with an AP00-0.5-RTCal reactor vessel with 0.5L capacity.

77 Mixing system is made of an impeller with one baffle. The experimental device is presented

in Fig. 1. The reactor has a temperature control system (between -20°C and +165°C) and an *RTCal* measurement technology based on thermal flow sensors located on the reactor wall.
The temperature regulation includes a thermostatic group which takes care of the various
regulation modes thanks to a fluid (Rodorsil 47 V20). This device provides real-time
monitoring of the heat released by the nitration reaction which is highly exothermic.



- 83
- 84

Fig. 1. Reaction calorimeter RC1-RTCal (Mettler®)

Differential Scanning Calorimeter DSC Q20

The reactive and products stability study was based on thermograms analysis obtained with the DSC Q20. The DSC was provided by TA Instruments with purge using extra pure nitrogen (50 mL·min⁻¹). It can work in isothermal and non-isothermal conditions. DSC measures temperature with accuracy of ± 0.05 K. Its specific sensitivity is 1mW·kg⁻¹[18].The device detects temperature changes between the sample and the reference to measure heat flow over time and temperature. Gold-plated high pressure crucibles (M20 crucibles from Swiss Institute for the Promotion of Safety and Security) were used for measurement [19].

93 • Chemical analysis materials

The FTIR IR Affinity-1S from Shimadzu (400 to 4000 cm⁻¹), GC-MS from Agilent
technology 7890A GC/5975C VL MSD, and the mass spectrometry with electro spray
ionization from Waters LCT Premier were used to identify and quantify chemical species.

97 GC-MS analyses were performed in a GC6850 gas chromatography coupled with a 5975C 98 MSD Quad Instrument with electrons impact ionization at 70 eV. A HP5-MS 5% Phenyl 99 Methyl Siloxane capillary column (Agilent 19091S-433E) with a 0.25 mm i.d., 30 m nominal 100 length and 0.25 μ m phase film diameter was used. The carrier gas was helium at a flow rate of 101 15 mL·min⁻¹.

102 3 Synthesis and chemical analysis

103 **3.1 Experiment**

104 Considering the chemical instability of the mixed acid (nitrating agent), it was prepared just 105 before the synthesis reaction (nitration). 86.4 g of sulfuric acid was introduced with a flow 106 rate of $4g \cdot min^{-1}$ into the reaction calorimeter filled with 57.6 g of nitric acid. The mixture was 107 stirred at 200 rpm and kept at 5°C during the addition. At the end, the mixture, composed of 108 HNO₃ 27 %, H₂SO₄ 58%, H₂O 15% (w/w), was kept in the fridge at the same temperature.

To carry out the synthesis reaction, 144g of mixed acid was dosed with a flow rate of 4g·min⁻¹ 109 into the reactor initially filled with 150 g of biodiesel composed of 92% of methyl oleate 110 (determined by GC-MS Table 1). These operating conditions are chosen after preliminary 111 study on the effect of parameters such as a flow rate, stirring speed on thermal behavior in 112 order to ensure the safe operation of the reactor. The synthesis reaction was carried out at 600 113 114 rpm stirring speed, in the isothermal mode. This experiment was realized at seven different temperatures (10-15-20-25-30-40 and 50°C). The Mettler RC1 operating software allows to 115 record the thermal signal (power profile) and to monitor the reaction progress. The final 116 product was then transferred to a separating funnel and separated in two phases. Only the 117 organic phase (which contains the nitrated products) was analyzed. Before the analysis, the 118 organic phase was, first, washed with a bicarbonate solution at 2% w/w, and then with 119 distilled water until a neutral pH was obtained. 120

121

Table 1: Fatty Acid Methyl Esters (FAME) from canola composition

Compounds	% w/w
Methyl palmitate	
H,C, L, CH,	2.2
Methyl oleate	92.0
H ₃ C ^A J	
Methyl linoleate	2.5
H,C~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~	
Methyl linoleneate	2.0
OCH3 CHa	2.8
Methyl stearate	
H ₃ C ^A J	0.5
H _y cr ^o y cH _y	0.5

123 3.2 Nitration Product analysis

124 Infrared analysis and electro-spray ionization mass spectrometry were used to identify and 125 quantify the different chemical compounds produced during the biodiesel nitration.

126 3.2.1 Infrared analysis

- 127 Fig. 2 shows the FTIR spectra of biodiesel and nitrated products at different temperatures.
- 128 These spectra were obtained after defining the baseline corresponding to the air spectrum with
- 129 50 scans. An absorbance difference is noted between 800 and 1700 cm⁻¹. It allows to identify
- 130 new functional groups present in the nitrated product (Table 2). The value of the nitrated
- 131 products absorbance depends on the synthesis temperature.
- 132 The characteristic ester frequency C=O bonds at 1750 cm⁻¹, alkane frequency C-H bonds
- between 2900-3000 cm⁻¹ and alkene frequency C=C stretch at 1650 cm⁻¹ with weak intensity,
- 134 obviously appear in all spectra. The spectrum of the nitrated product shows the presence of
- three new peaks at 1363, 1550 and at 1635 cm⁻¹. They respectively indicate the stretching of
- 136 symmetric NO_2 , that of asymptric NO_2 and the absorption of ONO_2 (fig.3).
- 137 The absorption spectrum at 1363cm⁻¹ (fig.3) indicating a symmetric vibration of R-NO₂ for
- 138 nitrated products, can also be observed in biodiesel but is less intense. This peak in the
- 139 biodiesel spectrum corresponds to the vibration of CH₂ groups which is supposed to appear at
- 140 1370 cm⁻¹.





Fig. 2. IR spectra of biodiesel and nitrated products at different temperatures



146

To complete this IR analysis which only identifies the functional groups, electro sprayionization mass spectrometry was used to identify the synthesized molecules.

149 3.2.2 Electro spray ionization mass spectrometry

The electro spray ionization mass spectrometry allows to avoid the degradation of the nitrated products during the heating in the chromatography column. The samples (biodiesel and nitro product) were diluted with acetonitrile to a concentration of 20 μ g/mL, before being introduced into a capillary tube with a flow rate of 15 μ L·min⁻¹. Peaks of the spectrum in Fig. 4a correspond to methyl oleate, methyl linolenate and the methyl linoleate. These molecules are in a ionic adduct form [M + Na] ⁺ at m / z = 319, m / z = 315 and m / z = 317.



- 162 This study reveals that the nitration reaction can be performed on the carbon atoms carrying
- the double bond as well as those in the beta position. This result contradicts Abdullah *et al* (2010) [16] work which indicates that during the nitration process the NO₂ or NO₃ groups are attached only on the unsaturated carbon atoms.
- 166 Three compounds were identified A (Methyl-8-nitro oleate), B (Methyl-10-nitrate 167 stearate) and C (Methyl-10-nitrate-9-nitrostearate).
- 168 3.3 Study of the reaction selectivity
- 169 GC-MS and iodine index measurement were used to determine the molar proportion of each170 compound A, B and C.

171 3.3.1 Measurement of the conversion rate

- 172 The nitration reaction's conversion rate was determined by using a GC-MS with addition of 173 an internal standard (methyl nonadecanoate) according to the 2011 EN14103 standard. Each 174 solution was dissolved in 10 mL of toluene (GC purity \geq 99.5%). 2µL of the sample was
- injected in the column previously heated at 60°C. This column was heated to 200°C with a
- 176 10° C/min heating rate then at 5 °C·min⁻¹ to 240°C. Finally, the column was maintained at this
- temperature during 7 min. The runtime was 30 min. Splitless mode was used.
- 178 Results are presented in Table 4
- 179

Table 4: Total conversion of the nitration reaction

Temperature (°C)	Conversion rate (%)		
25	94.6		
30	92.7		
40	97.0		
50	89.2		

- 181 Table 4 shows that the reaction conversion rate (the production of all molecules A, B and C)
- varies with temperature and is maximal at 40 °C. The selectivity of B and C was determined
- 183 by using the iodine index method.
- 184 3.3.2 Determination of the molecules selectivity
- 185 The iodine number of oils and fats measures their unsaturation degree. The Wijs method [20], 186 commonly used, requires 30 min absorption time. Sodium thiosulfate solution 0.1M was used
- 187 as a titration reactant. The measurement of the biodiesel iodine index before and after the
- 188 nitration reaction allowed to calculate the conversion of unsaturations (the loss of the double
- bonds). This value was used to determine the proportion of molecules B and C according to
- the equation 3-1.

191
$$\mathbf{X} = \frac{\text{iodine idex }_{t_0} - \text{iodine index }_{t_f}}{\text{iodine index }_{t_0}}$$
 3-1

The proportion of A was obtained by making a difference between the conversion rate of the reaction (Table 4) and the unsaturations conversion rate. Results are gathered in Table 5 which shows that at high synthesis temperature, the selectivity of B and C decreases.

Table 5: Determination of the molecule's selectivity			
Temperature °C	Total conversion rate (%)	Selectivity of B and C (%)	Selectivity of A (%)
25	94.6	95.2	4.8
30	92.7	68.0	32.0
40	97.0	42.9	57.1
50	89.2	41.6	58.4

196

197 The results obtained in this study show that the reaction mechanism of biodiesel nitration 198 (aliphatic chain) is more complex than that of the aromatic compounds. Indeed, three 199 molecules with different selectivity had been identified (Table 5).

During the synthesis at low temperature (below 20° C), the final product is a stable micro emulsion preventing phase separation. This stability may be due to the hydrophilic behavior of the saturated nitrated products (B and C) at low temperatures.

203 4 Calorimetric study

204 4.1 Determination of the reaction heat

The integration of the experimental power profiles (equation 4-1) obtained according to the 205 conditions presented in section 3, shows that the heat released by the reaction varies with the 206 temperature (Table 6). This change in the thermal behavior has also been observed by Chen et 207 al 2012 [21] in their work about the nitration of iso-octanol but no interpretation has been 208 given. Power profiles (q_r) are shown in Fig.5. Sudden variation of the thermal power with 209 time at the beginning of the reaction corresponds to the nitration of the small amount of the 210 products as Methyl linolenate and Methyl linoleate. Such thermal behavior may present a risk 211 of thermal runaway. 212

213
$$\mathbf{Q}_{\mathbf{R}}^{\mathbf{Exp}} = \int_{t_0}^{t} q_r dt$$
 4-1



The total heat released by the reaction (table 6) represents all the thermal effects linked to the products synthesis, to the mixing phenomena and to the possible decomposition in case of unstable compound. In section 3.3.2, a modification of the reaction mechanism according to the synthesis temperature was noticed. In addition to other phenomena mentioned above, the modification of the reaction mechanism is likely to contribute to the change in the total heat released by the reaction.

Heat related to the mixing phenomena and the decomposition of unstable compounds are presented in sections 4.2 and 4.3.

226 4.2 Heat of mixing measurement

To measure the heat of mixing, the power profile obtained without nitration reaction have to be integrated. The operating conditions were kept identical to those in the synthesis reaction (section 3.1) except for the biodiesel reactant. In fact, to avoid the nitration reaction, the biodiesel was replaced by a molecule close to its main molecule (methyl oleate): methyl palmitate.

The absence of the reaction was confirmed by the palmitate infrared spectrum after the 232 reaction (fig.6: no nitro group was detected). The non-reactivity of the methyl palmitate is due 233 to the absence of unsaturated carbons. 234



The heat of mixing below 40°C could not be measured because the melting point of methyl 237 palmitate is higher than 35°C. 238



- 239
- 240

Fig.7. Power profiles obtained with the palmitate

Fig.7. shows that the power profiles are identical regardless of the temperature. The average
heat is about 8J. All power profiles return to the baseline at the end of the addition,
demonstrating the absence of any chemical transformations.

4.3 Measurement of the decomposition heat

The measurement of the heat released during the decomposition was done in two steps. Pure products: nitrated products, nitric acid, sulfuric acid and mixed acid (sulfo-nitric acid) were analyzed first (fig.8), then samples of mixed acid with different percentages (w/w) of nitrated products (fig.9). These analyses were realized using a DSC in a non-isothermal mode with Gold-plated high-pressure crucibles and a heating rate of 2° C·min⁻¹. According to Liu et *al* [22], the advantage of DSC test under non-isothermal condition is its swiftness and high efficiency in a short time.

For pure products (fig.8) no signal of decomposition is observed in our range of synthesis 252 temperature (<50°C). The only thermal effects are detected beyond synthesis temperatures. 253 Nitric acid and mixed acid's DSC curves show an endothermic effect at $T_{onset} = 181.3^{\circ}C$ 254 255 which is attributed to the decomposition of the nitric acid [23]. This temperature was 256 determined by the tangent method from zero curvature. Regarding to the nitrated product, it exhibits an exothermic peak at $T_{onset} = 150.9^{\circ}$ C which correspond to its decomposition. Its 257 thermal instability was mentioned in other works [9] [24] [21]. The Tonset of our additive 258 decomposition is closed to that of fossil nitrated product (EHN) [8]. 259



Fig.9 shows the DSC curves of sulfo-nitric acid mixed with nitrated products. The initial decomposition temperatures T_{onset} are 48.83°C, 70.39°C and 77.96°C respectively for 50 %, 70% and 90% of mixed acid. Obviously, when the quantity of nitrated products added into the mixed acid increased, lower onset temperatures are observed. It is also noted that the specific enthalpy decreases with the amount of nitrated products (table 7). This enthalpy (ΔH) reported to the total sample mass was determined by integrating the area under the exothermic curve.

261



271

Fig.9. Study of the decomposition mixed sulfo-nitric and nitrated products

This study allows to demonstrate that the decomposition of the sulfo-nitric mixed acid and nitrated products also contributes to the modification of the total heat released during the synthesis reaction (Fig.5).

Table 7: Results of DSC analysis

Component of sample (w/w)	T_{onset} (°C)	ΔH (J/g)	
90% of mixed acid and 10% nitrated products	77.96	502.0	
70% of mixed acid 30% nitrated products	70.39	474.1	
50% of mixed acid 50% nitrated products	48.83	332.1	

276

277 4.4 Study of the safety parameters

In the light of the strong exothermicity of the nitration reaction and the mixed acid decomposition in the presence of the nitrated products, the determination of the Maximum Temperature of the Synthesis Reaction (*MTSR*) is more than necessary to avoid the possible risk of thermal runaway.

The Maximum Temperature of Synthesis Reaction (*MSTR*) is the temperature reached by the reaction mixture if the energy potential of the main reactions is released under adiabatic conditions [25].

This decomposition releases an excess of energy causing a thermal runaway. To evaluate this 285 temperature, it is necessary to determine the ΔT_{ad} (the temperature variation in adiabatic 286 mode) according to equation 4-2. 287

$$288 \qquad \Delta T_{ad} = \frac{Q_R^{exp}}{C_P M r X' r}$$

with Cp the heat capacity of reaction mixture obtained with reaction calorimeter, Mr the mass 289 of the reaction mixture and X'_r the full conversion of the biodiesel. 290

The calculation of the MTSR was done in semi-batch mode according to equation 4-3 [26] 291 292 [25]. The results are given in Table 8. They show a considerable increase in MTSR from an 293 isothermal of 40 °C. This can be explained by the fact that the value of the adiabatic temperature increase ΔT_{ad} used for the calculation of MTSR, considers the enthalpy of the 294 nitration reaction in addition to the decomposition enthalpy. 295

296
$$MTSR = T_P + \Delta T_{ad}$$
. X ac, may

301

with $X_{ac,max}$ the maximum accumulation of the unreacted reactant and Tp the synthesis 297 temperature. 298

In our case, the nitric acid is in stoichiometric excess over biodiesel. Thus X acc, max is obtained 299 300 at the end of the addition.

		51				
Temperature (°C)	Conversion (%)	$Cp \\ (J \cdot g^{-1} \cdot {}^{\circ}C^{-1})$	ΔT_{ad} (°C)	X ac,max (%)	MTSR (°C)	
25	94.6	2.1	194.4	30.3	83.8	-
30	92.8	2.0	194.8	36.5	101.2	
40	97.0	2.2	262.8	49.5	171.1	
50	89.2	2.1	313.6	50.5	208.5	

If we compare results in table 7 with those in table 8, it appears that the lowest MTSR 302 (83.8°C) is higher than the maximum T_{onset} obtained in decomposition study (77.96°C). In 303 case of loss of temperature control, this means that the decomposition reaction would be 304 triggered before completion of the synthesis reaction, which would further lead to very severe 305 consequences. According to Stoessel's criticality index used for the risk assessment of a 306 chemical reaction [27], this implies that the runaway is too fast for a safety barrier to be 307 efficient. These results correspond to a Stoessel's criticality class of 5 if the nitration reaction 308 conducted in these operated conditions. 309

Table 8: Safety parameters of nitration reaction

4-3

5 Measurement of the bio-additive cetane number (index)

The cetane number is the measurement of the diesel fuel ignition performance. It is obtained 311 by making some comparison with reference fuels in a standardized test. Higher cetane number 312 indicates that the ignition properties of the fuel are better [28]. This index is obtained 313 according to ASTM D 613. The equipment used was a Cooperative Fuel Research (CFR) 314 engine. A standard diesel of cetane number 50 was used to prepare two samples of 1% and 315 5% concentration in bio-additive. For each mixture, the cetane number was measured at two 316 317 synthesis temperatures 25 and 40 °C. The results of the cetane number analysis are listed in Table 9. They show that the bio-additive synthesized in this study allows to increase the 318 cetane number of the reference diesel. A 5% addition of the bio-additive to the reference 319 diesel improves the cetane number by 3 points. 320

321

Table 9: Cetane number with the CFR engine

Synthesis temperature (°C)	CN fuel	CN fuel +1% additive	CN fuel + 5% additive
25	50.0	50.9	52.9
40	50.0	50.9	53.2

Canoira et al 2012 [13] obtained a 5 points increase in the fuel cetane number by mixing their 322 nitrated biodiesel to fossil diesel in a concentration of 1000 mg.L⁻¹. With our bio-additive a 323 5% addition (concentration of $49g.L^{-1}$) to the reference diesel improves the cetane number by 324 3 points. It seems clear that our bio-additive is much less efficient than Canoira et al one. It 325 may be due to the fact that Canoira et al used a biodiesel containing 33.0 %, 54.20% and 16% 326 of methyl linoleate while ours contains only 2.5%. According to Abdullah et al 2010 [16], 327 during the nitration process of biodiesel, NO₃ or NO₂ groups are grafted to the double bonds 328 of carbon atoms. Based on this statement, biodiesel containing more double bonds, once 329 nitrated, tend to be more energetic than others. That could explain the big different between 330 these 2 results. 331

However, the difference between our additive and the EHN is not so high. Indeed a 2.5% and a 5% addition of EHN on BN20 (diesel with 20% of methyl ester) leads respectively to an increase in cetane number of 2.5 and 6.5 points [29].

335 6 Conclusion

The results of chemical analysis of the nitrated products showed the presence of 3 different compounds (methyl-8-nitro oleate, methyl-10-nitrate stearate and methyl-10-nitrate-9nitrostearate), whose selectivity varies according to the synthesis temperature. Some of these compounds, particularly the methyl-8-nitro oleate and the methyl-10-nitrate-9-nitrostearate, were also identified by Canoira et *al.* [13] and Malins et *al.* [30]. The heat released by the chemical transformation obtained with the reaction calorimeter RC1-*RTCal* varies with the synthesis temperature. This difference in the thermal behavior is due to

- the complexity of the reaction mechanism as well as the instability of the nitrated products
- and sulfo-nitric acid mixture. The study of the thermal stability shows that the T_{onset} of the
- decomposition is around 40°C. Thus, at high synthesis temperature (beyond the T_{onset}), the
- heat measured by the RC1 corresponds to the sum of the heat released by the nitration
- 347 reaction and that of the mixture decomposition. This thermal and chemical behavior shows
- 348 the complexity of the aliphatic compound nitration compared to the aromatic compounds one.

The modification of thermal behavior according to the synthesis temperature increases the risk of thermal runaway. The Maximum Temperature of the Synthesis Reaction (*MTSR*) obtained is higher than the sulfo-nitric acid temperature of decomposition, which leads to important risks of thermal runaway. To avoid thermal runaway while having a high conversion rate, the synthesis temperature, the flow rate of sulfo-nitric acid as well as the temperature control of the cooling fluid are the main parameters on which we can lean on.

355 Acknowledgments

The authors thank AMED project. The AMED project has been funded with the support of the European Union with the European Regional Development Fund (ERDF) and the Regional Council of Normandy.

359 The authors particularly thank Arnaud BARBIER for his help on chemical analyses.

360 **References**

- 361 [1] World Energy Outlook 2017. IEA Webstore n.d. https://webstore.iea.org/world-energy 362 outlook-2017 (accessed July 12, 2018).
- Courtils ND, Durand D, Mabilon G, Prigent M. La dépollution des gaz d'échappement diesel au moyen de pots catalytiques d'oxydation. Sci Total Environ 1993;134:295–304.
 doi:10.1016/0048-9697(93)90359-E.
- 366 [3] Song C. Chemistry of Diesel Fuels. CRC Press; 2000.
- 367 [4] Beatrice C, Bertoli C, Giacomo ND. The Influence of Fuel Formulations on Pollutant of
 368 a Light Duty D.I. Diesel Engine. Warrendale, PA: SAE International; 1996.
 369 doi:10.4271/961972.
- Suppes GJ, Rui Y, Rome AC, Chen Z. Cetane-Improver Analysis and Impact of Activation Energy on the Relative Performance of 2-Ethylhexyl Nitrate and Tetraethylene Glycol Dinitrate. Ind Eng Chem Res 1997;36:4397–404. doi:10.1021/ie9702284.
- 374 [6] Velmurugan K, Gowthamn S. Effect of cetane improver additives on emissions. Int J
 375 Mod Eng Res 2012;2:3372–3375.
- Quadros PA, Oliveira NMC, Baptista CMSG. Benzene nitration: validation of
 heterogeneous reaction models. Chem Eng Sci 2004;59:5449–54.
 doi:10.1016/j.ces.2004.07.107.
- [8] Chen L-P, Liu T-T, Yang Q, Chen W-H. Thermal hazard evaluation for iso-octanol nitration with mixed acid. J Loss Prev Process Ind 2012;25:631–5.
 doi:10.1016/j.jlp.2012.01.008.
- 382[9]Ting Yang, Liping Chen, Wanghua Chen. Thermal stability of 2-ethylhexyl nitrate with
acid.383acid.ResearchGaten.d.
- 384 https://www.researchgate.net/publication/271659120_Thermal_stability_of_2-
- ethylhexyl_nitrate_with_acid (accessed June 19, 2018).

- [10] Wang K, Liu D, Xu S, Cai G. Research on the thermal history's influence on the thermal
 stability of EHN and NC. Thermochim Acta 2015;610:23–8.
 doi:10.1016/j.tca.2015.04.022.
- [11] Schmidt CW. BIODIESEL Cultivating Alternative Fuels. Environ Health Perspect
 2007;115:A86–91.
- [12] Johnson DM, Edgar DW, Edgar LD, Pate M, Steffen RW. Biodiesel: Awareness, Use
 and Perceptions of Students at Four U. S. Universities. NACTA J 2015;59:54–62.
- [13] Canoira L, Alcántara R, Torcal S, Tsiouvaras N, Lois E, Korres DM. Nitration of
 biodiesel of waste oil: Nitrated biodiesel as a cetane number enhancer. Fuel
 2007;86:965–71. doi:10.1016/j.fuel.2006.10.022.
- [14] Madden MC. Comparative toxicity and mutagenicity of soy-biodiesel and petroleum diesel emissions: overview of studies from the U.S. EPA, Research Triangle Park, NC.
 Inhal Toxicol 2015;27:511–4. doi:10.3109/08958378.2015.1107153.
- Riadi L, Widianto AY, Purwanto E, Pono A, Theresia R. Synthesis of biodiesel from waste cooking oil by two steps process transesterification and ozonation 2015.
- 401 [16] Abdullah A, Wicakso DR, Junaidi AB, Badruzsaufari B. PRODUCTION OF CETANE
 402 IMPROVER FROM Jathropa curcas OIL. Indones J Chem 2010;10:396–400.
- [17] A. V. Topchiev. Nitration of Hydrocarbons and Other Organic Compounds 1st Edition
 1959. https://www.elsevier.com/books/nitration-of-hydrocarbons-and-other-organic compounds/topchiev/978-0-08-009154-9 (accessed September 14, 2018).
- 406 [18] Ben Talouba I, Balland L, Mouhab N, Bensahla N. Kinetic and safety parameters of
 407 decomposition of neat Tert-Butyl (2-Ethylhexyl) monoperoxy Carbonate and in organic
 408 solvents. Thermochim Acta 2018;659:105–12. doi:10.1016/j.tca.2017.09.022.
- 409 [19] Shimkin A. Optimization of DSC calibration procedure. Thermochim Acta
 410 2013;566:71–6. doi:10.1016/j.tca.2013.04.039.
- 411 [20] Sahoré AD, Abouattier JL. Quelques méthodes d'analyse biochimique de produits
 412 alimentaires. Editions Publibook; 2016.
- [21] Chen L-P, Liu T-T, Yang Q, Chen W-H. Thermal hazard evaluation for iso-octanol nitration with mixed acid. J Loss Prev Process Ind 2012;25:631–5.
 doi:10.1016/j.jlp.2012.01.008.
- Liu SH, Hou HY, Chen JW, Weng SY, Lin YC, Shu CM. Effects of thermal runaway
 hazard for three organic peroxides conducted by acids and alkalines with DSC, VSP2,
 and TAM III. Thermochim Acta 2013;566:226–32. doi:10.1016/j.tca.2013.05.029.
- [23] Kazakov AI, Rubtsov YI, Andrienko LP, Manelis GB. Kinetics and mechanism of
 thermal decomposition of nitric acid in sulfuric acid solutions. Russ Chem Bull
 1987;36:1999–2002.
- [24] Zeng X, Chen W, Liu J. Molecular Structure, Electronic Structure and Heats of
 Formation of Explosive Sensitizers. Acta Phys-Chim Sin 2007;23:192–7.
 doi:10.1016/S1872-1508(07)60015-1.
- [25] Lerena P, Wehner W, Weber H, Stoessel F. Assessment of hazards linked to
 accumulation in semi-batch reactors. Thermochim Acta 1996;289:127–42.
 doi:10.1016/S0040-6031(96)03024-9.
- [26] Zichao G, lerena, Peng Z, Liping C. Insights into maximum temperature of synthesis
 reactions in isothermal homogeneous semibatch reactors 2018.
 doi:10.1016/j.tca.2018.08.018.
- 431 [27] Stoessel F. Planning protection measures against runaway reactions using criticality
 432 classes. Process Saf Environ Prot 2009;87:105–12. doi:10.1016/j.psep.2008.08.003.
- [28] Li R, Wang Z, Ni P, Zhao Y, Li M, Li L. Effects of cetane number improvers on the
 performance of diesel engine fuelled with methanol/biodiesel blend. Fuel 2014;128:180–
 7. doi:10.1016/j.fuel.2014.03.011.

- [29] R. Sathiyamoorthi, S. Chezhian Babu, V. Rajangam, L. S. Tamizhselvan, Panimalar Engineering College, poonamallee, chennai, Tamil Nadu. Evaluation of Neem oil biodiesel with 2-Ethyl Hexyl Nitrate 2-EHN as Cetane Improver on Performance and Emission characteristics of a DI Diesel Engine. Int J Eng Res 2018;V6. doi:10.17577/IJERTCON071.
- [30] Malins DC, Houle CR. Nitration of methyl oleate with acetyl nitrate: a synthesis of
 methyl aminostearate. J Am Oil Chem Soc 1963;40:43–45.