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Parametric study of flow-induced vibrations in cylinder arrays under single-phase fluid cross flows using POD-ROM

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Modeling numerically Flow-Induced Vibrations in heat exchangers at a microscopic scale requires high computational resources and time which are still unreachable. Therefore model reduction is investigated in the present work in order to address the issue of simulation computational time reduction. In the framework of POD-Galerkin projection methods, the purpose is to propose optimal a posteriori reduction strategies enabling error control on approximation as well as Reduced-Order Model (ROM) interpolation to deal with sensitivity analysis of solutions to parameter perturbations. A multi-phase fluid-solid POD-Galerkin-based method is proposed for modeling flows and vibrations in cylinder arrangements under single-phase fluid cross-flows. Moreover a single-POD basis method is evaluated in the context of ROM interpolation. This work is a first step in the development of robust ROM describing fluid and solid dynamics in the presence of turbulence, heat transfer effects and large magnitude structure displacements and deformations.

0. Introduction

Optimization of safety barrier reliability and Uncertainty Quantification (UQ) of physical models give rise to long-term research programs involving designers and engineers working on maintaining systems under operating conditions. The present article focuses on vibration risk assessment in heat exchangers in the context of lifecycle control and increase of mechanical components in spite of the very constrained conditions they are submitted to. In Pressurized Water Reactors (PWR) steam generators ensure the transition between the primary and secondary loops and are used to convert water into steam from heat produced by the core made of fuel assemblies. Each heat exchanger can measure up to 20 m and is made of regular confined arrangements of several thousands of thin elongated cylinders whose section diameter may be less than 2 cm. These cylinders are conveying the primary fluid and steam is produced, coming from the water on the shell side, so-called the secondary fluid. The heat exchanges take place at this stage in this area. Then the secondary steam is delivered to turbines for electric power generation. A brief dimensionless analysis of this geometrically complex system shows that as a first approximation under current conditions the dynamical behavior of these vibrating cylinders is independent on heat transfers. Therefore it is not necessary to account for thermal effects in the context of dynamical analysis. Due to geometry and to thermohydraulics conditions, most effects responsible for vibrations of cylinder arrays are due to Fluid Structure Interaction (FSI) and Flow-Induced Vibration (FIV) occurring at the external shell of the cylinders. They are due

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to the hydrodynamic unsteady load exerted by the external fluid on these structures. Moreover the component is such that cylinders are submitted to two-phase flows at the top and to single-phase flows at the bottom. Therefore as a first step, in the present article, one focuses on single-phase FIV at the bottom of the heat exchanger where flows are crossing mostly transversally the array. The purpose is to address the multi-physics multi-scale issue of stability analysis of dynamical response of cylinder arrangements submitted to external single-phase fluid flows in order to be able to establish accurate stability maps applicable for design. Therefore parameter perturbations must be investigated in order to account for possible large variations of parameter values during the lifecycle of these mechanical components.

As far as numerical modeling is concerned, a fully three-dimensional microscopic-scale model of the bottom area of the heat exchanger tube array under single-phase fluid cross flow under real operating conditions characterized by Reynolds numbers of order of 10^5 would lead to solving systems involving more than 10^{10} degrees of freedom which is still unreachable in practice even by using most advanced High Performance Computing (HPC) resources. Therefore superposition methods have been introduced in the context of first order asymptotic developments in order to perform linear stability analysis of these systems and exhibit major mechanisms involved in dynamical instability occurrence. Using space domain decompositions dimensionless parameter effects have been studied independently. Nevertheless HPC simulations performed on small-size domains are not yet convenient for design since they still require long computations of several hours to several days according to Reynolds numbers to be considered and to turbulence models to be involved. Therefore Reduced-Order Modeling (ROM) is investigated in order to deal with this problematic of reducing computational time. It is investigated in the present work by considering as a first step a two-parameter configuration where only Reynolds number and reduced velocity can vary while other parameters like mass ratio, Scruton number and pitch ratio of the cylinder arrangement are given. The basic idea is to use few High-Fidelity (HF) computations with a classical method (such as Finite Volumes and Finite Elements) to build low computational time models. Then ROMs have an initial cost, but this cost can be charged off if the models are used for large set of parametric values. The success of such approaches can be quantified by the large field of their applications. For example, ROMs have been used for studying different configurations of thermal management of data centers (Samadiani and Joshi, 2010), for controlling wave energy converters (Hesam and Shoori, 2014), fluid flow control at high Reynolds numbers (Semaan et al., 2016; Balajewicz et al., 2016) or in aeronautics (Kim, 2016). One way also explored is computation on smartphone, for which ROM approaches seem to be the appropriate solution. For example, Modesto et al. (2015) proposed an application for smartphone for computing disturbances in the Barcelona harbor in quasi real time using a ROM approach. On the same thing, ROM using a few/small resources could be used in a context of volunteer computing (Nouman Durrani and Shamsi, 2014) for a large parametric studies.

Few works exists on ROM development for FIV or FSI context. All works consist in adapting or extending the Proper Orthogonal Decomposition (POD) to this problematic. The POD is the most famous method for ROM in fluid mechanics and it has naturally been extended and adapted to the cases of flow in the presence of moving boundaries. For FSI cases similar to aeroelasticity, i.e where the fluid domain could be considered as fixed, the Navier–Stokes equations are linearized and projected on a POD basis (Barone et al., 2009b; Lieu et al., 2006). For small vibrations at the surface of the structure, Bourguet et al. (2011) proposed a Hadamar formulation associated with a ROM-POD. For large fluid domain motion of deformation, Rozza (2009) used POD on a parametric mesh and next built ROM for stationary problems on different meshes. In case of imposed displacement of the structure, Balajewicz and Farhat (2014) proposed an immersed boundary ROM with a modified formulation. The ROM is directly built in an immersed boundary solver and is available only for imposed displacement of the solid domain. Among the previous proposed methods, none allows to solve a FSI problems with a large displacement of the structure, i.e cases where the fluid modifies the behavior of the structure, which interactively also changes the flow. The issue of using POD for moving domains deals with the paradox of computing a POD basis which is a spatial basis on a changing (i.e. a time-evolving) domain. Liberge and Hamdouni (2010) and Liberge et al. (2010) proposed a POD-multiphase formulation available for FSI problems with large displacement of the domain. The method consists in computing a POD basis of an interpolated velocity field on a reference grid, and next in projecting a multiphase formulation on this POD basis. It is recalled in the next section. This method has been successfully used for small and large displacements of a cylinder in a cross fluid flow for known parameters.

This paper explores the behavior of POD-multiphase ROM when the parameter values are different from those used to build the POD basis. In the first part, the principles of the POD, the POD-multiphase and the ROM parameter sensitivity analysis methods are explained. Next, the parameter sensitivity of the cylinder vibrations in a cross fluid flow is studied and results are discussed.

1. Theory

One considers $\Omega \subset \mathbb{R}^3$ such that $\Omega = \Omega_f(t) \cup \Omega_s(t) \cup \Gamma_i(t)$ with Ω_s the solid domain, Ω_f the fluid domain and Γ_i the fluid–solid interface. One defines the external boundary of the domain : $\Gamma_f = \partial\overline{\Omega} \setminus \Gamma_i$. The normal vector \mathbf{n} is oriented as pointing out towards outside the solid domain. One defines a velocity field \mathbf{u} over the whole domain $\Omega \times [0, T]$ where T corresponds to the last time where the dynamics of the system is considered.

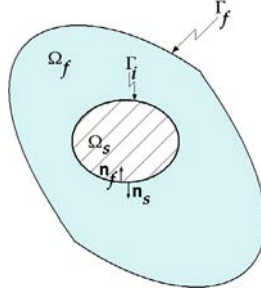


Fig. 1. Fluid structure interaction scheme.

1.1. The Proper Orthogonal Decomposition (POD)

The Proper Orthogonal Decomposition method being a well-known method, just a practical approach introduced by Sirovich (1987) and the principal properties are exposed in the following. For more informations, one can refer to Allery et al. (2004), Liberge and Hamdouni (2010) and Liberge et al. (2010).

Considering a set of M snapshots $\mathbf{u}(t_k)$, $k = 1 \dots M$ of the velocity field, the POD method consists in solving the following eigenvalue problem :

$$CA_k = \lambda_k A_k \quad (1)$$

with $C_{ij} = \int_{\Omega} \mathbf{u}(\mathbf{x}, t_i) \mathbf{u}(\mathbf{x}, t_j) d\mathbf{x}$ is a time correlation tensor of the snapshots of the velocity field. Next, the vectors of the spatial basis are obtained with the decomposition :

$$\Phi_k(\mathbf{x}) = \sum_{m=1}^M A_m^k \mathbf{u}(\mathbf{x}, t_m) \quad (2)$$

The POD basis has the following properties :

- There is a set of positive eigenvalues $(\lambda_i)_{i \geq 1}$ which decreases to 0,

$$\lambda_1 \geq \lambda_2 \geq \dots \geq \lambda_i \geq \dots \text{ and } \lambda_i \rightarrow 0 \quad (3)$$

and a set of vectors $(\Phi_i)_{i \geq 1}$ which is a Hilbertian basis.

- The vectors (Φ_i) are orthogonal and can be normalized:

$$(\Phi_i, \Phi_j) = \int_{\Omega} \Phi_i(\mathbf{x}) \cdot \Phi_j(\mathbf{x}) d\mathbf{x} = \delta_{ij} \quad (4)$$

In case of an incompressible flow, the POD basis fulfills the free divergence, i.e. $\text{div} \Phi_i = 0$, $i \geq 1$.

- The values of the temporal coefficients a_i at specific times t_k , $k = 1 \dots M$ are obtained from the projection of \mathbf{u} onto the basis :

$$a_i(t_k) = (\mathbf{u}(t_k), \Phi_i) \quad (5)$$

This procedure is called POD direct projection.

- The eigenvalue λ_i is the energy captured by the vector Φ_i . For a given N , the POD decomposition is the best energy decomposition that can be obtained.

Usually, in fluid mechanics, the POD is computed for the fluctuating velocity field \mathbf{u}' and the POD basis is (Φ'_i) .

1.2. The POD-multiphase formulation for FSI problems

The classical POD approach leads to a spatial basis, and needs fixed domains. Indeed, if the domain Ω is time dependent, the eigenvalue problem (1) cannot be computed since the snapshots do not have the same domain definition at times t_i and t_j . To cancel this drawback, Liberge and Hamdouni (2010) and Liberge et al. (2010) have proposed to use a global domain Ω with a fixed grid which recovers all the time variant domains $\Omega = \Omega_f(t) \cup \Omega_s(t) \cup \Gamma_i(t)$ as displayed in Fig. 2.

The method consists in computing snapshots using a classical Fluid Structure Interaction approach, which can use time variant grid. Next, the snapshots are interpolated from the time variant grid to the reference one. The snapshots can be

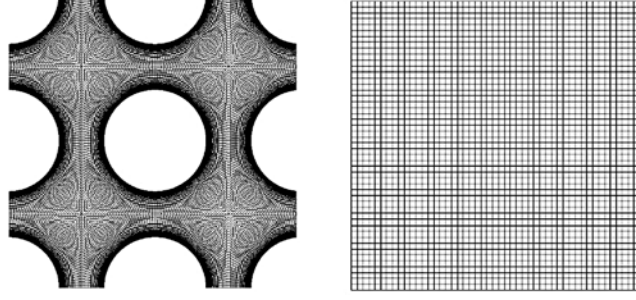


Fig. 2. Examples of grids for moving (left) and reference (right) domains to be introduced in order to account for time dependency of fluid–solid interface in a configuration involving a periodic cylinder arrangement with a moving central cylinder.

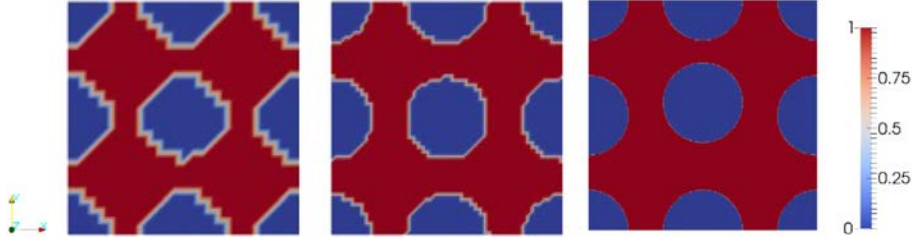


Fig. 3. Space- and time-dependent characteristic functions in the whole domain equal to 1 in the fluid and 0 in the solid domains for fluid and conversely for solid for coarse with 25×25 cells (left), refined with 50×50 cells (middle) and fine with 200×200 cells (right) cartesian grids for a two-dimensional configuration involving a periodic cylinder array.

computed by a classical solver using Arbitrary Lagrange Euler (ALE) method involving moving grid. Then a global velocity field is built on Ω as follows:

$$\mathbf{u}(\mathbf{x}, t) = \mathbf{u}_s(\mathbf{x}, t)1_{\Omega_s}(\mathbf{x}, t) + \mathbf{u}_f(\mathbf{x}, t)1_{\Omega_f}(\mathbf{x}, t) \quad (6)$$

with $\mathbf{u}_s(\mathbf{x}, t)$ the solid velocity field defined on space $\Omega_s(t)$ and $\mathbf{u}_f(\mathbf{x}, t)$ the fluid velocity field defined on space $\Omega_f(t)$ at time t . Characteristic functions are respectively expressed by $1_{\Omega_s}(\mathbf{x}, t)$ and $1_{\Omega_f}(\mathbf{x}, t)$ with $1_{\Omega_s}(\mathbf{x}, t) = 1 - 1_{\Omega_f}(\mathbf{x}, t)$. Each function 1_{Ω_i} (for $i = f$ or s) is defined by :

$$1_{\Omega_i}(\mathbf{x}, t) = \begin{cases} 1 & \text{if } \mathbf{x} \in \overline{\Omega}_i(t) \\ 0 & \text{else} \end{cases}$$

Each variable (density and viscosity) and each field is decomposed following the example of Eq. (6).

Examples of time-dependent space distributions of characteristic functions are displayed in Fig. 3 for several grid refinement.

1.3. Reduced-order dynamical model

Applying the POD to the velocity field (6) leads to a spatial basis defined on Ω .

We focus in this paper on cases where solid domain can be modeled using a rigid body coupled with springs and dampers. The non fluid constraints are expressed as external forces \mathcal{F}_f and momenta \mathcal{M}_s .

Then, the ROM is built using the method proposed by Liberge and Hamdouni (2010). The principle is developed in Liberge and Hamdouni (2010) and it is recalled in the present paper.

The formulation consists in extending the Navier–Stokes equations to the solid domain by adding a rigidity constraint Eq. (7) defined on the solid domain and a Lagrange multiplier Λ associated with the constraint as follows:

$$\mathbf{D}(\mathbf{u}) = 0 \text{ in } \Omega_s(t) \quad (7)$$

where $\mathbf{D}(\bullet)$ is defined by :

$$\mathbf{D}(\bullet) = \frac{1}{2} (\nabla \bullet + \nabla^T \bullet).$$

This leads to the following variational formulation on the global domain Ω :

$$H_{v_r} = \{ \mathbf{u} | \mathbf{u} \in H^1(\Omega), \mathbf{u} = \mathbf{u}_r(t) \text{ on } \partial\Omega \setminus \Gamma_1 \},$$

$H_0 = \{ \mathbf{u} | \mathbf{u} \in H^1(\Omega), \mathbf{u} = 0 \text{ on } \partial\Omega \setminus \Gamma_1 \}, L_0^2(\Omega) = \{ q \in L^2(\Omega) | \int_{\Omega} q dx = 0 \},$
 $\forall \mathbf{u}^* \in H_0 \text{ and } q \in L^2(\Omega), \text{ find } \mathbf{u} \in H_{v_f}, p \in L_0^2(\Omega), \Lambda \in H^1(\Omega_s(t)) \text{ such that}$

$$\int_{\Omega} \rho \left(\frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \nabla \mathbf{u} \right) \mathbf{u}^* dx - \int_{\Omega} p \nabla \cdot \mathbf{u}^* dx + \int_{\Omega} q \nabla \cdot v dx + \int_{\Omega} 2\mu \mathbf{D}(\mathbf{u}) : \mathbf{D}(\mathbf{u}^*) dx + \int_{\Omega_s(t)} \mathbf{D}(\Lambda) : \mathbf{D}(\mathbf{u}^*) dx = \int_{\Omega} \mathbf{f} \mathbf{u}^* dx \quad (8)$$

where ρ and μ are defined on the global domain Ω :

$$\rho = \rho_f (1 - 1_{\Omega_s}) + \rho_s 1_{\Omega_s}, \quad \mu = \mu_f (1 - 1_{\Omega_s}) + \mu_s 1_{\Omega_s}. \quad (9)$$

μ_s is the penalization factor associated with the Lagrange multiplier. \mathbf{f} denotes the global volumique forces defined as

$$\mathbf{f} = \mathbf{f}_f (1 - 1_{\Omega_s}) + \mathbf{f}_s 1_{\Omega_s} \quad (10)$$

where \mathbf{f}_f designates the standard external volumic hydrodynamic forces exerted by the fluid and \mathbf{f}_s is the other part of external volumic forces acting on the rigid body different from fluid forces. \mathbf{f}_s satisfies the two following equations :

$$\mathcal{F}_s = \int_{\Omega_s} \mathbf{f}_s dx \text{ and } \mathcal{M}_s = \int_{\Omega_s} \mathbf{f}_s \wedge \mathbf{x} dx \quad (11)$$

Next, the POD-ROM is built by choosing POD modes $\Phi_i, i = 1 \dots N$ for the virtual velocity field and the decomposition of \mathbf{u} on the POD basis.

For each $n = 1, \dots, N$:

$$\begin{cases} \sum_{i=1}^N \frac{da_i}{dt} A_{in} + \sum_{i=1}^N \sum_{j=1}^N a_i a_j B_{ijn} + \sum_{i=1}^N a_i C_{in} + D_n + E_n = 0 \\ \mathbf{D}(\mathbf{u}) = 0 \text{ in } \Omega_s(t) \\ \frac{\partial 1_{\Omega_s}}{\partial t} + \mathbf{u} \cdot \nabla 1_{\Omega_s} = 0 \end{cases} \quad (12)$$

where :

$$\begin{aligned} A_{in} &= \int_{\Omega} \rho \Phi_i \cdot \Phi_n dx & D_n &= \int_{\Omega} 1_{\Omega_s} \text{Tr}[\mathbf{D}(\Lambda) \mathbf{D}(\Phi_n)] dx \\ B_{ijn} &= \int_{\Omega} \rho (\Phi_i \cdot \nabla) \Phi_j \cdot \Phi_n dx & E_n &= \int_{\Omega} \mathbf{f} \Phi_n dx \\ C_{in} &= 2 \int_{\Omega} \mu \text{Tr}[\mathbf{D}(\Phi_i) \mathbf{D}(\Phi_n)] dx \end{aligned}$$

As explained in Liberge and Hamdouni (2010) the formulation (12) does not need to compute explicitly the fluid forces on the structure because they are intrinsic to the formulation. In addition, the equivalent formulation using the fluctuating velocity field is described in Appendix A. Moreover the method can be extended to the case of deformable structure as described in Appendix B.

Remark. A POD-Galerkin method is involved in the present work. It is well-known that it can lead to instabilities, that is why the use of additional viscosities associated to each POD mode (Cazemier et al., 1998) or Least-Square approach (Tallet et al., 2015; Carlberg et al., 2017) is often preferred in the context of fluid mechanics applications. However this is not necessary in the present study since as explained in Liberge and Hamdouni (2010), the solid viscosity used to penalize the rigid body plays the role of the viscosity of Cazemier et al. (1998) and avoids instabilities.

2. Application to FIV of cylinder array

2.1. Configuration

In what follows, the model reduction method is applied to a configuration involving a periodic cylinder array made of one central moving cylinder and 8 truncated non-moving cylinders submitted to an external cross flow. The problem is two-dimensional thanks to the choice of parameters since the Reynolds number does not exceed 1000. Reduced velocity varies between 1 and 4. Other parameters are fixed. Pitch ratio is 1.44, Scruton number is taken to 0 and mass ratio equals 7.8. (See Fig. 4).

These parameters are defined as follows: pitch ratio $P_r = P/D$ with D the cylinder diameter and P the distance between two centers of in-line neighbor cylinders in the square array; Scruton number or mass-damping parameter $Sc = (2\pi\xi m) / (\rho_f D^2)$ with ξ the solid reduced damping in presence of flow, m the solid mass and ρ_f the fluid density;

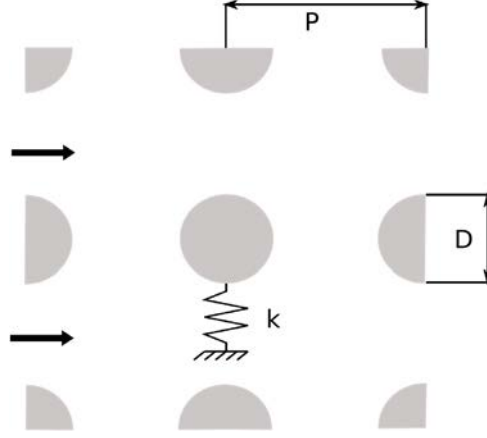


Fig. 4. Application to tube array.

mass ratio $M = \rho_f / \rho_s$ with ρ_s the solid density; Reynolds number $Re = (\rho_f U D) / \mu$ with U the characteristic fluid flow velocity and μ the kinematic fluid viscosity; reduced velocity $U_R = U / f_s D$ with f_s the characteristic solid frequency in the considered medium defined as $f_s = \frac{1}{2\pi} \sqrt{\frac{k}{m}}$ and the stiffness of the spring.

The expression of \mathbf{f}_s defined in Eq. (10) is :

$$\mathbf{f}_s = \frac{k}{|\Omega_s|} (\mathbf{x} - \mathbf{x}_0) \quad (13)$$

with $|\Omega_s|$ the volume of the solid, and \mathbf{x}_0 the solid position at rest. Thus,

$$\mathcal{F}_s(t) = \int_{\Omega_s(t)} \mathbf{f}_s dx = k(\mathbf{x}_G(t) - \mathbf{x}_0) \quad (14)$$

with \mathbf{x}_G the coordinate of the gravity center of the rigid body. For the studied case, $\mathbf{f}_f = 0$.

Using the fluid, solid and geometric characteristics, the dimensionless formulation of system (8) leads to the definition of two significant nondimensional parameters, the Reynolds number and the reduced velocity. This leads to a nondimensional form for the ROM as follows:

for each $n = 1, \dots, N$,

$$\begin{cases} \sum_{i=1}^N \frac{da_i}{d\tilde{t}} \tilde{A}_{in} + \sum_{i=1}^N \sum_{j=1}^N a_i a_j \tilde{B}_{ijn} + \sum_{i=1}^N a_i \tilde{C}_{in} + \tilde{D}_n + \tilde{E}_n = 0 \\ \tilde{\mathbf{D}}(\tilde{\mathbf{u}}) = 0 \text{ in } \tilde{\Omega}_s(\tilde{t}) \\ \frac{\partial 1_{\Omega_s}}{\partial \tilde{t}} + \tilde{\mathbf{u}} \cdot \tilde{\nabla} 1_{\Omega_s} = 0 \end{cases} \quad (15)$$

where:

$$\begin{aligned} \tilde{A}_{in} &= \int_{\Omega} h(\tilde{\mathbf{x}}, \tilde{t}) \tilde{\Phi}_i \cdot \tilde{\Phi}_n dx \\ \tilde{D}_n &= \int_{\Omega} 1_{\Omega_s} \text{Tr}[\tilde{\mathbf{D}}(\Lambda) \tilde{\mathbf{D}}(\tilde{\Phi}_n)] dx \\ \tilde{B}_{ijn} &= \int_{\Omega} h(\tilde{\mathbf{x}}, \tilde{t}) (\tilde{\Phi}_i \cdot \tilde{\nabla}) \tilde{\Phi}_j \cdot \tilde{\Phi}_n dx \\ \tilde{E}_n &= \frac{1}{M} \frac{4\pi^2}{U_R^2} \int_{\Omega} (\tilde{\mathbf{x}} - \tilde{\mathbf{x}}_G) \tilde{\Phi}_n dx \\ \tilde{C}_{in} &= \frac{2}{Re} \int_{\Omega} g(\tilde{\mathbf{x}}, \tilde{t}) \text{Tr}[\tilde{\mathbf{D}}(\tilde{\Phi}_i) \tilde{\mathbf{D}}(\tilde{\Phi}_n)] dx \end{aligned}$$

$\tilde{\phi}$ denotes the dimensionless form of the corresponding variable or operator ϕ .

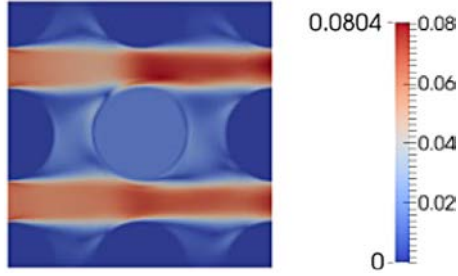


Fig. 5. Velocity field in $m.s^{-1}$ for Reynolds number $R_E = 612$ and reduced velocity $V_R = 1$. Pitch ratio is 1.44, Scruton number is 0 and mass ratio 7.8.

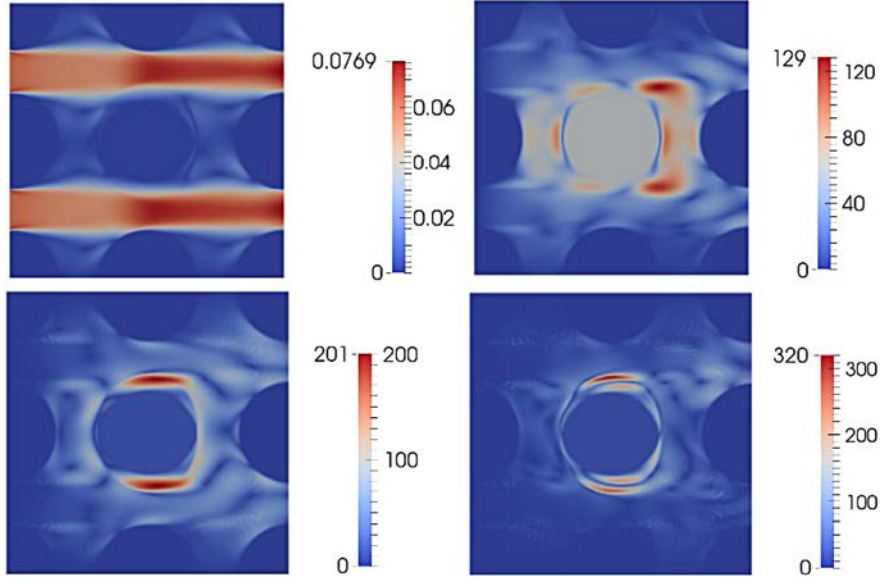


Fig. 6. Mean velocity field (top left), mode function shapes 1 (top right), 2 (bottom left) and 3 (bottom right) in $m.s^{-1}$ for Reynolds number $R_E = 612$ and reduced velocity $V_R = 1$. The pitch ratio of the cylinder array is 1.44. Scruton number is 0 and mass ratio 7.8.

2.2. POD basis generation

For POD basis generation HF simulations are performed on this configuration for several values of Reynolds number and reduced velocity. With the previous approach, each set of parameter values corresponds to an optimal POD-ROM. In the fluid domain, the HF computation involves a FV solver with colocalized pressure and velocity fields and a fractional time step approach as described in Archambeau et al. (2004). An ALE formulation based on an elliptic equation for grid deformation is involved to account for solid wall motion and the solid dynamics is modeled by using an oscillator equation solved by using a Newmark time scheme. A relaxation is introduced in order to ensure the stability of the explicit solver used to describe the dynamics and kinematics boundary conditions at the time-dependent fluid structure interface. An example of flow velocity field is reproduced in Fig. 5. This field was evaluated on the original reference grid. Then before ROM generation, it is interpolated on a cartesian coarser grid as displayed in Fig. 1.

2.3. ROM accuracy and control

Results provided by the reduced-order models of FIV in cylinder arrangements are displayed below. An example of mean flow velocity $\bar{\mathbf{u}}$ and first mode shapes Φ'_i (for $i = 1$ to 3) is plotted on Fig. 6 in a two-dimensional configuration involving a periodic cylinder arrangement under cross flow. The mean flow velocity does not allow to capture the velocity of the rigid body. This velocity is captured using the following modes which are non zero on the area traveled by the cylinder. These modes are also needed to have the velocity fluctuations. For example, the mode 3 has to be used to capture the fluid flow and the solid velocity for cylinder position near the maximum amplitude.

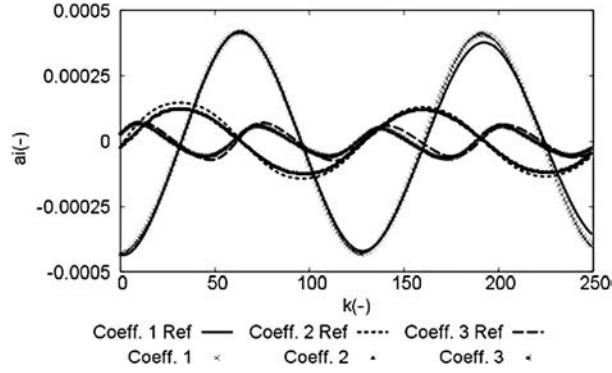


Fig. 7. Expected values deduced from reference solution versus reduced-order model values of time coefficients a_i (for $i = 1$ to 3) deduced from computation of the dynamical system for case of Figs. 5 and 6.

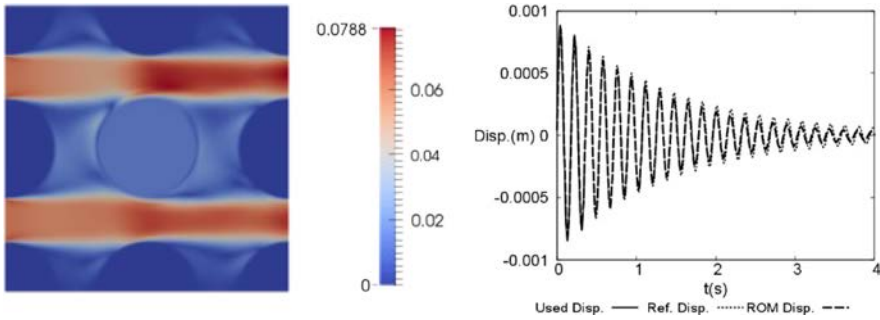


Fig. 8. Predicted flow velocity field on the cartesian grid using the POD-ROM (left). Solid displacement (right): reference solution (dots) versus predicted solution (lines) for case of Figs. 5 and 6.

Associated coefficients deduced from computation of the dynamical system (12) are displayed on Fig. 7. The coefficients are compared to expected values according to the sample of reference solutions as follows (for $i = 1$ to N):

$$a'_i = (\mathbf{u}', \Phi'_i) \quad (16)$$

Good adequacy has been found between the POD-ROM solution and the reference one. Finally the solution is reconstructed over the whole domain using the decomposition:

$$\mathbf{u}(\mathbf{x}, t) = \bar{\mathbf{u}}(\mathbf{x}) + \sum_{n=1}^N a'_n(t) \Phi'_n(\mathbf{x})$$

The reconstruction of the solution is compared to the solution of the reference system over the interpolation domain. The flow velocity field as well as the solid displacement are displayed in Fig. 8. With a truncate threshold fixed at 99%, the reduced order model solution reproduces reference values with a good agreement. The evolution of the relative error on the solution according to the mode number of the reduced model is given in Fig. 9. 10 modes are sufficient to stabilize the error. The size of the ROM is very small compared with the HF model. The sensitivity to grid refinement is also investigated. When increasing the number of cells of the cartesian grid, the slope is improved and the accuracy of the model for a given mode number is better. For the present study, refine the grid more than a 50×50 grid does not improve the quality of the ROM. The Fig. 3 shows a good description of the geometry with this grid. As displayed in Fig. 9, this grid is sufficient to capture the physics of the phenomena.

2.4. ROM stability

The sensitivity to penalization factor is plotted on Fig. 10. The stabilization compensates the effect of basis truncation which ensures a preservation of most energetic mode development but in the same time suppresses modes responsible for dissipation (Cazemier, 1997; Cazemier et al., 1998; Rempfer and Fasel, 1994). In the elementary configurations to be considered, an optimum is obtained for a solid viscosity close to the fluid value.

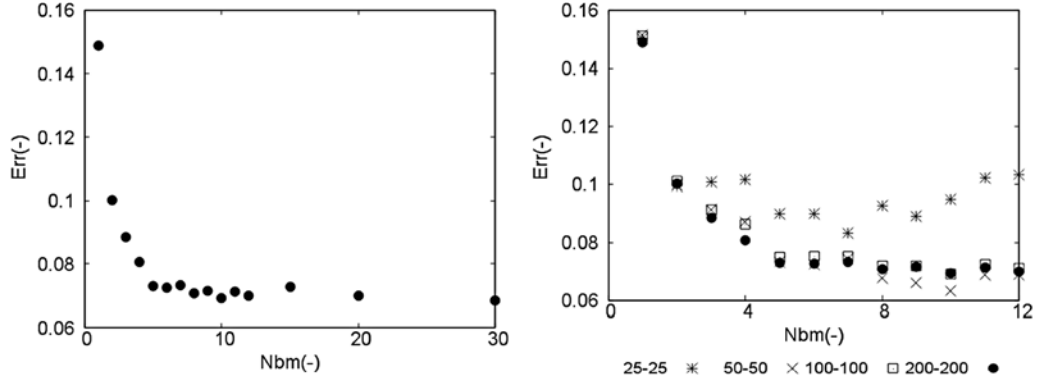


Fig. 9. Norm of the relative error on the solution according to number of modes of truncation from 1 to 30 (left) and to grid refinement for grids involving 25×25 to 200×200 cells (right) for case of Figs. 5 and 6.

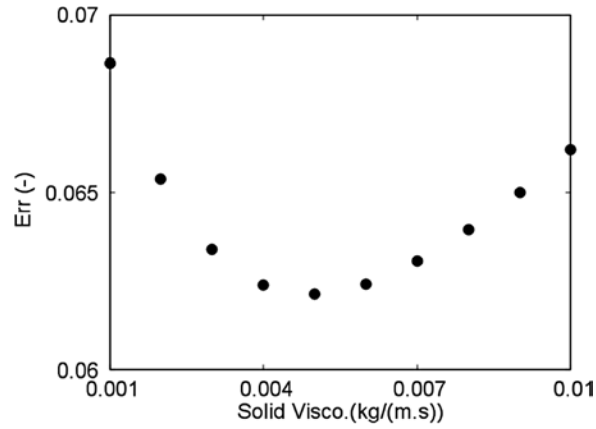


Fig. 10. Norm of relative error on the solution according to solid viscosity for case of Figs. 5 and 6.

2.5. Performances and CPU time reduction

The predictive capability of ROM over a long period of time is pointed out in several configurations for a given Reynolds number and several values of reduced velocity. The phase portrait of the dynamical response is displayed in Fig. 11 in three cases: for reduced velocity below, close to and above the critical value of the system dynamical stability limit. In each case the solution predicted by the ROM is in good agreement with reference Bourguet et al. (2011) and Barone et al. (2009a).

In terms of computational time the gain is displayed on Fig. 12. Comparisons of CPU times are performed by solving the ROM and High Fidelity (HF) model. In the present study, the HF model involves an ALE formulation of Navier–Stokes equations on a moving grid. The interpolation step from the moving grid to the reference grid as well as the POD basis computation are excluded. These two steps are considered as offline steps and only the online steps are compared. The gain in CPU time is expressed in % of gain per iteration, processor and cell. As shown in Fig. 12, the gain of CPU time is about of a factor 100 in the present configurations.

3. Small ROM parameter perturbations

3.1. Principle of sensitivity analysis

Here it is proposed to study the behavior of the POD-ROM when one considers different values of parameters than those used to compute the POD basis. Considering the problem (P_λ) :
Find \mathbf{u} in space H for parameter λ such that :

$$\begin{cases} \frac{\partial \mathbf{u}}{\partial t} = f(\mathbf{u}, \lambda) \\ \mathbf{u}(0) = \mathbf{u}_0 \end{cases} \quad (17)$$

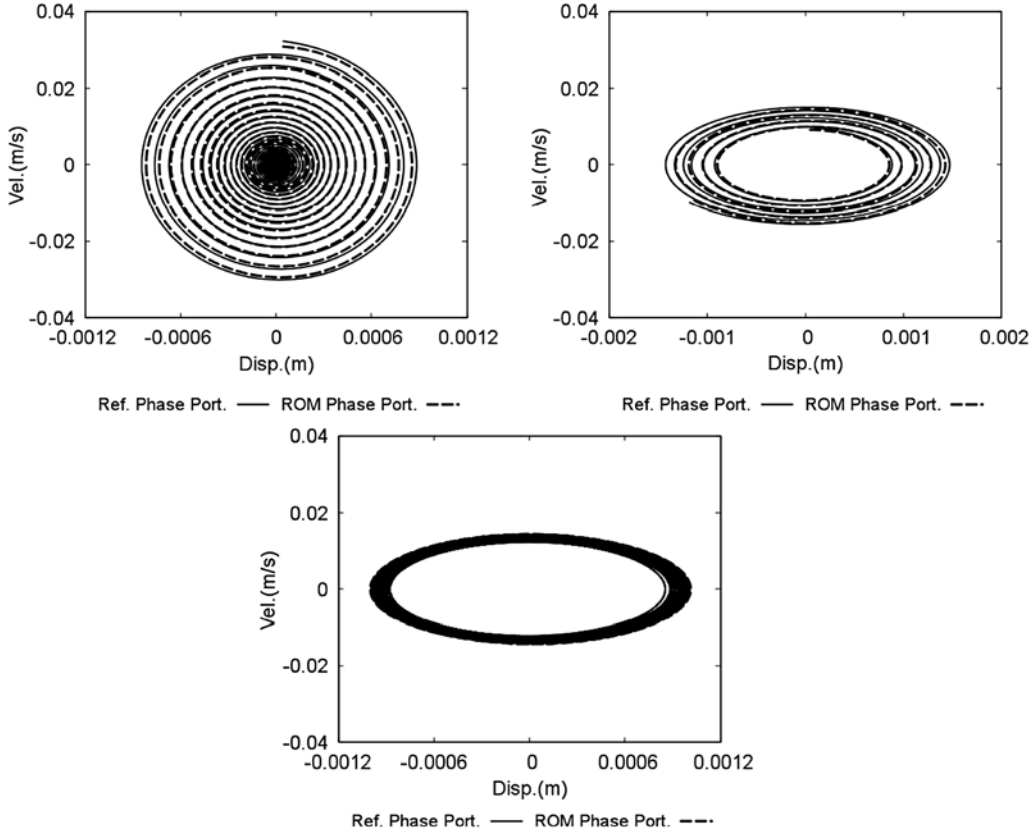


Fig. 11. Phase portrait of reference (lines) and ROM (dots) solutions for Reynolds number $R_e = 612$ and reduced velocity $U_r = 1$ (top left), $U_r = 3.273$ (top right) and $U_r = 2.448$ (bottom).

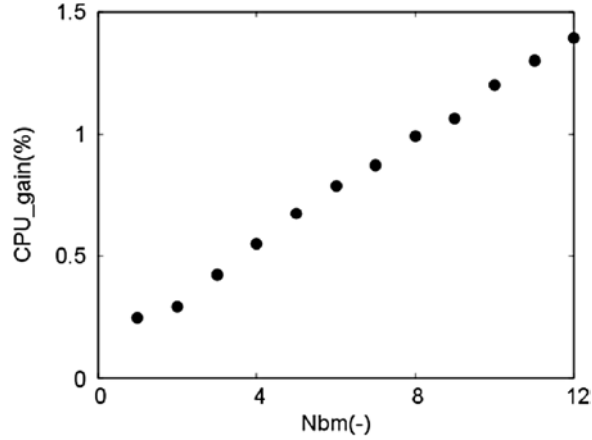


Fig. 12. Linear evolution of the gain in computational time compared to the reference simulation according to mode number of the reduced order model for case 3 of Fig. 11.

When a POD basis obtained for a parameter value λ_0 is used for a different value λ , Akkari et al. (2014b, a) proposed to bound the error by the number of POD modes involved in the POD-ROM :

$$\| \mathbf{u}_\lambda - \tilde{\mathbf{u}} \| \leq g(N) + |\lambda - \lambda_0|^\gamma h(N) \quad (18)$$

Table 1
Parameter values used for ROM interpolation with λ_1 and λ_2 respectively the Reynolds number and the reduced velocity of the problem.

| Case | Values of parameters for | POD basis generation | ROM generation |
|------|--------------------------|----------------------|----------------|
| 1 | λ_1 | 612 | 818 |
| | λ_2 | 3.27 | 3.27 |
| 2 | λ_1 | 818 | 612 |
| | λ_2 | 3.27 | 3.27 |
| 3 | λ_1 | 480 | 612 |
| | λ_2 | 1.00 | 1.00 |
| 4 | λ_1 | 612 | 480 |
| | λ_2 | 1.00 | 1.00 |
| 5 | λ_1 | 612 | 612 |
| | λ_2 | 2.44 | 3.27 |
| 6 | λ_1 | 612 | 612 |
| | λ_2 | 3.27 | 2.44 |
| 7 | λ_1 | 818 | 612 |
| | λ_2 | 3.27 | 2.44 |

where \mathbf{u}_λ is the approximation of the problem (P_λ) solution and $\tilde{\mathbf{u}}$ is given by :

$$\tilde{\mathbf{u}} = \sum_{n=1}^N a_n^{\lambda, \lambda_0} \Phi_n^{\lambda_0} \text{ or } \tilde{\mathbf{u}} = \bar{\mathbf{u}}^{\lambda, \lambda_0} + \sum_{n=1}^N a_n^{\prime \lambda, \lambda_0} \Phi_n^{\prime \lambda_0} \quad (19)$$

a_n^{λ, λ_0} is obtained by solving the POD-ROM resulting from the projection of the problem (P_λ) Eq. (17) on (Φ^{λ_0}) .

It is expected that for parameter values not too far from λ_0 , the ROM provides an accurate solution for a number of POD vectors N not too big.

3.2. Numerical results

In what follows, pitch ratio, Scruton number and mass ratio are given and the system is characterized by two parameters : Reynolds number and reduced velocity. The purpose is to evaluate the influence of small variations of these both parameters on the accuracy of the reduced model. Values of Reynolds number and reduced velocity are changed and reduced order model associated to each case is used for other cases.

In the present study, the Reynolds number is modified by changing the inlet velocity, and the Reduced velocity by changing the inlet velocity and the spring stiffness. Therefore, the initial values of the a_n^{λ, λ_0} (or $a_n^{\prime \lambda, \lambda_0}$) time coefficients of the ROM have to be modified. We note Γ the part of Γ_f with non zero Dirichlet boundary condition, and x_Γ a point of this boundary. The Reynolds number and the reduced velocity can be written :

$$Re = \frac{\rho_f u(x_\Gamma)}{\mu_f} \quad U_R = \frac{u(x_\Gamma)}{f_s D} \quad (20)$$

At the initial step, one gets :

$$\mathbf{u}^\lambda(x_\Gamma, 0) = \bar{\mathbf{u}}^{\lambda, \lambda_0}(x_\Gamma) + \sum_{n=1}^N a_n^{\prime \lambda, \lambda_0}(0) \Phi_n^{\prime \lambda_0}(x_\Gamma) \quad (21)$$

It is proposed to use a scaling coefficient α defined by :

$$\alpha(\lambda, \lambda_0) = \frac{u^\lambda(x_\Gamma, 0)}{u^{\lambda_0}(x_\Gamma, 0)}. \quad (22)$$

Then

$$\bar{\mathbf{u}}^{\lambda, \lambda_0} = \alpha(\lambda, \lambda_0) \bar{\mathbf{u}}^{\lambda_0} \quad (23)$$

and

$$a_n^{\prime \lambda, \lambda_0}(0) = \alpha(\lambda, \lambda_0) a_n^{\prime \lambda_0}(0) \quad (24)$$

Several configurations for stable and unstable dynamical behaviors are considered. Values of parameters of the configurations to be considered are described in Table 1.

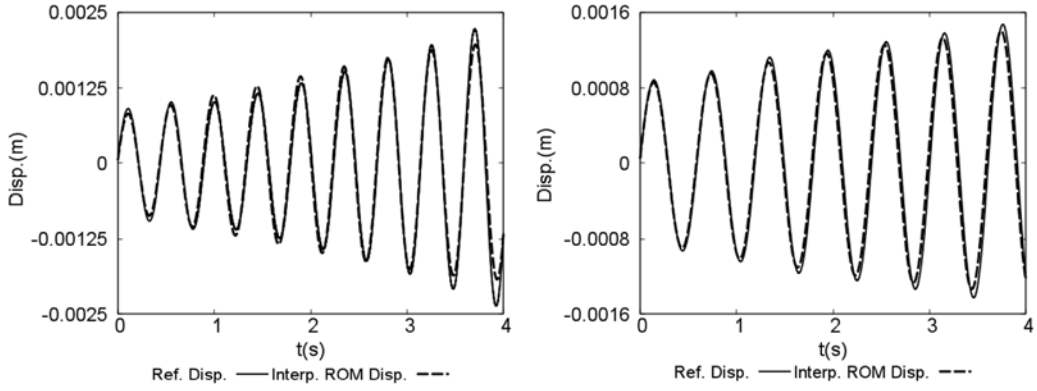


Fig. 13. Small perturbation of Reynolds number: case 1 (left), case 2 (right).

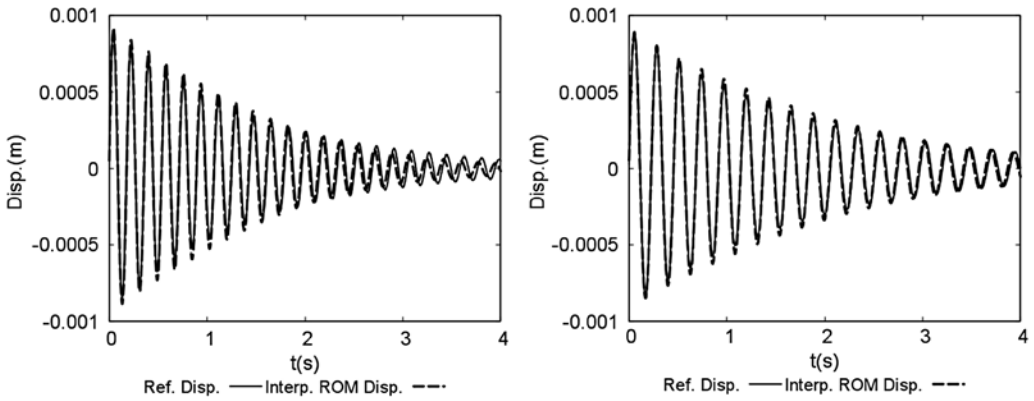


Fig. 14. Small perturbation of Reynolds number: case 3 (left), case 4 (right).

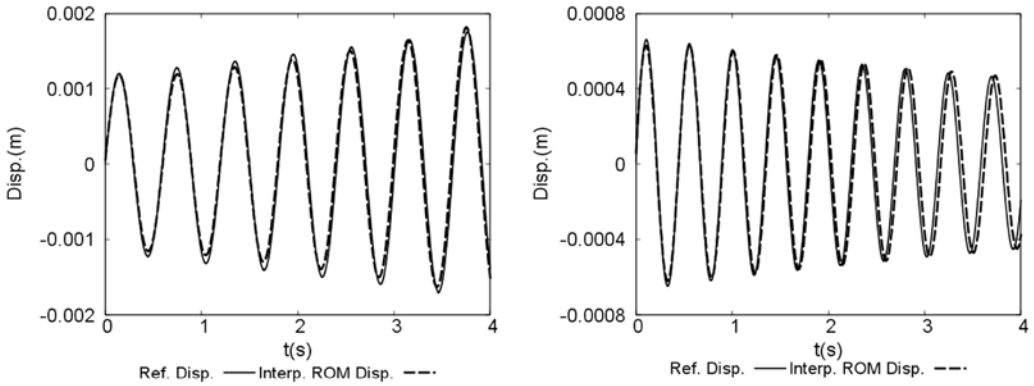


Fig. 15. Small perturbation of reduced velocity: case 5 (left), case 6 (right).

Three values of the Reynolds number are considered : 480,612 and 818. In that range of perturbation the flow regime is not changing. Three values are considered for reduced velocity too : a dynamical stable case ($U_r = 1$), a second dynamical stable case close to the critical stability ($U_r = 2.44$) and an unstable case ($U_r = 3.27$). Sensitivity to Reynolds number deviation is displayed in Figs. 13 and 14 respectively in dynamically unstable and stable cases. Reduced velocity deviation is investigated in Fig. 15.

POD basis associated with stable case is used for prediction of unstable solution and conversely. Finally both parameters Reynolds number and reduced velocity are changed simultaneously in Fig. 16. For each case, good behavior of the rigid body has been obtained by the ROM. It means that the ROM built for a parameter couple can be used for another near values

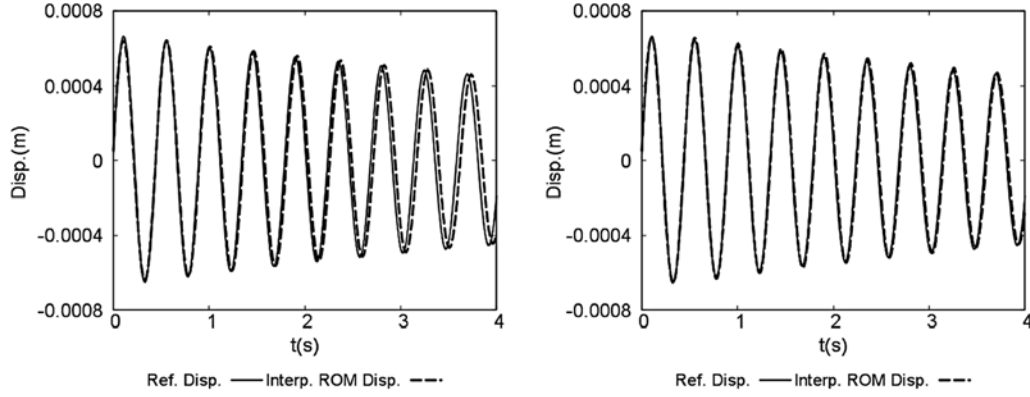


Fig. 16. Small perturbation of both Reynolds number and reduced velocity: case 7 with 10 (left) and 15 modes (right).

of parameters. In the case treated, the ROM is enough robust to model another behavior, i.e from stable to unstable or conversely. Change only one parameter or two in the same time does not affect the results. Increasing number of modes improves accuracy of results.

4. Conclusion

The multiphase-POD method has been applied for fluid structure interaction study in case of a 2D model of tube array. The proposed reduction method is efficient for velocity field prediction in a domain involving flows in interaction with solid dynamics. It relies on a standard POD-Galerkin projection method combined with an interpolation over a non-moving cartesian grid and a penalization method for dealing with heterogeneity of medium in the whole domain with possible unsteadiness. Both fluid and solid may feature a dynamical behavior. The robustness of the multiphase-POD methods is investigated in order to make possible real-scale real-time parameter sensitivity analysis and preserve the optimality of the generated ROM in terms of error control and computational time reduction. Good agreement has been found between the ROM solution and HF model, even if the ROM is used for another set of parameters than these used to build the POD basis. An extension of the method is now under development to account for turbulence and thermal effects.

Acknowledgments

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Appendix A. POD-Multiphase ROM for fluctuating velocity field

It has been observed that in fluid mechanics, the first POD mode is similar to the average velocity field and capture the most important part of the energy. Then, a practical approach consists in writing the POD-ROM for the fluctuating velocity field \mathbf{u}' such as:

$$\mathbf{u}'(\mathbf{x}, t) = \mathbf{u}(\mathbf{x}, t) - \bar{\mathbf{u}}(\mathbf{x})$$

where $\bar{\mathbf{u}}$ designates the mean flow velocity field and :

$$\mathbf{u}'(\mathbf{x}, t) = \mathbf{u}'_s(\mathbf{x}, t)1_{\Omega_s}(\mathbf{x}, t) + \mathbf{u}'_f(\mathbf{x}, t)1_{\Omega_f}(\mathbf{x}, t)$$

A POD basis is computed for this field :

$$\mathbf{u}'(\mathbf{x}, t) \simeq \sum_{n=1}^N a^n(t) \Phi'_n(\mathbf{x}) \quad (25)$$

The Navier–Stokes equations for a domain Ω_i , $i = f, s$ become :

$$\begin{cases} \rho_i \frac{\partial \mathbf{u}'_i}{\partial t} + \rho_i (\bar{\mathbf{u}}_i \nabla \bar{\mathbf{u}}_i + \bar{\mathbf{u}}_i \nabla \mathbf{u}'_i + \mathbf{u}'_i \nabla \bar{\mathbf{u}}_i + \mathbf{u}'_i \nabla \mathbf{u}'_i) - \nabla \cdot \sigma_i = \mathbf{f}_i \text{ in } \Omega_i \\ \nabla \cdot \mathbf{u}'_i = 0 \text{ in } \Omega_i \\ \mathbf{D}(u) = 0 \text{ in } \Omega_s(t) \end{cases} \quad (26)$$

The same procedure as that presented in Section 1.3 leads to the following ROM:
for each $n = 1, \dots, N$,

$$\left\{ \begin{array}{l} \sum_{i=1}^N \frac{da'_i}{dt} A'_{in} = \sum_{i=1}^N \sum_{j=1}^N B'_{ijn} a'_i a'_j + \sum_{i=1}^N C'_{in} a'_i + D'_n + E'_n \\ \mathbf{D}(\mathbf{u}) = 0 \text{ in } \Omega_s \\ \frac{\partial 1_{\Omega_s}}{\partial t} + \mathbf{u} \cdot \nabla 1_{\Omega_s} = 0 \end{array} \right. \quad (27)$$

with :

$$A'_{in} = \int_{\Omega} \rho \boldsymbol{\Phi}'_i \cdot \boldsymbol{\Phi}'_n dx$$

$$B'_{ijn} = - \int_{\Omega} \rho (\boldsymbol{\Phi}'_i \cdot \nabla) \boldsymbol{\Phi}'_j \cdot \boldsymbol{\Phi}'_n dx$$

$$\begin{aligned} C'_{in} &= - \int_{\Omega} \rho [(\bar{\mathbf{u}} \cdot \nabla) \boldsymbol{\Phi}'_i + ((\boldsymbol{\Phi}'_i \cdot \nabla) \bar{\mathbf{u}})] \cdot \boldsymbol{\Phi}'_n dx \\ &\quad - 2 \int_{\Omega} \mu \text{Tr}[\mathbf{D}(\boldsymbol{\Phi}'_i) \mathbf{D}(\boldsymbol{\Phi}'_n)] dx \\ &\quad - 2 \int_{\Gamma_f} \mu \mathbf{D}(\boldsymbol{\Phi}'_i) \boldsymbol{\Phi}'_n \mathbf{n} d\gamma \end{aligned}$$

$$\begin{aligned} D'_n &= - \int_{\Omega} \rho (\bar{\mathbf{u}} \cdot \nabla) \bar{\mathbf{u}} \cdot \boldsymbol{\Phi}'_n dx - 2 \int_{\Omega} \mu \text{Tr}[\mathbf{D}(\bar{\mathbf{u}}) \mathbf{D}(\boldsymbol{\Phi}'_n)] dx \\ &\quad - \int_{\Omega} 1_{\Omega_s} \text{Tr}[\mathbf{D}(\Lambda) \mathbf{D}(\boldsymbol{\Phi}'_n)] dx \end{aligned}$$

$$E'_n = \int_{\Omega} 1_{\Omega_s} f_s \boldsymbol{\Phi}'_n dx$$

where

$$\begin{aligned} \rho &= \rho_f (1 - 1_{\Omega_s}) + \rho_s 1_{\Omega_s}, \\ \mu &= \mu_f (1 - 1_{\Omega_s}) + \mu_s 1_{\Omega_s}, \end{aligned}$$

and Λ is the Lagrange multiplier.

Appendix B. Multiphase formulation for deformable structure with small deformations

The case of a domain containing a fluid and a solid (with a linear elastic behavior) is considered. The aim is to propose a monolithic formulation of the system. Small deformations of the solid are superposed by large displacements of a rigid solid. The extension to large deformations and large displacements of the solid are considered in Favrie et al. (2009).

The solid is first considered as a structure with viscoelastic characteristics. As Hachem et al. (2010) and El Feghali et al. (2010) propose, one can write a monolithic formulation of Navier–Stokes equations in Ω . Hachem et al. (2010) and El Feghali et al. are interested by this monolithic formulation in the framework of finite–element models.

If one considers the equation governing the fluid domain, one gets the classical incompressible Navier–Stokes equations:

$$\left\{ \begin{array}{l} \rho_f \frac{\partial \mathbf{u}_f}{\partial t} + \rho_f (\mathbf{u}_f \cdot \nabla) \mathbf{u}_f - \nabla \cdot \boldsymbol{\sigma}_f = \mathbf{f}_f \text{ in } \Omega_f \\ \nabla \cdot \mathbf{u}_f = 0 \text{ in } \Omega_f \end{array} \right. \quad (28)$$

with associated boundary conditions, where ρ_f is the fluid density, p_f the fluid pressure term and $\boldsymbol{\sigma}_f$ the stress tensor in the fluid part, defined by:

$$\boldsymbol{\sigma}_f = -p_f I_d + 2\mu_f \mathbf{D}(\mathbf{u}_f) \quad (29)$$

μ_f is the fluid dynamical viscosity and I_d represents the identity tensor and $\mathbf{D}(\mathbf{u}_f)$ is the deformation rate tensor, itself defined by $\mathbf{D}(\mathbf{u}_f) = \frac{1}{2} (\nabla \mathbf{u}_f + \nabla^T \mathbf{u}_f)$.

The solved equation in the solid for \mathbf{u}_s with $\mathbf{u}_s(t) = \frac{\partial \mathbf{d}}{\partial t}$, where \mathbf{d} is the solid displacement, is:

$$\rho_s \frac{\partial \mathbf{u}_s}{\partial t} + \rho_s (\mathbf{u}_s \cdot \nabla \mathbf{u}_s) - \nabla \cdot \sigma_s = \mathbf{f}_s \quad \text{in } \Omega_s \quad (30)$$

ρ_s is the solid density. The solid stress tensor σ_s is defined by:

$$\sigma_s = 2\alpha \mathbf{D}(\mathbf{d}) + \beta \text{Tr}(\mathbf{D}(\mathbf{d})) I_d \quad (31)$$

where α and β are the Lamé constants. This leads to its time derivate form $\dot{\sigma}_s$:

$$\dot{\sigma}_s = 2\alpha \mathbf{D}(\mathbf{u}_s) + \beta \text{Tr}(\mathbf{D}(\mathbf{u}_s)) I_d \quad (32)$$

If we consider the hypothesis of small deformations, we can define the linearized Lagrangian deformation rate tensor as:

$$\mathbf{D}(\mathbf{u}_s) = \frac{1}{2} (\nabla \mathbf{u}_s + \nabla^T \mathbf{u}_s) \quad (33)$$

To Eqs. (28) and (30), we have to add continuity equations for velocity and stress fields (\mathbf{n} the external normal unity vector):

$$\begin{cases} \mathbf{u}_{s|_{\Gamma_i}} = \mathbf{u}_{f|_{\Gamma_i}} \\ \sigma_{s|_{\Gamma_i}} \cdot \mathbf{n} = -\sigma_{f|_{\Gamma_i}} \cdot \mathbf{n} \end{cases} \quad (34)$$

We can choose to rewrite Eq. (32) as:

$$\dot{\sigma}_s = 2\alpha \mathbf{D}(\mathbf{u}_s) - \dot{p}_s I_d \quad (35)$$

with $\dot{p}_s = -\beta \text{Tr}(\mathbf{D}(\mathbf{u}_s)) I_d$ and we note $\dot{\tau} = 2\alpha \mathbf{D}(\mathbf{u}_s)$. By coupling Eqs. (28) and (30) and with the stress tensors definition, we deduce the following total strong formulation:

$$\begin{cases} \rho \frac{\partial \mathbf{u}}{\partial t} + \rho (\mathbf{u} \cdot \nabla \mathbf{u}) - \nabla \cdot (-p I_d + 2\mu_f 1_{\Omega_f} \mathbf{D}(\mathbf{u}) + 1_{\Omega_s} \tau) = \mathbf{f} \quad \text{in } \Omega \\ \nabla \cdot \mathbf{u} + \frac{1}{\kappa} \dot{p}_s = \nabla \cdot \mathbf{u} + \frac{1}{\kappa} \left[\frac{\partial p_s}{\partial t} + \mathbf{u} \nabla p_s \right] = 0 \quad \text{in } \Omega_s \end{cases} \quad (36)$$

where $p = p_f 1_{\Omega_f} + p_s 1_{\Omega_s}$ and $\kappa = 1_{\Omega_s} \beta$, κ represents a compressibility coefficient.

Taking into account Eq. (36), a total weak form of Navier–Stokes equations in Ω reads:

Find $\mathbf{u} \in H(\Omega)$, $p \in L^2(\Omega)$ and $\tau \in L^2(\Omega)^{N \times N}$ such as: $\forall \mathbf{u}^* \in \{\mathbf{v} | \mathbf{v} \in H(\Omega), \mathbf{u} = 0 \text{ on } \partial\Omega \setminus \Gamma_i\}$ and for $q \in L_0^2(\Omega) = \{r \in L^2(\Omega) | \int_{\Omega} r dx = 0\}$:

$$\begin{cases} \int_{\Omega} \rho \frac{\partial \mathbf{u}}{\partial t} \mathbf{u}^* dx + \int_{\Omega} (\mathbf{u} \cdot \nabla \mathbf{u}) \cdot \mathbf{u}^* dx - \int_{\Omega} p \nabla \cdot \mathbf{u}^* - 2 \int_{\Omega} \mu_f 1_{\Omega_f} \mathbf{D}(\mathbf{u}) : \mathbf{D}(\mathbf{u}^*) dx \\ \quad - \int_{\Omega} 1_{\Omega_s} \tau : \mathbf{D}(\mathbf{u}^*) dx = \int_{\Omega} \mathbf{f} \mathbf{u}^* dx \\ \int_{\Omega} \nabla \cdot \mathbf{u} q dx + \int_{\Omega} \frac{1}{\kappa} \left[\frac{\partial p_s}{\partial t} + \mathbf{u} \nabla p_s \right] q dx = 0 \end{cases} \quad (37)$$

El Feghali et al. (2010) choose to introduce a viscosity μ_s in the solid as a penalization term. Thus, this equation becomes:

$$\begin{cases} \int_{\Omega} \rho \frac{\partial \mathbf{u}}{\partial t} \mathbf{u}^* dx + \int_{\Omega} (\mathbf{u} \cdot \nabla \mathbf{u}) \cdot \mathbf{u}^* dx - \int_{\Omega} p \nabla \cdot \mathbf{u}^* - 2 \int_{\Omega} \mu \mathbf{D}(\mathbf{u}) : \mathbf{D}(\mathbf{u}^*) dx \\ \quad - \int_{\Omega} 1_{\Omega_s} \tau : \mathbf{D}(\mathbf{u}^*) dx = \int_{\Omega} \mathbf{f} \mathbf{u}^* dx \\ \int_{\Omega} \nabla \cdot \mathbf{u} q dx + \int_{\Omega} \frac{1}{\kappa} \left[\frac{\partial p_s}{\partial t} + \mathbf{u} \nabla p_s \right] q dx = 0 \end{cases} \quad (38)$$

where $\mu = \mu_s 1_{\Omega_s} + \mu_f (1 - 1_{\Omega_s})$. In the case of the POD, trial functions \mathbf{u}^* are the POD modes. Global velocity and pressure fields are decomposed along space and time as:

$$\begin{cases} \mathbf{u}(\mathbf{x}, t) = \sum_{n=1}^N a_n(t) \Phi_n(\mathbf{x}) \\ p(\mathbf{x}, t) = \sum_{m=1}^M b_m(t) \Psi_m(\mathbf{x}) \end{cases} \quad (39)$$

where Φ_n, Ψ_m are elements of POD basis respectively for the velocity and the pressure fields for each n and each m , and $a_n(t), b_m(t)$ are time coefficients. The final low-order dynamical system is the following, for each $\Phi_i, i = 1, \dots, N$ and each $\Psi_i, i = 1, \dots, M$:

$$\begin{cases} \sum_{n=1}^N \frac{da_n}{dt} A_{ni} + \sum_{n=1}^N \sum_{l=1}^N a_n a_l C_{nli}^u - \sum_{m=1}^M b_m B_{1,mi}^p - 2 \sum_{n=1}^N a_n B_{1,ni}^u \\ -2 \sum_{n=1}^N \int_0^t a_n(s) ds B_{2,mi}^u = E_i \quad \text{in } \Omega \end{cases} \quad (40a)$$

$$\sum_{n=1}^N a_n B_{2,ni}^p + \sum_{m=1}^M \frac{db_m}{dt} B_{mi}^k + \sum_{n=1}^N \sum_{m=1}^M a_n b_m C_{nmi}^p = 0 \quad (40b)$$

with the system coefficients:

$$A_{ni} = \int_{\Omega} \rho \Phi_n \cdot \Phi_i dx \quad C_{nli}^u = \int_{\Omega} (\Phi_n \cdot \nabla \Phi_l) \cdot \Phi_i dx$$

$$B_{1,mi}^p = \int_{\Omega} \Psi_m \nabla \cdot \Phi_i dx \quad B_{1,ni}^u = \int_{\Omega} \mu \mathbf{D}(\Phi_n) : \mathbf{D}(\Phi_i) dx$$

$$B_{2,mi}^u = \int_{\Omega} \alpha \mathbf{1}_{\Omega_s} \mathbf{D}(\Phi_n) : \mathbf{D}(\Phi_i) dx \quad E_i = \int_{\Omega} f \Phi_i dx$$

$$B_{2,ni}^p = \int_{\Omega} (\nabla \cdot \Phi_n) \cdot \Psi_i dx \quad B_{mi}^k = \int_{\Omega} \frac{1}{\kappa} \Psi_m \cdot \Psi_i dx$$

$$C_{nmi}^p = \int_{\Omega} \frac{1}{\kappa} (\Phi_n \cdot \nabla \Psi_m) \cdot \Psi_i dx$$

Taking into account the viscoelastic characteristic of the solid, this formulation has the advantage to offer a quasi-classical Navier–Stokes dynamical system to solve, with only a penalization term for the solid viscosity, and the introduction of τ leads to an integro-differential equation.

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