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Understanding the origins of N<sub>2</sub>O decomposition activity in Mn-Co-Al-O<sub>x</sub> hydrotalcite derived mixed metal oxides.

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## **Abstract**

The catalytic decomposition of N<sub>2</sub>O was studied over a series of calcined (Mn,Fe)-Co-Al hydrotalcite-like compounds. The precursors were prepared by coprecipitation and characterized by XRD and TGA. While the mixed metal oxides derived after calcination at 600 °C were characterized by XRD, N<sub>2</sub> adsorption, H<sub>2</sub>-TPR and XPS. Moreover, *in situ* XAFS measurements over selected mixed metal oxides were performed. Such investigations under reaction conditions are rare, while a comprehensive understanding of the involved active

species may facilitate a knowledge-based catalyst optimization. The activity of the Co-Al (Co/Al = 3/1, mol.%) catalyst varied depending on the loading of Mn or Fe (0.0575, 0.0821, 0.1150, 0.1725, 0.2300, mol.%). In the investigated series,  $\text{Mn}_{0.1725}\text{Co}_3\text{Al}$  mixed metal oxides reached the highest activity with  $T_{50}$  of about 305 and 376 °C under  $\text{N}_2\text{O}/\text{N}_2$  and  $\text{N}_2\text{O}, \text{NO}, \text{O}_2/\text{N}_2$  feed, respectively. *In situ* X-ray absorption experiments over  $\text{Mn}_{0.1725}\text{Co}_3\text{AlO}_x$  suggested that  $\text{Mn}_x\text{Co}_y\text{O}_4$  spinel undergo reduction to CoO and MnO upon heating up to 600 °C in He. Under  $\text{N}_2\text{O}/\text{He}$  conditions initial reoxidation of cobalt species began at 350 °C. The lower activity obtained for  $\text{Fe}_{0.1725}\text{Co}_3\text{AlO}_x$  is explained by the fact that the majority of Fe was not incorporated into the  $\text{Co}_3\text{O}_4$  structure but instead formed less reactive iron oxide clusters.

**Keywords:** hydrotalcite-like compounds, mixed metal oxides, cobalt,  $\text{N}_2\text{O}$  decomposition, XAFS.

## 1. Introduction

The catalytic decomposition of  $\text{N}_2\text{O}$  (de $\text{N}_2\text{O}$ ) belongs to the best available technologies for  $\text{N}_2\text{O}$  abatement from nitric acid production, which is one of the major industrial sources of  $\text{N}_2\text{O}$  emission. The broad collection of catalysts were applied at temperatures below 450-500 °C [1]. As implied by the published results, hydrotalcite derived mixed metal oxides present high activity for de $\text{N}_2\text{O}$  even in the presence of  $\text{H}_2\text{O}$ ,  $\text{O}_2$ ,  $\text{SO}_2$  and/or  $\text{NO}_x$ . The hydrotalcite-like compounds with a general formula of  $\text{M}^{2+}_{1-x}\text{M}^{3+}_x(\text{OH})_2(\text{A}^{n-})_{x/n} \cdot m\text{H}_2\text{O}$ , where  $\text{M}^{2+}$  and  $\text{M}^{3+}$  – bi- and trivalent metal cations, respectively,  $\text{A}^{n-}$  – an interlayer anion, and  $x = \text{M}^{3+}/(\text{M}^{3+} + \text{M}^{2+})$  with a value between 0.17 - 0.50 [2,3], serve as excellent precursors for the preparation of the catalysts of the desired chemical and phase composition for de $\text{N}_2\text{O}$ . Thermal decomposition of hydrotalcite-like compounds at middle temperatures ( $\leq 600$  °C) results in the formation of the relatively high surface mixed metal oxides, with a high dispersion of introduced transition oxide metal species [4–6]. Recently, Jabłońska and Palkovits [1,7] reviewed hydrotalcite derived mixed metal oxides in de $\text{N}_2\text{O}$ , and concluded that the activity of the mixed metal oxides varied depending on the type and loading of the catalytically active metal, its oxidation state as well as dispersion and aggregation state, etc. The research of hydrotalcite derived mixed metal oxides focusses mainly on cobalt-based materials: Co-Al- $\text{O}_x$  (e.g. [8,9]), Co-(Mg)-Mn-(Al)- $\text{O}_x$  (e.g. [10–12]), Co-Mg-

Al-O<sub>x</sub> or Co-Cu-Mg-Al-O<sub>x</sub> (e.g. [13]), etc. Kannan et al. [14–16] and furthermore Pérez-Ramírez et al. [8] found Co/Al with 3/1 molar ratio as optimal hydrotalcite derived catalyst dedicated to deN<sub>2</sub>O among catalysts varied between Co/Al = 3-1/1, mol.%. The Co<sub>3</sub>Al<sub>1</sub> mixed metal oxides reached 84-100% conversion at 450 °C. Kannan et al. [15,16] reported that the activity of Co-Al mixed metal oxides correlated with the Co/Al bulk composition, but, an even better correlation in the activity was obtained with the Co<sup>2+</sup> (generated by surface reduction and reconstruction) of mixed metal oxides, as determined by XPS. Obalová et al. [10,11,17] investigated numerous combinations of Co(Mg)-Mn(Al), and found Co<sub>4</sub>Mn<sub>1</sub>Al<sub>1</sub>O<sub>x</sub> as optimum catalyst for deN<sub>2</sub>O (82-97% conversion at 450 °C). The authors reported an optimum surface amount of Co<sup>2+</sup>/Co<sup>3+</sup> and Mn<sup>2+</sup>/Mn<sup>3+</sup> molar ratios at 1.13 and 2.27 by XPS. Moreover, as determined from H<sub>2</sub>-TPR, Co<sub>4</sub>Mn<sub>1</sub>Al<sub>1</sub>O<sub>x</sub> possessed an optimum amount of components reducible in the temperatures of the maximum conversion of N<sub>2</sub>O (between 350-450 °C) [11]. Since the detailed study of the involved active species of the hydrotalcite derived catalysts under reaction conditions was beyond of the previously published results. ~~Thus, the above studies were the inspiration for~~ Our present investigation focused on identifying *in situ* the exact nature of cobalt species in Mn(Fe)CoAl hydrotalcite-derived mixed metal oxides applied to deN<sub>2</sub>O. Moreover, precursors and/or mixed metal oxides were characterized by XRD, TG, N<sub>2</sub> adsorption and H<sub>2</sub>-TPR, in order to explore additional structure-activity correlations.

## 2. Experimental

### 2.1. Catalysts preparation

A series of Mn(Fe)<sub>x</sub>Co<sub>3</sub>Al<sub>1</sub> (x = 0.0575, 0.0821, 0.1150, 0.1725, 0.2300, mol.%) hydrotalcite-like compounds was prepared by the coprecipitation. An aqueous solution containing appropriate amounts of following metal nitrates: Co(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O (Roth), Al(NO<sub>3</sub>)<sub>3</sub>·9H<sub>2</sub>O (Sigma), Mn(NO<sub>3</sub>)<sub>2</sub>·4H<sub>2</sub>O (Roth), Fe(NO<sub>3</sub>)<sub>3</sub>·9 H<sub>2</sub>O (Roth) and 1 M NaOH (Chemsolute) was dropped simultaneously to a vigorously stirred at 60 °C aqueous solution containing a slight over-stoichiometric excess of Na<sub>2</sub>CO<sub>3</sub> (Sigma). The pH of the reaction mixture was maintained constant at 10.0 ± 0.2 throughout the whole synthesis by NaOH addition. The obtained suspension was aged at 60 °C for another 0.5 h after complete coprecipitation. The solid was filtered, washed carefully

with distilled water and dried at room temperature. Finally, the prepared hydrotalcite-like compounds were crushed and calcined at 600 °C for 6 h with a heating ramp of 10 °C/min and in static air. The hydrotalcite derived mixed metal oxides were kept in a desiccator in order to avoid the reconstruction of the hydroxide-like structure. For catalytic experiments, a fraction of particle size in the range of 0.250-0.500 mm was used.

## 2.2. Catalysts characterization

The X-Ray diffraction (XRD) measurements of the all as-synthesized hydrotalcite-like compounds and mixed metal oxides formed by their thermal decomposition was performed applying a Siemens D5000 XRD diffractometer using Cu-K $\alpha$  radiation ( $\lambda = 1.54056 \text{ \AA}$ , 45 kV, 40 mA). The difference thermogravimetric analysis (DTG) of the hydrotalcite-like compounds (~20 mg) was carried out using a Netzsch STA 409C/CD operated under a flow of air (10 cm<sup>3</sup>/min) in the temperature range of 30-1000 °C with a linear heating rate of 5 °C /min. The specific surface area ( $S_{\text{BET}}$ ) of the mixed metal oxides was determined by low-temperature (-196 °C) N<sub>2</sub> sorption using a Quantachrome Quadrasorb SI. Prior to nitrogen adsorption the samples were outgassed at 250 °C for 12 h using a Quantachrome Flovac degasser. The specific surface area ( $S_{\text{BET}}$ ) was calculated using the Brunauer-Emmett-Teller (BET) multiple point method in the  $p/p_0$  range from 0.05 to 0.3. The chemical analysis of mixed metal oxides was determined by ICP-MS using an Agilent Technologies 8800 Triple Quad spectrometer. Prior to measurement, sample (50 mg) was dissolved in 6 cm<sup>3</sup> mixture of concentrated acids (HCl:HNO<sub>3</sub>, 1:1), and afterwards the resulted mixture was diluted with 64 cm<sup>3</sup> deionized water before warming up to 40 °C for 24 h. The redox properties of the selected mixed metal oxides were studied by the temperature-programmed reduction (H<sub>2</sub>-TPR) using Quantachrome ChemBET Pulsar TPR/TPD. H<sub>2</sub>-TPR runs for the samples (30 mg) were carried out starting from room temperature to 1000 °C, with a linear heating rate of 10 °C /min and in a flow (25 cm<sup>3</sup>/min) of 5.0 vol.% H<sub>2</sub>/Ar. Water vapour was removed from effluent gas by the means of a cold trap placed in an ice-water bath. The H<sub>2</sub> consumption was detected and recorded by TCD detector. The X-ray photoelectron spectra (XPS) of selected mixed metal oxides were measured on a VSW spectrometer equipped with a hemispherical analyzer. The photoelectron spectra were measured using a magnesium MgK $\alpha$  source ( $E = 1253.6 \text{ eV}$ ). The base pressure in the analysis chamber during the measurements was  $3 \cdot 10^{-6} \text{ Pa}$  and the spectra were calibrated on a main carbon C 1s peak at 284.6 eV. The composition and

chemical surrounding of the sample surface were investigated based on the areas and binding energies of Co 2p, Mn 2p, Fe 2p, Al 2p, O 1s and C 1s photoelectron peaks. Mathematical analyses of the XPS spectra were carried out using the XPSpeak 4.1 computer software (RWM. Kwok, The Chinese University of Hong Kong). The X-ray absorption spectra (XAS) of selected samples were collected *in situ* using the quartz capillary flow reactor cells, and gas delivery systems available on the beamline, on station B18 at the Diamond Light Source synchrotron facility. The measurements were carried out using a Si(111) monochromator at the Co K-edge, Mn K-edge or Fe K-edge with the respective Co, Mn or Fe monometallic foils (10  $\mu\text{m}$ ) used as an energy calibrant for the monochromator. The catalyst diluted with  $\text{SiO}_2$  (1:5) was sieved into 0.200-0.250 mm and placed into the reactor. Prior to the reaction the catalyst was outgassed at 600  $^{\circ}\text{C}$  for 1 h in a flow of pure He (10  $\text{cm}^3/\text{min}$ ), and subsequently cooled down to 100  $^{\circ}\text{C}$ . The reactant concentrations at the reactor inlet composed of  $[\text{N}_2\text{O}] = 0.1 \text{ vol.}\%$  and  $[\text{He}] = 99.9 \text{ vol.}\%$  (10  $\text{cm}^3/\text{min}$ ). The temperature was raised in steps of 50-100  $^{\circ}\text{C}$  up to 600  $^{\circ}\text{C}$ . Each temperature was hold for 30 min. X-ray absorption spectra at appropriate K-edges was collected in fluorescence mode for 240 s for Co, Fe or Mn K-edges. At least three spectra for each sample were taken at room temperature, appropriate temperatures and after reaction at room temperature.  $\text{CoO}$ ,  $\text{Co}_3\text{O}_4$ ,  $\text{FeO}$ ,  $\text{Fe}_2\text{O}_3$ ,  $\text{MnO}_2$  references were measured only at room temperature. The data were analysed using the Demeter software package [18,19]); the edge position was determined as the first maximum – after the pre-edge peak – of the derivative of the XANES spectra.

### 2.3. Catalytic tests

The catalytic performance of the mixed metal oxides was evaluated in the  $\text{N}_2\text{O}$  decomposition. The catalytic experiments were carried out under atmospheric pressure in a fixed-bed flow microreactor (i.d., 6 mm; l., 270 mm). Prior to the reaction the catalyst (350 mg) was outgassed at 600  $^{\circ}\text{C}$  for 1 h in a flow of pure  $\text{N}_2$  (100  $\text{cm}^3/\text{min}$ ). The reactant concentrations at the reactor inlet composed of: (i)  $[\text{N}_2\text{O}] = 0.1 \text{ vol.}\%$ ,  $\text{N}_2$  balance, (ii)  $[\text{N}_2\text{O}] = 0.1 \text{ vol.}\%$ ,  $[\text{NO}] = 0.03 \text{ vol.}\%$ ,  $[\text{O}_2] = 4.5 \text{ vol.}\%$ ,  $\text{N}_2$  balance (100  $\text{cm}^3/\text{min}$ ; WHSV = 17  $\text{L} (\text{h g})^{-1}$ ), were analyzed by infrared spectroscopy using a Perkin Elmer Spectrum Two equipped with a Pike 5 m heated gas cell. The temperature was raised in steps of 50  $^{\circ}\text{C}$  starting from 100 up to 600  $^{\circ}\text{C}$ . Each temperature was set constant for 0.5 h.

For selected material, additional tests were carried out in the presence of water vapour. Such catalytic experiments were carried out under atmospheric pressure in a fixed-bed flow microreactor (i.d., X mm; l., X mm). Prior to the reaction, the catalyst (70-150 mg) was activated at 580 °C for 0.5 h in a flow of pure He (75 cm<sup>3</sup>/min). After reactor cooled down, the following composition was applied: [N<sub>2</sub>O] = 0.1 vol.%, ([H<sub>2</sub>O] = 3.5 wt.%), He balance (75 cm<sup>3</sup>/min; WHSV = 30-64 L (h g)<sup>-1</sup>), were analyzed by a Pfeiffer Omnistar quadrupole mass spectrometer equipped with Channeltron and Faraday detectors (0-200 amu).

The conversion of N<sub>2</sub>O (X(N<sub>2</sub>O)) was estimated according to  $X(N_2O) = ([c(N_2O)_{in} - c(N_2O)_{out}] / c(N_2O)_{in}) \times 100\%$ , where:  $c(N_2O)_{in}$  and  $c(N_2O)_{out}$  – concentration of N<sub>2</sub>O in the inlet gas, and concentration of N<sub>2</sub>O in the outlet gas.

### 3. Results and discussion

Fig. 1 presents the XRD patterns of Mn(Fe)<sub>x</sub>Co<sub>3</sub>Al<sub>1</sub> (x = 0.0575, 0.0821, 0.1150, 0.1725, 0.2300, mol.%) hydrotalcite-like compounds, exhibiting rhombohedral symmetry (space group R3m, 3R<sub>1</sub> polytype) [20] with sharp and symmetrical reflections (0 0 3), (0 0 6), (1 1 0) and (1 1 3), and broad and asymmetrical reflections (0 1 2), (0 1 5) and (0 1 8). The intensity of the reflection corresponding to the hydrotalcite-like phase were very weak for samples with 0.0575 mol.% of Mn or Fe. However, the intensity of such phases increased with increasing loading of both transition metals. Table 1 summarizes the unit cell parameters of the hydrotalcite-like compounds and their derivatives. The cell parameters were calculated using a position of (1 0 1) reflection:  $a = 2(d_{1\ 0\ 1})$  and positions of basal reflections:  $c = [3(d_{0\ 0\ 3}) + 6(d_{0\ 0\ 6})]/2$ . The lattice parameter  $a$  depends on the size of the cation in the brucite-like layers, while the parameter  $c$  refers to the interlayer thickness. The  $a$  values for Mn(Fe)<sub>x</sub>Co<sub>3</sub>Al<sub>1</sub> (x = 0.0575, 0.0821, 0.1150, 0.1725, 0.2300, mol.%) hydrotalcite-like compounds varied only slightly with increasing Mn or Fe content and were close to the one obtained for Co<sub>3</sub>Al<sub>1</sub>. The  $a$  values depends mainly on the ionic radii of the cations in octahedral coordination (0.070 nm Co<sup>2+</sup>, 0.070 nm Mn<sup>2+</sup> and 0.070 nm Fe<sup>3+</sup> [21], as cations of metal precursors). The  $c$  values of about 2.3 nm stay characteristic for hydrotalcite-like compounds containing carbonates located in the interlayer space [2]. The interlayer distances increased upon decreasing electronegativity of the cations: Co (1.70) > Fe (1.64) > Mn (1.60) > Al (1.47)

(according to Allred-Rochow scale) [22]. The crystal sizes were calculated from the Scherrer equation  $D = 0.89 \cdot \lambda / \beta \cdot \theta$ , where  $D$  is the crystallite size,  $\lambda$  is the X-ray wavelength,  $\beta$  is the line broadening and  $\theta$  is the Bragg angle. The Fe-containing materials revealed overall higher crystal size (with the exception of  $\text{Fe}_{0.0575}\text{Co}_3\text{Al}_1$ ) than corresponding  $\text{MnCo}_3\text{Al}_1$  compounds.

Fig. 2 presents the DTG profiles of  $\text{Mn}(\text{Fe})_x\text{Co}_3\text{Al}_1$  ( $x = 0.0575, 0.0821, 0.1150, 0.1725, 0.2300$ , mol.%) hydrotalcite-like compounds, while Table 2 gathers total mass loss of these materials. DTG profiles revealed the presence of two stages of weight loss, providing an additional proof of the achievement of the hydrotalcite-like structure. The thermal decomposition of  $\text{Mn}(\text{Fe})$ -Co-Al precursors proceeded in two main stages with total mass losses of about 30-33%. The first DTG minimum centered at about 190-200 °C corresponded to the removal of interlayer and weakly adsorbed water without collapse of the structure. The second peak located at about 230-235 °C appeared due to the dehydroxylation of the brucite-like layers and thermal decomposition of interlayer carbonates and nitrates (e.g. [5,6,20]). The temperatures and peak intensities did not change significantly among studied precursors, possibly due to small differences in the Mn or Fe loading as well as similar size of  $\text{Mn}^{2+}$  and  $\text{Fe}^{3+}$  (as cations of metal precursors) in octahedral coordination of 0.058 and 0.055 nm, respectively [21].

Fig. 3 shows the XRD patterns of calcined  $\text{Mn}(\text{Fe})\text{CoAl}$  hydrotalcite-like compounds. The hydrotalcite-like structure was completely destroyed upon heating at 600 °C with possible formation of  $\text{Co}_3\text{O}_4/\text{CoAl}_2\text{O}_4/\text{Co}_2\text{AlO}_4$  spinels ( $2\theta$  at 19, 31, 37, 39, 45, 56, 59, 65, 77°) (e.g. [8,16]), exhibiting cubic symmetry (space group  $\text{Fd}\bar{3}\text{m}$ ) [24]. The lattice parameter  $a$  in the range of 0.8073-0.8099 nm was close to  $\text{Co}_3\text{O}_4$  ( $a = 0.8084$  nm). Mn- or Fe- containing materials did not reveal any diffraction characteristic for transition metal oxides in the XRD patterns, which confirmed the absence of bigger crystallites. Crystal sizes of 26-33 nm were calculated from (3 1 1) bragg reflection in the XRD patterns using the Scherrer equation.

**Fig. 1, Fig. 2, Fig. 3**



Table 1. Lattice parameters of (Mn,Fe)-Co-Al hydrotalcite-like compounds and corresponding mixed metal oxides.

Hydrotalcite-like compounds	Cell parameter	Cell parameter	Crystallite size	Crystallite size	Mixed metal oxides	Cell parameter	Crystallite size
	$a$ [nm]	$c$ [nm]	$D_a$ [nm]	$D_c$ [nm]		$a$ [nm]	$D_a$ [nm]
$\text{Co}_3\text{Al}_1$	0.3079	2.2956	29	20	$\text{Co}_3\text{Al}_1\text{O}_x$	27	0.8093
$\text{Mn}_{0.0575}\text{Co}_3\text{Al}_1$	0.3085	2.3065	33	22	$\text{Mn}_{0.0575}\text{Co}_3\text{Al}_1\text{O}_x$	32	0.8076
$\text{Mn}_{0.0821}\text{Co}_3\text{Al}_1$	0.3086	2.3060	34	21	$\text{Mn}_{0.0821}\text{Co}_3\text{Al}_1\text{O}_x$	32	0.8083
$\text{Mn}_{0.1150}\text{Co}_3\text{Al}_1$	0.3085	2.3006	25	24	$\text{Mn}_{0.1150}\text{Co}_3\text{Al}_1\text{O}_x$	27	0.8099
$\text{Mn}_{0.1725}\text{Co}_3\text{Al}_1$	0.3080	2.2800	33	24	$\text{Mn}_{0.1725}\text{Co}_3\text{Al}_1\text{O}_x$	26	0.8079
$\text{Mn}_{0.2300}\text{Co}_3\text{Al}_1$	0.3078	0.2790	27	24	$\text{Mn}_{0.2300}\text{Co}_3\text{Al}_1\text{O}_x$	26	0.8099
$\text{Fe}_{0.0575}\text{Co}_3\text{Al}_1$	0.3085	2.3215	22	22	$\text{Fe}_{0.0575}\text{Co}_3\text{Al}_1\text{O}_x$	30	0.8073
$\text{Fe}_{0.0821}\text{Co}_3\text{Al}_1$	0.3086	2.3100	39	26	$\text{Fe}_{0.0821}\text{Co}_3\text{Al}_1\text{O}_x$	33	0.8076
$\text{Fe}_{0.1150}\text{Co}_3\text{Al}_1$	0.3085	2.3065	39	28	$\text{Fe}_{0.1150}\text{Co}_3\text{Al}_1\text{O}_x$	33	0.8093
$\text{Fe}_{0.1725}\text{Co}_3\text{Al}_1$	0.3081	2.2839	34	28	$\text{Fe}_{0.1725}\text{Co}_3\text{Al}_1\text{O}_x$	30	0.8083
$\text{Fe}_{0.2300}\text{Co}_3\text{Al}_1$	0.3081	2.2790	42	30	$\text{Fe}_{0.2300}\text{Co}_3\text{Al}_1\text{O}_x$	31	0.8096

Table 2 lists the specific surface areas ( $S_{\text{BET}}$ ) of the (Mn,Fe)-Co-Al mixed metal oxides.  $S_{\text{BET}}$  for Co-Al-O<sub>x</sub> of 82 m<sup>2</sup>/g, significantly decreased after introduction of Mn or Fe within its structure. A similar trend was observed for both series, i.e. decrease for materials with 0.0821 mol.% then increase up to 0.1725 mol.%, and finally drop in  $S_{\text{BET}}$  for materials with the highest loading of transition metal (0.2300 mol.%). However, slightly higher values for  $S_{\text{BET}}$  were reached over Mn-containing mixed metal oxides. Chemical analysis identified by ICP-MS evidenced sodium residual from preparation procedure up to 2.3 wt.%.

Table 2. Total mass losses of (Mn,Fe)-Co-Al hydrotalcite-like compounds, specific surface areas ( $S_{\text{BET}}$ ), sodium residuals of mixed metal oxides, and  $T_{50}$  of mixed metal oxides in N<sub>2</sub>O/N<sub>2</sub>, N<sub>2</sub>O,NO,O<sub>2</sub>/N<sub>2</sub>\* and N<sub>2</sub>O,H<sub>2</sub>O/He\*\* gas mixtures.

Hydrotalcite-like compounds	Total mass loss [%]	Mixed metal oxides	$S_{\text{BET}}$ [m <sup>2</sup> /g]	Na [wt.%]	$T_{50}$ [° C]
Co <sub>3</sub> Al <sub>1</sub>	32.62	Co <sub>3</sub> Al <sub>1</sub> O <sub>x</sub>	82	1.4	352 <sup>a</sup> *409 <sup>a</sup> **549 <sup>b</sup>
Mn <sub>0.0575</sub> Co <sub>3</sub> Al <sub>1</sub>	31.90	Mn <sub>0.0575</sub> Co <sub>3</sub> Al <sub>1</sub> O <sub>x</sub>	59	0.7	317 <sup>a</sup>
Mn <sub>0.0821</sub> Co <sub>3</sub> Al <sub>1</sub>	31.54	Mn <sub>0.0821</sub> Co <sub>3</sub> Al <sub>1</sub> O <sub>x</sub>	57	1.3	332 <sup>a</sup>
Mn <sub>0.1150</sub> Co <sub>3</sub> Al <sub>1</sub>	30.53	Mn <sub>0.1150</sub> Co <sub>3</sub> Al <sub>1</sub> O <sub>x</sub>	61	1.0	320 <sup>a</sup>
Mn <sub>0.1725</sub> Co <sub>3</sub> Al <sub>1</sub>	30.89	Mn <sub>0.1725</sub> Co <sub>3</sub> Al <sub>1</sub> O <sub>x</sub>	76	2.3	305 <sup>a</sup> *376 <sup>a</sup> **528 <sup>b</sup>
Mn <sub>0.2300</sub> Co <sub>3</sub> Al <sub>1</sub>	31.03	Mn <sub>0.2300</sub> Co <sub>3</sub> Al <sub>1</sub> O <sub>x</sub>	65	0.8	316 <sup>a</sup>
Fe <sub>0.0575</sub> Co <sub>3</sub> Al <sub>1</sub>	31.43	Fe <sub>0.0575</sub> Co <sub>3</sub> Al <sub>1</sub> O <sub>x</sub>	56	0.8	356 <sup>a</sup>
Fe <sub>0.0821</sub> Co <sub>3</sub> Al <sub>1</sub>	31.34	Fe <sub>0.0821</sub> Co <sub>3</sub> Al <sub>1</sub> O <sub>x</sub>	53	0.8	325 <sup>a</sup>
Fe <sub>0.1150</sub> Co <sub>3</sub> Al <sub>1</sub>	31.10	Fe <sub>0.1150</sub> Co <sub>3</sub> Al <sub>1</sub> O <sub>x</sub>	54	1.6	333 <sup>a</sup>
Fe <sub>0.1725</sub> Co <sub>3</sub> Al <sub>1</sub>	30.27	Fe <sub>0.1725</sub> Co <sub>3</sub> Al <sub>1</sub> O <sub>x</sub>	54	0.9	327 <sup>a</sup> *380 <sup>a</sup> **549 <sup>b</sup>
Fe <sub>0.2300</sub> Co <sub>3</sub> Al <sub>1</sub>	31.00	Fe <sub>0.2300</sub> Co <sub>3</sub> Al <sub>1</sub> O <sub>x</sub>	50	0.9	355 <sup>a</sup>

<sup>a</sup>350 mg of catalyst, 100 cm<sup>3</sup>/min total flow; <sup>b</sup>70 mg of catalyst, 75 cm<sup>3</sup>/min total flow.

Fig. 4 presents the H<sub>2</sub>-TPR profiles for the Co<sub>3</sub>Al<sub>1</sub> and selected Mn(Fe)<sub>x</sub>Co<sub>3</sub>Al<sub>1</sub> (x = 0.1725, 0.2300, mol.%) mixed metal oxides. The H<sub>2</sub>-TPR profile for Co<sub>3</sub>Al material revealed the presence of two main reduction peaks, with maxima centered at around 465 and 839 °C. The peak at lower temperatures appeared due to the complete reduction of Co<sub>3</sub>O<sub>4</sub> to metallic cobalt [25–27]. While the high temperature reduction peak was related to the reduction of cobalt in Co<sub>2</sub>AlO<sub>4</sub>/CoAl<sub>2</sub>O<sub>4</sub> [28]. Mn(Fe)<sub>x</sub>Co<sub>3</sub>Al (x = 0.1725, 0.2300, mol.%) revealed similar H<sub>2</sub>-TPR profiles to Co<sub>3</sub>Al<sub>1</sub>. However, the modification of Co<sub>3</sub>Al with Mn or Fe

influenced its redox properties, i.e. the position of the first reduction peaks shifted to higher temperatures for Mn- or Fe-doped materials than for  $\text{Co}_3\text{Al}_1\text{O}_x$ , while the position of the second peak shifted to lower temperatures, indicating depressed reducibility of  $\text{Co}_3\text{O}_4$  and improved of cobalt in  $\text{Co}_2\text{AlO}_4$  and  $\text{CoAl}_2\text{O}_4$ . Such effect was more visible for  $\text{FeCoAlO}_x$ . Additionally, for the Fe-containing samples a broad shoulder appeared at about 700 °C possibly due to reduction of iron oxide species [4,5]. Table 3 summarizes  $\text{H}_2$ -TPR data of the studied materials. The  $\text{H}_2$  uptake varied in the range of 5.22-6.64 mmol/g in the temperature range of 50-530 °C (where  $\text{N}_2\text{O}$  decomposition proceeded). Furthermore, analysis of reduction peak areas ( $A^b/A^c$ , estimated from the integrated areas of the respective  $\text{H}_2$ -TPR peaks) revealed comparable ratio (0.29 to 0.35) across the samples. Due to different oxidation states of metal oxide species in spinel forms, the calculations of the  $\text{H}_2$  uptake based on materials composition could be speculative. Fig. 5 shows the Co 2p, O 1s, Mn 2p and Fe 2p XPS spectra of  $\text{Co}_3\text{Al}_1\text{O}_x$  and  $\text{Mn(Fe)}_{0.1725}\text{Co}_3\text{Al}_1\text{O}_x$ , while Table 3 summarizes the peaks positions, their binding energies, peak areas, full width at half maximum (FWHM) and  $\text{O}_\alpha/(\text{O}_\beta+\text{O}_\gamma)$  molar ratio. The Co 2p XPS spectra exhibited two main peaks characterized by binding energies in the ranges of 781.6-779.6 and 796.9-795.0 eV corresponding to the  $\text{Co}2p_{3/2}$  and  $2p_{1/2}$  spin-orbit peaks, respectively [29]. Thus, since the spin-orbit values for the tested materials have varied in the range of 15.3-15.4 eV, we concluded that mainly  $\text{Co}_3\text{O}_4$  (spin-orbit value of 15.2 eV) together with  $\text{CoAl}_2\text{O}_4$  (as minor compound; spin-orbit value of 15.9 eV) existed on the catalysts surface [29–31]. Considering that Mn or Fe are present only in small amounts in the materials, determination of manganese or iron chemical state in the measured  $\text{Mn(Fe)}_{0.1725}\text{Co}_3\text{Al}_1\text{O}_x$  based on the position of the binding energy could be speculative. Furthermore, Mn or Fe may be present in several chemical states with the overlapping spectra, which are close in energy [11,32]. The O 1s spectra were deconvoluted to lattice oxygen –  $\text{O}_\alpha$ , surface adsorbed oxygen, OH groups and oxygen vacancies –  $\text{O}_\beta$  and adsorbed molecular water –  $\text{O}_\gamma$  [33]. Additional low peaks at about 527-528 eV appeared possibly due to the differential charging of the materials [34]. The molar ratio of  $\text{O}_\alpha/(\text{O}_\beta+\text{O}_\gamma)$  varied in the range of 0.21-0.32.

**Fig. 4, Fig. 5**

Table 3. Amounts of H<sub>2</sub> consumed during H<sub>2</sub>-TPR measurements (H<sub>2</sub> uptake), the peaks positions, their binding energies, peak areas, full width at half maximum (FWHM) and O<sub>α</sub>/(O<sub>β</sub>+O<sub>γ</sub>) molar ratio of mixed metal oxides.

Mixed metal oxides	H <sub>2</sub> uptake <sup>a</sup> [mmol/g]	A <sup>b</sup> /A <sup>c</sup> [a.u.]	Position Co 2p <sub>3/2</sub> *O 1s ■Mn 2p <sub>3/2</sub> □Fe 2p <sub>3/2</sub>	FWHM [eV]	Area [a.u.]	O <sub>α</sub> /(O <sub>β</sub> +O <sub>γ</sub> ) <sup>d</sup>
Co <sub>3</sub> Al <sub>1</sub> O <sub>x</sub>	26.48	0.33	780.35	4.09	11998	0.23
	6.64 <sup>b</sup>		786.26	7.90	4073	
	19.84 <sup>c</sup>		802.84	6.75	2239	
			*527.07	1.72	462	
			*528.77	1.92	2066	
			*530.38	2.08	6369	
			*531.91	2.10	2697	
Mn <sub>0.1725</sub> Co <sub>3</sub> Al <sub>1</sub> O <sub>x</sub>	22.84	0.35	781.63	3.79	8333	0.21
	5.90 <sup>b</sup>		785.80	8.90	2826	
	16.94 <sup>c</sup>		804.53	8.64	1134	
			*528.51	1.43	239	
			*530.07	2.09	2126	
			*531.72	2.25	7926	
			*533.41	1.95	2106	
Fe <sub>0.1725</sub> Co <sub>3</sub> Al <sub>1</sub> O <sub>x</sub>	23.46	0.29	■643.03	4.00	1080	0.32
	5.22 <sup>b</sup>		779.63	3.94	7137	
	18.24 <sup>c</sup>		784.18	8.19	2085	
			802.17	8.64	1244	
			*526.58	1.63	324	
			*528.37	2.20	2077	
			*529.81	2.04	4523	
			*531.28	2.06	1933	
			□710.44	5.20	956	

<sup>a</sup>Calculated by equation:  $Y = 1E-08X + 1E-07$ ,  $R^2 = 0.9996$ , and X, Y referred to the area of each reduction peak and the H<sub>2</sub> consumption, respectively. <sup>b</sup>In the region 50-530 °C. <sup>c</sup>In the region 530-1000 °C. <sup>d</sup>Estimated from the integrated areas of the respective XPS peaks.

Fig. 6 shows the XANES spectra of Mn(Fe)<sub>0.1725</sub>Co<sub>3</sub>Al<sub>1</sub>O<sub>x</sub> mixed metal oxides. In comparison to the Co<sub>3</sub>O<sub>4</sub> reference spectrum (Co K-edge), the spectrum of Mn<sub>0.1725</sub>Co<sub>3</sub>Al<sub>1</sub>O<sub>x</sub> at room temperature showed a more intense pre-edge peak which could be rationalized as being caused by a greater degree of Co in a non-centrosymmetric geometry in this sample. Furthermore, an adsorption edge at lower energies – 7717.100 eV at room temperature versus 7716.440 eV after the thermal treatment in He – indicated a lower overall Co oxidation state (Fig 6A). This suggested the presence of a CoAl<sub>2</sub>O<sub>4</sub> type spinel where the substitution of Co<sup>3+</sup> by Al<sup>3+</sup> in the octahedral position leads to a higher contribution of Co<sup>2+</sup> Td. Indeed it has previously been shown that CoAl<sub>2</sub>O<sub>4</sub> type

spinel phase can form at temperatures as low as 390 °C [35]. The Mn K-edge spectra acquired at room temperature (Fig. 6B) closely resembled that of a  $\text{Mn}_3\text{O}_4$  spinel reported previously [36]. To date no XAFS data exists concerning mixed Mn and Co spinels although a detailed XRD/vibrational spectroscopic study of Co/Mn substitution suggests that such phases can readily be formed and therefore a mixed  $\text{Mn}_x\text{Co}_y\text{O}_4$  and/or  $\text{Mn}_x\text{Co}_y\text{Al}_z\text{O}_4$  could be present in our  $\text{Mn}_{0.1725}\text{Co}_3\text{Al}_1\text{O}_x$  [37]. For  $\text{Fe}_{0.1725}\text{Co}_3\text{Al}_1\text{O}_x$  mixed metal oxides measured at room temperature, Co K-edge XANES revealed comparable Co speciation to the Mn-containing sample (Fig. 6E). Nevertheless, the Fe near-edge spectrum closely resembled that of  $\alpha\text{-Fe}_2\text{O}_3$  (Fig. 6F), suggesting that unlike Mn, Fe did not incorporate so readily into the  $\text{Co}_3\text{O}_4$  structure. In agreement, our  $\text{H}_2$ -TPR results showed separate reduction of iron oxide species in  $\text{Fe}_{0.1725}\text{Co}_3\text{Al}_1\text{O}_x$ ; however, the shift to higher temperatures of  $\text{Co}_3\text{O}_4$  reduction peak suggests that small amounts of iron must have incorporated into the spinel structure thereby affecting its redox properties.

Changes occurring in  $\text{Mn}_{0.1725}\text{Co}_3\text{Al}_1\text{O}_x$  mixed metal oxides, in the presence of He and  $\text{N}_2\text{O}/\text{He}$ , were followed by studying the Co and Mn K-edge XANES spectra between room temperature and 600 °C. A shift in the Co absorption edge to lower energies as well as a decrease in the pre-edge intensity were observed upon He treatment at 600 °C, which is also consistent with a decrease in the nominal valence of Co in the material (Fig. 6A). The spectra resembled that of the CoO reference constituted by  $\text{Co}^{2+}$  in an octahedral environment. However, the sample's higher pre-edge intensity when compared to  $\text{CoO}/\text{Co}_3\text{O}_4$  suggested some  $\text{Co}^{2+}$  was still present in a tetrahedral environment. Considering the  $\text{H}_2$ -TPR results pertaining to the reducibility of both cobalt oxide species present in the catalyst, it seems that  $\text{Mn}_x\text{Co}_y\text{O}_4$  is reduced to (Mn)CoO while  $\text{CoAl}_2\text{O}_4$ , with  $\text{Co}^{2+}$  in a tetrahedral environment, remained unchanged. EXAFS  $k$ -plots for Co and Mn in  $\text{Mn}_{0.1725}\text{Co}_3\text{Al}_1\text{O}_x$  before and after reduction are shown in Fig.1S. in the supplementary information. At room temperature the Mn and Co fine structure resembled closely the  $\text{Co}_3\text{O}_4$  reference while in the reduced sample the fine structure is similar to CoO. This further confirms the presence of the initial spinel environment for both Mn and Co and that in both cases this evolves into the rock salt  $\text{M}^{2+}\text{O}$  phase. Similar to Co, Mn also undergoes reduction upon activation in He at 600 °C; the reduced spectra resembling features of MnO [36]. Finally, in the presence of  $\text{N}_2\text{O}/\text{He}$ , both Co and Mn oxide species reoxidized to their initial state. Fig 6C and D show the temperature dependence of this reoxidation process; the spectral changes were observed at 300-450 °C

temperature range which coincided with the temperature needed to obtain full N<sub>2</sub>O conversion. The MnO appeared easier to reoxidize than CoO since the spectral changes in Mn K-edge XANES commenced at 300 °C while changes in Co K-edge occurred at 350 °C.

Furthermore, the changes in the oxidation state of Co at different reaction stages in Mn<sub>0.1725</sub>Co<sub>3</sub>Al<sub>1</sub>O<sub>x</sub> were studied by the investigation of the position of the absorption edge (defined as the first maximum of the derivative plot beyond the pre-edge peak). Table 4 presents the Co K-edge absorption positions relative to Co foil ( $\Delta E = E_{\text{sample}} - E_{\text{foil}}$ ) of Mn<sub>0.1725</sub>Co<sub>3</sub>Al<sub>1</sub>O<sub>x</sub> mixed metal oxides at different stages of the experiment as well as the  $\Delta E$  of Co<sub>3</sub>O<sub>4</sub> and CoO as references. Again, the  $\Delta E$  of the sample after treatment with He at 600 °C was comparable to CoO. While the reoxidation, under N<sub>2</sub>O/He conditions, leads to the recovery of its initial oxidation state. Table 5 lists the results of the curve-fitting analysis for the first coordination shell. First shell quick fit analysis of the EXAFS was carried out to gain insight into the average Co-O distances and coordination numbers. Fitting revealed higher coordination numbers and Co-O bond distances of 0.208 nm for Mn<sub>0.1725</sub>Co<sub>3</sub>Al<sub>1</sub>O<sub>x</sub> mixed metal oxide pretreated with He at 600 °C, which is consistent with the appearance of CoO type structure. Otherwise, Mn<sub>0.1725</sub>Co<sub>3</sub>Al<sub>1</sub>O<sub>x</sub> at room temperature or in the presence of N<sub>2</sub>O/He at 600 °C showed a shorter Co-O of ~0.191 nm, corresponding to the presence of a majority spinel phase. As expected from XANES, the Co-O shell fitting results Mn<sub>0.1725</sub>Co<sub>3</sub>Al<sub>1</sub>O<sub>x</sub> and Fe<sub>0.1725</sub>Co<sub>3</sub>Al<sub>1</sub>O<sub>x</sub> at room temperature gave very similar results.

**Fig. 6**

Table 4. Co K-edge energy positions relative to Co foil ( $E_0$ ) for Mn<sub>0.1725</sub>Co<sub>3</sub>Al<sub>1</sub>O<sub>x</sub> mixed metal oxides at room temperature, after reduction under He and after reoxidation under N<sub>2</sub>O/He at 600 °C as well as references at room temperature.

Mixed metal oxides	$\Delta E$ [eV]	References	$\Delta E$ [eV]
Mn <sub>0.1725</sub> Co <sub>3</sub> Al <sub>1</sub> O <sub>x</sub>		room temperature	
room temperature	8.1	CoO	7.4
600 °C He	7.4	Co <sub>3</sub> O <sub>4</sub>	8.5
600 °C N <sub>2</sub> O/He	8.1		

Table 5. Coordination numbers (CN), bond distances between adsorbed and backscatter atoms (R), inner potential corrections to account for the difference in the inner potential between the sample and the reference compound (E), Debye-Waller factors ( $2\sigma^2$ ), and residual factors (Rf) of  $\text{Mn}_{0.1725}\text{Co}_3\text{Al}_1\text{O}_x$  mixed metal oxides.

Mixed metal oxides	Shell Co-O	CN	R [nm]	$\Delta E_0$ [eV]	$10^2 * \sigma^2$ [nm]	R <sub>f</sub> [%]
$\text{Fe}_{0.1725}\text{Co}_3\text{Al}_1\text{O}_x$ room temperature He		2.9	0.192	4.65	0.012	0.16
$\text{Mn}_{0.1725}\text{Co}_3\text{Al}_1\text{O}_x$ room temperature He		2.8	0.191	4.64	0.016	1.30
after He 600 °C		4	0.208	2.29	0.16	3.2
after N <sub>2</sub> O 600 °C		2.2	0.191	5.40	0.084	1.9

Fig. 7 presents the results of catalytic tests performed over  $\text{Mn}(\text{Fe})_x\text{Co}_3\text{Al}_1$  ( $x = 0.0575, 0.0821, 0.1150, 0.1725, 0.2300$ , mol.%) mixed metal oxides, while Table 2 lists temperature necessary to obtain 50% N<sub>2</sub>O conversion ( $T_{50}$ ). The N<sub>2</sub>O conversion from the reaction mixture started at about 150-200 °C, while full conversion was reached at about 450-500 °C for all tested materials.  $\text{Co}_3\text{Al}_1$  reached  $T_{50}$  at about 352 °C with the full conversion at 500 °C. Incorporation of Mn or Fe into  $\text{Co}_3\text{Al}_1$  structure improved catalytic activity of mixed metal oxides. An exception was  $\text{Fe}_{0.2300}\text{Co}_3\text{Al}_1$ , which showed catalytic activity similar to  $\text{Co}_3\text{Al}_1$ . Reproducibility of our results of catalytic tests was confirmed by repeated measurements. The activity differentiated among tested materials without clear trend neither related to the Mn or Fe nor Na (up to 2.3 wt.%) content in the materials. Obalová et al. [32] pointed out that 1.15 wt.% of Na introduced by impregnation already slightly enhanced activity of  $\text{Co}_4\text{MnAlO}_x$ . While materials with Na loaded by impregnation was reported to facilitate N<sub>2</sub>O decomposition than materials with Na present after preparation procedure [33,34]. The optimum of deposited Na content varied also depending on the applied mixed metal oxides: 0.75 wt.% for  $\text{Co}_{2.5}\text{Rh}_{0.05}\text{Al}_1\text{O}_x$  [33], 1.5 wt.% for  $\text{Co}_3\text{Al}_1\text{O}_x$  [35] or 1.4 wt.% for  $\text{Co}_4\text{Mn}_1\text{Al}_1\text{O}_x$  [36]. Farris et al. [37] found out an optimum Na residual content in the range of 3.0-6.0 wt.% in Co-Al-O<sub>x</sub> was supposed to promote the decomposition of N<sub>2</sub>O facilitating over 80% conversion at 475 °C. Doping with 1.0-2.0 wt.% of Na resulted in comparable results. Further research should be carried out in order to clarify these remarkable observations over investigated mixed metal oxides.

The highest activity among tested materials reached  $\text{Mn}_{0.1725}\text{Co}_3\text{Al}_1$ . Such catalyst reached with  $T_{50}$  at 305 °C with and full conversion at 400 °C. Furthermore,  $\text{Mn}_{0.1725}\text{Co}_3\text{Al}_1$  possessed similar activity to the Ag-doped catalysts – (0.7 wt.%) $\text{AgCo}_3(\text{Mg}_1)\text{Al}_1$ , and only slightly lower to the (0.7 wt.%) $\text{RhCo}_3\text{Mg}_1\text{Al}_1$ , reported as one of the most active and stable hydrotalcite derived mixed metal oxides in the  $\text{N}_2\text{O}$  decomposition with excellent activity and stability performance [7,38]. Catalytic tests were carried out under the same reaction conditions (Fig. 6C).  $\text{Co}_3\text{Al}_1$  and  $\text{Mn}(\text{Fe})_{0.1725}\text{Co}_3\text{Al}_1$  were also tested in the presence of NO and  $\text{O}_2$  (350 mg of catalyst, 100  $\text{cm}^3/\text{min}$  total flow).  $\text{Mn}_{0.1725}\text{Co}_3\text{Al}_1$  presented  $T_{50}$  of 376 °C, thus temperature of about 70 °C higher than for tests without NO and  $\text{O}_2$ . Slightly lower activity above 350 °C was obtained over  $\text{Fe}_{0.1725}\text{Co}_3\text{Al}_1$  with  $T_{50}$  at 380 °C. Furthermore, for practical applications,  $\text{Co}_3\text{Al}_1$  and  $\text{Mn}(\text{Fe})_{0.1725}\text{Co}_3\text{Al}_1$  were tested in the presence of  $\text{H}_2\text{O}$  (70 mg of catalyst, 75  $\text{cm}^3/\text{min}$ ), as displayed on Fig. 2SA. The highest resistance to water vapour showed  $\text{Mn}_{0.1725}\text{Co}_3\text{Al}_1$  with  $T_{50}$  of 549 °C. Other materials presented significantly lower resistance to water vapour. Fig. 2SB presents the contribution of NO formation over  $\text{Co}_3\text{Al}_1$  and  $\text{Mn}(\text{Fe})_{0.1725}\text{Co}_3\text{Al}_1$ . The highest amount of such by-product in  $\text{N}_2\text{O}$  decomposition appeared over  $\text{Fe}_{0.1725}\text{Co}_3\text{Al}_1$ . For other materials the formation of NO did not exceed 15 ppm in the studied temperatures of 200-550 °C. Notably, for catalytic tests carried out in the presence of water vapour NO formation decreased. In Fig. 3S, a time-on-stream tests was conducted to evaluate the stability of  $\text{Co}_3\text{Al}_1$  and  $\text{Mn}(\text{Fe})_{0.1725}\text{Co}_3\text{Al}_1$  at 450 °C. All materials showed stable conversion during first 85 min in the  $\text{N}_2\text{O}/\text{N}_2$  feed. Subsequently, after introduction water vapour into the feed, the conversion for all materials significantly dropped, and reached stable level below 20%. However, switching from wet to dry reaction mixture resulted in an increase of the catalysts conversion to the former level. Thus, the introduction of  $\text{H}_2\text{O}$  into the feed did not result in the permanent deactivation of the catalysts.

Obalová et al. [10,16] reported that the high activity of  $\text{Co}_4\text{Mn}_1\text{Al}_1$  hydrotalcite derived mixed metal oxides appeared due to an optimum content of components reducible in the temperatures of the maximum conversion of  $\text{N}_2\text{O}$  (between 350-450 °C). Analysis of our reduction peak areas showed similar ratio (0.29 to 0.35) across the samples. Crystal sizes were calculated from (3 1 1) bragg reflection in the XRD patterns using the Scherrer equation; the comparable results of 27, 26 and 30 nm for  $\text{Co}_3\text{Al}_1\text{O}_x$ ,  $\text{Mn}_{0.1725}\text{Co}_3\text{Al}_1\text{O}_x$  and  $\text{Fe}_{0.1725}\text{Co}_3\text{Al}_1\text{O}_x$  respectively discard size effects in the catalytic performance. Although, the strength of lattice oxygen-metal bonds was reported to determine the catalysts activity in  $\text{deN}_2\text{O}$  [11], we did not observe clear correlation



between  $O_{\alpha}/(O_{\beta}+O_{\gamma})$  molar ratio and catalytic activity of mixed metal oxides. ~~Thus it seems that the samples' different reactivity was related mainly to the Mn and Fe speciation observed by XAS. Mn in  $Mn_{0.1725}Co_3Al_1O_x$  appeared incorporated within spinel structure; MnO and CoO phases present after activation reoxidize under  $N_2O/He$  feed, showing that both take part in redox processes for de $N_2O$ . Indeed it appears that MnO seemed to undergo faster reoxidation suggesting it may act as better electron donor in  $N_2O$  activation step considered the rate determining stem of the mechanism [39,40].~~ Indeed this observation of Mn being easier to oxidise back to 3+ than Co, yet harder to reduce to 2+ is completely consistent with the respective redox potentials for the two elements [31]. Iron in  $Fe_{0.1725}Co_3Al_1O_x$  could have similar role as Mn due to its higher oxidability compared with cobalt oxides. Nevertheless, as most of the iron was not incorporated to the spinel but appeared as separate  $Fe_2O_3$  phase, its effect in catalytic activity was less pronounced than for Mn in the  $Mn_{0.1725}Co_3Al_1O_x$  sample. Accordingly, decomposition of  $N_2O$  over tested mixed metal oxides followed the cationic redox mechanism [11,24], consisting of  $N_2O$  activation by electron transfer from metal sites, and diffusive recombination of the surface oxygen intermediates into oxygen, concerted with the back electron transfer that restores the oxidation state of the active sites. The regeneration of the active sites through oxygen desorption is considered as the rate-determining step. In this context, Co oxidizes when  $N_2O$  is adsorbed and then Co is again reduced when  $O_2$  is released. Thus, during reaction under  $N_2O/He$  conditions, Co is continuously oxidizing and reducing. The doping, in particular Mn, may generate new redox sites at the surface or may enhance the oxygen desorption from cobalt sites. Taking into account the very weak amount of manganese added and the fact that manganese appeared incorporated within structure, the latter assumption seems more likely.

**Fig. 7**

#### **4. Conclusion**

$Mn(Fe)_xCo_3Al_1$  ( $x = 0.0575, 0.0821, 0.115, 0.1725$  and  $0.2300$ , mol.%) hydrotalcite derived mixed metal oxides were synthesized by coprecipitation and subsequent calcination. The catalytic activity of  $Co_3Al_1$  mixed metal oxides was improved in de $N_2O$  by incorporation of appropriate amount of Mn or Fe.  $Mn_{0.1725}Co_3Al_1$  mixed metal

oxides reached the highest activity with  $T_{50}$  of about 305 and 376 °C under  $N_2O/N_2$  and  $N_2O, NO, O_2/N_2$  feed, respectively. The trend for catalytic conversion was  $Mn_{0.1725}Co_3AlO_x > Fe_{0.1725}Co_3AlO_x > Co_3AlO_x$ . Detailed evaluation of the active species was realized by *in situ* XAFS study. Correlation of the catalytic data with the XAS results suggested that doping  $Co_yO_4$  spinel by Mn (Fe), easier to oxidise, leads to a better facility to desorb oxygen, ~~as the active phase for  $de-N_2O$~~ . The presence of Mn in the spinel structure seemed to provide surface Co active sites easier to release oxygen. The lower activity of the  $Fe_{0.1725}Co_3AlO_4$  mixed metal oxides was attributed to the fact that Fe did not incorporate so readily into the cobalt spinel structure forming less active iron oxide clusters instead.

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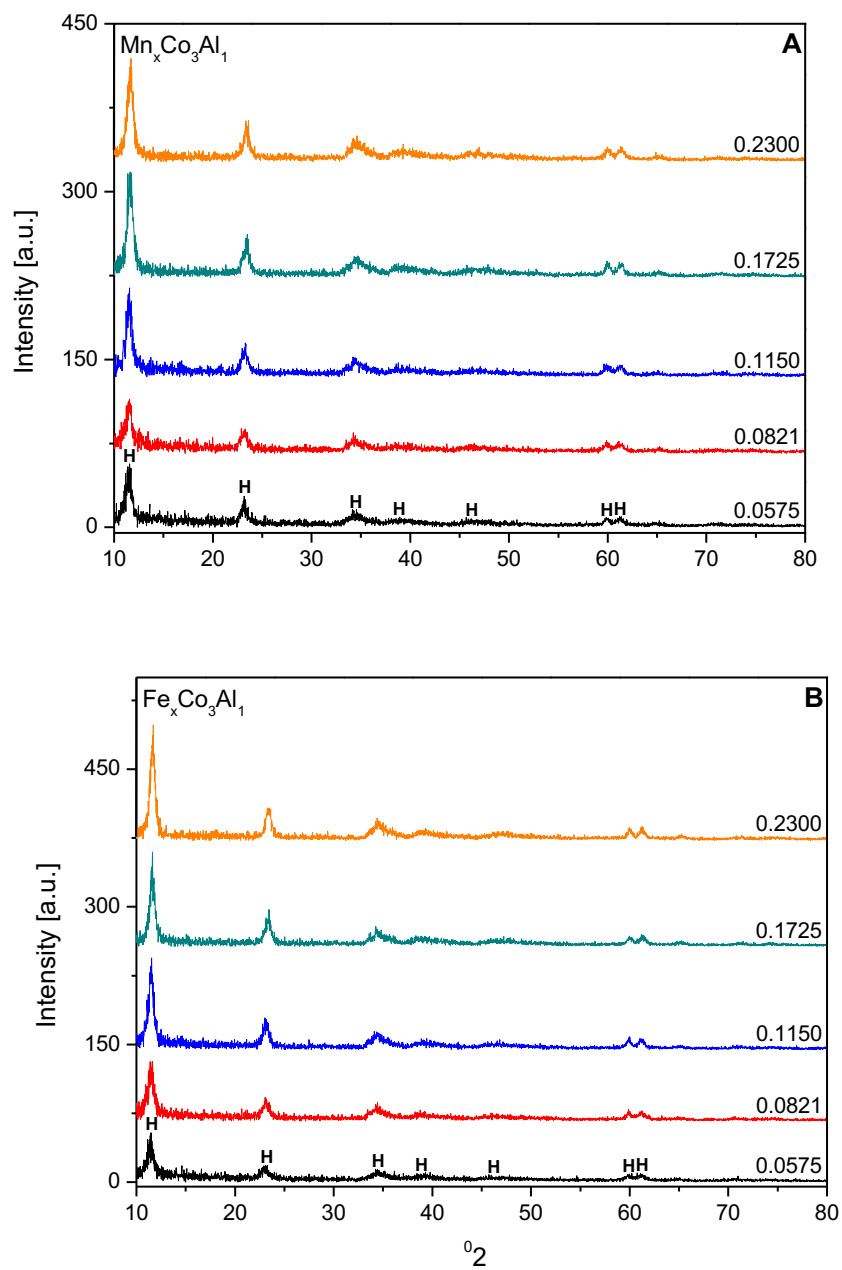


Fig. 1. X-ray diffraction patterns of Mn(Fe)-Co-Al hydrotalcite-like compounds; H – hydrotalcite-like phase.

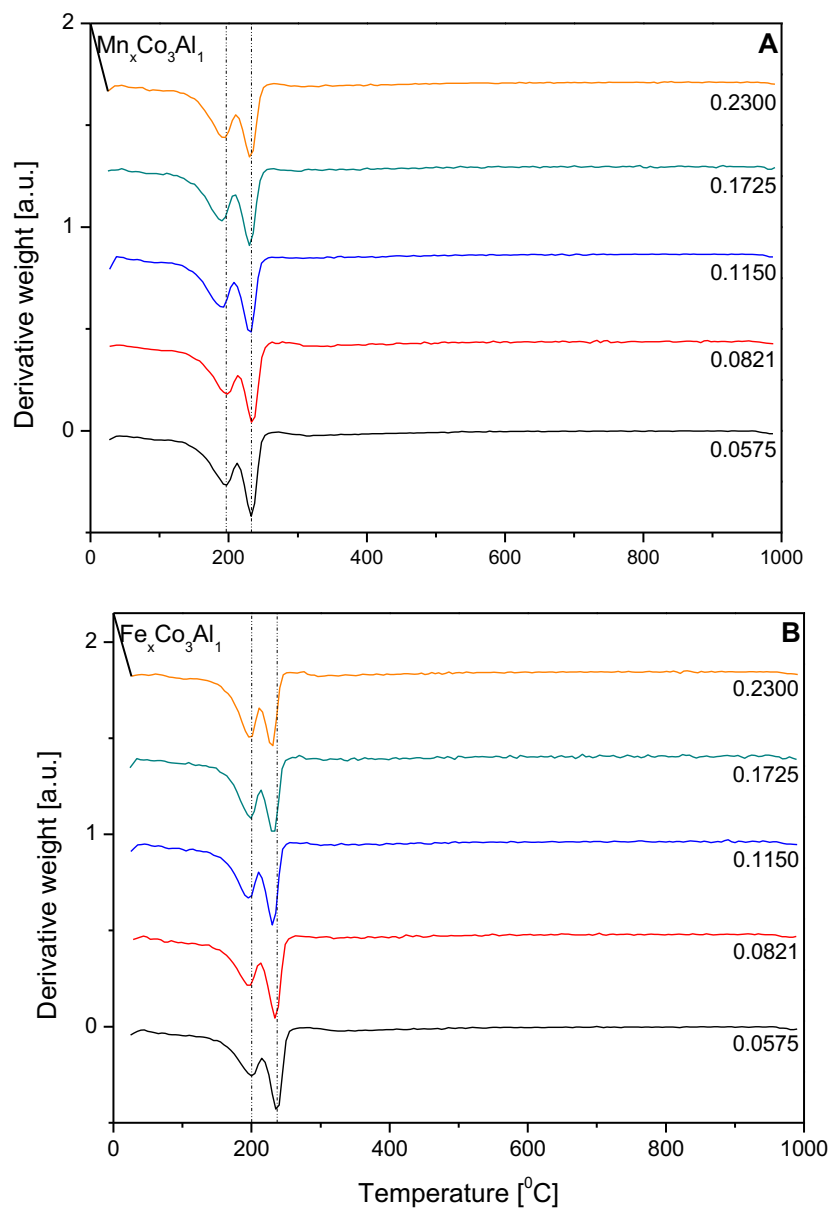


Fig. 2. DTG profiles of Mn(Fe)-Co-Al hydrotalcite-like compounds; experimental conditions: mass of sample = 20 mg, flow of synthetic air = 10 cm<sup>3</sup>/min, liner heating rate of 5 K/min.



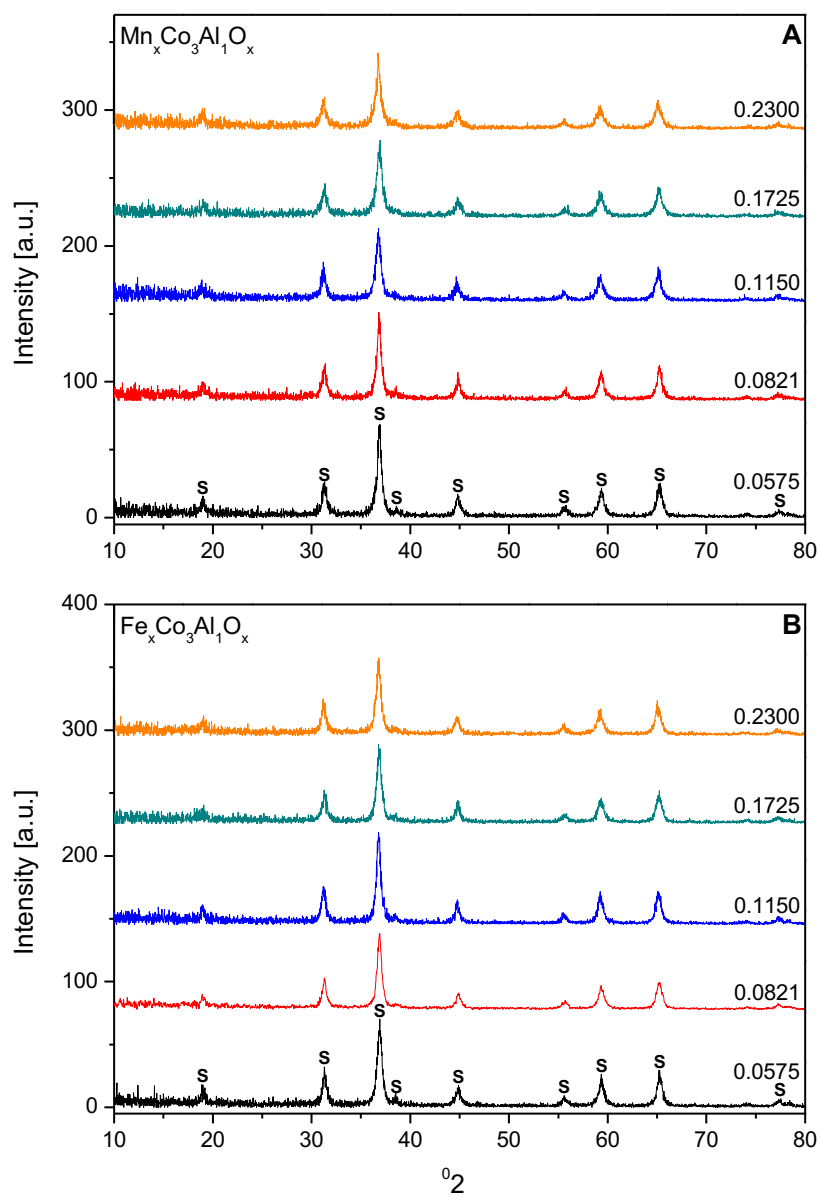


Fig. 3. X-ray diffraction patterns of Mn(Fe)-Co-Al mixed metal oxides; S –  $\text{Co}_3\text{O}_4/\text{CoAl}_2\text{O}_4/\text{Co}_2\text{AlO}_4$ .

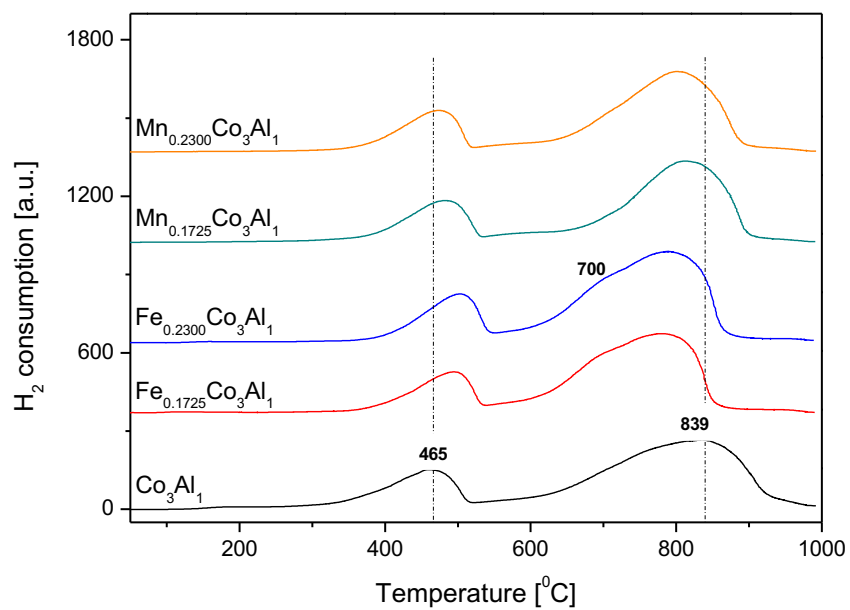


Fig. 4. H<sub>2</sub>-TPR profiles of selected (Mn,Fe)-Co-Al mixed metal oxides; experimental conditions: mass of catalysts = 30 mg, [H<sub>2</sub>] = 5.0 vol.%, [Ar] = 95.0 vol.%, flow rate = 25 cm<sup>3</sup>/min, linear heating of 5 K/min.

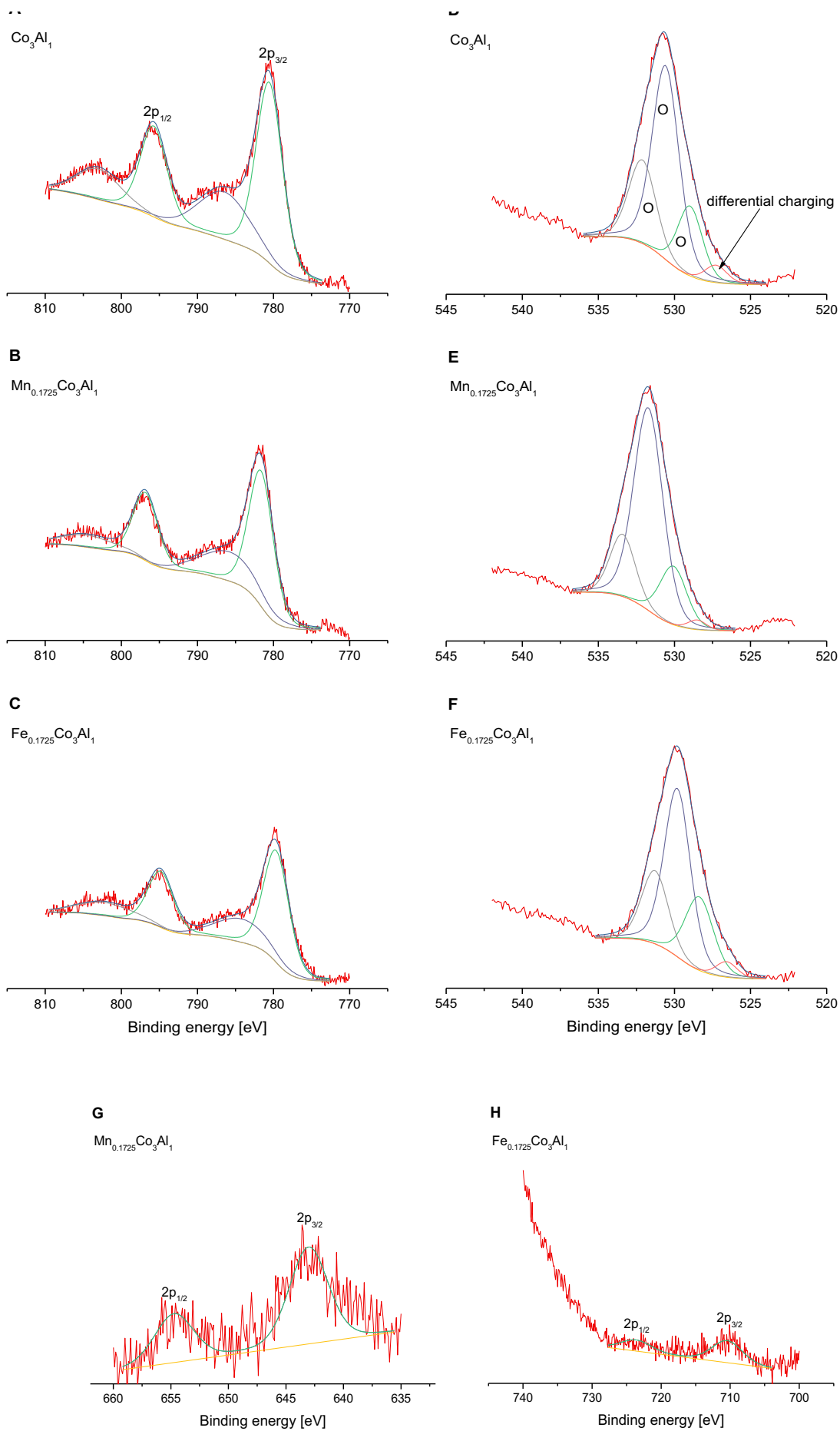


Fig. 5. XPS spectra of selected (Mn,Fe)-Co-Al mixed metal oxides; Co 2p (A-C), O 1s (D-F), Mn 2p (G) and Fe 2p (H).

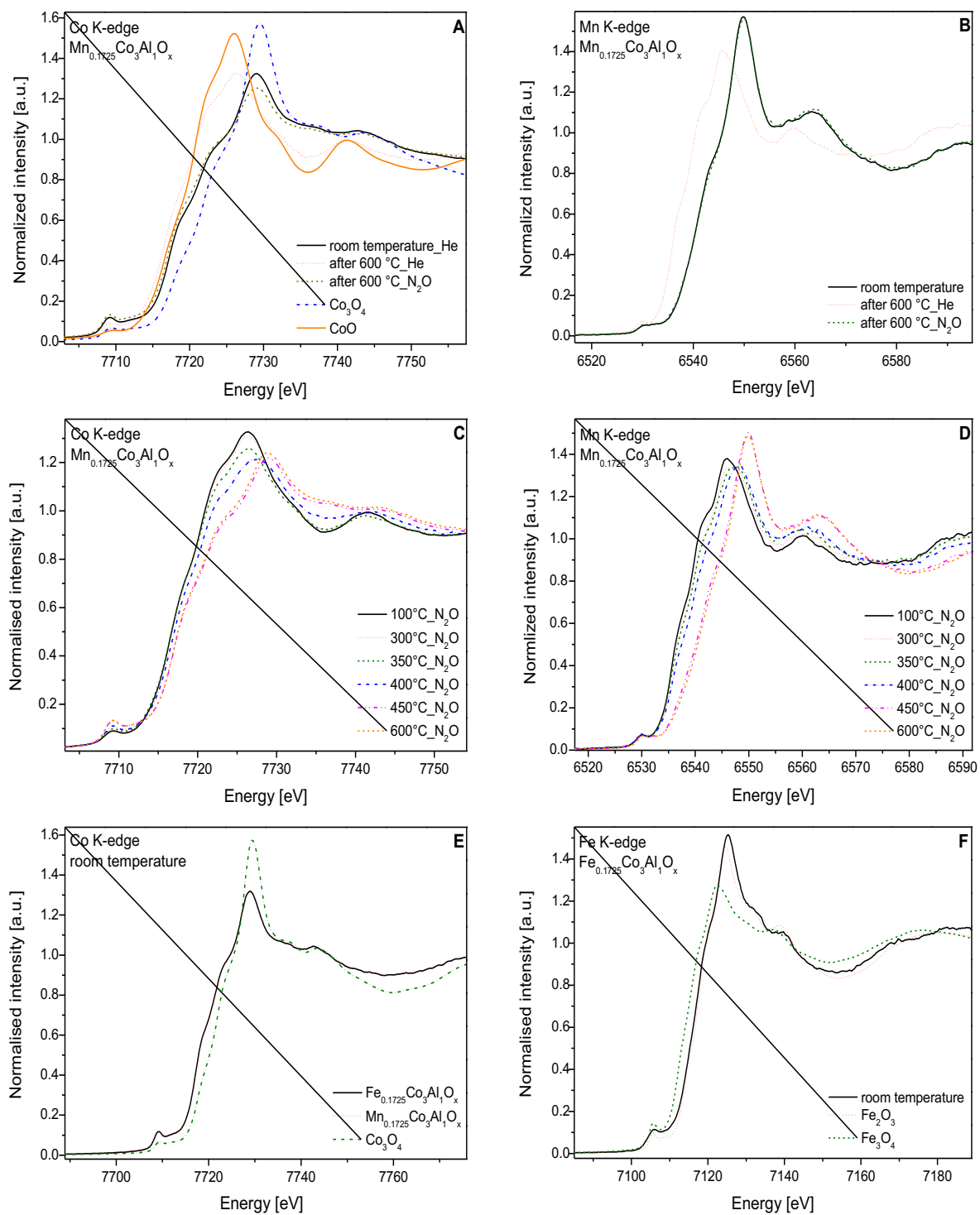


Fig. 6. *In situ* XANES spectra of A) Co K-edge for  $\text{Mn}_{0.1725}\text{Co}_3\text{Al}_1\text{O}_x$  at different reaction stages and Co references; B) Mn K-edge for  $\text{Mn}_{0.1725}\text{Co}_3\text{Al}_1\text{O}_x$  sample acquired at different stages of reaction; C) Co K-edge during the temperature ramp under  $\text{N}_2\text{O}$ ; D) Mn K-edge during the temperature ram under  $\text{N}_2\text{O}$ ; E) Co K-edge for  $\text{Mn}_{0.1725}\text{Co}_3\text{Al}_1\text{O}_x$ ,  $\text{Fe}_{0.1725}\text{Co}_3\text{Al}_1\text{O}_x$  and  $\text{Co}_3\text{O}_4$  reference at room temperature; and F) Fe K-edge for  $\text{Fe}_{0.1725}\text{Co}_3\text{Al}_1\text{O}_x$  and references.

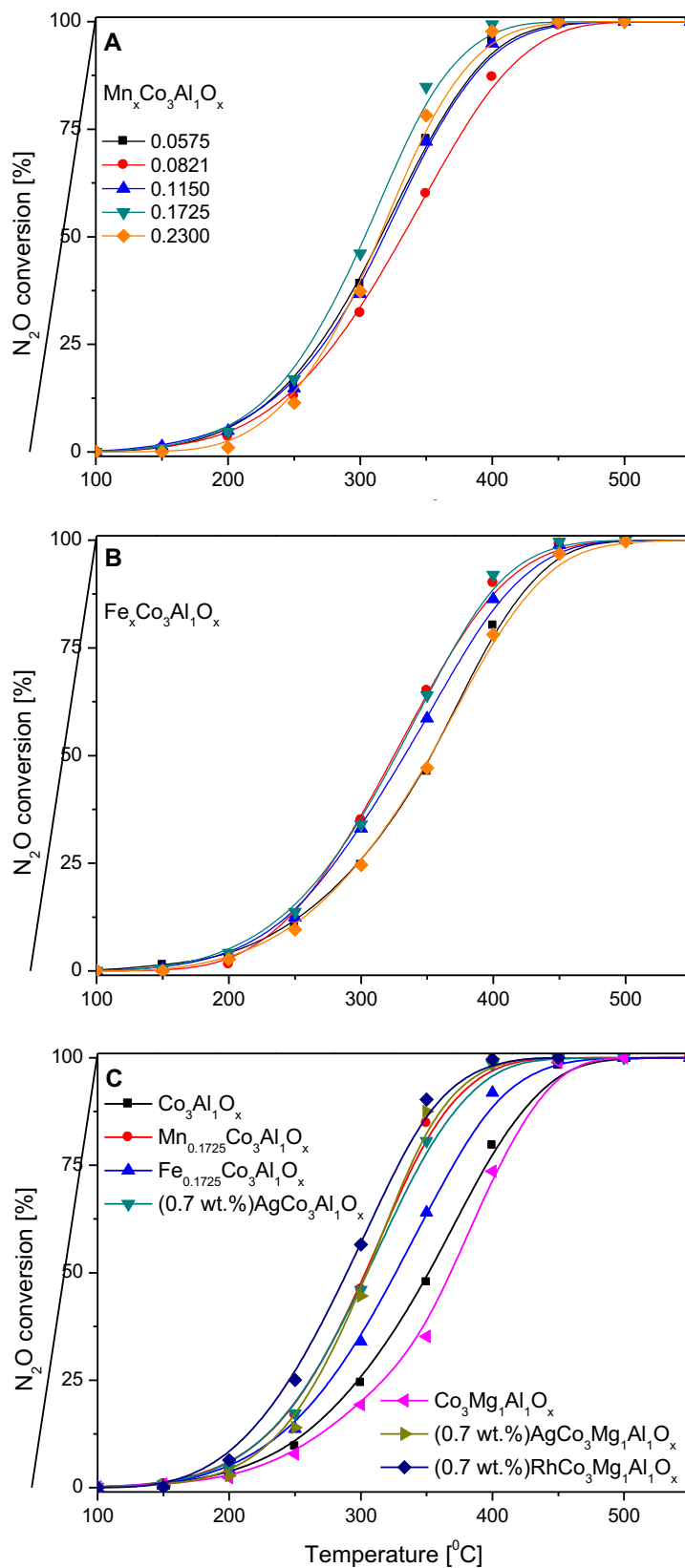


Fig. 7. Results of catalytic tests performed over  $\text{Co}_3\text{Al}_1\text{O}_x$ ,  $(\text{Mn,Fe})_x\text{Co}_3\text{Al}_1\text{O}_x$  ( $x = 0, 0.0575, 0.0821, 0.1150, 0.1725, 0.2300$ ) and  $(0.7 \text{ wt. \%})\text{Ag}(\text{Rh})\text{Co}_3(\text{Mg}_1)\text{Al}_1\text{O}_x$  mixed metal oxides; reaction conditions: mass of catalysts = 350 mg,  $[\text{N}_2\text{O}] = 0.1 \text{ vol. \%}$ ,  $\text{N}_2$  balance, total flow rate =  $100 \text{ cm}^3/\text{min}$ , WHSV of  $17 \text{ L (h g)}^{-1}$ .