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**Title:** Remarkably stable and efficient Ni and Ni-Co catalysts for CO<sub>2</sub> methanation

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## 1 **Abstract**

---

2 CO<sub>2</sub> methanation is one of the most promising ways to store energy based on the power-to-gas  
3 concept. In this study, efficient nickel (Ni) and nickel-cobalt (Ni-Co), supported on alumina  
4 catalysts with different amounts of Ni and Co were prepared, characterized and used for CO<sub>2</sub>  
5 methanation under the atmospheric pressure. The catalysts were prepared in the form of  
6 extrudates for catalytic tests. The effect of Ni content and the influence of Co on Ni catalysts  
7 were studied in a packed bed methanation reactor at laboratory scale. An optimal Ni-Co content  
8 was identified based on CO<sub>2</sub> and H<sub>2</sub> conversion and CH<sub>4</sub> selectivity and yield. The addition of Co  
9 improved the reducibility of Ni species and Ni particles' dispersion over the support. Therefore,  
10 the presence of Co enhanced the catalyst activity and selectivity towards CH<sub>4</sub>. Moreover, it was  
11 observed that low reaction temperatures (lower than 350 °C) can be used when lowering the Ni  
12 content (i.e. 10% wt.). This major fact is favourable to the reduction of the overall process energy  
13 consumption and to the decrease of the catalysts' deactivation at high temperature (>400 °C),  
14 such as the active phase sintering. Finally, the Ni and Ni-Co catalysts prepared in this work for  
15 CO<sub>2</sub> methanation presented a remarkably high stability over 200 h of continuous reaction.

16 **Keywords:** Methanation, Ni-Co catalyst, Green process, CO<sub>2</sub> valorisation, Power-to-gas.

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## 17 **1 Introduction**

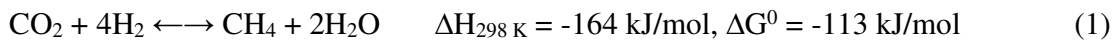
18  
19 One of the most serious issues in the climate debates and the countries' agreements is focused on  
20 the continuous increase in CO<sub>2</sub> emissions. The CO<sub>2</sub> concentration in our atmosphere has already  
21 reached 408 ppm in 2018 [1]. CO<sub>2</sub> is the most abundant greenhouse effect gas emitted by the  
22 humans activities, representing more than 77% of the greenhouse gas emissions. It contributes to  
23 the global warming and climate change [2,3]. Other consequences, such as sea-level rise,  
24 resulting from the thermal expansion or melting of glaciers and polar ice caps, and changes in  
25 agriculture, water and human health have been reported as well [4]. On this matter, several  
26 agreements have been made, for example the Paris Agreement in 2015 at the International  
27 Conference on Climate, COP21. Despite the fact that some countries have reneged this  
28 commitment, CO<sub>2</sub> emissions control remains a key point for the future and objectives set in those  
29 agreements are still needed to be targeted. The main objective is the reduction of earth's

30 temperature and CO<sub>2</sub> emissions through the promotion of renewable energy sources. European  
31 commission has prospected a target of 20% renewable energy by 2020 in its “Energy Roadmap  
32 21” [5]. Recent agreements are pushing the countries for the use of renewable energies alongside  
33 the fossil energies, which would be substituted by the renewables at mid-term.

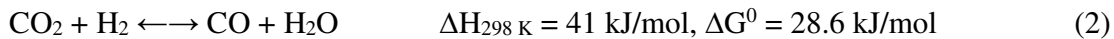
34 The renewable energy resources, such as wind, solar, hydrothermal and hydraulic energy are  
35 converted to electricity, because the transport of energy is the easiest in this form. However, one  
36 of the main problems of renewable energy sources is the difficulty of storing the energy  
37 produced. Indeed, solar panels or wind turbines allow an intermittent generation of electricity,  
38 because of its dependency on the weather; thus, this production cannot fulfil the load demand of  
39 the electric energy. One of the major challenges in the coming years is to find large capacities and  
40 long term solution to store the surplus electricity. The current storage technologies, including  
41 pumped-storage hydroelectricity (PSH)—the most massive storage technology available—can  
42 store only limited amounts of energy over short period of time [6].

43 In this context, hydrogen can be obtained by the electrolysis of water, which can store large  
44 quantities of electrical energy in form of hydrogen and oxygen. These two molecules can be used  
45 directly or as intermediates in the chemical reactions to either reproduce energy or synthesize  
46 chemical products. However, low molecular weight of hydrogen gives it a relatively low  
47 volumetric energy density compared to other fuels, and induces necessary large storage capacities  
48 at high pressures. In addition, its explosive properties entail drastic safety management. Besides,  
49 hydrogen cannot be injected directly into the natural gas grid, because its concentration usually  
50 overcomes the grid technical specifications [7].

51 CO<sub>2</sub> methanation uses the hydrogen produced by water electrolysis and CO<sub>2</sub> for further  
52 production of methane. The methanation reaction, known as Sabatier reaction, can be written as  
53 follows:



54 Carbon monoxide can be a product in the methanation by reverse water gas shift reaction [8]:



55 The Sabatier reaction leads to an improvement in energy density; the energy density of methane  
56 is 40 MJ/m<sup>3</sup>, while that of hydrogen is just 12.7 MJ/m<sup>3</sup>. In terms of greenhouse gas emissions,  
57 methane is the major constituent of natural gas, and is the world's third-most-consumed source of  
58 energy. It is the cleanest gas among fuels currently being used. In addition, unlike hydrogen,  
59 methane has its own distribution infrastructure, which makes it a convenient fuel for modern  
60 economies [8]. The existing gas networks provide high storage capacity and possibility to  
61 transport methane easily and safely. Methane can then be used for heating, industries or mobility  
62 uses.

63 The development of an industrial CO<sub>2</sub> methanation process is still limited despite the discovery of  
64 the reaction since more than a century [9]. However, some industrial applications of CO<sub>2</sub>  
65 methanation already exist, but they are still poorly developed. Many of those processes date back  
66 to the '60s and '80s. In these processes, two types of reactors are mainly used: fluidized bed and  
67 packed bed reactors. Packed bed reactors are mostly used in industry, because of the ease of  
68 setting up and low cost of maintenance. The heat management is mandatory for this sort of  
69 reactor. Poor heat transfer could easily be the cause of hot spots generation within the catalytic  
70 bed and of catalyst thermal degradation, particularly in the case of exothermic reactions like CO<sub>2</sub>

71 methanation. To manage the thermal issues using packed bed reactors, CO<sub>2</sub> methanation  
 72 processes usually involve multiple reactors in series separated by heat exchangers. Table 1 shows  
 73 some of those processes with their operating conditions [8,10,11].

74

**Table 1** : Existing methanation processes

Process / Company	Reactor type	Number of beds	Pressure (bar)	Temperature (°C)
TREMP/Haldor Topsøe (Denmark, Germany)	Fixed bed	3	30	300–700
Hicom/British Gas Corp (UK)	Fixed bed	4	25–70	230–640
RMP/Ralph M. Parsons Co (US)	Fixed bed	4–6	1–70	315–780
SuperMeth, ConoMeth/Conoco (US)	Fixed bed	4	80	-
Hygas/Institute of Gas Technology (US)	Fixed bed	2	70	280–480
Lurgi, Sasol/Lurgi GmbH (US)	Fixed bed	2	18	450
ICI, Koppers/Imperial Chemical industries (UK)	Fixed bed	3	-	400–700
Comflux/Thysengas GmbH (Germany)	Fluidized bed	1	20–60	400–500
Bi-Gas/Bituminous Coal Res. Inc (US)	Fluidized bed	1	86	-

75

76 Some recent projects [12,13], such as the Audi e-gas project and the one developed at University  
 77 of Corsica are in operation since 2013. Other projects are being developed, such as Jupiter 1000,  
 78 the first French experience in power-to-gas technology at megawatt (MW) level [14].

79 CO<sub>2</sub> methanation is a volume-reducing and exothermic reaction. As a consequence, it is  
 80 thermodynamically favoured at low temperature (Van't Hoff) and high pressure (Le Chatellier).  
 81 CO<sub>2</sub> methanation mechanism implies firstly, the CO<sub>2</sub> dissociation into CO, which has been  
 82 proposed as reaction intermediate during the last decades. CO is then dissociated into C (and O)  
 83 atoms on the metallic active sites to be further hydrogenated into methane by combination with  
 84 the dissociated H<sub>2</sub>. The rate-limiting step of the CO<sub>2</sub> methanation reaction is the dissociation of  
 85 the adsorbed CO into C and O atoms on the metallic sites. The overall reaction rate is slow and

86 considerable attention needs to be paid to develop more efficient catalysts for achieving high  
87 reaction rates. However, an efficient catalyst should be able to ensure a good catalytic activity,  
88 selectivity, stability and also it should be capable of being recovered and regenerated after use by  
89 keeping its initial properties.

90 In the last decades, CO<sub>2</sub> methanation has been extensively investigated on the use of different  
91 metals (Ni, Co, Fe, Cu, Ru, Rh, Ir, Pd, Pt) and supports (TiO<sub>2</sub>, SiO<sub>2</sub>, SiO<sub>2</sub>-Al<sub>2</sub>O<sub>3</sub>, Al<sub>2</sub>O<sub>3</sub>,  
92 MgAl<sub>2</sub>O<sub>4</sub>, MgO, ZrO<sub>2</sub>, CeO<sub>2</sub>, C, MSN, MCM-41, SBA-15, HY, USY)[15–19]. Group VIIIIB  
93 metals, such as Rh, Ru, Ni, Co were found to be very active [3,20]. Noble metals present high  
94 activity and stability under low temperature [21–23]. They are more resistive to catalyst  
95 deactivation (coking and sintering) than other used metals. However, their industrial utilization is  
96 avoided because of their high price and low availability. Cobalt (Co) based catalysts were tested  
97 on methanation, but they were found to be not very selective towards methane [24]. Most of the  
98 studies have come to terms on the use of nickel metal because it is one of the best active metals  
99 for the CO<sub>2</sub> methanation, available at a lower price compared to other metals [19]. These  
100 properties make its industrial utilization possible. Ni catalysts are active only at high temperature  
101 (300–450 °C). At low temperature (lower than 300 °C), the interaction between Ni and CO leads  
102 to the formation of subcarbonyls and methanation is inhibited [25]. The activity of a Ni catalyst  
103 depends on various parameters, such as support type, preparation method of the catalyst, Ni  
104 loading and the presence of a second metal.

105 The nature of the support greatly influences the morphology, dispersion and reducibility of the  
106 active phase (metal), and consequently the final properties of the catalyst. Several types of  
107 materials can be used as catalytic supports for CO<sub>2</sub> methanation, such as alumina, silica, zeolites,

108 etc.[19,26]. Alumina is the widely preferred support because of its low price, thermal stability  
 109 and relatively high surface area.

110 Table 2 synthesizes some methanation results from the literature, obtained with various Ni-based  
 111 catalysts supported on oxides. Metal loading is presented as wt%.

112 **Table 2:** CO<sub>2</sub> conversion ( $X_{CO_2}$ ), CH<sub>4</sub> selectivity ( $S_{CH_4}$ ) and yield ( $Y_{CH_4}$ )

Catalyst	T (°C)	$X_{CO_2}$ (mol%)	$S_{CH_4}$ (mol%)	$Y_{CH_4}$ (mol%)
10%Ni/CeO <sub>2</sub> [27]	340	91	100	91
20%Ni/Al <sub>2</sub> O <sub>3</sub> [28]	350	80	100	80
10%Ni/Y <sub>2</sub> O <sub>3</sub> [29]	300	80	100	80
23%Ni/CaO-Al <sub>2</sub> O <sub>3</sub> [30]	400	81	99	80
15%Ni/ZrO <sub>2</sub> [31]	300	60	100	60
15 %Ni- Ce <sub>0.72</sub> Zr <sub>0.28</sub> O <sub>2</sub> [32]	350	90	98	88
14%NiUSY [33]	450	65	94	62
60%NiO/SiO <sub>2</sub> [34]	350	86	95	81
15%Ni/TiO <sub>2</sub> [35]	340	80	96	77
10%Ni / Al <sub>2</sub> O <sub>3</sub> [36]	400	60	95	57
10%Ni3%Co/ Al <sub>2</sub> O <sub>3</sub> [36]	400	70	96	68
10%Ni/OMA(ordered mesoporous alumina) [36]	400	70	95	66
10%Ni3%Co/OMA(ordered mesoporous alumina) [36]	400	78	99	77
14%NiUSY [37]	400	25	61	15
CeNiUSY [38]	400	55	86	47

113  
 114 Despite their high activity, Ni catalysts are very sensitive to coke deposition or metal sintering  
 115 because of high temperature reaction. An interesting solution to catalyst deactivation, that has  
 116 been widely studied in the last years, is the addition of a second metal. Among these additional  
 117 metals, Co was found to be interesting, because it has shown to improve the metallic Ni



118 dispersion and to increase the catalyst stability and resistance to deactivation [39–41]. Moreover,  
119 the price of cobalt is relatively lower than other metals used as second metal in methanation  
120 catalysts such as noble metals and cerium.

121 CO<sub>2</sub> methanation still needs to be improved in terms of process efficiency, reactor design and  
122 catalyst design. Therefore, our main objective is to contribute to the catalyst design improvement  
123 through the development of an efficient Ni or Ni-Co based catalyst with high stability and  
124 resistance to deactivation for further utilization in the industrial application. The use of the  
125 efficient catalysts, prepared in this work, will allow performing the CO<sub>2</sub> methanation reaction at  
126 relatively low temperatures and lowering the overall process energy consumption.

127 In this work, efficient Ni and Ni-Co supported alumina catalysts were prepared. Ni content was  
128 varied from 5 to 25% wt. and Co from 3 to 10% wt. The catalysts were characterized and tested  
129 in a CO<sub>2</sub> methanation reactor under atmospheric pressure. The optimized Ni-Co formulation was  
130 given. Finally, the remarkable stability of the efficient Ni based catalysts was proven through  
131 CO<sub>2</sub> methanation catalytic long duration tests (over 200 h).

## 132 **2 Experimental**

### 133 *2.1 Catalysts preparation and characterization*

134  
135 Ni/Al<sub>2</sub>O<sub>3</sub> and Ni-Co/Al<sub>2</sub>O<sub>3</sub> catalysts were prepared by an original method developed by  
136 Azzolina-Jury [42]. The first step is the preparation of alumina extrudates.  $\gamma$ -alumina was  
137 prepared by calcination of boehmite powders (Sasol DISPAL 23N4-80) at 600°C for 4 h. Then a  
138 binder was added to alumina and the extrusion of the mixture was performed. The extrudates  
139 were calcined at 600°C for 4 h. Alumina extrudates of 3 mm diameter and 5 mm length were

140 impregnated with an aqueous solution of  $\text{Ni}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$  (Acros Organics), or co-impregnated  
141 with both  $\text{Ni}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$  and  $\text{Co}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$  (Acros Organics) at 80 °C under partial vacuum.  
142 Catalyst samples were calcined for 4 h at 450 °C. Table 3 lists the prepared catalysts with their  
143 metal loading.

144

**Table 3:** List of Ni and Ni-Co catalysts

Catalyst	Ni (% wt.)	Co (% wt.)
5Ni	5%	0%
10Ni	10%	0%
15Ni	15%	0%
20Ni	20%	0%
25Ni	25%	0%
15Co	0%	15%
10Ni,10Co	10%	10%
15Ni,5Co	15%	5%
20Ni,3Co	20%	3%
20Ni,5Co	20%	5%
20Ni,8Co	20%	8%
20Ni,10Co	20%	10%

145

146 The surface area and porosity of the catalysts were estimated by nitrogen adsorption in a  $\text{N}_2$   
147 sorption analyser (Micromeritics ASAP 2020) at -196 °C. Before adsorption, samples were  
148 outgassed at 200 °C. X-ray diffraction (XRD) was performed using PANalytical X'Pert Pro  
149 diffractometer, equipped with a  $\text{Cu-K}\alpha$  radiation source to examine the crystallinity of the  
150 catalysts and to estimate the metal particle size. Temperature programmed reduction ( $\text{H}_2$ -TPR)  
151 was carried out in Micromeritics AutoChem II, equipped with a thermal conductivity detector  
152 (TCD), for evaluating the reducibility of the catalysts and for identifying Ni and Co states. TPR  
153 was performed under flow of 5% v/v  $\text{H}_2$  in Ar from room temperature to 1000 °C. FTIR (Fourier

154 Transformation Infra-Red) measurements were performed using a Nicolet FTIR spectrometer.  
155 Catalyst powders were pressed into self-supported wafers (15-20 mg) and placed inside the IR  
156 cell under partial vacuum ( $10^{-6}$  Torr). Wafers were activated at 400 °C for 4 h and then reduced  
157 twice under 100 Torr H<sub>2</sub> for 30 minutes. Two molecule probes were used: CO and pyridine. The  
158 adsorption of CO on the wafer surfaces was carried out at room temperature, while the adsorption  
159 of pyridine was performed at 150 °C to guarantee a good diffusion of the molecule. CO  
160 adsorption provided information about Ni dispersion on the support surface. Several CO-metal  
161 species can be formed from the interaction between CO and the metal (Ni or Ni-Co), which are  
162 used to identify whether the metal is highly, moderately or poorly dispersed. The adsorption of  
163 pyridine was used to evaluate the acidity (Lewis in this case) of the catalysts. All characterization  
164 results will be developed and discussed in detail in a forthcoming paper. However, the useful  
165 results for the catalytic activity interpretation are presented in Section 3.

166 Prior to the catalytic tests, all catalysts were sieved (1000  $\mu\text{m}$ –1400  $\mu\text{m}$ ). An analysis by laser  
167 granulometry (Malvern Mastersizer 3000) was carried out on five of our catalysts to precisely  
168 measure the mean diameter of the particles. For each catalyst, the measurement was repeated for  
169 five times, and the volume mean diameter D[4,3] (Brouckere Mean Diameter) [43] is presented in  
170 Table 4. The values confirm that all the tested catalysts have a similar diameter around 1350  $\mu\text{m}$ .

171  
172

**Table 4** : Volume mean diameter

Catalyst	D ( $\mu\text{m}$ )	Standard deviation ( $\mu\text{m}$ )
10Ni	1152	72
20Ni	1302	127
10Ni,10Co	1332	46
15Ni,5Co	1434	46

173

## 174 **2.2 CO<sub>2</sub> methanation set-up**

175

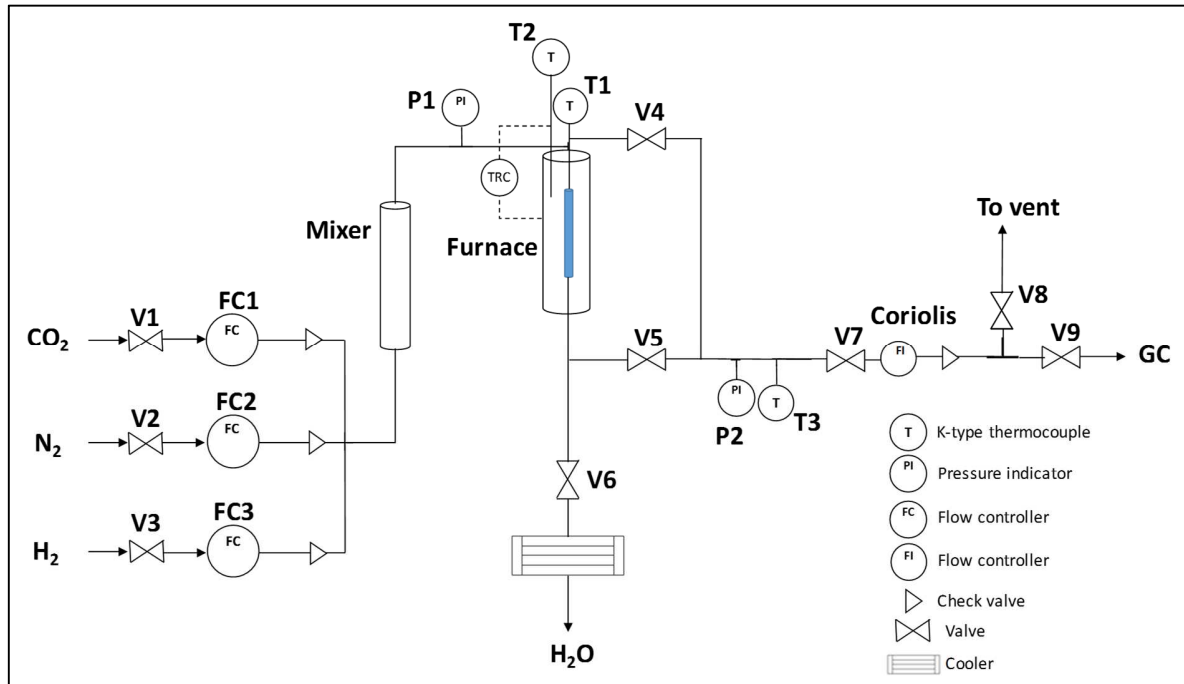
### 176 *2.2.1 Experimental set-up*

177

178 The methanation catalytic tests were performed under atmospheric pressure using the laboratory  
179 scale set-up shown in Figure 1. The reactor consists of a tubular stainless steel tube of 4 mm of  
180 inner diameter and 20 mm length. It was filled with 0.92 g of catalyst. Glass wool was introduced  
181 on both sides of the catalytic bed to ensure good gas dispersion and to maintain the catalytic bed  
182 at the centre of the tube. This reactor was inserted in a tubular furnace (Eraly). A K-type  
183 thermocouple T1 was inserted at the centre of the catalyst bed to measure the temperature during  
184 the reduction and methanation reaction. A second thermocouple T2, placed at the wall of the  
185 furnace, was used to regulate its temperature.

186 CO<sub>2</sub>, N<sub>2</sub>, and H<sub>2</sub> bottles were provided by Linde. The reactants' flow rates were controlled by  
187 three mass flowmeters. Gas mixtures were introduced into the reactor through a "mixer"  
188 consisting of a bed of inert particles. At the reactor outlet, a cold trap made from water ice (0 °C)  
189 allowed to remove the main part of water vapour from the outgoing gas stream. The by-pass  
190 between V4 and V5 was used for GC calibration. During methanation runs, V4 was closed, V5  
191 was open, and the feed gas went through the reactor. The outgoing mass flowrate was then  
192 measured by a Coriolis flowmeter (Bronkhorst ML120). Piezoresistive pressure transducers  
193 (Keller PR-23 and Corame PTX-5072) were used to measure the operating pressure at two  
194 different places of the process.

195



196

197

Figure 1: CO<sub>2</sub> methanation set-up at the atmospheric pressure

198

199 The outgoing gas was analysed using an on-line gas chromatograph from Perkin Elmer (Clarus  
200 590). It is equipped with three columns, a methanizer and two detectors. Two Hayesep columns  
201 were used to separate CO<sub>2</sub>, H<sub>2</sub>/N<sub>2</sub>, CO and CH<sub>4</sub>, and a MolSieve column was used to quantify H<sub>2</sub>  
202 and N<sub>2</sub>. TCD was used to measure H<sub>2</sub> and N<sub>2</sub> concentrations and Flame ionization detector (FID)  
203 was used to quantify CO<sub>2</sub>, CO and CH<sub>4</sub> concentrations. FID detector was equipped with a  
204 methanizer consisting of a bed of catalyst that reduces CO and CO<sub>2</sub> to methane, which can be  
205 further detected by FID detector. TCD and FID temperatures were maintained at 150 °C and 400  
206 °C, respectively. The calibration of peak areas was done using already known gas compositions.  
207 Coriolis flowmeter gives an accurate value of mass flow rate of the outgoing gas and coupled to  
208 the results of the GC, it leads to the composition of the output gas. CO<sub>2</sub> or H<sub>2</sub> conversion,

209 methane selectivity from H<sub>2</sub> or CO<sub>2</sub> conversion and methane yield from H<sub>2</sub> or CO<sub>2</sub> conversion  
210 were estimated using Equations (3)–(5):

$$X_i = 100 \times \frac{\dot{n}_i^0 - \dot{n}_i}{\dot{n}_i^0}, \quad (3)$$

$$S_{\text{CH}_4} = 100 \times \frac{\dot{n}_{\text{CH}_4}}{\dot{n}_i^0 \times X_{\text{CO}_2}} \text{ or } S_{\text{CH}_4} = 100 \times 4 \times \frac{\dot{n}_{\text{CH}_4}}{\dot{n}_i^0 \times X_{\text{H}_2}}, \quad (4)$$

$$Y_{\text{CH}_4} = 100 \times \frac{\dot{n}_{\text{CH}_4}}{\dot{n}_{\text{CO}_2}^0} \text{ or } Y_{\text{CH}_4} = 100 \times 4 \times \frac{\dot{n}_{\text{CH}_4}}{\dot{n}_{\text{H}_2}^0}, \quad (5)$$

211  
212 where i CO<sub>2</sub> or H<sub>2</sub>;  $\dot{n}_i$  and  $\dot{n}_i^0$  are the molar flowrate of i at the outlet and at inlet of the reactor  
213 respectively.

214 The catalytic activity and stability of the catalyst were evaluated by following CO<sub>2</sub> and H<sub>2</sub>  
215 conversion. The methane selectivity and yield were calculated with respect to CO<sub>2</sub> or H<sub>2</sub>,  
216 according to Equations (4) and (5). The overall material balance was checked for each analysis. It  
217 was within  $\pm 5\%$  mol. It was noticed that no other product was detected and that CO<sub>2</sub> and H<sub>2</sub>  
218 conversions were identical, within experimental error  $\pm 5\%$ .

219

### 220 2.2.2 *Experimental procedure and operating conditions*

221  
222 For each experiment, 0.92 g of sieved catalyst particles (1350  $\mu\text{m}$  of mean diameter) was loaded  
223 into the reactor and then the reactor was vibrated, packed and assembled. The height of catalyst  
224 bed was measured and it was 10 cm for all experiments. A leak test was accomplished to ensure  
225 the sealing of the set-up and to avoid any hydrogen leak. Then, the catalyst was reduced under a  
226 continuous flow of 5% v/v H<sub>2</sub> in N<sub>2</sub> at the total flow rate of 200 mL/min STP (Standard

227 Temperature and Pressure conditions) and at 400 °C under atmospheric pressure. The  
228 composition of the inlet gas mixture was first estimated by gas chromatography (GC) analysis  
229 using the bypass before being introduced into the reactor. The methanation reaction was  
230 conducted at several temperatures under atmospheric pressure. For each temperature, GC  
231 analyses were conducted every ten minutes until steady state was well established. Thereon, three  
232 samples were taken each 10 minutes, analysed and the mean values calculated as results. After  
233 the analysis, the temperature of the furnace was adjusted to the next value to obtain a new  
234 operating point. The temperature was increased from 100 °C to 400 °C, followed by a decrease  
235 from 400 °C to 100 °C to detect the possible hysteresis phenomena. The feed gas mixture  
236 containing CO<sub>2</sub> and H<sub>2</sub> was passed continuously through the catalyst bed with a total flow rate of  
237 200 mL/min STP and a molar composition CO<sub>2</sub>:H<sub>2</sub>:N<sub>2</sub> = 1:4:5. The CO<sub>2</sub>:H<sub>2</sub> ratio = 1:4 has been  
238 chosen considering the results of Goa et al.(2012)[44], and Sahebdehfar et al.(2015)[45] who  
239 found that a ratio equal to 1:4 is the optimum for CO<sub>2</sub> conversion and methane selectivity and that  
240 a ratio equal or lower than ¼ avoids carbon deposition [44]. The feed has been diluted with N<sub>2</sub> to  
241 ensure good hydrodynamic conditions in the catalytic bed such as a non-laminar flow and a  
242 sufficiently efficient external transfer and by the time, to avoid an excessive temperature increase  
243 in the catalytic bed due to the exothermicity of the reaction.

### 244 **3 Results and discussion**

245

#### 246 *3.1 Preliminary results and discussions*

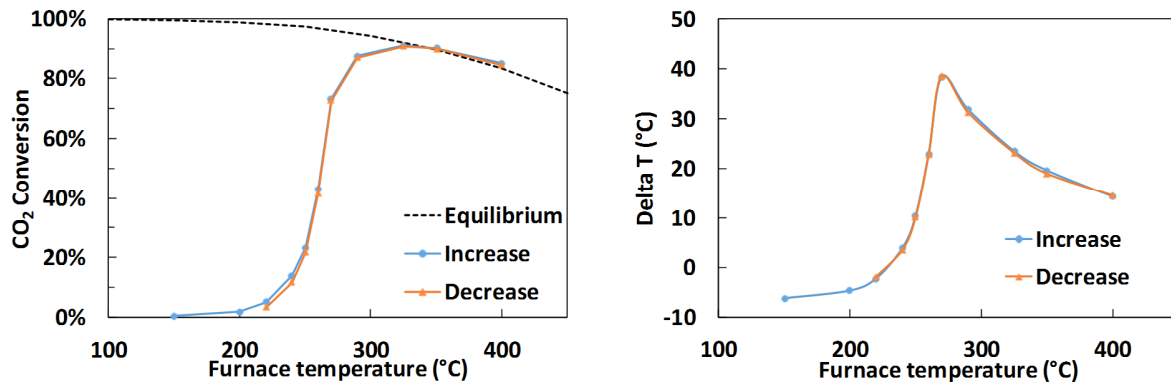
247

248 Concerning the CO<sub>2</sub> methanation, some preliminary results are worthwhile to be given:

249 a) No conversion ( $\text{CO}_2$  or  $\text{H}_2$ ) has been observed below 150 °C, irrespective of the catalyst being  
250 used. The reaction is not occurring. Catalytic results are then presented from 150°C.

251 b) Figure 2 shows the typical results for any Ni or Ni-Co catalyst.

252



253  
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256

Figure 2: Hysteresis test on methanation results for 20Ni catalyst

257 In Figure 2a, conversion is reported for a 20% wt. Ni catalyst and the thermodynamic equilibrium  
258 of the reaction, which was obtained by simulation using Aspen Plus. The reaction starts around  
259 200 °C and hydrogen (or  $\text{CO}_2$ ) conversion increases with the increase in the furnace temperature  
260 and the reaction temperature. The shape of the conversion curve indicates a sharp acceleration of  
261 the reaction rate around 250 °C, which corresponds to the transition from the extinct state to a  
262 lighted state of the bed. When the bed is extinct, methanation occurs progressively all along the  
263 catalytic bed; but when the bed is lighted, the main part of the reaction occurs in a small zone of  
264 the catalytic bed, where the temperature is much higher than the furnace one (+40°C), because of  
265 the reaction exothermicity. This state leads to high conversions (around 80-90%). When the  
266 furnace temperature is increased above 350 °C, the  $\text{CO}_2$  conversion decreases (Figure 2a) because  
267 of the thermodynamic equilibrium limitation (dotted line). The difference of temperature between  
268 the centre of the bed and the furnace temperature, called DeltaT, is presented in Figure 2b. A



269 maximum of DeltaT can be observed when the furnace temperature approaches 280 °C. The  
270 shape of this curve clearly indicates that, for each steady state, the temperature is not  
271 homogeneous all along the catalytic bed and a temperature gradient is verified. The temperature  
272 all along the bed passes by a maximum value, but the position of this value depends on the  
273 operating conditions. The position of this peak is directly linked to the activity of the catalyst.  
274 The more active it is, the highest this peak is and positioned close to the inlet of the bed. That is  
275 the reason why the DeltaT curve, measured at the centre of the bed, also passes through a  
276 maximum when increasing the furnace temperature. It is also important to note that the measured  
277 DeltaT does not obviously include the real maximum. In fact, this curve is always very sharp and  
278 the real maximum value is probably missed, but it gives an order of magnitude.

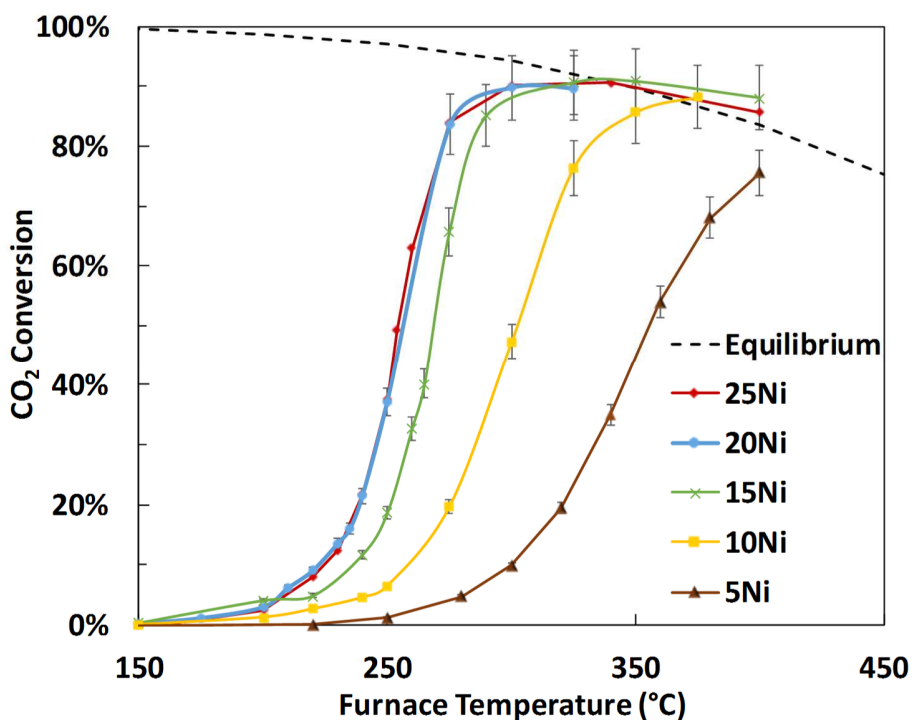
279 c) Because hysteresis is an indication of the existence of multiple steady states and has already  
280 been reported in fixed bed reactors for similar reactions [46,47], we first investigated this  
281 phenomenon in our system. As shown in Figure 2, no hysteresis was observed when conducting  
282 the experiments with an increasing or a decreasing temperature. The conversions and the DeltaT  
283 curves were rigorously the same. These curves also prove the good reproducibility of the  
284 experiments and whether any deactivation occurs, at least after one run going back and forth.

285 d) The GC analysis detects by-products that can be formed during the methanation, such as CO,  
286 and C1-C4 hydrocarbons. For all of our GC measurements made, while studying and comparing  
287 methanation products for different Ni and Ni-Co catalysts, no C1-C4 hydrocarbon by-products  
288 were detected. Only methane was detected and then quantified. CO was detected but in extremely  
289 low quantities (<1/1000)—smaller than the standard deviation of the method. Hence, the  
290 selectivity of CH<sub>4</sub> is 100% with all catalysts, and its yield is equal to the conversion of CO<sub>2</sub> or H<sub>2</sub>.

291 3.2 Effect of Ni loading on catalytic activity and selectivity  
292

293 The catalytic activity as a function of furnace temperature of various Ni/Al<sub>2</sub>O<sub>3</sub> catalysts with Ni  
294 content varying from 5 to 25% wt. is shown in Figure 3.

295  
296



297  
298 **Figure 3:** Effect of Ni content on H<sub>2</sub> conversion. Gas Hourly Space Velocity (GHSV) = 9554 h<sup>-1</sup> (=13043 mL STP/g<sub>cat</sub> h),  
299 H<sub>2</sub>/CO<sub>2</sub>=4/1

300

301 CO<sub>2</sub> conversion increases with temperature for all catalysts. The temperature ignition of the  
302 reactor is observed to happen between 200 and 250 °C. At this temperature, the conversion  
303 dramatically increases to reach a maximum of about 90% for all the catalysts, with Ni content  
304 higher than 5%. Afterwards, the conversion starts decreasing with increasing temperature. As  
305 explained above, the reaction takes place essentially on a limited zone of the catalyst bed and the

306 rest of the bed is used to establish the equilibrium. This is proved by the superposition of  
 307 conversion curves on the equilibrium curve at the highest temperature for all the catalysts. For the  
 308 high temperatures of the furnace, the thermodynamic equilibrium is reached at the outlet of the  
 309 reactor. It is known that the methanation reaction is accompanied with CO production via reverse  
 310 water-gas shift reaction (Equation 2). The methanation of CO can then occur, according to the  
 311 following the reaction (Equation 6):



312  
 313 The produced CO, formed in the first part of the catalytic bed, is converted in the rest of the bed  
 314 into methane, and this is why the selectivity of methane is always 100%.

315 The catalytic activity increases with Ni loading between 5 and 20% wt., as expected (Figure 3).  
 316 The more Ni is incorporated, the more catalytic sites are usually available for the reaction.  
 317 Nevertheless, the catalyst with 25 % wt. Ni loading shows an activity very similar to that of the  
 318 catalyst with 20% wt. Ni. This indicates that there is no benefit in using a Ni catalyst with higher  
 319 Ni loading than 20%. This trend can easily be explained by our characterization results presented  
 320 in Table 5, that summarizes the textural properties of our Ni catalysts and their percentage of  
 321 reduced Ni.

322 **Table 5:** The properties of Ni catalysts

Catalyst	BET surface area (m <sup>2</sup> /g)	Pore volume <sup>a</sup> (cm <sup>3</sup> /g)	Crystallite size <sup>b</sup> (nm)	Reduced Ni at 500 °C <sup>c</sup> (%)
5Ni	166	0.40	nd	nd
10Ni	153	0.36	6	1.8
15Ni	144	0.32	8	2.0
20Ni	141	0.30	10	6.2
25Ni	141	0.29	10	4.4

323 <sup>a</sup> BJH desorption pore volume.

324 <sup>b</sup> NiO (220) crystallite diameter calculated using Scherrer equation [48] from X-ray diffraction (XRD) patterns.

325 ° percentage of reduced Ni at 500 °C calculated from TPR profiles.

326 nd = non detectable

327

328 The X-ray diffraction (XRD) analysis confirmed the presence of Ni on  $\gamma$ -alumina. The peaks of  
329 Ni were identified and they became, as expected, sharper as the metal loading increased. The  
330 surface areas were estimated between 166 and 140 m<sup>2</sup>/g and decreased when increasing the Ni  
331 content. For instance, a decrease in the surface area of 15% was observed, when the Ni amount  
332 was varied from 5% to 25% wt. The porous volume was also affected and decreased by 25%,  
333 from 0.4 cm<sup>3</sup>/g to 0.3 cm<sup>3</sup>/g. This fact can be explained by the increase of the Ni amount within  
334 alumina pores [28,49]. The average size of NiO particles were estimated using the Scherrer  
335 equation. NiO particle size increases with Ni loading from 6 to 10 nm. For 5 % wt. Ni, NiO  
336 particle size cannot be estimated, because NiO is highly dispersed and is not detectable by XRD  
337 analysis. Ni active particles are more available with the increasing Ni content, but they are less  
338 dispersed over the support. Thus, Ni particle size is increased. This fact is verified through FTIR  
339 CO adsorption. Table 6 presents the percentage of moderately and highly dispersed Ni on  
340 prepared Ni catalysts, calculated from FTIR CO adsorption characterization. This percentage  
341 decreases from 43.8% to 37.7%, when increasing Ni loading from 5% to 25%. These results  
342 correspond to the sum of the two adsorption states of CO [50] on reduced Ni, in the region  
343 between 2030 and 2070 cm<sup>-1</sup>. Both adsorption states are linear—the first corresponds to mono-  
344 carbonyls and the second to multi-carbonyls. The results of CO adsorption are consistent with  
345 those reported in the literature [28] and prove that the Ni dispersion decreases with its increased  
346 loading.

347

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**Table 6:** Ni dispersion by FTIR CO adsorption

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Moderately and Highly dispersed Ni

---

Configurations Catalysts	CO	CO	CO	CO
	Ni		Ni	
5Ni	43.8%			
10Ni	41.4%			
15Ni	36.9%			
20Ni	34.3%			
25Ni	37.7%			

348

349 Concerning the reducibility of the species, the percentages of reduced Ni at 500 °C, given in  
350 Table 5, were calculated from H<sub>2</sub>-TPR profiles. It increases up to 6.2% for 20% wt. Ni, then  
351 decreases to 4.4% for 25% wt. Ni catalyst. This shows that the reducibility of Ni catalyst  
352 increases with the Ni loading from 5% wt. Ni to 20% wt. Ni, but decreases hereafter. In fact, the  
353 species that may be present on the surface of the prepared catalysts are NiO and NiAl<sub>2</sub>O<sub>4</sub>. To  
354 reduce NiAl<sub>2</sub>O<sub>4</sub> species, a very high temperature (over 800 °C) is required, while the reduction of  
355 oxides usually begins at 300 °C. NiO may either be weakly or strongly bonded to the support. For  
356 example, if the particles are hemispherical, 25% of the NiO phase will be in contact with the  
357 alumina support surface. Such intimate contact between the two phases would result in a strong  
358 interaction and the NiO species' reducibility could be difficult [51]. Indeed, a relation between  
359 the results of particle size to those of TPR could be established in this way. The increase in the  
360 NiO particle size, between 5Ni and 20Ni (Table 5), results in the formation of weakly bonded  
361 NiO to alumina support, and thus the reducibility of the catalysts is increased.

362 DeltaT for several Ni catalysts is presented in Figure 4.

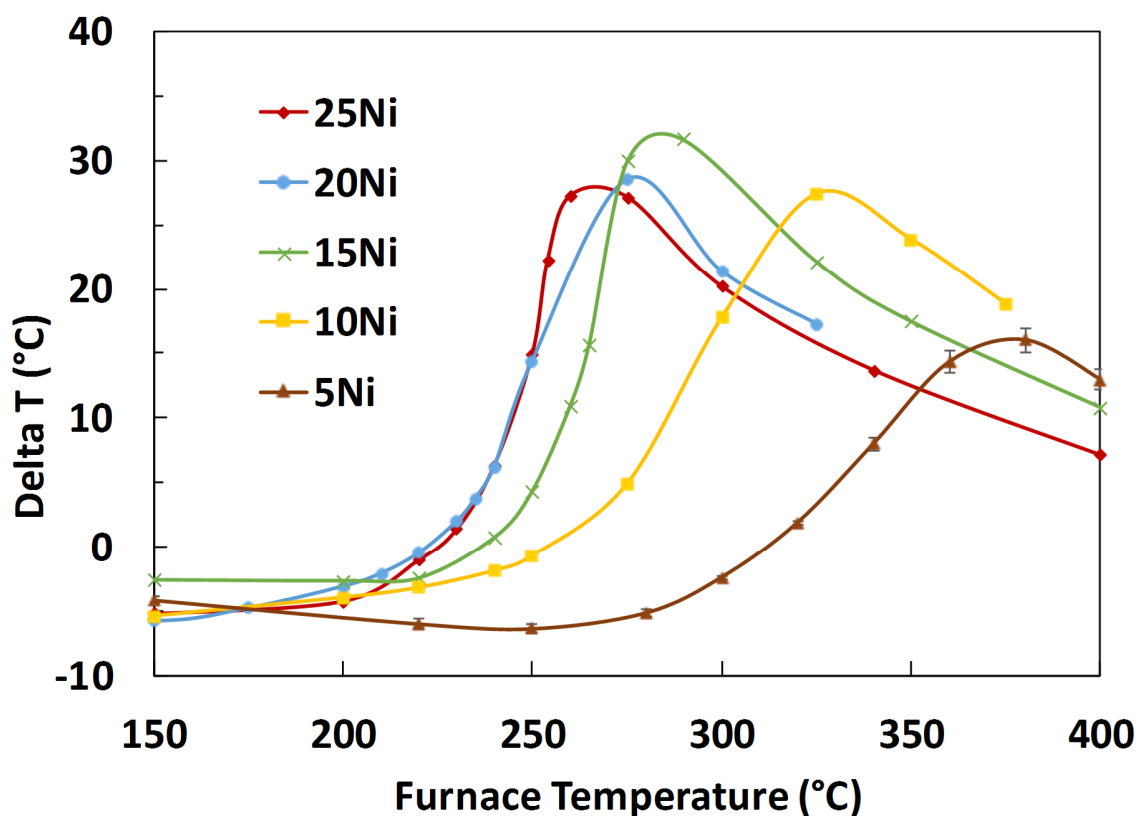


Figure 4: Temperature increase from the inlet to the centre of the bed for several Ni contents

363  
 364  
 365  
 366 DeltaT curves show evidence of the exothermicity of the methanation reaction. Because of the  
 367 thermal resistances, when the reaction does not occur or is very slow, DeltaT can be negative; but  
 368 it reaches a maximum of 34 °C with the 15Ni catalyst, when the regulated furnace temperature is  
 369 290 °C. The catalysts with 20% wt. and 25% wt. Ni show similar DeltaT profiles, in accordance  
 370 with their similar activity. 5Ni and 10Ni catalysts have lower delta T values. The furnace  
 371 temperature, for which DeltaT is maximum, is not the same for all the catalysts; and the more the  
 372 catalyst is active, the lower the temperature is. So, this maximum value shifts to the right, towards  
 373 high furnace temperatures, as the Ni content decreases. This means that with less Ni, it is  
 374 necessary to raise the temperature of the oven to carry out the methanation reaction and to obtain

375 a significant conversion of CO<sub>2</sub>. The maximum values, showed in Figure 4, do not necessarily fit  
376 the maximum temperature in the whole bed. The highest temperature is reached in the narrow  
377 zone, where most of the reactions take place. This hot zone becomes larger when the catalyst is  
378 less loaded with Ni. When the temperature of the furnace is increased, the conversion peak, and  
379 therefore the hot zone are moved towards the reactor inlet. The K-type thermocouple, placed at  
380 the centre of the bed, will detect the increase and decrease in temperatures, because it will be  
381 crossed by the hot zone during the variation in the furnace temperature.

382 Finally, increasing the Ni content in the catalysts offers numerous and reducible active sites, that  
383 are less dispersed and accessible. The global activity of the catalysts, showed in Figure 3, is the  
384 result of all these combined effects showing that 20% is close to the optimum value for Ni  
385 content. The exothermicity is moderate in our conditions and the maximum value of DeltaT (and  
386 its position on Figure 4) is an indication of the catalysts' activity.

### 387 3.3 *Effect of Co content on CO<sub>2</sub> conversion*

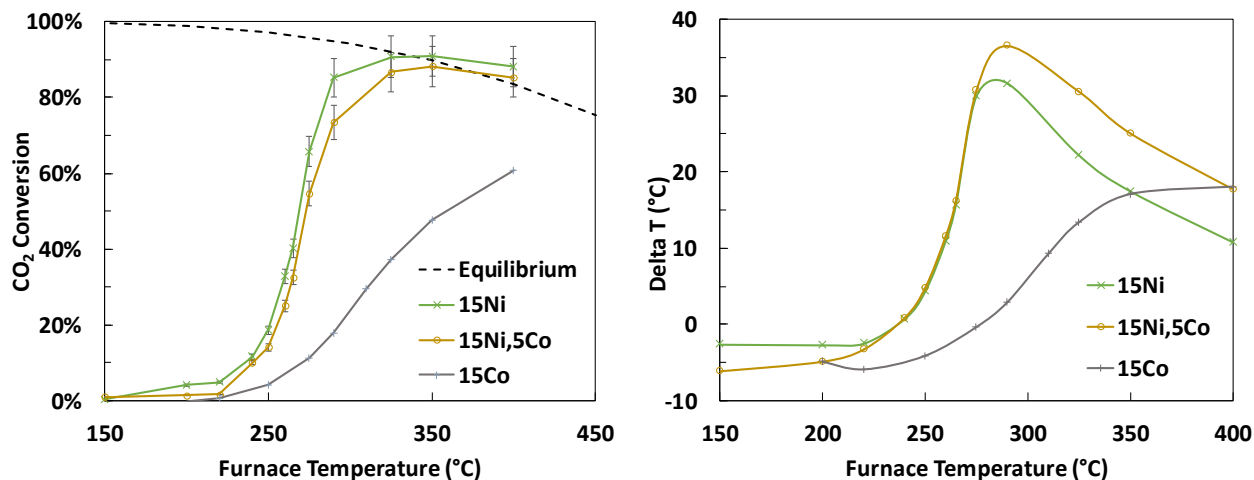
388  
389 The effect of Co addition on methanation reaction was investigated based on H<sub>2</sub> and CO<sub>2</sub>  
390 conversion and CH<sub>4</sub> selectivity. The synthesized catalysts of Table 3 were tested in the CO<sub>2</sub>  
391 methanation pilot at several reaction temperatures under atmospheric pressure with a molar ratio  
392 H<sub>2</sub>/CO<sub>2</sub> = 4/1.

393 The catalytic effect of Co on CO<sub>2</sub> methanation was firstly evaluated by performing a test with a  
394 catalyst containing Co only (15Co), supported on gamma-alumina. In Figure 5, the results are  
395 compared with those obtained with 15Ni and with a third catalyst containing 15% wt. Ni, 5% wt.  
396 Co (15Ni,5Co).

397

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401

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Figure 5: CO<sub>2</sub> conversion and DeltaT for 15Co, 15Ni and 15Ni, 5Co catalysts

403

404 It was found that Co is an active catalyst for CO<sub>2</sub> methanation reaction, because CO<sub>2</sub> and H<sub>2</sub> are  
405 partially converted into methane. The methane selectivity was found to be 100%, when Co alone  
406 was used as in the case of 15Ni (Ni alone). Co was less active than Ni. No catalytic activity  
407 enhancement was observed while using a catalyst containing 15Ni, 5Co.

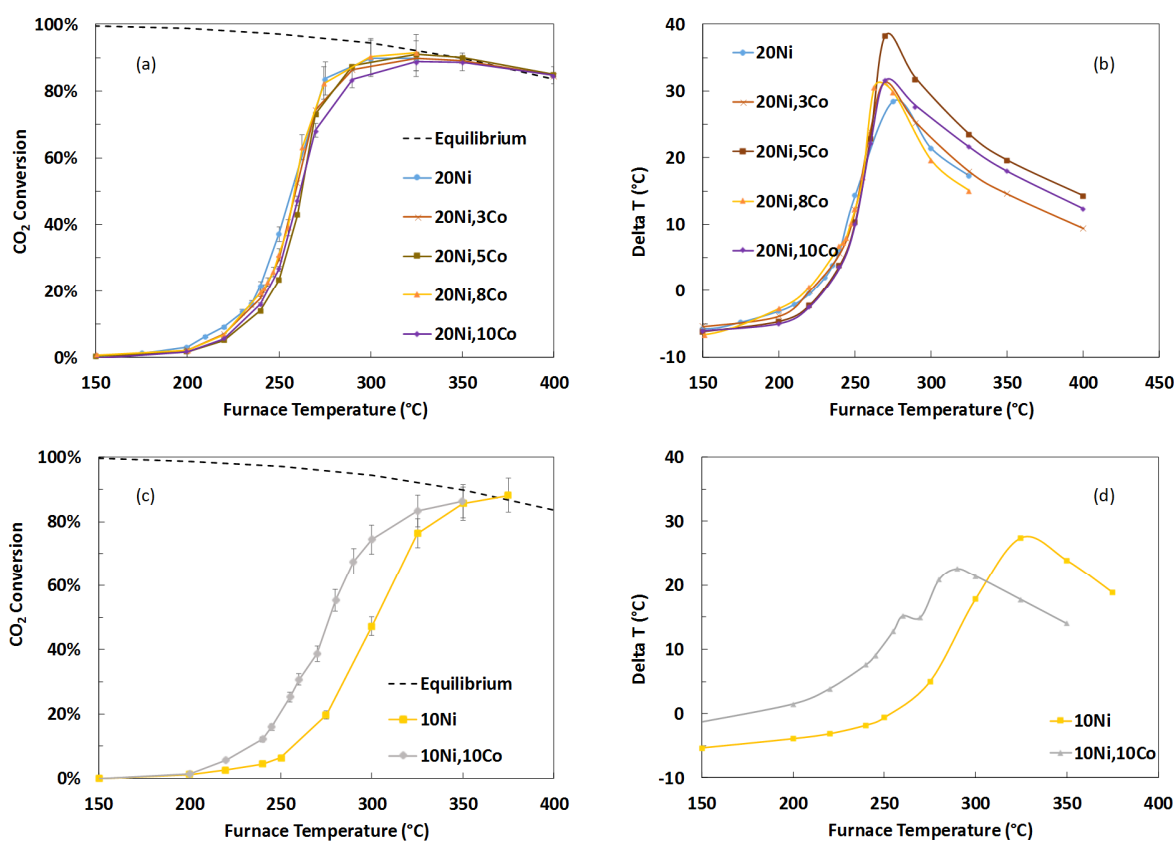
408 Figure 6a shows CO<sub>2</sub> conversion for 20% wt. Ni catalysts, with and without Co. The conversion  
409 for all the five catalysts is nearly the same and no differences in the catalysts' activity were  
410 observed. DeltaT curves (Figure 6b) are also very similar for 20Ni without Co, and with 3%, 5%,  
411 8% and 10% Co indicate that adding Co to a 20Ni catalyst is not worthwhile in terms of activity.  
412 Otherwise, the catalyst with 10Ni, 10Co behaves differently and shows a higher activity than the  
413 one containing 10% wt. Ni at low temperature (Figure 4c and 4d). At 300 °C, conversion with  
414 10Ni catalyst is around 47%, but is increased to 75% when adding 10% Co to the catalyst. DeltaT



415 maximum is also shifted towards the lower furnace temperatures. This indicates that for low Ni  
 416 content, Co addition improves the conversion, but that is not the case with higher Ni loadings.  
 417 The catalyst 10Ni,10Co offers good performances allowing less Ni usage and obtaining slightly  
 418 lower conversion than 20Ni, which is still an interesting finding.

419

420



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422

423

424 **Figure 6:** CO<sub>2</sub> conversion (a,c) and DeltaT (b, d) for methanation with Ni-Co catalysts of various contents

425 The main characterization results of Ni-Co are summarized in Table 7.

426

**Table 7:** Ni- Co catalysts characterization

Catalyst	BET surface area (m <sup>2</sup> /g)	Pore volume <sup>a</sup> (cm <sup>3</sup> /g)	Reduced Ni/Co at 500 °C <sup>b</sup> (%)	Adsorbed CO (μmol/g)
----------	--------------------------------------	---	--	----------------------

20Ni	140	0.30	6	71.5
20Ni,5Co	134	0.30	13	63.1
20Ni,10Co	132	0.28	28	52.2
15Ni	144	0.32	2	66.6
15Ni,5Co	143	0.32	nm	145
10Ni	153	0.36	2	49.9
10Ni,10 Co	141	0.32	31	48.5
15Co	137	0.32	23	9.5

427 <sup>a</sup> BJH desorption pore volume.

428 <sup>b</sup> percentage of reduced Ni/Co at 500 °C calculated from TPR profiles.

429 nm = not measured

430

431 BET surface and pore volume are not much affected by Co addition, despite the fact that it  
432 overcharges this catalyst with metals. But the percentage of reduced species at 500 °C is strongly  
433 increased when Co is added as shown for 20%Ni-Co and 10%Ni-Co catalysts. Thus, Co addition  
434 increases the reducibility of the Ni catalyst, which has a positive effect on activity. The CO  
435 adsorption of catalysts is also influenced by Co addition. For high Ni content (20%wt.), the  
436 adsorbed CO decreases with the Co content. Ni dispersion is not favoured by the Co introduction,  
437 because the total amount of metal (Co + Ni) is high. However, for intermediate Ni content (15%  
438 wt.), Ni dispersion was remarkably improved by Co introduction. No differences in terms of Ni  
439 dispersion were observed after lowering the Ni content (10% wt.) and increasing the Co amount  
440 (10% wt.). The Co introduction improves Ni reducibility in all cases. Nevertheless, the Co  
441 introduction favours Ni dispersion, when the catalyst is not overcharged with both metals. For  
442 high Ni loaded catalysts, the benefits of Co addition, through a better reducibility, are  
443 counterbalanced by the overcharge of the catalyst and a worse dispersion of the active species.  
444 These results are in good agreement with the recent studies of Liu et al. [36] and Xu et al. [52],  
445 who also found a promotion effect of Co on Ni catalysts.

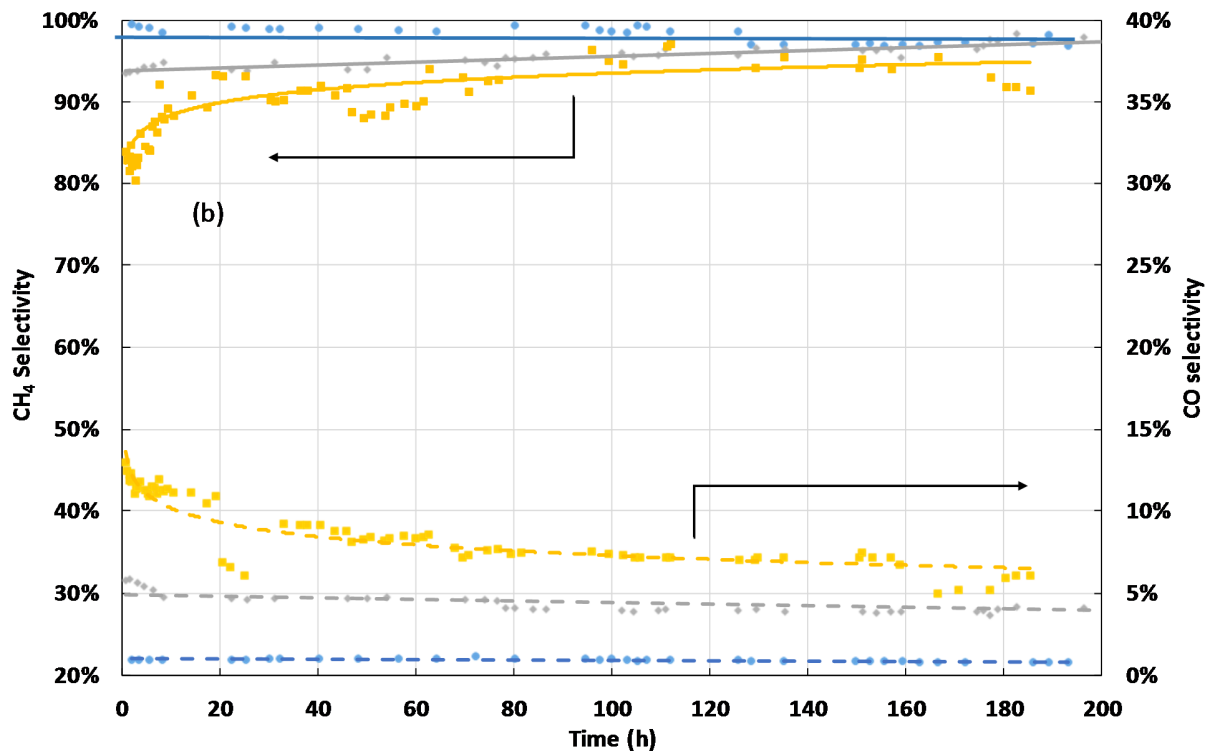
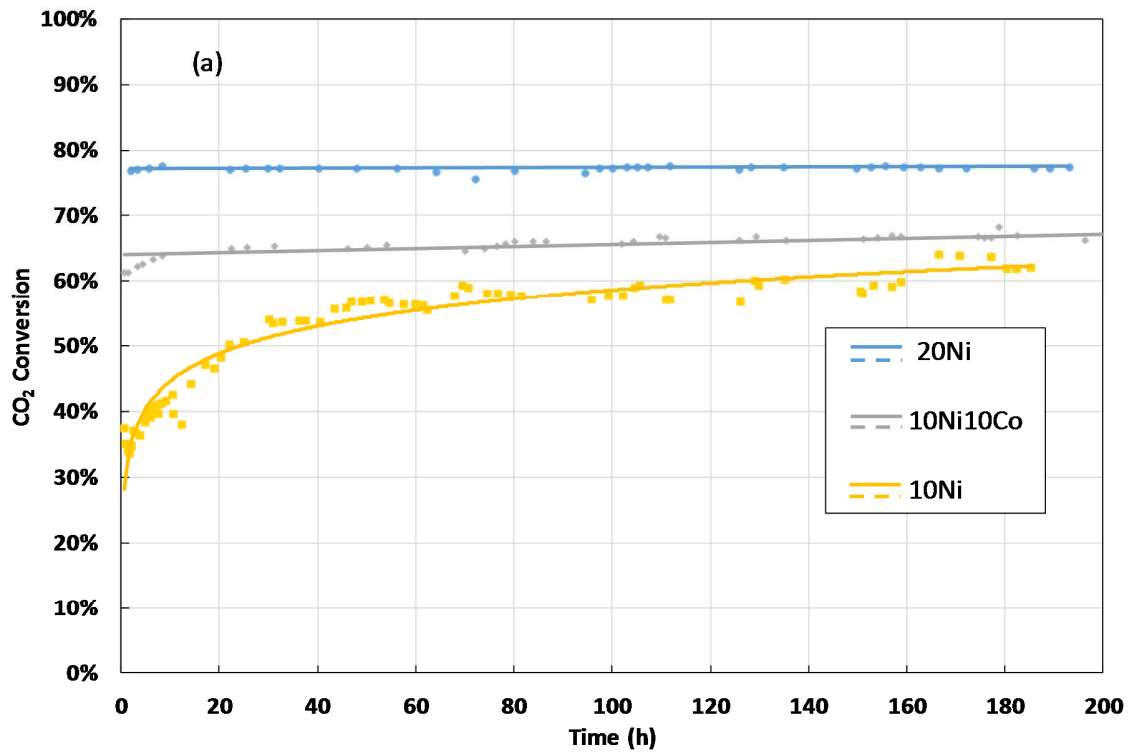
446

### 447 3.4 Deactivation-Stability

448

449 The stability of the catalysts is a very important point that has to be examined when designing  
450 new catalytic processes. Considering the above results, it was decided to perform long catalytic  
451 methanation tests over 200 h with 0.09 g of 10Ni, 10Ni,10Co, and 20Ni catalysts at 350 °C. The  
452 catalysts were first reduced under a continuous flow of 5% v/v H<sub>2</sub> in N<sub>2</sub> at the total flow rate of  
453 200 mL/min STP and at 400 °C under atmospheric pressure. Relatively low reaction temperature  
454 (350 °C) was chosen, because it already allowed a very high conversion of CO<sub>2</sub> into methane  
455 (85% for 10Ni catalyst in Figure 6c) for 0.92 g of catalyst, despite choosing the low temperature.  
456 We also decided to divide the catalyst weight by 10 to run it with high methanation rates all along  
457 the bed, which is now only one centimetre long. The objective was to limit the lifetime test and  
458 see whether deactivation occurs. Figure 7 shows CO<sub>2</sub> conversion and CH<sub>4</sub> and CO selectivity  
459 during the 200 h of reaction.

460



461

462  
463

Figure 7. Stability test on 10Ni, 10Ni,10Co, and 20Ni catalysts: (a) CO<sub>2</sub> conversion, (b) CH<sub>4</sub> and CO selectivity (T= 350 °C, Catalyst mass= 0.09g)

464  
465 As shown in Figure 7, the initial conversions obtained with 10Ni; 10Ni,10Co and 20Ni catalysts  
466 are 32%, 61.5% and 77% respectively. These conversions are observed with 0.09 g of catalyst  
467 only. CO is now detected and quantified so methane selectivity is not 100% anymore (Figure 7  
468 (b)). CO is the only by-product that is detected using the three catalysts. In this configuration, the  
469 catalytic bed is not long enough to fully convert CO<sub>2</sub> and transform CO in methane, according to  
470 Equation (6), but this configuration is very helpful to follow the course of the reaction with time.  
471 Figure 7 shows that 10Ni and 10Ni,10Co catalysts exhibit an activation phase, for which CO<sub>2</sub>  
472 conversion and methane selectivity keep on increasing, whereas CO selectivity decreases. The  
473 more active the catalyst is, the faster the activation phase is and this latter is even not visible for  
474 20Ni catalyst. 20Ni catalyst maintains a CO<sub>2</sub> conversion of 77% and a CH<sub>4</sub> selectivity equal to  
475 98% during all the 200 h of stability test. For 10Ni catalyst, during the first eighty hours, CO<sub>2</sub>  
476 conversion increases from 32% to 56% and then stabilizes. Methane selectivity also stabilizes at  
477 around 95%. During the following 120 h, the catalyst activity and selectivity are maintained and  
478 no deactivation is observed. For 10Ni,10Co catalyst, CO<sub>2</sub> conversion stabilizes at 67 % and CH<sub>4</sub>  
479 selectivity at 97% after 20 h of reaction until the end of the long-term test. The three tested  
480 catalysts show high stability during 200 h of reaction. This result is remarkable and, with the  
481 exception of Liu et al. (2012) [59] who reported the good stability of a 15%Ni on alumina  
482 catalyst doped with 2%CeO<sub>2</sub> over 120h, such long-term experiments without deactivation are  
483 rarely reported in the literature.

484 Concerning the activation phase, an additional reduction of the NiO particles probably occurs at  
485 the beginning of the run. The preliminary reduction of the catalyst, done before methanation, is  
486 perhaps not long enough to fully reduce all the NiO particles, especially the ones which are not

487 well dispersed. Due to the heat of reaction, the bed temperature reaches at least 390°C for the  
 488 10Ni catalyst. This value is comparable to the reduction's one of 400°C, leading to additional  
 489 reduction.

490 The methane production rates in mol.h<sup>-1</sup>.gNi<sup>-1</sup> have also been calculated for our 10Ni; 10Ni,10Co  
 491 and 20Ni catalysts and are compared to the reported values from the literature (Table 8). Our  
 492 10Ni catalyst shows a high methane production rate, better than most of the other catalysts  
 493 containing 10% wt of Ni and comparable to the 10% Ni/CeO<sub>2</sub> tested by Tada et al.[53]. Our Ni  
 494 on alumina support gives comparable results to the one supported on CeO<sub>2</sub> with the main  
 495 advantage of a lower price and availability. Our 20Ni catalyst also exhibits good performances; at  
 496 325 °C, methane production rate is only 2.71 times less than the one presented in Garbarino et al.  
 497 [57]. However, these authors reported results obtained at 400 °C with a 5:1 H<sub>2</sub>:CO<sub>2</sub> ratio,  
 498 representing much favourable conditions for the reaction. The 10Ni,10Co catalyst also shows a  
 499 higher efficiency than other Ni-Co catalysts reported in the literature, even higher than those  
 500 supported on ordered mesoporous Alumina [52] or doped with cerium [59] which is more  
 501 expensive than cobalt. Finally, even some more active Ni catalysts can be found in the literature  
 502 [54–56]. They all use more expensive supports than alumina—sometimes structured—that create  
 503 additional costs to the process.

504 **Table 8:** Comparison of methane production rate for various Ni catalysts on alumina

Author	Catalyst	Methane production rate (mol.h <sup>-1</sup> .g Ni <sup>-1</sup> )	GSHV (mL.g <sub>cat</sub> <sup>-1</sup> . h <sup>-1</sup> )	T (°C)	H <sub>2</sub> / CO <sub>2</sub>	m <sub>cata</sub> (g)	X <sub>CO<sub>2</sub></sub>	S <sub>CH<sub>4</sub></sub>
10Ni (this study)	10%Ni/ Al <sub>2</sub> O <sub>3</sub>	3.2	133000	350	4	0.09	56	95
Tada et al. [53]	10%Ni/ CeO <sub>2</sub>	3.32		10000	350	4	0.3	90
Zhou et al. [27]	10%Ni/ CeO <sub>2</sub>	0.9	22000		340	4.6	0.1	91.1
Xu et al. [52]	10%Ni/ Al <sub>2</sub> O <sub>3</sub> -	0.85	15000		400	4	0.1	68

Rahmani et al. [28]	OMA 10%Ni/ Al <sub>2</sub> O <sub>3</sub>	0.58	9000		350	3.5	-	70	91
Le et al. [57]	10%Ni/ CeO <sub>2</sub>	0.27	60000		220	50	0.1	100	100
Liu et al. [36]	10%Ni/ Al <sub>2</sub> O <sub>3</sub>	0.16	10000		350	4	0.1	25	94
<b>20Ni (this study)</b>	20%Ni/ Al <sub>2</sub> O <sub>3</sub>	2.2	120000		325	4	0.92	90	100
Garbarino et al.[58]	20%Ni/ Al <sub>2</sub> O <sub>3</sub>	5.97		55000	400	5	-	80	78
Zhou et al.[54]	6.17% Ni/TiO <sub>2</sub>	24.27		60000	350	4	0.05	73.2	96
Aziz et al. [55]	5%Ni/ MSN	11.75	50000		300	4	0.2	64.1	99.9
Aldana et al.[56]	5%Ni/S iO <sub>2</sub>	3.89	22000		400	4	0.15	35	88.3
<b>10Ni,10Co (this study)</b>	10%Ni/ Al <sub>2</sub> O <sub>3</sub>	3.25	133000		350	4	0.09	61.5	95
Xu et al.[52]	8%Ni <sub>2</sub> %Co/ OMA	1.22	15000		400	4	0.1	80	97.5
Liu et al.[59]	15%Ni 2%CeO 2/Al <sub>2</sub> O <sub>3</sub>	0.71	10000		350	4	0.1	85	94
Liu et al.[36]	10%Ni 3%Co/ Al <sub>2</sub> O <sub>3</sub>	0.49	10000		350	4	0.1	78	99

505

506 Finally, it is obvious that a global costs balance including the metals and support prices and the  
507 lifetime of the catalyst, as well as mass and energy balances and heat losses calculations would  
508 lead to a more precise analysis. However, considering our results, the Ni and Ni-Co catalysts  
509 prepared in this study are likely to represent an improvement for further developments of  
510 methanation processes: they combine a very good efficiency with a remarkable stability at low  
511 temperature of 350°C. Stability ensures savings on catalysts costs. High methane production rates  
512 per gram of Ni are reached at a lower level of temperature than the classical one, which is  
513 favourable to energy savings. Moreover, cobalt can be used to dope low content Ni catalysts

514 (10%wt Ni as an example): it improves the catalyst activity by improving Ni reducibility and  
515 dispersion and its excellent stability has also been demonstrated.

516

## 517 **4 Conclusion**

518

519 Ni and Ni-Co/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> catalysts with optimum amounts of Ni and Co toward methanation  
520 were prepared and characterized by several techniques. They were tested for CO<sub>2</sub> methanation  
521 under atmospheric pressure. The experimental results showed that these catalysts were very  
522 active even at low temperature (300–350 °C) for the CO<sub>2</sub> and H<sub>2</sub> conversion. The selectivity in  
523 CH<sub>4</sub> was 100% as long as the catalytic bed was long enough to allow CO methanation and  
524 equilibrium at the outlet of the reactor. The conversion and CH<sub>4</sub> selectivity were strongly affected  
525 by Ni metal content. The addition of Co improved the reducibility of Ni species and metal  
526 dispersion. The positive effect of Co addition was only observed with catalysts having low Ni  
527 loading (below 10% in weight). From our results, the Co doped catalyst (10Ni,10Co) is more  
528 active than the 10Ni at low temperature. It could be operated at 300°C and give comparable CO<sub>2</sub>  
529 conversion and methane yields to 10Ni at 350°C, which from a process point of view, should  
530 reduce the energy consumption. Long life-test experiments at 350 °C with the 10Ni; 10Ni,10Co  
531 and 20Ni catalysts already showed a higher CO<sub>2</sub> hydrogenation rate and a higher methane  
532 production rate when compared with other similar catalysts in literature and presented a  
533 remarkably good stability over 200 h run. The very good stability of our novel catalysts tested  
534 over 200 h, and their high activity compared to other catalysts in the literature make them good  
535 candidates for developing greener methanation processes.

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