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Ana Neto, Sébastien Thomas, Gary Bond, Frederic Thibault-Starzyk, Filipa Ribeiro, et al.. The Oil Shale Transformation in the Presence of an Acidic BEA Zeolite under Microwave Irradiation. *Energy & Fuels*, 2014, 28 (4), pp.2365 - 2377. 10.1021/ef4023898 . hal-01831409

HAL Id: hal-01831409

<https://hal.science/hal-01831409>

Submitted on 8 Dec 2023

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The oil shale transformation in the presence of an acidic BEA zeolite under microwave irradiation

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KEYWORDS

Oil shale, Microwave heating, Zeolite BEA, Kerogen

ABSTRACT

The transformation of an oil shale sample from the Autun Basin in the Massif Central, France, was studied using two different heating strategies: microwave irradiation and conventional heating. Microwave heating was performed using a single mode cavity operating at a frequency of 2.45 GHz, under inert atmosphere. Heating of the sample generated liquid products of similar composition, either using microwave or conventional heating. The liquid products yield was similar in both cases, while the overall energy requirements were much lower using microwave irradiation. The influence of water vapour in the oil shale decomposition was also studied under microwave energy. In order to simulate the oil shale organic fraction conversion in the presence of an acidic zeolite catalyst, the oil shale sample was mixed with 5 wt.% BEA zeolite and heated under microwave irradiation. It was found that the liquid products yield decreased, along with an increase in the coke produced. Gaseous and liquid products recovered showed a tendency for the production of lighter components when in the presence of zeolite. The aromatic character of the oils was more important when using microwaves, especially in the presence of zeolite.

1 INTRODUCTION

2 Global demand for crude oil has been increasing for several decades and it is expected to
3 continue to grow ¹. The depletion of light crude oil reserves has meant that the development of
4 alternative energy sources has become vital. Hence, the use of heavy oils and other heavy
5 feedstocks for liquid fuel production has been increasing. In fact, recent efforts in the petroleum
6 industry have been focused on improving the existent technology so that a larger fraction of the
7 oil recovered (the barrel “bottom” fraction) can be converted to higher valuable products ^{2, 3}.
8 Unconventional hydrocarbon resources, including heavy oil, oil sands and oil shale, also have
9 potential to provide a valuable source of liquid hydrocarbons, since they exist in significant
10 quantities. Conventional oil reserves worldwide are estimated at 1.0 trillion barrels with an
11 additional 1.7 trillion barrels of possible/undiscovered reserves ⁴. Canadian oil sands reserves are
12 estimated at 1.7 trillion barrels, while oil shale known resources are estimated at 2.9 trillion
13 barrels, with 2.0 trillion barrels located in the USA ^{4, 5}.

14 Oil shale is a fine-grained sedimentary rock containing relatively large amounts of organic
15 matter, *kerogen*. This is a carbonaceous material from which oil and combustible gas can be
16 extracted by destructive distillation ⁶. Several studies have been carried out concerning the
17 characterization of different oil shale types and their potential for liquid hydrocarbon generation
18 ⁷⁻⁹. The most important techniques used for characterization of potential source rocks are Rock-
19 Eval pyrolysis ¹⁰, vitrinite reflectance measurements, X-Ray diffraction, FTIR and thermal
20 analysis (DTA-TGA).

21 Regarding oil shale processing, there are two main approaches: mining with subsequent surface
22 retorting and the *in situ* retorting processes ⁶. In order to overcome the limitations imposed by
23 mining and retorting of oil shale, namely the disposal of spent shale, water resource needs and

land surface alteration during the mining process, energy companies and petroleum researchers have been trying to develop new technologies for *in situ* oil shale transformation, differing mainly in the heating strategies that have been applied. The methodology proposed by Shell, known as *In situ* Conversion Process (ICP), appears in this context ¹¹⁻¹³, with several patents filled over the years and successful field pilots conducted in Colorado ¹¹. This process consists of a series of underground heaters installed in holes drilled into the oil shale deposit; the electrical resistance heaters heat the surrounding shale deposit to temperatures in the range of 250 – 400°C ¹². It takes several years to convert the kerogen contained in the oil shale into lighter hydrocarbons, which are then pumped to the surface using conventional methods. Drawbacks inherent to this approach are high energy requirements, long time needed to obtain significant amounts of oil, as well as environmental issues, mostly related to groundwater contaminations due to global heating of the soil.

Microwaves and radio frequency energy have also been proposed as alternative heating methods for recovery of oil and gas from oil shale and oil sands ¹⁴⁻¹⁹. The application of microwave energy for oil shale transformation has been documented since at least 1981, in the patent by Dumbaugh *et al.* ²⁰, which refers to the retorting process of oil shale and tar sand using microwave irradiation at 2450 MHz to heat the samples to temperatures about 370 – 650°C. Balint *et al.* ²¹ developed a method using microwave irradiation of the natural mineral in a pressure vessel, using an expelling medium to extract the kerogen, such as gaseous or liquefied carbon dioxide or other gaseous or vapour hydrocarbon solvents. Both processes refer to experiments performed at the laboratory scale. Several methods and apparatuses have been proposed for the *in situ* recovery of liquid hydrocarbons from oil shale ²²⁻²⁵, involving volumetric, selective, rapid and controlled heating ²⁶, sometimes in combination with critical fluids or carbon

sequestration. This latter case refers to the technology developed by Raytheon and Critical Fluids Technologies²⁷ in 2007 and is based on earlier radio-frequency based technologies from Raytheon²⁸. The process involves injecting carbon dioxide as a super critical fluid and a catalyst into the well; *in situ* radio-frequency energy is applied to heat the rock formation. The resulting product stream obtained, requiring further processing, consists of CO₂, CH₄, oil, steam/water and organic vapours.

When using electromagnetic heating, the energy is directly absorbed by the material subjected to radiation, avoiding energy losses to the system environment, which improves heating rates and reduces thermal gradients. Dielectric heating is caused by an increase of the kinetic energy of dipolar components of molecules under the effect of an electromagnetic field. Polar molecules or ions tend to couple and align themselves to be in phase with the field (dipole relaxation); since the microwave field is alternating in time, the dipoles are constantly oscillating at the microwave frequency, (300 MHz to 300 GHz); this oscillation increases the kinetic energy and collisions between molecules, producing random motion and, consequently heat^{29, 30}. The extent to which a material can be heated under microwave irradiation is dependent on its dielectric properties. The complex relative permittivity, ϵ_r , describes the ability of a material to store electric energy and it is characterized by the dielectric constant, ϵ_r' , and the dielectric loss factor, ϵ_r'' :

$$\epsilon_r = \epsilon_r' + i\epsilon_r'' \quad (1)$$

The dielectric constant reflects the capability of a material to be polarized by an electric field, while the dielectric loss factor is related to the amount of energy actually absorbed and subsequently dissipated as heat. The ratio of the dielectric loss by the dielectric constant defines the dielectric loss tangent, which measures the ability of a material to convert electromagnetic energy into heat at a given frequency and temperature.

$$\tan \delta = \frac{\varepsilon''}{\varepsilon'} \quad (2)$$

Absorption of microwave radiation by a material depends not only on the frequency of the electromagnetic waves and the material temperature, but also moisture content, physical state, composition and dimensions of the irradiated material ^{30, 31}. When applying microwaves to heat oil shale, it is expected that oil and moisture content will have an important influence on its dielectric properties. Moreover, heating of the oil shale will depend on the kerogen polarizability. Given the polar nature of kerogen, dipole relaxation effects are improved and the material is effectively heated. In fact, it was found that the loss factor would increase with increasing oil shale richness at a frequency of 500 MHz ²⁹. The presence of heteroatoms, namely sulfur, nitrogen and oxygen, also contribute to the increase of the polarization of this substance when under the effect of electromagnetic radiation ²⁹. Finally, metals in the form of powders are good microwave radiation absorbers ^{15, 16}.

Water is known to absorb microwave energy very strongly, given its polar characteristics. In many industrial microwave processes, the presence of water in the workload is essential for their adequate operation ³⁰. Water present in the oil shale can therefore affect the electromagnetic energy absorption ³². Some studies report the variation of the dielectric properties of some oil shale samples (Green River oil shale) with the variation in their water content. It was reported that with increasing percentage of water saturation in the oil shale samples, both ε' and ε'' increased (frequency range of 1 MHz to 1.8 GHz), therefore improving energy propagation and absorption by the material ³³. A study to the dielectric properties of Jordanian oil shales ³⁴ also showed that samples with higher moisture content presented higher loss factor values.

1 The oil obtained from oil shale retorting often requires additional upgrading processes, when
2 compared to conventional crude oil ³⁵. Having this in mind, the present study tested the influence
3 of a zeolite, with acidic character, on oil shale transformation and resulting products recovered.
4 The goal was to try to obtain lighter products via direct contact of the oil obtained from kerogen
5 transformation with a catalyst under microwave irradiation which would possibly require less
6 processing for subsequent liquid fuels production.

7 The use of zeolite-based catalysts for cracking of high molecular weight compounds to lighter
8 and more valuable products is well known ³⁶. This type of catalysts has also been applied to shale
9 oil upgrading ^{37, 38}. Williams *et al.* ³⁸ studied a two stage oil shale pyrolysis, where the reaction
10 products from kerogen decomposition flowed through a ZSM-5 catalyst bed at 400 – 550°C prior
11 to recovery. Pore dimensions of ZSM-5 zeolite prevent the formation of voluminous intermediary
12 compounds and consequently minimizes the formation of coke ³⁹. However, when the cracking of
13 large molecules is intended, a large pore structure is usually advantageous. For that reason, a
14 commercial BEA zeolite was used in this study.

15 The application of zeolite catalysts under microwave radiation has also been studied for various
16 reactions ^{31, 40}. Dielectric heating of zeolites is possible and this phenomenon has been associated
17 to the migration of cations in the zeolite framework ³².

18 In the present work, the transformation of an oil shale sample under microwave irradiation was
19 performed and the results obtained were compared to the transformation under conventional
20 heating. The influence of the presence of water vapour in the oil shale transformation under
21 microwave irradiation was evaluated. Moreover, the presence of a BEA zeolite together with the
22 oil shale was studied using microwave energy. Oil fractions obtained from decomposition of the

oil shale in such conditions were characterized and compared with the results obtained under conventional heating.

The purpose of this work resides on the feasibility study of the transformation of oil shale in the presence of zeolite, under microwave radiation, and no *scale-up* was yet intended in this context.

MATERIAL AND METHODS

Experimental apparatus and operating conditions. Experimental studies using microwave irradiation were conducted in a microwave system as represented in Figure 1. The microwave system comprises a generator operating at a frequency of 2.45 GHz with a maximum power output of 1000 W. From the generator, the microwaves pass through a water-cooled circulator, which is used to prevent any reflected power from damaging the magnetron. This device only allows microwaves to flow in one direction, towards the waveguide, while the reflected power is diverted into a water-cooled load. The reflected power is measured using a probe at the inlet of the water load. From the circulator, the microwaves then go through a standard rectangular brass 9A waveguide (86×43 mm), which can incorporate a variable coupling aperture, which consists of a thin aluminium sheet with a rectangular orifice of variable dimension. The dimensions of the coupling aperture affect the Q-factor of the cavity, which has the result of varying the E-field density. For the experiments performed in the present study, the dimensions of the rectangular orifice used were 31×21 mm.

The sample section of the waveguide has two vertical ports (47 mm diameter) where the reactor is introduced and two smaller horizontal ports (17 mm diameter) to allow access to an IR thermometer (OMEGA ®). To prevent microwave leakage, the ports length is over than twice

1 their diameter. At the end of the waveguide a short circuit, or plunge tuner, is installed. The
2 plunge tuner is used to alter the internal length of the waveguide so that a standing wave is
3 generated. In this situation, it is possible to locate the position of maximum E-field in the center
4 of the sample section, where the reactor is placed. Maximum energy absorption means minimum
5 reflected power. Accordingly, tuning of the microwave cavity was performed by minimizing the
6 reflected power measured at the level of the water-cooled circulator.

7 The sample temperature, as measured by an infrared pyrometer, was used to control the power
8 supplied to the generator, by means of a PID control algorithm. The PID algorithm takes as input
9 the difference between the actual sample temperature (the IR thermometer measurement) and the
10 temperature set point and then acts on the forward power from the generator. Since the IR
11 thermometer measures the external surface temperature of the reactor wall, this temperature
12 reading had to be corrected to the actual sample temperature inside the reactor. This correction
13 was performed by introducing a thermocouple in the reactor after microwave heating. As the
14 system cooled down, both temperature readings (IR thermometer versus reading from the
15 thermocouple) were registered.

16 A quartz reactor was used to place the oil shale sample inside the microwave cavity, using 6 g
17 of the sample (bed height of about 2 cm). Helium was used as carrier gas with a flow rate of
18 20 mL/min.

19 The liquid products, obtained from oil shale decomposition, were recovered at the bottom of
20 the reactor using a cold trap (-80 °C). As the liquid products formed were quite viscous, they
21 were recovered from the reactor and from the collecting vessel via dilution in the minimal
22 amount possible of acetone. Pure samples were also recovered for elemental analysis of the oil. A

1 gas collecting tube was placed after the cold trap. At the setup's outlet, the gas would flow
2 through a soap bubble flow meter for monitoring of the gas flow rate during reaction.

3 In order to study the oil shale transformation under microwave irradiation, the sample was
4 heated in a first step to 300°C, where it was held for 10min, and then to 500°C. The forward
5 power from the generator was altered to maintain a constant heating rate of 10°C/min. A
6 programmed temperature methodology was chosen so that the time of exposure at a given
7 temperature could be comparable with the conventional heating experiments.

8 To study the effect of water in the system under microwave irradiation, the carrier gas was
9 passed through a saturator filled with water at room temperature placed at the reactor entry, ca.
10 2.5% H₂O.

11 The presence of the zeolite was investigated using the mechanical mixture of 5 wt.% of zeolite
12 with the oil shale sample.

13 The same temperature program was used when testing the oil shale transformation in a
14 conventional oven. An electrical oven from Adamel – Lhomargy with automatic control,
15 Termolab, was used. Helium flow of 3 mL/min/g was also used to improve liquid flow through
16 the reactor into the oil recovery system. Products recovery was performed in the same way as for
17 microwave heating.

18 **Materials Characterization.** The oil shale sample used in this study was provided by Total
19 and originated from the “Assise de Millery” of the Autun Basin in the Massif Central, France.
20 The sample was crushed and sieved to a 40 µm powder. The zeolite sample was a BEA zeolite
21 provided by Zeolyst (CP811 E-75) with global Si/Al ratio of 31.7.

22 Rock-Eval analysis was performed over the oil shale sample using 100 mg of powder on a
23 Rock-Eval 6 apparatus. The sample was first maintained at 300°C where free hydrocarbons were

1 volatilized and detected by FID (*S1* peak is then obtained). Afterwards, the temperature was
2 progressively increased to release heavy hydrocarbons, along with the products from thermal
3 cracking of non-volatile organic matter in the rock (*S2* peak). *S2* indicates the rock's existing
4 potential to produce hydrocarbons. Finally, the residual carbon fraction, for Total Organic Carbon
5 (TOC) calculation, was determined by an oxidation step of the remaining sample at 850°C.

6 The oils obtained were injected in a GC Shimadzu-9A, with a capillary column CP- Sil 5 CB
7 and equipped with a FID detector. The gas samples recovered in the gas collecting tube were
8 analyzed using GC-MS, for the experiments performed under microwave irradiation, and using
9 the GC Shimadzu-9A for the conventional heating experiments. The GC-MS used was a Trace
10 GC Ultra/DSQ II, with a Restek capillary column, Rxi®-5 Sil MS. The GC-MS was also used
11 for characterization of the liquids obtained.

12 Simulated distillation was performed with the oil samples (after roto-evaporation of the
13 solvent) according to the ASTM method D7500. FTIR – ATR was used for analysis of the liquid
14 samples. The spectrometer (Nicolet Magna 750, provided with a MCT detector) was equipped
15 with an ATR accessory from Specac, with a single reflection diamond crystal. TGA analysis was
16 used to evaluate the amount of organic matter left in the spent shale recovered from the reactor
17 after each experiment. The thermo-gravimetric experiments were recorded on a Setaram TG-
18 DTA 92 instrument operating under nitrogen with a flow rate of 30 mL/min through the furnace
19 in the following conditions: sample weight about 30 mg, heating from room temperature up to
20 900°C at 5°C/min. Afterwards, the sample was calcined at 1000°C, under air flow at 30 mL/min.
21 Carbon, hydrogen, nitrogen and sulphur contents were determined for both the spent shale
22 samples and the oil sample obtained from oil shale decomposition under microwave irradiation.

RESULTS AND DISCUSSION.

The oil shale sample was first characterized using Rock-Eval pyrolysis⁴¹ to evaluate its potential for hydrocarbons generation. The total oil potential of the sample, defined as the sum of peaks *S1* and *S2*⁴¹ was found to be 488.6 mg of hydrocarbon per gram of rock (~48.9 wt.%). The amount of residual carbon in the sample after pyrolysis is not significant, given that the Total Organic Carbon (TOC) determined was of 49.8%. T_{max} , where maximum release of hydrocarbons takes place, also given by Rock-Eval analysis⁴¹, was 444 °C, indicating an early mature stage of the organic matter in the source rock⁴². T_{max} is indicative of the source rock maturation degree, but it is also affected by the organic matter type, soil contaminations and the mineral matrix⁴³. For this reason, the T_{max} value found should be interpreted with caution. The application of this parameter to oil shale samples is useful when comparing a series of rocks of different origins, since higher T_{max} values indicate higher maturity of the organic matter⁴⁴.

The Production Index, *PI*, defined in equation (3), can also be used for the evaluation of the organic matter maturity. The *PI* resulted in a value of 0.002, since the value of the *S1* peak (0.93 mg hydrocarbons/g of rock) was much lower than the *S2* peak (487.71 mg hydrocarbons/g of rock), indicating the presence of immature organic matter⁴².

$$PI = \frac{S_1}{S_1 + S_2} \quad (3)$$

The quality or type of the organic matter can be described by the Hydrogen Index, *HI*, commonly used for kerogen classification, as described by Peters and Cassa⁴². Hydrogen index is defined as the amount of hydrocarbons generated by kerogen cracking (*S2* peak) referred to the TOC. This parameter is proportional to the amount of hydrogen present in the kerogen and it is, for that reason, a measure of the rock's potential to generate oil. The hydrogen index obtained

was 979 mg HC/g TOC. The kerogen present in the oil shale sample is thus of type I⁴² and it shows great potential for oil production.

Oil shale transformation under microwave irradiation. Heating of the oil shale sample under microwave irradiation resulted in the formation of a liquid product flowing down from the oil shale bed, along with intense vapour formation. Vapours were then condensed in cold traps. Samples from the gas product were recovered in a gas collecting tube and were subsequently analyzed by GC-MS. After the oil shale transformation, the solid residue (spent shale) was retrieved from the reactor for posterior analysis.

Data recorded from the PID control of the power supplied to the microwave generator was useful to estimate the actual temperature where the oil shale transformation took place. As shown in **Figure 2**, the power level behaviour is rather constant during heating of an oil shale sample, until the power output suffers a sudden increase, corresponding, in this case, to a temperature of 300°C. This temperature is assigned to the decomposition temperature of the oil shale. The rapid variation in the power level is believed to be related to the change in the loss factor (dielectric loss tangent) of the sample, which may be affected by changes at the molecular or structural levels of the material, such as its decomposition⁴⁵.

Considering the result from Rock-Eval analysis, where T_{\max} was observed at 444°C, it is interesting to note the difference in the transformation temperature between both heating methods. In fact, the temperature reading during microwave irradiation using the infrared temperature probe is taken as an average of the sample's bed temperature. Hot spots caused by increased local absorption of radiation could promote oil shale transformation, while the mean temperature of the bed is lower than the one observed during conventional heating. Hot spot formation in gas/solid heterogeneous catalytic systems, as well as selective heating of certain

1 active centres, has been suggested in the literature ^{31, 46-48}. In the case of an oil shale sample,
2 selective heating would occur due to the presence of metal particles, which can be heated to high
3 temperatures under microwave irradiation³¹ originating a local temperature increase within the oil
4 shale bed.

5 Additionally, as the sample is heated under microwave irradiation, the oil trapped in the solid
6 becomes liquid, interacting more strongly with the microwave field, the result of which is to force
7 the layered structure of the oil shale apart, allowing the oil to be released at lower temperature.

8 On the other hand, important temperature gradients from the bulk to the reactor walls could
9 also be present during microwave heating. Since the reactor walls are in contact with ambient air,
10 the sample's temperature is lower closer to these points, decreasing the average oil shale
11 temperature observed. Calibration of the temperature reading by the IR thermometer during
12 microwave heating was performed so that the average temperature of the sample would be close
13 the desired temperature, for comparison with conventional thermal heating experiments. The
14 maximum temperature difference observed between the reactor walls and the bulk of the sample
15 was of 87°C.

16
17 **Oil shale transformation under conventional heating.** In order to assess the microwave
18 heating system for oil shale conversion, the sample was also tested under conventional heating
19 using an electrical furnace and the same flow rate conditions previously used.

20 A thermocouple was employed for temperature monitoring in the oil shale bed. In this case, the
21 identification of the transformation temperature was based on the gas flow rate monitoring at the
22 setup outlet. **Figure 3** shows the gas flow rate variation during heating of the oil shale, as well as

1 the temperature reading during the experiment. The point where the gas flow rate started to
2 increase was considered as the transformation temperature.

3 When heating the oil shale sample under these conditions the transformation was observed
4 around 380°C. The temperature for maximum gas flow rate was observed in the range 442 –
5 445°C, which is in complete agreement with Rock-Eval analysis, where maximum hydrocarbons
6 release was detected at 444°C.

7 Simulated distillation of the oil samples obtained under conventional and microwave heating
8 show very similar results. The variation in product distribution is almost negligible between both
9 samples.

10 The elemental weight composition of the oil obtained from oil shale transformation under
11 microwave heating is presented in **Table 1**, as well as the usual proportions of these elements
12 found in conventional petroleum ⁶. The composition of the liquid fraction obtained from the oil
13 shale decomposition is within the same limits found for conventional petroleum. The hydrogen-
14 to-carbon molar ratio obtained was of 1.4, which is close to the lower limit for this parameter. A
15 higher hydrogen-to-carbon ratio is normally desired for use as a refinery feedstock. However, it is
16 known that unconventional hydrocarbon sources are not as advantageous as conventional crude
17 oil for the same purpose. Hydrogen-to-carbon ratios of 1.5 are typical for oil sands bitumen, but a
18 ratio as low as 1.3 has been found for U.S. tar sands ⁶.

19 Thermo-gravimetric analysis of fresh and spent shale samples allowed the estimation of the
20 remaining organic material in the treated samples. Oil shale pyrolysis using thermogravimetric
21 analysis has been previously investigated ^{9, 49, 50}. It was found that, depending on the oil shale
22 type, its decomposition exhibits either single or a two-stage evolution of hydrocarbon material, in

1 the temperature range of 250 – 620°C. At temperatures higher than 600°C, thermal decomposition
2 of carbonates takes place, due to the presence of minerals, such as calcite or dolomite.

3 Thermal treatment of fresh oil shale under nitrogen flow showed a two-stage decomposition
4 process (**Figure 4A** and **B**) where the transformation step at 720°C is most likely due to
5 carbonates decomposition ⁴⁹. Afterwards, an oxidation step allowed the combustion of residual
6 carbon from refractory material, such as heavy oils, tar-mats, coke ¹⁰. The organic content was
7 then estimated summing the weight loss due to the first decomposition step, at temperature below
8 600°C, and the residual carbon from the oxidation phase. For the fresh oil shale sample, the
9 organic content obtained was of 47%, while the total organic content given by Rock-Eval
10 analysis was of 50%.

11 Accordingly, TGA under nitrogen flow performed with the spent shale after microwave or
12 conventional heating showed different remaining organic contents, as shown in **Figure 4**. Total
13 weight loss due to organic carbon after microwave heating was of 23%, as opposed to 14% for
14 the sample treated under conventional heating. Also, **Figure 4** shows different thermal
15 behaviours regarding said samples. Both fresh oil shale and spent shale from microwave heating
16 present two decomposition steps, at 450 – 460°C and 720°C (**Figure 4B**). On the other hand,
17 spent shale from conventional heating only presents the step at higher temperature (**Figure 4A**),
18 meaning that it mainly contains the heavier products fraction. This result suggests that the spent
19 shale from microwave heating contains a higher amount of organic matter yet to be recovered, as
20 opposed to the spent shale from conventional heating. This observation is consistent with the
21 average lower temperature of the oil shale bed during microwave irradiation, due to lack of
22 reactor insulation, suggesting that part of the sample did not reach the optimum temperature to
23 promote kerogen transformation.

1 Elemental analysis of the solids obtained after oil shale decomposition (**Table 2**) also shows
2 lower carbon content in the spent shale when using conventional heating than when microwaves
3 were applied, which is in agreement with the TGA results.

4 The oil obtained after microwave irradiation of the oil shale has a hydrogen-to-carbon ratio
5 (H/C) of 1.4, as previously referred, while fresh oil shale presents a ratio of 1.3. A good
6 correspondence between both values was expected, since the organic matter that constitutes the
7 oil recovered is originated from kerogen decomposition present in the fresh oil shale.

8 The recovered spent shale samples, in general, present a lower hydrogen-to-carbon ratio, when
9 compared to fresh oil shale, mainly due to the decrease in the total carbon content of the spent
10 shale.

11 **Zeolite influence in oil shale transformation.** Mixing a zeolite with the oil shale sample
12 under microwave heating caused a decrease in the transformation temperature, which was
13 observed at 245°C, as shown in **Table 3**. The temperature reading was recorded as previously
14 described and the sample's decomposition was observed at lower temperature than the one of
15 pure oil shale transformation under microwave irradiation (**Figure 5**). A sudden increase in
16 power during heating of the sample mixed with zeolite is also observed in **Figure 5**, indicating
17 the moment where transformation of the oil shale takes place. This process is endothermic and, as
18 the sample heats, it can cool easily. However, as the oil is released from the sample, its organic
19 content decreases and higher power is needed to maintain the temperature. The result is the
20 appearance that two powers are applied for one temperature.

21 When conventional heating was used, the observed transformation temperature was basically
22 the same for both cases studied.

Table 3 also presents the mass balance relating to the initial organic content, using as calculation basis the amount of organic material determined with TGA in the initial sample, m_i .

The calculation basis was chosen assuming that the mineral matrix of the oil shale stays constant during heating of the sample.

The liquid products yield, Y_{liquid} , was determined using the amount of liquid recovered in the condenser and the initial amount of organic matter in the oil shale sample.

$$Y_{liquid} = \frac{m_{liquid}}{m_i} \times 100 \quad (4)$$

The amount of organics not recovered in the liquid or gas fractions, $m_{not\ recovered}$, was determined using the data from TGA of the spent shale.

$$m_{not\ recovered} = OM_{spent} \times m_{spent} \quad (5)$$

where OM_{spent} refers to the organic material in the spent shale determined by TGA and m_{spent} is the weight of spent shale recovered from the reactor. This parameter was then related to the initial amount of organic material in the sample.

The amount of organic material in the gas produced was calculated considering that

$$m_i = m_{liquid} + m_{not\ recovered} + m_{gas} \quad (6)$$

The gas products yield was then defined as

$$Y_{gas} = \frac{m_{gas}}{m_i} \times 100 \quad (7)$$

The conversion of the oil shale was used to evaluate the degree of transformation of the organic material under microwaves or conventional heating.

$$Conversion = \frac{m_{products}}{m_i} \quad (8)$$

where

$$m_{products} = m_{liquid} + m_{coke} + m_{gas} \quad (9)$$

The organic material present in the spent shale is due (i) to the presence of non-transformed kerogen – evidenced by the first weight loss in the TGA weight profile for the spent shale from microwave heating (**Figure 4**), and (ii) to the presence of heavier compounds that remain in the solid, after decomposition. These compounds came from the transformation of the organic material and thus were considered as coke, m_{coke} .

The amount of coke produced was calculated from the increment observed in the weight loss upon TG analysis during the oxidation step of the spent shale. In fact, the weight loss during TGA using air flow is due to a heavier products fraction, given that it was not decomposed under nitrogen flow. Since this fraction of heavier products is also present in fresh oil shale, the amount of coke produced during oil shale decomposition was estimated using the increment in the weight loss observed under air flow:

$$m_{spent} \times \frac{\{\% \text{ weight loss}_{air}^{spent}\}}{100} = m_{heavy} + m_{coke} \quad (10)$$

Where m_{heavy} refers to the heavier products weight in the initial oil shale sample.

$$m_{heavy} = m_{oil\ shale}^{fresh} \times \frac{\{\% \text{ weight loss}_{air}^{fresh}\}}{100} \quad (11)$$

Table 3 shows that liquid products yields resulting from microwave and conventional heating were similar. However, as previously seen, the amount of organic matter in the spent shale after conventional heating was lower, meaning that the amount of gas formed increased in this case.

When adding the zeolite to the oil shale under microwave irradiation, liquid products yield decreased significantly. Nevertheless, total conversion of the oil shale under microwave heating was about 70% of the initial organic content, with and without zeolite (**Table 4**). Total conversion considers the total weight of liquid and gas formed, as well as the products adsorbed in the spent shale (coke). The addition of zeolite caused an increase of the organics remaining in

the spent shale, evidencing the increase in coke production, probably due to hydrocarbon oligomerization reactions promoted in the acid sites of the zeolite. Williams *et al.*³⁸ also used a zeolite-based catalyst for the two stage pyrolysis of oil shale and obtained a similar result, with an increased gas yield, while decreasing oil production, due to coke formation in the catalyst.

Under conventional heating, total oil shale conversion was also similar for both experiments, with and without zeolite, while coke production was fairly the same in both cases (**Figure 6**).

Figure 6 shows higher organic content in the spent shale obtained after microwave heating, when compared to conventional heating. This result could be associated to the lower temperatures observed in the oil shale bed when using microwave irradiation, and is not necessarily related to an increased coke production in these conditions. When heating the oil shale sample to promote hydrocarbons release from the mineral matrix, cracking of the resulting compounds can also take place at sufficient high temperatures¹⁴. When microwave heating was used, part of the sample was at lower temperatures than when using conventional heating, which resulted in lower tendency for cracking, leading to adsorption of heavier compounds in the spent shale.

Liquid products were analyzed, in the first instance, via gas chromatography, using a flame ionization detector. Several reference compounds were used to divide the chromatogram in different intervals of retention time (retention windows), which were then correlated with the amount of sample eluted from the column within each retention window. The weight composition determined this way was then related to the amount of liquid and gas products obtained, resulting in the products yield shown in **Figure 7**.

The selectivity towards liquid products was defined as

$$S_{liquids} = \frac{m_{liquids}}{m_{products}} \times 100 \quad (12)$$

While the selectivity towards gas products,

$$S_{gas} = \frac{m_{gas}}{m_{products}} \times 100 \quad (13)$$

1 For the light products fraction, “< C₆” the selectivity is given by

$$S_{<C6} = \frac{m_{gas} + w_{<C6} m_{liquids}}{m_{products}} \times 100 = S_{gas} + w_{<C6} S_{liquids} \quad (14)$$

2 And for the remaining product fractions:

$$S_i = w_i S_{liquids} \quad (15)$$

3 The amount of gas produced was considered in the “< C₆” product fraction. As noted before,
 4 the overall products yield decreased when adding the zeolite to the system under microwave
 5 heating. On the other hand, the global product yield was practically unaffected by the presence of
 6 zeolite under conventional heating. When looking at each product fraction, light products yield
 7 (“< C₆” fraction) increased in the presence of zeolite under microwave irradiation (Figure 7A)
 8 mainly because the selectivity towards gas products increased (**Table 4**). In fact, it was rather
 9 expected that the amount of gas produced, related to the total amount of oil shale transformed,
 10 would increase in the presence of zeolite due to an intrinsic catalytic cracking activity associated
 11 with its acidic character. **Figure 7B** shows that the “< C₆” and “C₆ – C₁₀” products yield
 12 increased in the presence of the zeolite. This fact can also be related to the zeolite catalytic
 13 activity.

14 A gas sample was collected when the gas flow rate measured at the setup outlet started to
 15 increase. The gas was then analyzed using GC-MS, which allowed the identification of the main
 16 compounds present in the gas. It was found that the major contributions were from ethane,
 17 propane and propylene (fraction designated as C₂ & C₃), followed by butane and 2-butene.
 18 Pentane and 1-pentene were also identified, and finally, to a lesser extent, hexane and 1-hexene.
 19 This analysis was used as a qualitative approach for gas characterization (**Figure 8A**).

1 For the conventional heating experiments, the gas recovered was analyzed using only gas
2 chromatography. In this case, methane was identified in the gas products, as well as the
3 compounds previously described in **Figure 8B**.

4 **Water vapour influence, under microwave irradiation.** The oil shale transformation was
5 also tested using microwave heating with Helium flow saturated in water vapour. The sample's
6 decomposition was observed around 242°C, similar to what was observed when zeolite was used
7 (Figure 5). Since water is a polar molecule, it heats very easily when under the influence of an
8 electromagnetic field ³¹. When water vapour is inside the microwave cavity along with the oil
9 shale sample, it helps heating the material and hence the proper conditions for the oil shale
10 decomposition are more easily achieved. The water vapour in the system, either from the
11 saturator or from desorption from the zeolite, can be adsorbed by the structure of the oil shale.
12 When interacting with the microwave field, steam is formed between the layers of this structure,
13 forcing them apart and releasing the oil at a lower temperature than the one observed when no
14 water vapour or zeolite were used.

15 In the presence of water vapour and heating under microwave irradiation, the liquid products
16 yield decreased (Table 3). Table 2 shows that the total carbon content did not decrease as much
17 as when only oil shale was used, which implies lower organic matter recovery. Consequently,
18 total oil shale conversion decreased, which was found to be around 49% (**Table 4**).

19 **ATR-FTIR of the oil samples.** Attenuated Total Reflectance (ATR) is a widely adopted, non-
20 destructive, technique for the determination of chemical composition of materials based on their
21 chemical bonding. ATR analysis of the liquid samples from oil shale decomposition was used in
22 this work as a first approach to the oils characterization.

In all samples analyzed, the normal $\nu(\text{C-H})$ stretching vibration bands are present, corresponding to methyl and methylene bridge groups present in hydrocarbon chains. These bands appear in the $2840 - 3000 \text{ cm}^{-1}$ region ⁵¹ (**Table 5**). Bending vibrations for methyl groups appear at lower frequencies compared to their corresponding stretching vibrations. For the symmetric vibration mode the band appears at 1375 cm^{-1} , and at 1450 cm^{-1} for the asymmetric mode ⁵¹. For the $-\text{CH}_2-$ group, there are four possible vibration modes: scissoring, rocking, wagging and twisting. Scissoring vibration appears normally at 1465 cm^{-1} , while the rocking vibration mode appears at 720 cm^{-1} , which was not possible to identify in the spectra obtained (**Figure 10**). The other two vibration modes are normally less intense ^{51, 52}. **Table 5** presents the bands identified in the spectra corresponding to CH_3 and CH_2 groups present in hydrocarbon compounds in the shale oils.

Figure 9 and Figure 10 show the IR spectra for the shale oils obtained using microwaves and conventional heating, with and without zeolite. The band at 2730 cm^{-1} may correspond to the C-H stretching vibration of groups $\text{H}-\text{C}=\text{O}$, characteristic of aldehydes (these groups would appear between $2650 - 2800 \text{ cm}^{-1}$ ⁵³).

It is generally accepted that for wavenumbers greater than 3000 cm^{-1} the vibrations are due to stretching of the C-H bond of an ethylene or aromatic groups ⁵¹. It is possible to distinguish the presence of unsaturated compounds, shoulder around 3050 cm^{-1} , in all samples, corresponding to the $\nu(\text{Csp}^2-\text{H})$ vibration ⁵⁴. Aromatic compounds are also present, as verified by the 3004 cm^{-1} band for the $\nu(\text{C}_{\text{aromatic}}-\text{H})$ vibration and at 1603 cm^{-1} for the $\delta(\text{C}=\text{C})$ vibration of the aromatic ring ⁵⁴. The bands at 1709 cm^{-1} , corresponding to the C=O stretching vibration ⁵¹, 1220 cm^{-1} , C-O stretching vibration ⁵⁵ and 1360 cm^{-1} corresponding to the CH_3 group bending vibration in ketones ⁵¹, are all due to the solvent ⁵⁶.

The results are inconclusive about the presence of sulphur or nitrogen compounds in the oil samples. For example, thiophene ring stretching would result in a band at $1350 - 1550 \text{ cm}^{-1}$ and S = O stretching vibrations would appear at $1030 - 1070 \text{ cm}^{-1}$ ⁵⁷. In the regions referred, there are many contributions, making the assignment of the bands to a given compound or group very difficult.

ATR analysis was used only as a qualitative approach to the oils characterization. No conclusions were taken regarding which one of the samples would present heavier or lighter compounds.

Simulated distillation. The liquid samples obtained from oil shale decomposition under microwave and conventional heating were analyzed according to the ASTM method described above. Prior to analysis, the solvent was evaporated. The oil samples analyzed contain a mixture of hydrocarbons with carbon number lower than 110, corresponding to an atmospheric equivalent boiling point (AEBP) of 735°C , as described in API Research Project 44^{58, 59}. The AEBP of $704 - 712^{\circ}\text{C}$ corresponds to n-alkanes with carbon number between 92 and 96.

Figure 11 shows the result derived from simulated distillation data of the oils obtained under microwave irradiation. The curves represent the weight fraction recovered for each boiling point, while the bar graph represents the result of the division of both curves into intervals related to the number of carbon atoms found in conventional hydrocarbon mixtures⁶⁰. The separation into ranges was defined as follows:

Naphtha: $< 175^{\circ}\text{C}$

Kerosene: $175 - 343^{\circ}\text{C}$

Gas oil: $343 - 525^{\circ}\text{C}$

Vacuum residue: $525 - 800^{\circ}\text{C}$

Coke: > 800°C

The liquid sample obtained under microwave irradiation in the presence of BEA zeolite shows very similar characteristics with the sample obtained in the absence of zeolite, as shown in Figure 11A. The naphtha fraction (Figure 11B) decreased when the zeolite was used, while the kerosene fraction increased. For boiling points lower than 200°C, the curve in Figure 11A referring to the oil obtained adding zeolite is not well defined, which increases the uncertainty in this result. On the other hand, it would be expected a higher amount of light compounds in the oil obtained with zeolite, due to the cracking activity associated with its acidic character, which was previously observed for the kerosene fraction.

When water vapour was used during oil shale decomposition, the differences between the simulated distillation curves (Figure 11A) were around 20°C. Compared to the previous samples, the residue boiling fraction (Figure 11B) increased, which indicates that the presence of high boiling point products is more significant in this oil sample.

GC-MS analysis. GC-MS application for the characterization of petroleum-like products has been known for many years. The application of both GC and GC-MS techniques was used for the characterization of heavy residual oils of different sources⁶¹. Quantification of normal paraffins and isoprenoids was used to evaluate if various pairs of oils were from a common source or not. Shale oil has also been analyzed using GC-MS for the evaluation of the presence of biological markers, such as isoprenoids, steranes and terpanes, in extracted and pyrolyzed oils^{62, 63}. This type of description is important when referring to the overall structure characterization and origin of the kerogen. In the present study, GC-MS was used for identification of the classes of compounds present in the oils obtained from oil shale decomposition using different heating methods, as described above.

1 Data treatment for GC-MS analysis was performed using Thermo Scientific Xcalibur®
2 software. The spectrum associated to each peak in the chromatogram was compared to the NIST
3 Standard Reference Database mass spectral library (NIST05) and a probable identification for the
4 components was found.

5 In order to better distinguish the liquids obtained under microwave irradiation, the several
6 compounds found with GC-MS were divided into classes, according to functional groups. Their
7 respective areas in the chromatogram were then compared (Figure 12), since the response
8 observed in the mass spectrometer for a given compound is proportional to its concentration in
9 the gas stream. In the presence of zeolite, it was observed a significant change in the aromatic
10 character of the liquid sample: the contribution from aromatics and polycyclic aromatic
11 hydrocarbons increased, while the alkane fraction was not changed. When water vapour was used
12 under microwave irradiation, the alkene fraction increased significantly, as well as the polycyclic
13 aromatic compounds.

14 Other studies relating to shale oil characterization by compound type, such as Wood *et al.* ⁶⁴,
15 make reference to an oil rich in paraffins and cycloparaffins, with carbon number extending to
16 C₃₅. Also, Jones *et al.* ⁶⁵ compared shale and crude oil and found similar aromaticity for both
17 products. However, the oil obtained from decomposition of the oil shale under microwave
18 irradiation shows a highly aromatic character.

19 When comparing ion chromatograms for m/z 57, fragment ion characteristic of alkanes ⁶⁴, the
20 differences between the oils obtained under microwave or conventional heating are negligible, as
21 shown in Figure 13A. The intensity was normalized in Figure 13 due to the different dilution
22 degrees in both oils. However, when looking at the aromatic fraction (Figure 13B), defined for
23 m/z from 78 to 142, the obtained pattern is different. For instance, the intensity in the ion

1 chromatogram of the oil obtained under conventional heating is much lower, and therefore, the
2 noise increases. It is also possible to observe the presence of peaks at 4.7, 7.3 and 10.2 min in the
3 microwave heated sample which are not present in the conventional heating sample. These peaks
4 correspond, with a good match, to aromatic compounds such as styrene, indene and naphthalene,
5 respectively. As a result, the aromatic fraction in the oil from conventional heating is not as
6 important as for the shale oil obtained when microwave irradiation was used. This result is in
7 agreement with what was found regarding the amount of coke present in the spent shale samples
8 (Figure 6).

9 **Total energy requirements.** An important aspect to take into consideration when comparing
10 conventional and microwave heating is the energy consumption during both processes.

11 When the transformation of the oil shale was performed using conventional heating, an electric
12 oven was used, with automatic temperature control. The temperature increase is achieved via
13 pulses of electric current into the resistance heater. Figure 14 shows the power variation during
14 heating of the oil shale and compares it with the oven set point temperature. Integrating power as
15 a function of operating time, it is possible to calculate a rough estimate of the total energy
16 consumption for the operating conditions used. For the oil shale transformation under
17 conventional heating the energy consumed to heat the sample was about 506 Wh.

18 During microwave irradiation of the oil shale, the control unit would vary the magnetron
19 current according to the temperature requirements inside the microwave cavity. In this case, the
20 power output would be continuous as illustrated in Figure 15. Using these conditions, the energy
21 consumption was about 252 Wh to heat the oil shale sample. Considering that the liquid products
22 yield was very similar for both cases, the energy consumption when using microwave irradiation
23 was about 50% of the energy consumed using conventional means.

1 To maintain the dwell temperature at 300 or 500°C, the electric oven needed about 600 to
2 1200 W. Using microwave heating the power needed was of 400 W. Additionally, tuning of the
3 microwave cavity decreased the power sent to the magnetron to about 100 W for the dwell at
4 300°C. Automatic tuning of the cavity during microwave heating could greatly improve energy
5 absorption by the sample and decrease the total energy consumption, making this point a key
6 factor for the process to be really advantageous, as far as energy requirements are concerned.

7

1 CONCLUSION

2 The oil shale transformation in the presence of an acidic catalyst was achieved under flow
3 conditions and microwave radiation. The average temperature at which it occurs was found to be
4 lower than the one observed when heating by conventional means, related to the presence of
5 important temperature gradients within the oil shale bed. Insulation of the reactor to improve
6 temperature control inside the microwave cavity could help overcoming this problem.

7 Thermo-gravimetric analysis of the spent shale samples from microwave heating showed a
8 two-stage process, with a first step at 450 – 460°C and a second one at 720°C, similar to what was
9 observed with the fresh oil shale sample. In contrast, after conventional heating of the oil shale,
10 the spent samples only presented the carbonate decomposition step, meaning that, under these
11 conditions, the organic matter was transformed to a greater extent than when using microwave
12 irradiation. Liquid products yield and composition were very similar for both microwave and
13 conventional heating. On the contrary, gas production was intensified in the latter case.

14 When adding water to the system under microwave heating, the average decomposition
15 temperature decreased. However, the products yield also decreased significantly. Shale oil
16 conversion was promoted by adding BEA zeolite to the oil shale sample. Under microwave
17 heating, a decrease in the average transformation temperature was detected, when comparing
18 with conventional heating. The total conversion of organic material was similar to the one
19 obtained for oil shale decomposition, performed without zeolite. However, coke production
20 increased at the expense of liquid products yield. Nevertheless, selectivity towards gas products
21 was improved, causing the yield for the “< C₆” fraction to increase, which is most likely due to
22 the intrinsic cracking activity associated with the zeolite. This effect was also observed under

1 conventional heating, where the transformation temperature was similar with and without BEA
2 zeolite. Both “< C₆” and “C₆ – C₁₀” products selectivity increased in the presence of the zeolite.
3 Analysis of the oils obtained revealed an increase of the aromatic character of the products
4 obtained when using microwaves. This effect was clear when the zeolite was added to the system.
5 Adding zeolite and water to the system simultaneously, in a limited temperature range, could be a
6 solution to overcome increased coke formation due to the presence of the zeolite, since water
7 molecules could work as hydrogen supplier to the system, decreasing the formation of coke
8 precursors.

9 Finally, when comparing the energy consumed to heat the oil shale sample under microwave
10 and conventional heating, it was concluded that the use of microwaves is advantageous, given
11 that, for the same liquid products yield, the energy consumption is much lower.

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ACKNOWLEDGMENTS

The authors would like to thank the Centre Scientifique et Technique de Pau, TOTAL, for the oil shale samples supplied and Galp Energia for the simulated distillation analyses of the oil samples recovered. We are also grateful to Runjie Mao, Centre for Materials Science, University of Central Lancashire, Preston, for the technical support with the microwave setup which made this work possible.

A. Neto would like to thank the financial support from Fundação para a Ciência e Tecnologia (FCT) (ref. SFRH/BD/45051/2008).

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Table 1. Elemental weight composition of the oil obtained using microwave heating to decompose the oil shale; comparison with conventional crude oil.

Element	Shale oil from microwave heating, wt. %	Conventional Petroleum ⁶ , wt. %
C	86.5 ± 0.2	83.0 – 87.0
H	10.0 ± 0.2	10.0 – 14.0
N	1.30 ± 0.01	0.1 – 2.0
S	< 2	0.05 – 6.0

Table 2. Elemental analysis results of fresh and spent shale samples.

Content, wt. %	Fresh oil shale	Spent shale samples		
		mw	mw & water	Conventional heating
C	42.42	26.31	35.42	18.85
H	4.75	< 2	3.28	< 2
N	0.70	0.51	0.66	0.51
S	< 2	< 2	< 2	< 2
H/C (mol ratio)	1.3	0.9	1.1	1.3

Table 3. Transformation temperatures obtained for oil shale decomposition under microwave irradiation; organic matter balance for each experiment.

Experiment	Transformation temperature (start) °C	Initial organic content ^a wt. %	Liquid products yield wt. %	Organics not recovered wt. %	Gas produced wt. %
Microwave heating					
Oil shale transformation	300	47	49	34	18
Addition of 5 wt. % BEA	245	45	30	49	21
Presence of water vapour	242	47	32	55	12
Conventional heating					
Oil shale transformation	380	47	51	18	31
Addition of 5 wt. % BEA	380	45	52	16	32

^afrom TGA.

Table 4. Total conversion and selectivity by product fraction, using microwave irradiation and conventional heating.

Experiment	Total Conversion %	Selectivity, %			
		< C ₆	C ₆ – C ₁₀	C ₁₀ – C ₁₆	> C ₁₆
Microwave heating					
Oil shale transformation	70	36	28	23	8
Addition of 5 wt.% BEA	70	44	16	9	2
Presence of water vapour	49	43	26	18	5
Conventional heating					
Oil shale transformation	84	45	26	21	6
Addition of 5 wt.% BEA	85	47	30	16	6

Table 5. Identification of the bands observed in the regions 3500–2400 cm⁻¹ and 2000–700 cm⁻¹.

Vibration type			Wavenumber, cm ⁻¹
Methyl groups	Asymmetric stretching	$\nu_{\text{as}}(\text{CH}_3)$	2960
	Symmetric stretching	$\nu_{\text{s}}(\text{CH}_3)$:	2872
	Asymmetric bending	$\delta_{\text{as}}(\text{CH}_3)$	1454
	Symmetric bending	$\delta_{\text{s}}(\text{CH}_3)$	1377
Methylene bridge	Asymmetric stretching	$\nu_{\text{as}}(\text{CH}_2)$	2921
	Symmetric stretching	$\nu_{\text{s}}(\text{CH}_2)$	2852
	Scissoring	$\delta_{\text{s}}(\text{CH}_2)$	1460

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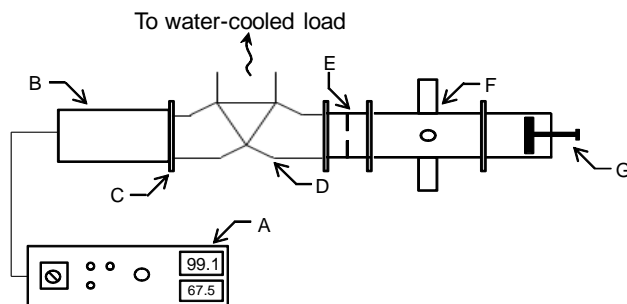


Figure 1. Schematic diagram of the microwave setup used in the study. (A) Variable power generator, (B) magnetron, (C) waveguide flange connector, (D) water-cooled circulator, (E) variable coupling aperture, (F) sample section, (G) plunge tuner.

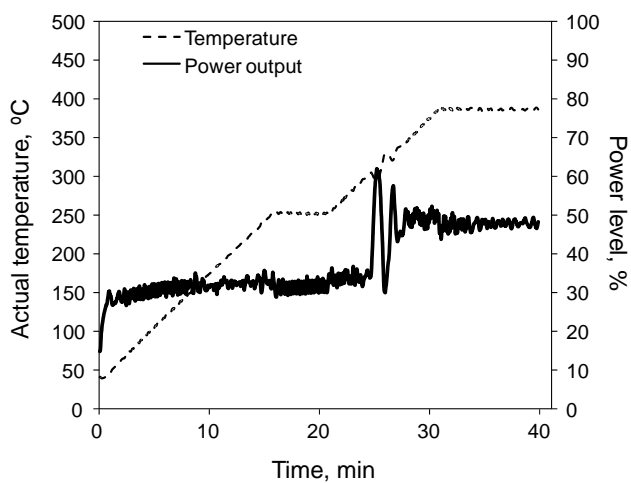


Figure 2. Data obtained from the power output control system of the microwave generator for a given temperature program.

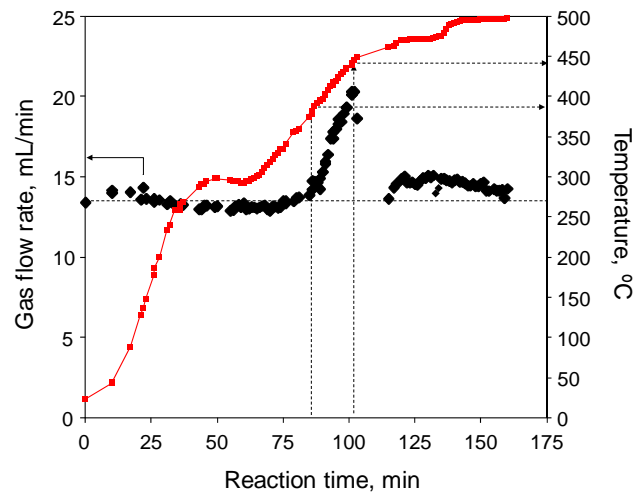


Figure 3. Gas flow rate measurement (♦) during oil shale transformation under conventional heating; relation with sample's temperature (■).

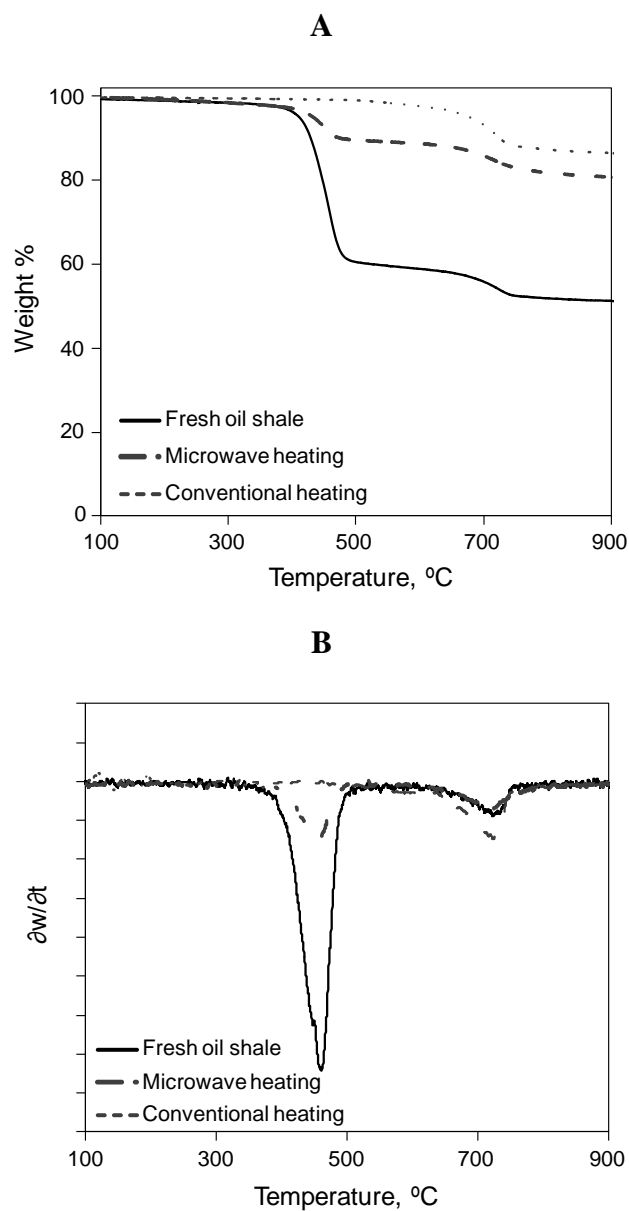


Figure 4. TGA of fresh and spent shale samples from decomposition under microwave irradiation and conventional heating, experiments under nitrogen flow (A); weight derivative in function of time (B).

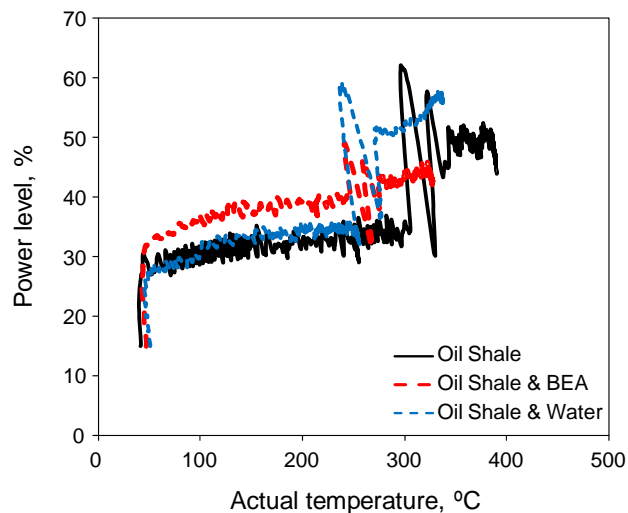


Figure 5. Power level from the microwave generator control system reported to the sample temperature; comparison between all experiments using microwave heating.

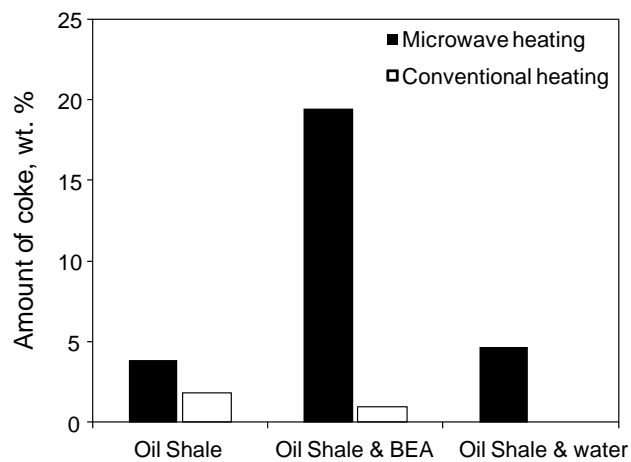


Figure 6. Comparison of the amount of coke produced for the experiments using microwave and conventional heating.

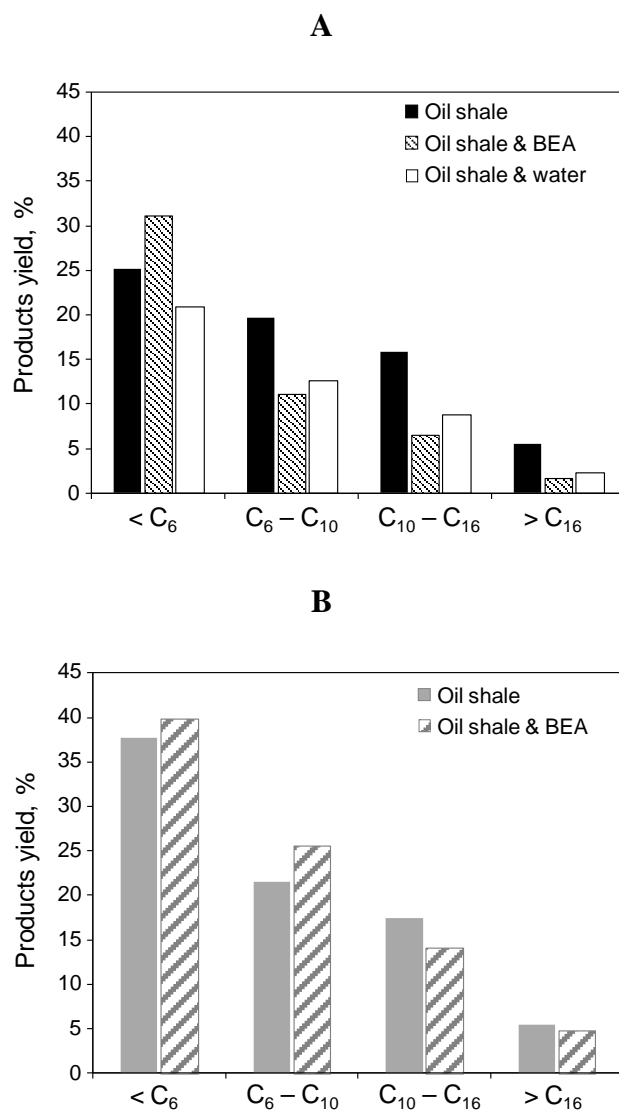


Figure 7. Products yield for the cases studied under microwave irradiation (A) and conventional heating (B).

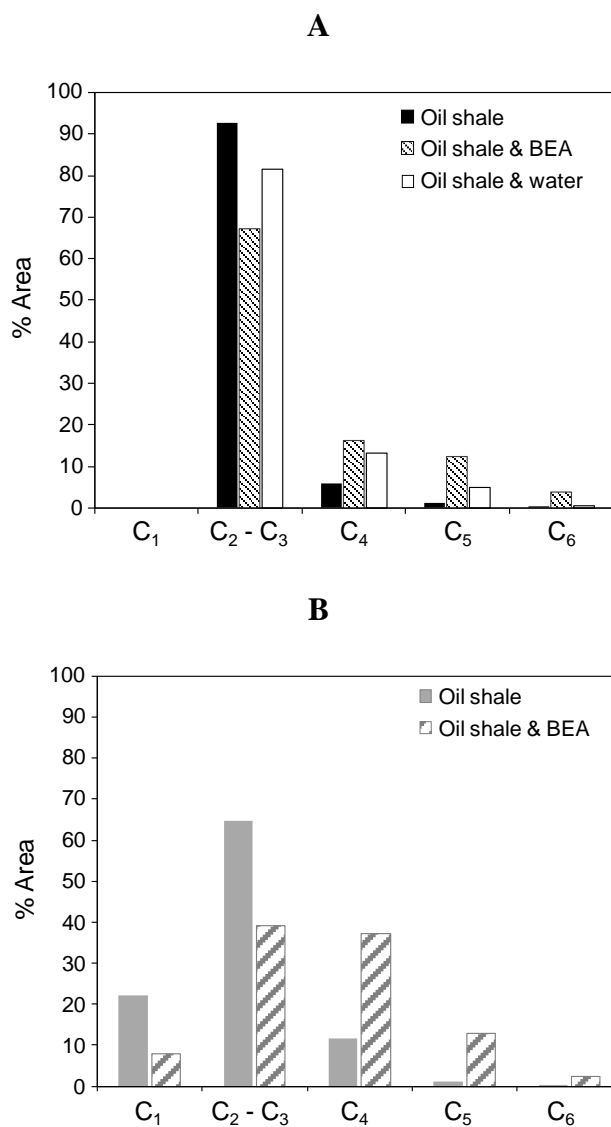


Figure 8. Result from peak integration of the GC-MS chromatogram for the gas samples obtained via microwave irradiation (A); peak integration of the chromatogram from GC of the gas samples obtained via conventional heating (B).

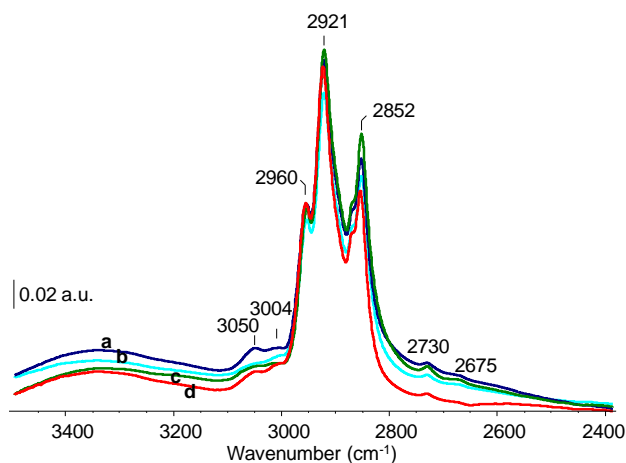


Figure 9. Normalized IR spectra in the $\nu(\text{C-H})$ vibration region: a – microwave heating; b – conventional heating with BEA zeolite; c – conventional heating; d – microwave heating with BEA zeolite.

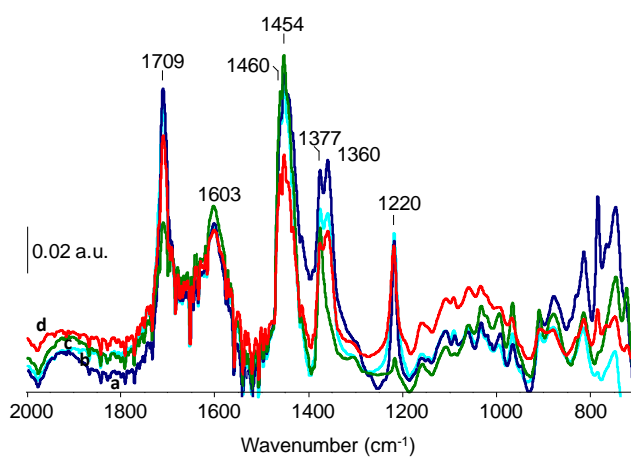


Figure 10. Normalized IR spectra in the $\delta(\text{C-H})$ vibration region: a – microwave heating; b – conventional heating with BEA zeolite; c – conventional heating; d – microwave heating with BEA zeolite.

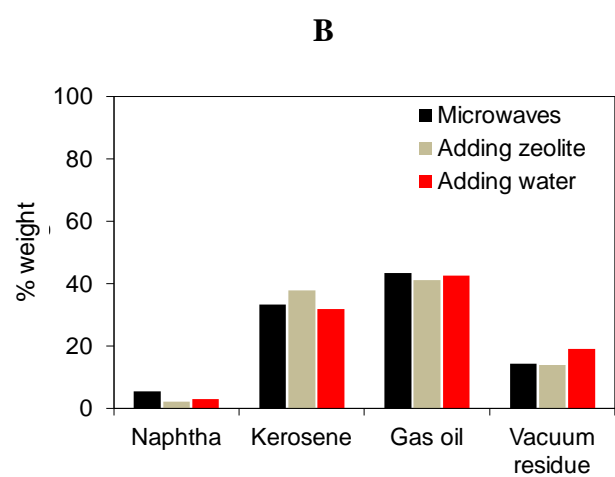
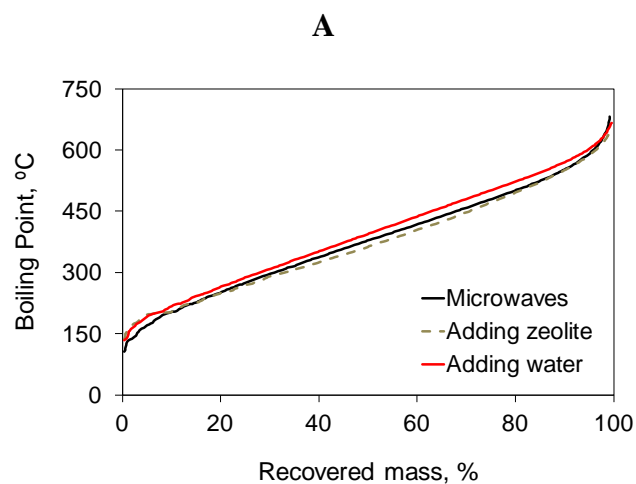


Figure 11. For all the liquids obtained using microwave heating, simulated distillation curves (A) and percent mass recovered per boiling point cut (B).

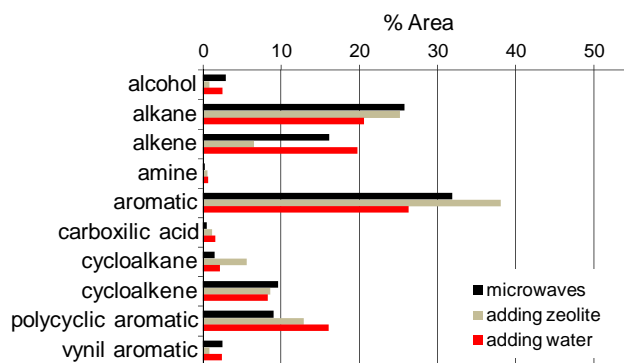


Figure 12. Percent area obtained for each group of organic compounds found in the liquids obtained in the experiments using microwave irradiation.

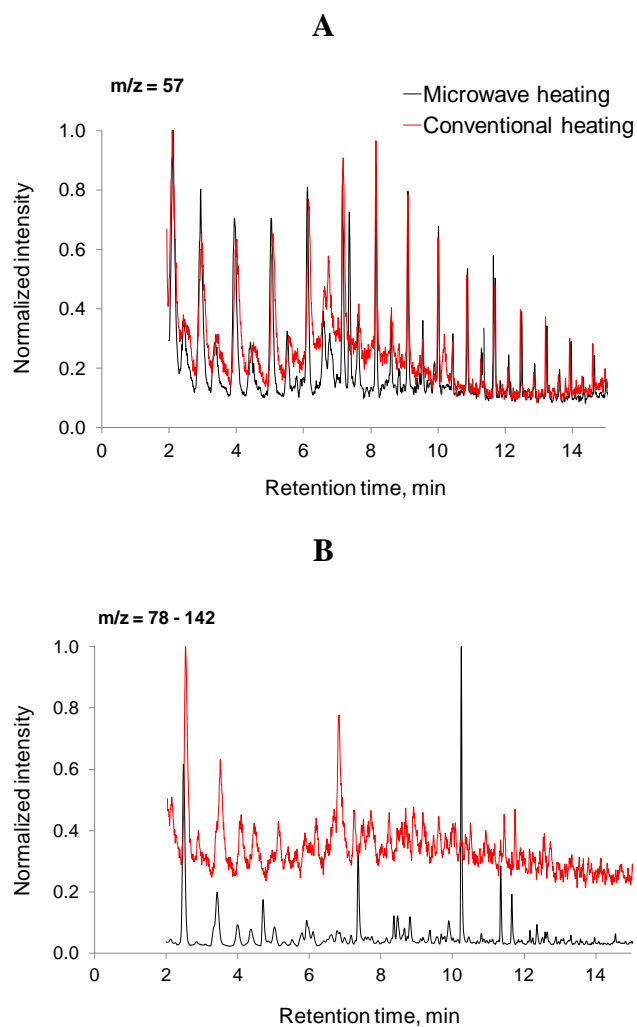


Figure 13. Normalized ion chromatograms for (A) m/z of 57 and (B) m/z of 78 to 142, with respect to the oils obtained under microwave and conventional heating.

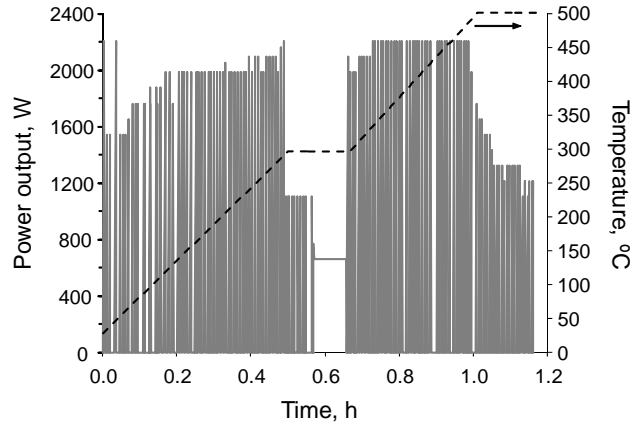


Figure 14. Power variation (—) during operation of the oven for oil shale transformation and relation with the oven temperature set point (---).

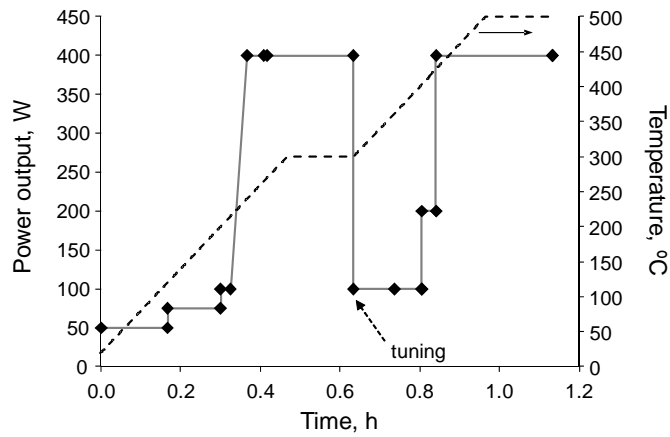


Figure 15. Power output during microwave irradiation of the oil shale sample (◆); comparison with temperature set point (---).