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Experimental and numerical studies of the influence of diluent on characteristic micro-scale combustion flame behaviour

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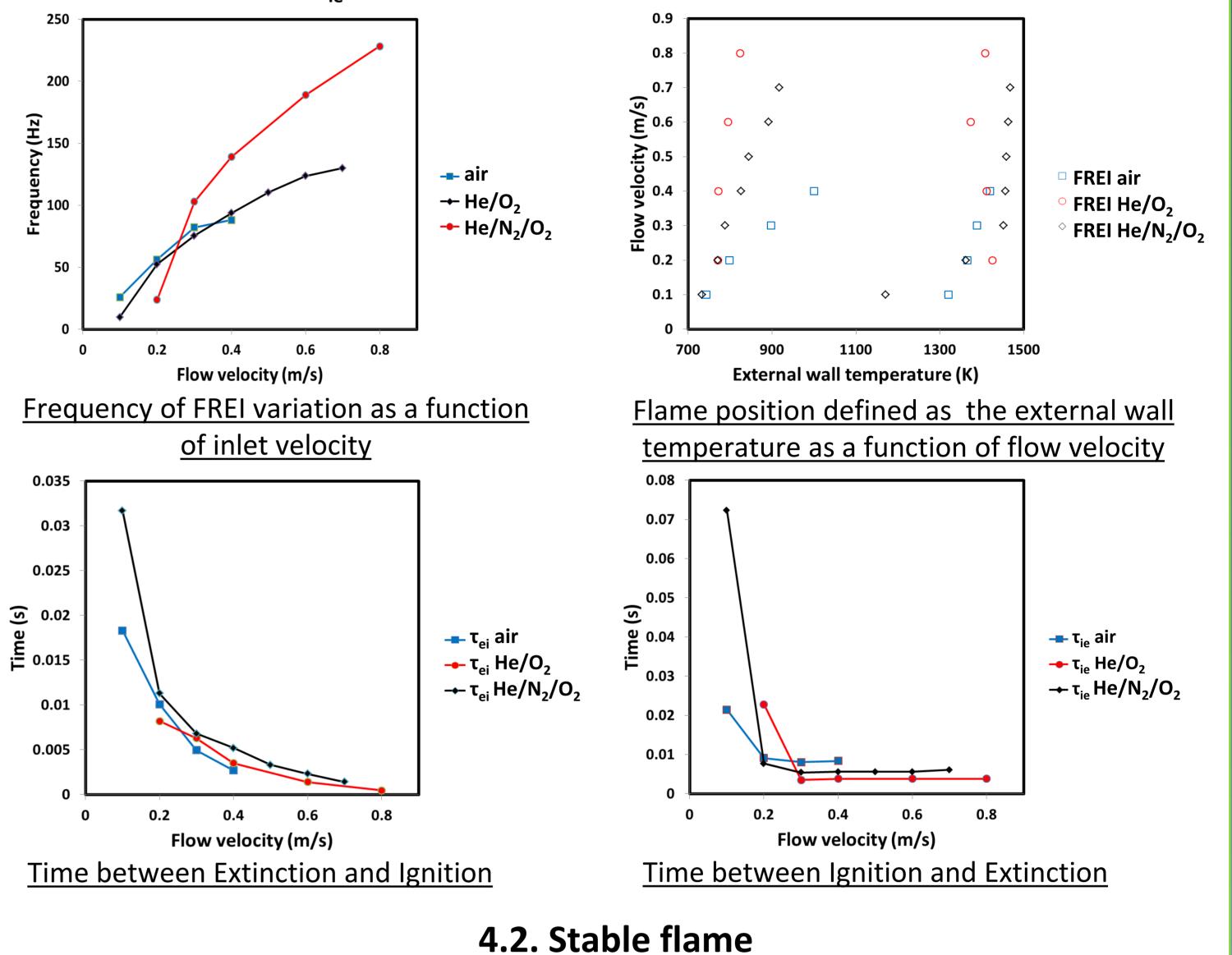
### 1. Goal of the study

- Growing need to improve knowledge in the field of small-scale combustion and take advantage of high energy density of fuel [1] in different applications such as portable power device [2], micro-satellite thrusters [3], heat sources [4].
- Previous studies have been done with fuel/air mixtures. Combustion of a  $CH_4/O_2$  $\bullet$ mixture with different diluents can improve the understanding of flame behaviour in micro-scale reactor by changing physical properties of the environment. Hence, be able to point out physico-chemical properties that play an important role in micro-scale combustion.

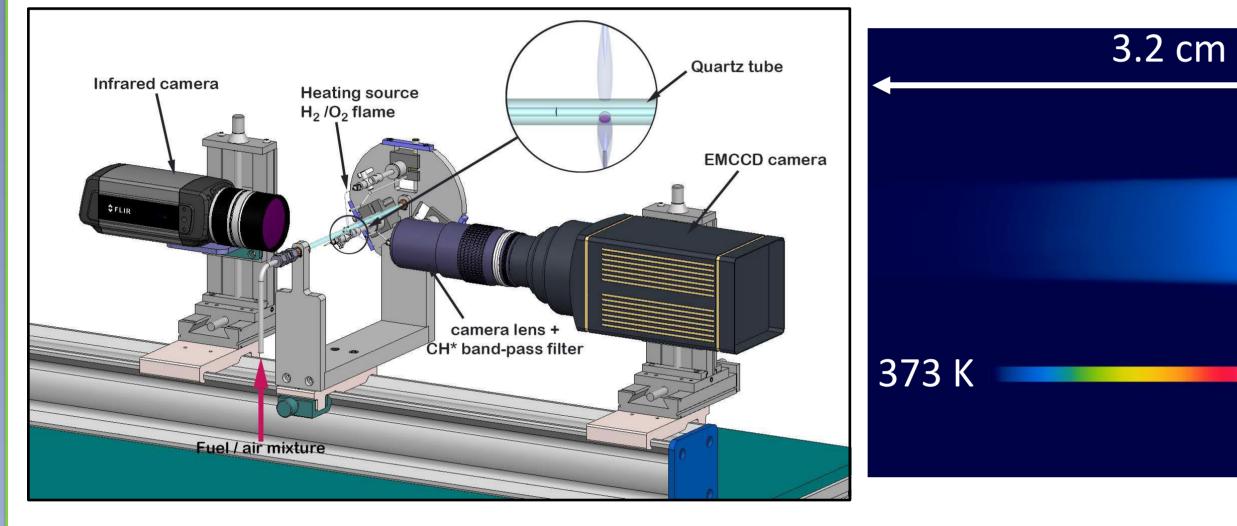
## **2. Experimental set-up**

### **4.1. FREI**

- For a given fuel/oxydant mixture: when the flow velocity increases  $\rightarrow$  frequency increases.
- For a given flow velocity: when the flame propagation speed of a mixture A is bigger than a mixture  $B \rightarrow \tau_{i_e}$  in A is smaller than in B.



- Cylindrical quartz tube heated by 3 hydrogen/oxygen blowtorches.
- The temperature profile on the outer side is measured by a infrared camera A655sc.
- A spectroscopy EMCCD camera ProEM 1600 with a CH\* band-pass filter (20BPF1\_430) is used to detect the flame positions.
- CH<sub>4</sub>/diluent mixture is supplied in a 1.85 mm internal diameter reactor. (Quenching distance of  $CH_{4}$ /air is 2.50 mm)



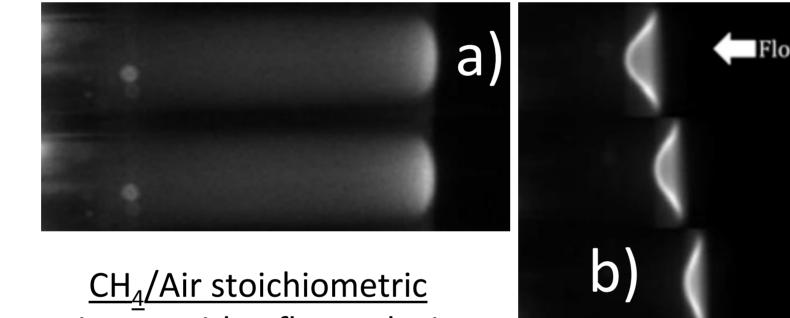
Schematic of the data acquisition system and microreactor [6]

Image from FLIR camera of the external temperature for a stoichiometric mixture of CH<sub>4</sub>/air, a flow velocity of 0.7 m/s, in a 1.85 mm internal diameter tube

1500 K

# **3. Different flame behaviour**

a) <u>FREI</u> (Flame with Repetitive



## Solution methods and solvers

- Steady state simulation
- The Stiff Chemistry Solver of ANSYS Fluent is used to solve the reactive flow
- PISO method for velocity-pressure coupling is used to solve the discretized form of the • Navier-Stokes system

#### Geometry/ Meshing:

- A 2D-axisymmetric geometry
- Total length of 10 cm, inner diameter of 0.925 mm, external diameter of 3.0 mm
- Quadrilateral elements
- 25 elements to mesh the inner radius, 20 elements for the wall. A constant size

- Extinction and Ignition): the ignition occurs downstream in high temperature region and extinction occurs upstream in low temperature region.
- Stable flame: flames with no relative motion with the reactor wall.

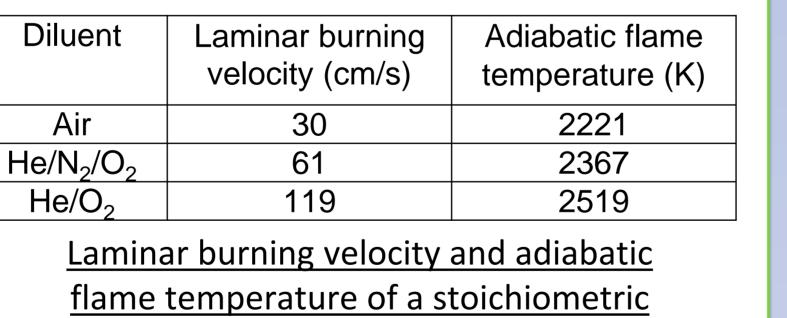
mixture with a flow velocity of a) 0.4 m/s, 0.415 m/s, b) 0.7 to 1.0 m/s [6]

# **4. Experimental and numerical results**

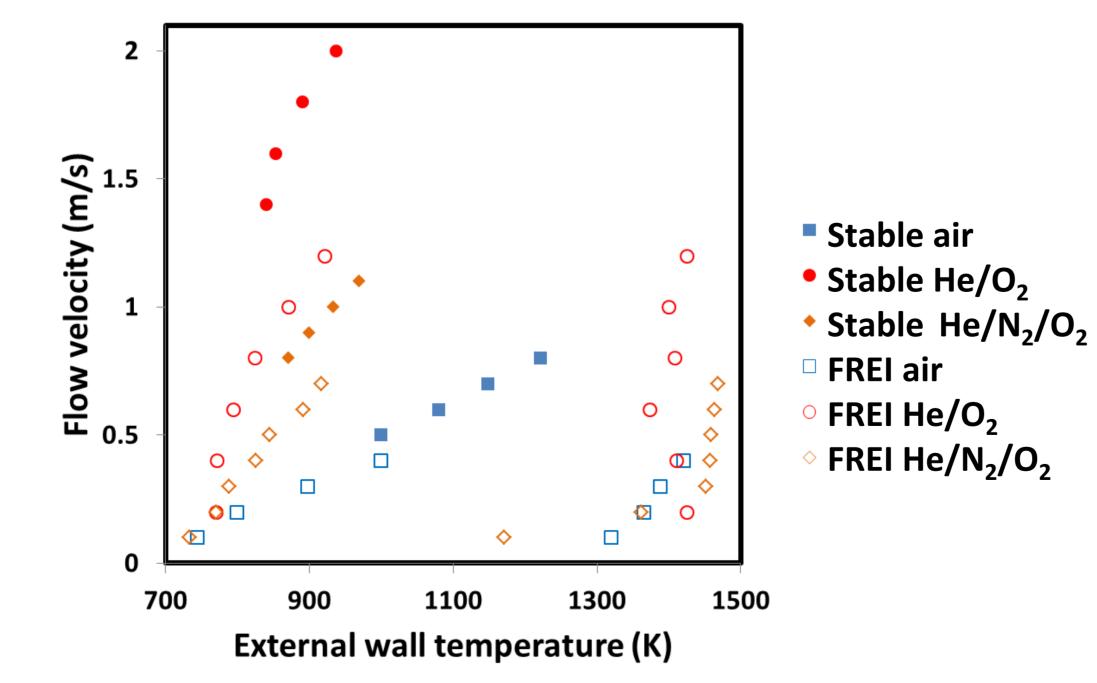
Air

Diluent	O <sub>2</sub>	He	N <sub>2</sub>
Air	20%	0%	80%
He/N <sub>2</sub> /O <sub>2</sub>	21.18%	39.20%	39.62%
He/O <sub>2</sub>	21.68%	78.32%	0%

Compositions of diluents used in this study in molar fraction



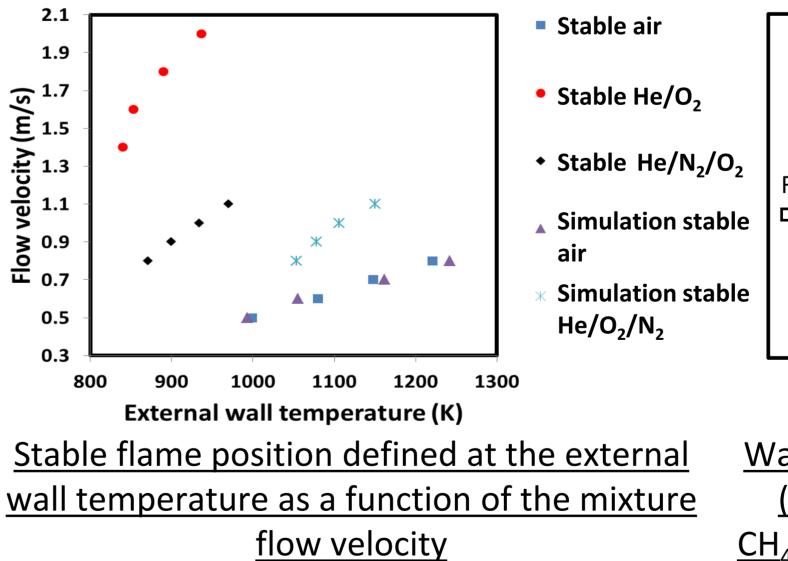
<u>mixture CH₄/diluent</u>



A second order upwind spatial discretization is used and a least squares cell-based method for the evaluation of gradients

#### Boundary conditions:

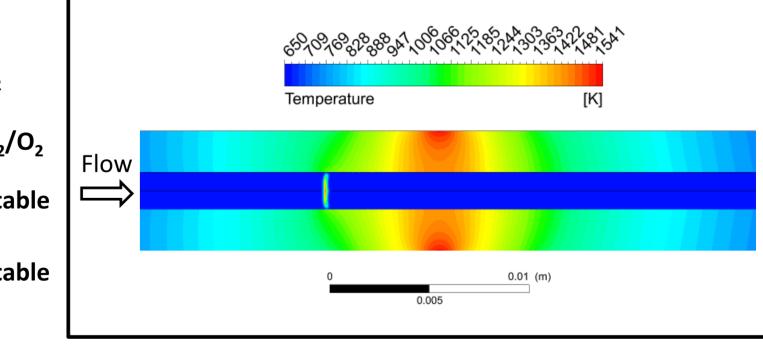
- Experimental external wall temperature is averaged and used as boundary condition
- A velocity inlet boundary condition is applied on the left part of the geometry, and a . pressure outlet boundary condition (1 atm) on . the right part



mesh of 33  $\mu$ m where the temperature is the highest, and a progressively bigger size toward the coldest region  $\rightarrow$  22500 elements for all the domain

#### Models:

- A laminar viscous model
- The effect of enthalpy transport due to species diffusion in the energy equation Ideal gas
- Chemical, transport and thermodynamics properties are computed with the GRI-Mech 3.0 scheme



Wall temperature and flame front visualisation (CH\* molar fraction) of the simulation of a <u>CH<sub>4</sub>/air mixture with an inlet velocity of 0.6 m/s</u>

• For a given fuel/oxydant mixture: flow velocity increases  $\rightarrow$  the flame front goes toward colder wall reactor region

## Flame position defined at the wall temperature as a function of the

#### mixture flow velocity

- [1] A. C. Fernandez-Pello, "Micropower generation using combustion: Issues and approaches," Proceedings of the Combustion Institute, vol. 29, no. 1, pp. 883–899, Jan. 2002.
- [2] K. H. Lee and O. C. Kwon, "Studies on a heat-recirculating microemitter for a micro thermophotovoltaic system," Combustion and Flame, vol. 153, no. 1, pp. 161–172, Apr. 2008.
- [3] P. Galie, B. Xu, and Y. Ju, "Kinetic Enhancement of Mesoscale Combustion by Using a Novel Nested Doll Combustor," 2007.
- [4] T. A. Wierzbicki, I. C. Lee, and A. K. Gupta, "Rh assisted catalytic oxidation of jet fuel surrogates in a meso-scale combustor," Applied Energy, vol. 145, pp. 1–7, May 2015.

[5] A. Di Stazio, "Caractérisation expérimentale de la dynamique de la combustion à micro-échelle," Thesis, Orléans, 2016.

For a given flow velocity: when the adiabatic flame temperature of a mixture A is bigger  $\bullet$ than a mixture  $B \rightarrow$  the front flame is located to colder wall reactor region.

# **5.** Conclusions

- All characteristic flame behaviours are conserved with different diluents studied  $\bullet$
- The increase in He molar fraction in diluent  $\rightarrow$  a. FREI velocity domains increases  $\bullet$ 
  - b. Extinction is located to colder wall region
  - c. Stable flame is located to colder wall

#### region

Flame/wall thermal interaction clearly identified experimentally with stable flames but not  $\bullet$ numerically

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