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# High-temperature thermochemical energy storage based on redox reactions using Co-Fe and Mn-Fe mixed metal oxides

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## A B S T R A C T

### Keywords:

Metal oxide  
Thermal heat storage  
Solid-gas reaction  
Reduction  
Oxidation  
Thermodynamic equilibrium calculations

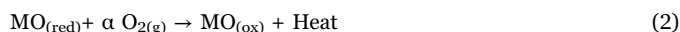
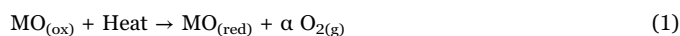
Metal oxides are potential materials for thermochemical heat storage via reversible endothermic/exothermic redox reactions, and among them, cobalt oxide and manganese oxide are attracting attention. The synthesis of mixed oxides is considered as a way to answer the drawbacks of pure metal oxides, such as slow reaction kinetics, loss-in-capacity over cycles or sintering issues, and the materials potential for thermochemical heat storage application needs to be assessed. This work proposes a study combining thermodynamic calculations and experimental measurements by simultaneous thermogravimetric analysis and calorimetry, in order to identify the impact of iron oxide addition to Co and Mn-based oxides. Fe addition decreased the redox activity and energy storage capacity of  $\text{Co}_3\text{O}_4/\text{CoO}$ , whereas the reaction rate, reversibility and cycling stability of  $\text{Mn}_2\text{O}_3/\text{Mn}_3\text{O}_4$  was significantly enhanced with added Fe amounts above ~15 mol%, and the energy storage capacity was slightly improved. The formation of a reactive cubic spinel explained the improved re-oxidation yield of Mn-based oxides that could be cycled between bixbyite and cubic spinel phases, whereas a low reactive tetragonal spinel phase showing poor re-oxidation was formed below 15 mol% Fe. Thermodynamic equilibrium calculations predict accurately the behavior of both systems. The possibility to identify other suitable mixed oxides becomes conceivable, by enabling the selection of transition metal additives for tuning the redox properties of mixed metal oxides destined for thermochemical energy storage applications.

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## 1. Introduction

The purpose of thermal energy storage (TES) in solar thermal power plants is to store solar heat in the form of sensible, latent or chemical energy during on-sun hours and then to use it during off-sun hours in order to match a variable electricity demand with an intermittent energy source supply, thus enabling energy production according to needs and enhancing energy generation dispatchability [1]. This study focuses on thermochemical heat storage, which shows advantages over latent and sensible heat storage, including higher energy storage densities, possible heat storage at room temperature in the form of stable solid materials, and long term storage in a broad temperature range (400–1200 °C) with heat released at a constant restitution temperature defined by the reaction equilibrium. Concentrated solar power (CSP) provides the heat source required for endothermic/exothermic reversible reactions involved in thermochemical energy storage (Eqs. (1) and (2)) in order to store solar energy in the form of chemical bonds. When combined with CSP systems, the continuous production of electricity in thermal power plants becomes

possible. The reaction enthalpy is stored in the reaction products during the heat charge (Eq. (1)), and can be released by reversing the reaction during the discharge (Eq. (2)).

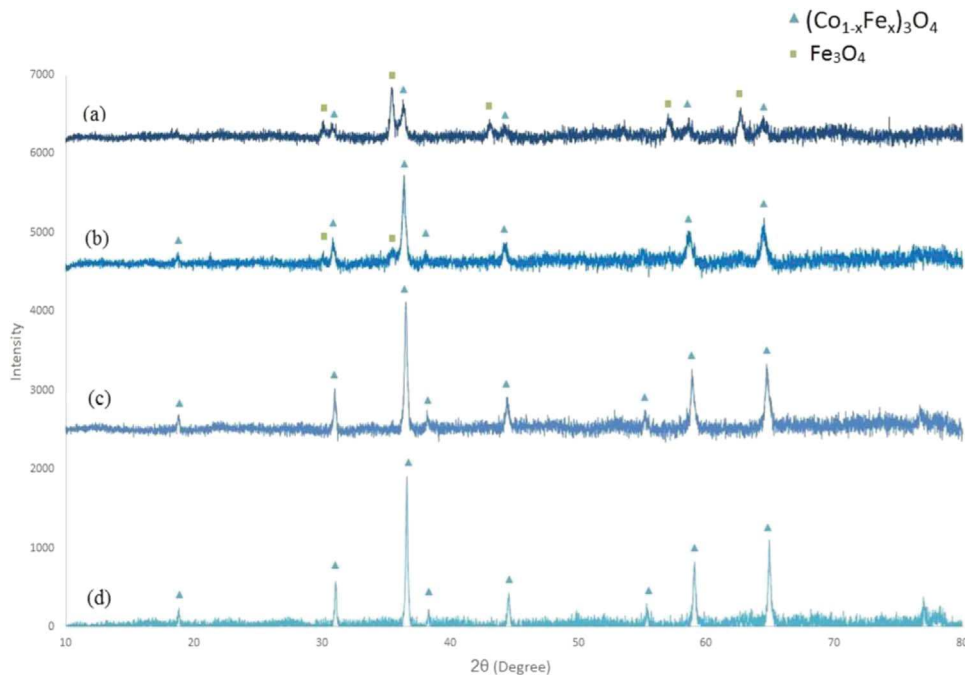


An advantage of using metal oxides as TES materials is the use of air as the heat transfer fluid that can be processed in an open-loop system. Such thermochemical systems are suitable for application in high-temperature solar power plants based on central air receiver (pressurized air-based solar tower receivers for power generation via gas turbines). Cobalt oxide ( $\text{Co}_3\text{O}_4$ ) and manganese oxide ( $\text{Mn}_2\text{O}_3$ ), which reduce into CoO and  $\text{Mn}_3\text{O}_4$  respectively, are among the most studied metal oxides considered as promising materials for thermochemical energy storage. Experiments showed that  $\text{Co}_3\text{O}_4$  is the most suited raw material given the fast reaction kinetics, complete reaction reversibility and cycling stability with a measured gravimetric energy storage density of 576 kJ/kg [2] (while reported theoretical enthalpy is

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**Fig. 1.** XRD analysis of fresh synthetic  $\text{Co}_3\text{O}_4$  with (a) 40 mol% Fe, (b) 25 mol% Fe, (c) 10 mol% Fe, and (d) 5 mol% Fe.

844 kJ/kg [3–6]). However, the cost and potential toxicity of cobalt oxide may require the development of other alternative materials. The reduction step of  $\text{Mn}_2\text{O}_3$  was observed in the range of 920–1000 °C, with notably slow re-oxidation in the range of 850–500 °C, with a reported gravimetric energy storage density of 110–160 kJ/kg [7,8] and a theoretical enthalpy of 202 kJ/kg [8]. The re-oxidation usually happens in two steps, the first one being during the cooling and in between 700 °C and 500 °C and the second one being during the re-heating and in the range of 500–850 °C [9] because of strong kinetic limitations. In order to complete the slow re-oxidation during the cooling step, it needs to last long enough by decreasing drastically the cooling rate.

Optimization of materials reactivity is generally required for metal oxide species by using e.g. doping strategies, controlled synthesis techniques for tailored morphology, or stabilization with inert materials to alleviate sintering effects. Improvement of materials properties and flexibility such as reaction kinetics and reaction temperature tuning can be obtained by the addition of dopants. In the specific case of the  $\text{Mn}_2\text{O}_3/\text{Mn}_3\text{O}_4$  cycle, the doping with transition metals is an option to relieve the slow re-oxidation issue [2,4].

The present study aims at investigating the effect of Fe addition on the performances of Co and Mn metal oxides, which have been identified as interesting candidates for TES [10]. The optimal mixed metal oxide composition to reach the highest performances for TES is addressed, encompassing high reaction enthalpy, stability upon cycling, low temperature gap between reduction and re-oxidation, and reaction in a temperature range adapted to CSP. The addition of transition metals is investigated as a way to answer the drawbacks of simple metal oxides, including slow reaction kinetics [5], sintering [11], loss-in-capacity over cycles [8], etc. Block et al. [2] reported that both addition of iron to cobalt oxide or addition of cobalt to iron oxide results in lower enthalpies of reaction compared to those of the pure oxides. However, they estimated that cobalt oxide doped with 10% of iron possesses higher reduction/oxidation reversibility than pure cobalt oxide and still shows high enthalpy of reaction. Pagkoura et al. [9] showed that cobalt oxide with 10–20 wt% of iron shows good thermo-mechanical stability over ten redox cycles. Carrillo et al. [11] showed that the addition of iron does not allow avoiding the sintering encountered with  $\text{Mn}_2\text{O}_3$  but helps to increase the heat storage density

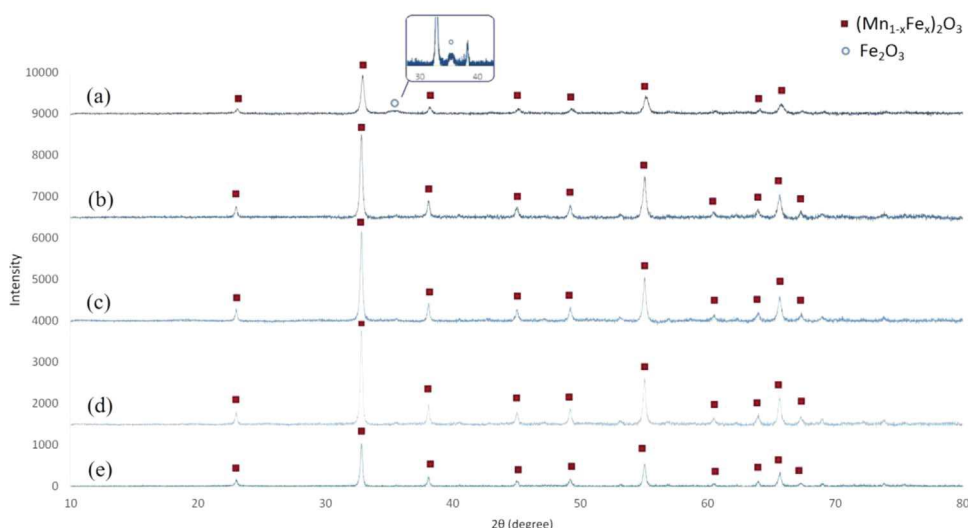
of the material. Furthermore, the addition of iron helped to stabilize and enhance the oxidation rate of manganese oxide over thirty redox cycles. According to their study, the fastest and most stable oxidation reaction was obtained for  $\text{Mn}_2\text{O}_3$  doped with 20 mol% Fe. In another study, the authors also considered Fe-Cu co-doping in manganese oxide and showed that the incorporation of Cu diminished the reduction temperature, whereas the incorporation of Fe increased the oxidation temperature [12].

Recent models provide thermodynamic descriptions of the Co-Fe-O [13,14] and Mn-Fe-O [15,16] systems, based on exhaustive studies of available experimental data. In the present work, some of these models were used to calculate the nature and composition of solid phases at equilibrium, the oxygen storage capacity (equal to the mass loss during reduction), the transition temperature, and the reaction enthalpy of Co-Fe and Mn-Fe mixed oxides, with Fe content up to 50 mol%. Equilibrium calculations were compared to experimental (thermogravimetric and calorimetric) measurements carried out with various oxide compositions, under 20% $\text{O}_2$ /Ar atmosphere, in the 750–1050 °C temperature range. The combination of experimental data and thermodynamics aims at providing a better understanding of the behavior of the mixed oxides and defining the optimal composition.

## 2. Materials and methods

### 2.1. Synthesis and characterization

Pure  $\text{Co}_3\text{O}_4$  and cobalt oxide mixed with 5, 10, 25, and 40 mol% Fe as well as pure  $\text{Mn}_2\text{O}_3$  and manganese oxide mixed with 10, 15, 20, 30, 40 and 50 mol% Fe were synthesized. In the following, the oxides compositions are either noted  $x(\text{Fe})$  or mol% Fe, referring to the molar content of Fe on metal basis (based on a  $\text{Fe}/(\text{Fe}+\text{Co})$  and  $\text{Fe}/(\text{Fe}+\text{Mn})$  mole ratio). All the powders were synthesized via a modified Pechini method [2], using metal nitrates (> 98% purity), citric acid (> 99% purity) and ethylene glycol (> 99% purity) in aqueous solution. The solution was heated up until obtaining a viscous solution. The powders were then calcined in air at 200 °C for 2 h and at 750 °C for 4 h in order to fully eliminate the organic fraction and residues of the synthesis, and to stabilize the structure. Higher calcination temperatures were not considered to avoid the reduction of the materials during the synthesis.



**Fig. 2.** XRD analysis of fresh synthetic  $\text{Mn}_2\text{O}_3$  with (a) 50 mol% Fe, (b) 40 mol% Fe, (c) 30 mol% Fe, (d) 20 mol% Fe, and (e) 10 mol% Fe.

The powders were characterized by X-ray diffraction (XRD) before being studied in redox cycles. XRD analysis was performed (Figs. 1 and 2, SI1, SI2) at room temperature using a PANalytical XPert Pro diffractometer (CuK $\alpha$  radiation,  $\lambda = 0.15418$  nm). X-ray diffraction measurements of  $\theta$ - $\theta$  symmetrical scans were made over an angular range of 10–80°. The step size and the time per step were fixed at 0.01° and 20 s, respectively. The contribution from K $\alpha_2$  was removed and the X-ray diffractograms were recorded and studied using the PANalytical software. The instrumental function was determined using a reference material (SRM 660, lanthanum hexaboride, LaB $_6$  polycrystalline sample) and can be expressed by a polynomial function [17]. The synthesized oxide phases were corresponding to the structures of (i) a cubic spinel solution ( $\text{Co}_{1-x}\text{Fe}_x$ ) $_3\text{O}_4$  (Fig. 1) and (ii) a bixbyite solution ( $\text{Mn}_{1-x}\text{Fe}_x$ ) $_2\text{O}_3$  [18] (Fig. 2), with traces of iron oxide only detected for the materials containing the largest amount of iron (Figs. 1a and b, and 2a). Above 20 mol% Fe added to  $\text{Co}_3\text{O}_4$ , the material is no longer a single spinel phase but a mixture of two spinels.

The morphology of the synthesized ( $\text{Mn}_{1-x}\text{Fe}_x$ ) $_2\text{O}_3$  phase was also characterized (Fig. SI3) by SEM (FESEM, HITACHI S4800). The very porous structure obtained with the Pechini method can be observed in  $\text{Mn}_2\text{O}_3$  samples synthesized with no iron (Fig. SI3a and b). The porous structure is still present with the addition of iron during the synthesis; however, the porosity reduces with increasing iron content. The sample with 10 mol% Fe (Fig. SI3c and d) still resembles the pure  $\text{Mn}_2\text{O}_3$  sample, while the sample with 50 mol% Fe appears different (Fig. SI3e and f), with thicker necks forming the pore walls. This change in morphology does not alter the reactivity, as evidenced in the experimental section.

## 2.2. Experimental procedure for thermochemical redox cycling

Experimental data concerning transition temperatures during redox process, oxygen storage capacity and reaction enthalpies were obtained by coupled thermogravimetric analysis (TGA) and differential scanning calorimetry (DSC), using a Netzsch STA 449 F3 System. About 50 mg of powder was placed into an alumina crucible and then subjected to simultaneous thermal analysis (STA) consisting of TGA coupled with DSC.

Reduction-oxidation cycles were performed in a 20%  $\text{O}_2/\text{Ar}$  atmosphere (10 N mL/min  $\text{O}_2$  and 40 N mL/min Ar), between 800 °C and 1050 °C for cobalt based oxides and between 750 °C and 1050 °C for manganese based oxides. Each run also included a last reduction step under Ar (99.999% purity), in order to get information about the reduction temperature of the material under inert atmosphere. The

heating rate was 20 °C/min for the reduction step, and the cooling rate was 10 °C/min for the re-oxidation step. For some runs with cobalt based oxides, the temperature was maintained for 15 min at 1050 °C and at 800 °C for achieving the state of reaction equilibrium. For all the materials, a series of three cycles was performed for each studied formulation in order to determine their suitability for achieving reversible reactions and to assess a possible chemical deactivation of the materials as a result of a loss of redox stability during thermal treatment.

## 2.3. Thermodynamic calculations

Equilibrium calculations were performed with the FactSage 7.0 software [19] and the FToxid database, which includes models of the thermochemical properties of the oxide phases in Fe-Co-O [13] and Fe-Mn-O [15] systems. For calculations in the Fe-Co-O system, the following solid phases were considered: the  $\text{Fe}_2\text{O}_3$  compound, the cubic spinel solution ( $\text{Co}_{1-x}\text{Fe}_x$ ) $_3\text{O}_4$  (C-Spin) and the monoxide solution ( $\text{Co}_{1-x}\text{Fe}_x$ ) $\text{O}_{1+y}$  (Monoxide). For the Fe-Mn-O systems, four phases were considered: two spinel solutions ( $\text{Mn}_{1-x}\text{Fe}_x$ ) $_3\text{O}_4$ , one with cubic structure (C-Spin) and the other with tetragonal structure (T-Spin), the bixbyite solution ( $\text{Mn}_{1-x}\text{Fe}_x$ ) $_2\text{O}_3$  (Bixb) and the corundum solution ( $\text{Fe}_{1-x}\text{Mn}_x$ ) $_2\text{O}_3$  (Cor). The monoxide and spinel solid solutions were described within the framework of the Compound Energy Formalism [20], with two and three ionic sublattices, respectively (see [13,15] for more details). The bixbyite and corundum phases were modelled as a random mixture of the two end-members ( $\text{Fe}_2\text{O}_3$  and  $\text{Mn}_2\text{O}_3$ ), with no interaction parameter [15]. Two gaseous components,  $\text{O}_2$  and Ar, were taken into account, with ideal mixing properties. The total pressure was always 1 atm.

For both systems, two kinds of calculations were carried out: (i) plot of phase diagrams, (ii) system equilibrium at various compositions and temperatures, providing, for each composition and at each temperature step, the phase assemblage and the cationic distribution in each solution phases, as well as the total enthalpy of the system.

The second type of calculations gives access to the theoretical mass loss (i.e. oxygen storage capacity),  $\Delta m$ , as defined by (Eq. (3)). This quantity is directly comparable to the mass change measured by TGA.

$$\Delta m (\%) = 100 \cdot \frac{\text{mass of solid at } T_{\max} - \text{mass of solid at } T_{\min}}{\text{mass of solid at } T_{\min}} \quad (3)$$

where  $T_{\min}$  and  $T_{\max}$  are referring to the minimal and maximal temperature of the thermochemical cycle.

The enthalpy of the reduction reaction (Eq. (1)),  $\Delta_r H$ , was

calculated according to (Eq. (4)). This quantity is compared to the heat of reaction determined by DSC analysis. For reactions occurring on a large temperature range (see Section 3), this calculation includes a contribution due to the calorific capacity of the compounds (sensible heat), which leads to an overestimation of the enthalpy strictly related to the reaction.

$$\Delta_r H \text{ (kJ/kg of } s^0) = \frac{1}{m_s^0} [m_s^1 H^{s^1}(T_{end}) + m_s^2 H^{s^2}(T_{end}) + m_{O_2} H^{O_2}(T_{end})] - H^s(T_{beg}) \quad (4)$$

where  $T_{end}$  is the temperature ( $^{\circ}\text{C}$ ) at the end of the phase transition or the maximal temperature of the cycle;  $T_{beg}$  is the temperature ( $^{\circ}\text{C}$ ) at the beginning of the phase transition;  $m_s^0$  is the mass (kg) of the solid phase at  $T_{min}$ ;  $m_s^1$  and  $m_s^2$  are the mass (kg) of the solid phases at  $T_{end}$ ;  $m_{O_2}$  is the mass (kg) of dioxygen at  $T_{end}$ ;  $H^s(T)$  is the enthalpy (kJ/kg) of the compound  $x$  at the temperature  $T$ .

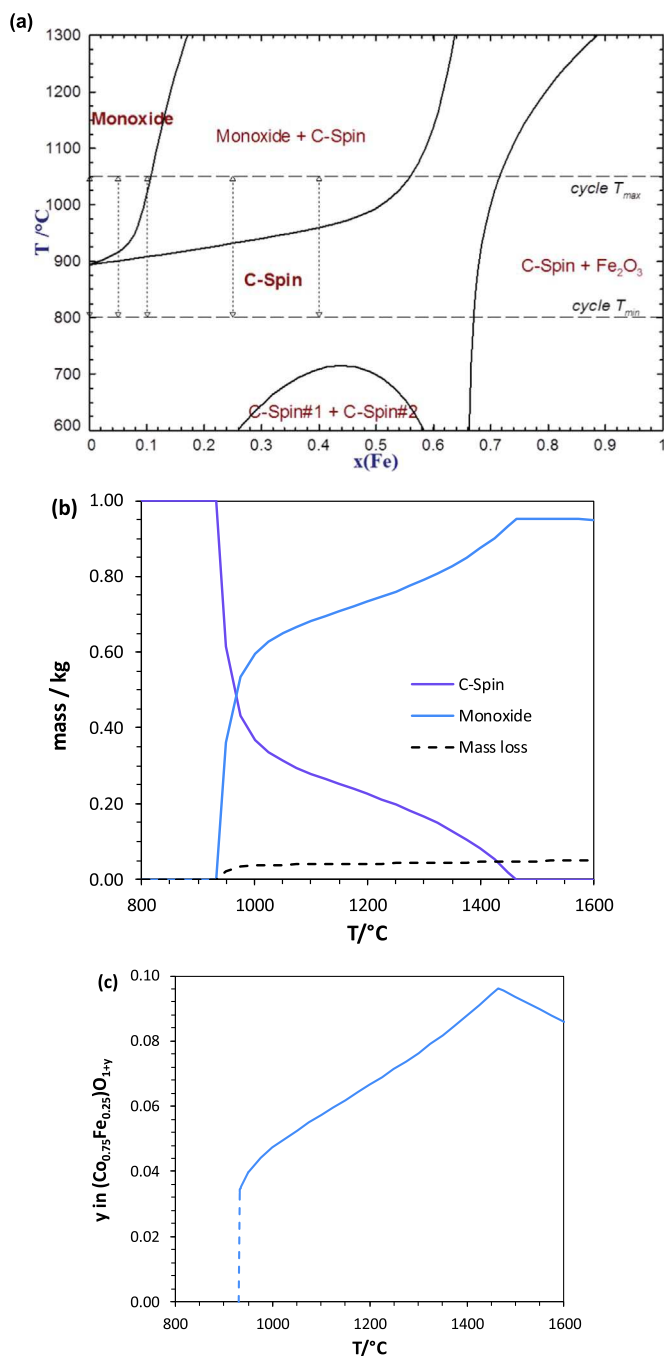
### 3. Results and discussion

#### 3.1. Cobalt-based mixed oxides

The calculated Co-Fe-O phase diagram for  $p_{O_2} = 0.20$  atm is presented in Fig. 3a. It shows that, at equilibrium, the iron content greatly influences the composition and the amount of the monoxide phase formed at  $1050$   $^{\circ}\text{C}$  when heating the spinel phase from  $800$   $^{\circ}\text{C}$ . For small Fe additions ( $0 < x(\text{Fe}) < 0.1$ ), the spinel phase is fully converted into the monoxide phase. At very high Fe content ( $x(\text{Fe}) > 0.6$ ), there is no phase transition achievable below  $1200$   $^{\circ}\text{C}$ , which is the upper temperature limit usually considered for TES applications. For intermediate Fe content ( $0.1 < x(\text{Fe}) < 0.6$ ), an increasing proportion of spinel phase is not converted into monoxide. As an example, Fig. 3b presents the influence of the temperature on the phases amount for  $x(\text{Fe}) = 0.25$ . A temperature of about  $1460$   $^{\circ}\text{C}$  is required to fully convert the spinel phase into the monoxide phase. Furthermore, as illustrated in Fig. 3c for  $x(\text{Fe}) = 0.25$ , the monoxide phase ( $\text{Co}_{1-x}\text{Fe}_x\text{O}_{1+y}$ ) presents a noticeable over-stoichiometry ( $y$ ) in oxygen, which increases with temperature.

The TGAs of cobalt-based oxides are presented in Figs. 4 and 5 with different temperature programs. A first observation is that a noticeable change in the re-oxidation onset temperature (Fig. S14) is measured between the samples with 0–10 mol% Fe (Figs. 4b–c, 5c–e) and with 25–40 mol% Fe (Figs. 4a, 5a–b). Indeed, the re-oxidation step starts at the beginning of the temperature decrease (i.e.  $1050$   $^{\circ}\text{C}$ ) for the samples containing 25 mol% Fe and 40 mol% Fe, which is in line with the phase diagram (Fig. 3a) since the two-phase equilibrium strongly depends on the temperature. The Co-Fe samples were kept in a reduced state after TGA (final cooling step in Ar to avoid re-oxidation in Fig. 5) and analysed via XRD (Fig. S11). Phase identification confirmed the presence of the single monoxide phase for low Fe contents (0 and 5 mol %), whereas the samples consisted of a mixture of monoxide and spinel phases for higher Fe contents (10–40 mol%), in agreement with the calculated phase diagram.

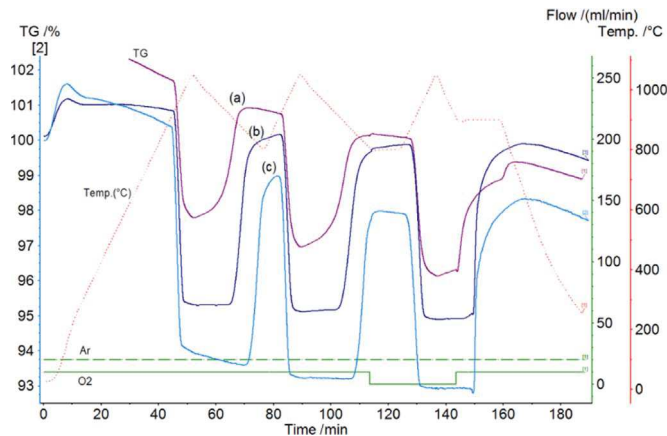
The influence of Fe incorporation on reaction temperatures is reported in Fig. 6 (Fig. S14 compares data under Ar and 20% $\text{O}_2$ /Ar atmosphere). Both temperatures at peak reaction rate (i.e. temperatures at which the reaction kinetics reached its maximum, Fig. 6) and onset temperatures (Fig. S14) were measured. The measured onset temperature for reduction of  $\text{Co}_3\text{O}_4$  to  $\text{CoO}$  is about  $920$   $^{\circ}\text{C}$ , which is in good accordance with previous studies carried out in air atmosphere, reporting temperatures ranging from  $880$  to  $930$   $^{\circ}\text{C}$  [6,7,9,21]. A gradual increase of the reduction and oxidation temperatures is observed with increasing amount of iron in the material, which is consistent with the phase diagram (Fig. 3a). An effect of Fe addition on the temperature gap between reduction and oxidation is also evi-



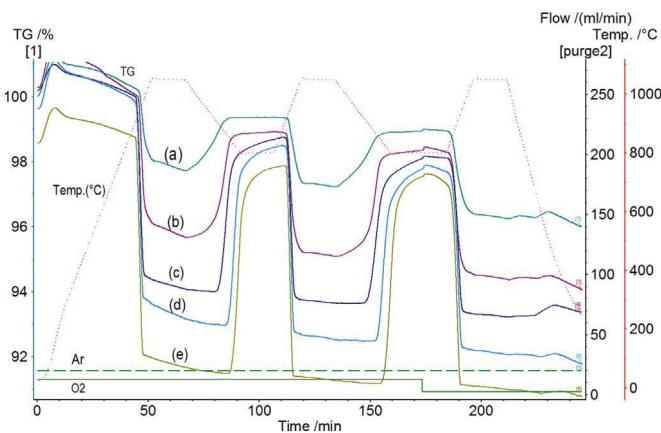
**Fig. 3.** (a) Calculated Co-Fe-O phase diagram at  $p_{O_2} = 0.20$  atm, (b) calculated temperature evolution of the mass of solid phases for  $x(\text{Fe}) = 0.25$ , (c) calculated temperature evolution of oxygen over-stoichiometry ( $y$ ) in the monoxide phase ( $\text{Co}_{0.75}\text{Fe}_{0.25}\text{O}_{1+y}$ ).

denced. Indeed, as both temperatures rise with Fe addition, it can be noticed that the gap between the reduction and oxidation temperatures reduces. For 40 mol% Fe, the onset temperature for reduction has increased by  $50$   $^{\circ}\text{C}$  compared to pure  $\text{Co}_3\text{O}_4$ , while the onset temperature for oxidation has increased by  $90$   $^{\circ}\text{C}$ . The reduction of this temperature gap is an asset for large-scale applications since it reduces the amount of energy spent for the heating and cooling of the system between the charge and the discharge steps. However, an increase in the oxidation temperature may also be a disadvantage if the system must be externally heated to initiate the oxidation (in case the material is stored in reduced form at room temperature).

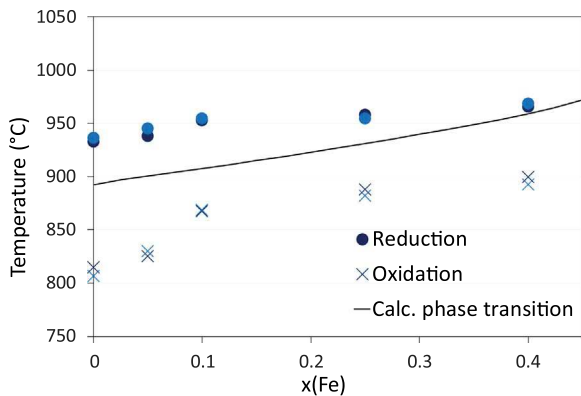
In Fig. 7 are reported, along with the calculated equilibrium values,



**Fig. 4.** TGA of  $\text{Co}_3\text{O}_4/\text{CoO}$  with addition of (a) 25 mol% Fe, (b) 10 mol% Fe, (c) 5 mol% Fe, including a final re-oxidation step under 20%  $\text{O}_2/\text{Ar}$  at the end.



**Fig. 5.** TGA of  $\text{Co}_3\text{O}_4/\text{CoO}$  with addition of (a) 40 mol% Fe, (b) 25 mol% Fe, (c) 10 mol% Fe, (d) 5 mol% Fe, (e) no Fe added, ending on a final reduction step under Ar.

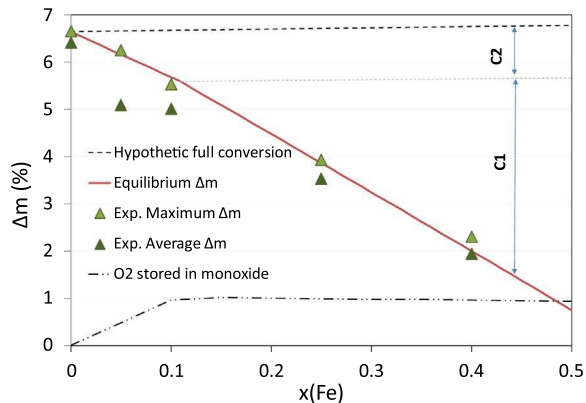


**Fig. 6.** Experimental temperatures at peak reaction rate for cobalt-based oxides in 20%  $\text{O}_2/\text{Ar}$  and comparison with the calculated temperature of the C-Spin/Monoxide transition.

the maximum values of  $\Delta m$  measured for each oxide composition, which means the highest amount of  $\text{O}_2$  released during reduction, and the average  $\Delta m$  for the three redox cycles. The hypothetical case of a full conversion of the initial spinel into a stoichiometric monoxide, calculated according to (Eq. (5)), is also plotted in Fig. 7.

$$(\text{Co}_{1-x}\text{Fe}_x)_3\text{O}_{4(s)} = 3(\text{Co}_{1-x}\text{Fe}_x)\text{O}_{(s)} + 0.5\text{O}_2(\text{g}) \quad (5)$$

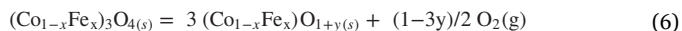
Measurements of the  $\Delta m$  values clearly show that increasing the amount of iron in the material reduces the amount of  $\text{O}_2$  it is able to release at a given temperature. Furthermore, the maximum  $\Delta m$  values are in excellent accordance with equilibrium calculations, which



**Fig. 7.** Average and maximal experimental mass loss ( $\Delta m$  in %) of the Co-Fe mixed oxide between 800 °C and 1050 °C compared to  $\Delta m$  at thermodynamic equilibrium.

implies that a full conversion has been reached.

According to the thermodynamic model, the decrease in  $\text{O}_2$  storage capacity with increasing Fe content is due to a combination of two factors. First, as evidenced by the phase diagram and the temperature profile for  $x(\text{Fe}) = 0.25$  (Fig. 3b), the upper temperature limit of 1050 °C does not lead to a full conversion of the spinel phase when  $x(\text{Fe}) > 0.10$ . This contribution is represented as C1 in Fig. 7. It does not account for the decrease in  $\Delta m$  evidenced for  $x(\text{Fe}) = 0.05$  and 0.10 (C2 in Fig. 7), which should be closer to the mass loss calculated according to (Eq. (5)) since a full conversion into monoxide occurs. This second factor is linked with the fact that the monoxide solid solution becomes non stoichiometric with the incorporation of Fe (Fig. 3c). This leads to a residual storage of oxygen in the monoxide phase, according to (Eq. (6)):

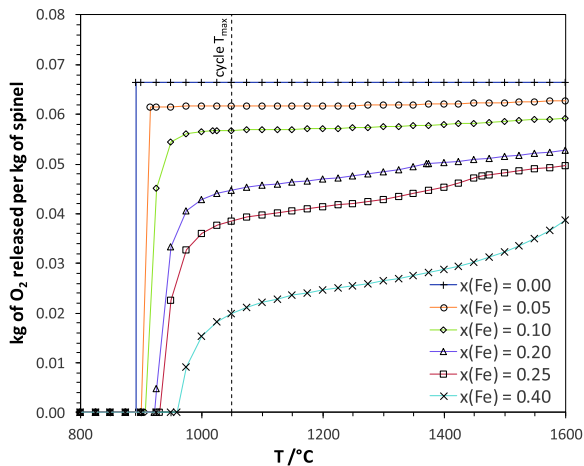


where  $y$  is the over-stoichiometry of oxygen in the monoxide phase.

As illustrated in Fig. 7, the calculated contribution of the oxygen over-stoichiometry in the monoxide phase at 1050 °C accounts for a loss of storage capacity of about 1% per unit mass of spinel when  $x(\text{Fe}) > 0.10$ , as compared to a maximum capacity of 6.6% for pure cobalt oxide.

As for the cycling stability, for pure  $\text{Co}_3\text{O}_4$ , the average  $\Delta m$  is the same as both the theoretical value and the maximum value measured experimentally. This means that the amount of  $\text{O}_2$  released and regained did not change, confirming the good material cycling stability over three cycles, as already reported by several authors [2–7]. For the samples containing 5 and 10 mol% iron, since the average  $\Delta m$  falls slightly below the theoretical and maximum value, a minor loss in  $\text{O}_2$  exchange capacity upon cycling is evidenced. Conversely, the amount of  $\text{O}_2$  exchanged remains stable over cycles for larger Fe contents ( $x(\text{Fe}) > 0.10$ ) at the expense of a decreased oxygen storage capacity. Thus, the cycling stability of cobalt oxide does not suffer from the addition of iron, as the re-oxidation conversion rate is not significantly decreasing over multiple cycles for Co-Fe mixed oxides, similarly to pure  $\text{Co}_3\text{O}_4$ . An additional cycling test was performed with a Co-Fe mixed oxide (10 mol% Fe) subjected to multiple consecutive cycles (12 cycles) in order to demonstrate the stability of the material regarding both oxygen storage capacities and energy storage densities (Fig. S15). This confirms the robustness of the active redox materials and the ability to cycle without deactivation.

Regarding the effect of the gas flow composition, the measured  $\Delta m$  due to the reduction under pure Ar was not significantly different from the one measured with 20%  $\text{O}_2/80\%$  Ar. However, as illustrated by Fig. S14, the reduction onset temperature under Ar was decreased by 60–80 °C, to reach a value of about 860 °C, almost independent of  $x(\text{Fe})$ . These data are rather different from the equilibrium state calculated with the thermodynamic model (Fig. S16). Indeed, under pure Ar, the



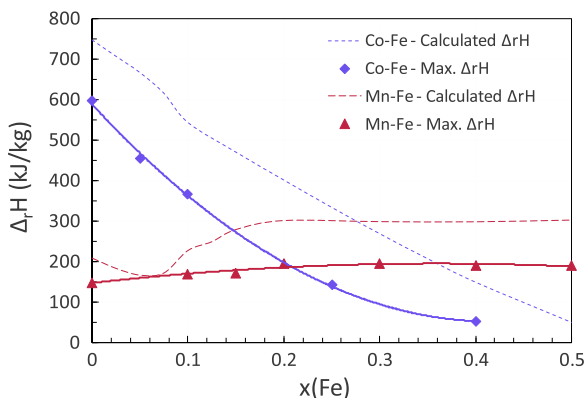
**Fig. 8.** Temperature evolution of the amount (kg) of  $O_2(g)$  released per kg of cobalt-based spinel containing various amounts of Fe.

experimental oxygen partial pressure should be around  $10^{-5}$  atm (10 ppm  $O_2$ ), which corresponds to a transition temperature of about 650–700 °C but it increases with a higher  $p_{O_2}$ . Furthermore, the calculated transition temperature depends noticeably on the composition of the system. It is thus concluded that, with a heating rate of 20 °C/min, the system does not reach equilibrium at low temperature, most likely because of solid-state diffusion limitations. Independently of the system composition, a minimum temperature threshold of about 850 °C is required to achieve the phase transition.

The effect of applying a higher temperature limit than 1050 °C was also estimated, both with experimental measurements and calculations. Cycles with a maximal temperature of 1150 °C were carried out on  $Co_3O_4$  with 5 mol% Fe (Fig. S17). While this sample behaved well with a maximum temperature set at 1050 °C, the heating up to 1150 °C clearly affected its reactivity. Indeed, the sample did not regain the whole mass on cooling (67% average instead of 86% when heating at 1050 °C) and was sintered at the end of the run.

Furthermore, equilibrium calculations show that applying a temperature limit higher than 1050 °C will not increase drastically the oxygen storage capacity of mixed Co-Fe oxides, as illustrated by Fig. 8. Indeed, for Fe contents between 0% and 10%, the oxygen storage capacity is almost constant with temperature, because the non-stoichiometry of the monoxide is stable. For higher Fe contents ( $0.10 < x(Fe) < 0.40$ ), a small increase of the storage capacity is evidenced at high temperature, due to a higher conversion rate of the spinel phase (Fig. 3b), but Fe addition is still detrimental for the total storage capacity.

As reported in Fig. 9, the measured reaction enthalpies are



**Fig. 9.** Experimental and calculated enthalpies of reaction for the Co-Fe and Mn-Fe mixed oxides.

decreasing with increasing amount of Fe: the highest measured enthalpy is 597 kJ/kg for pure  $Co_3O_4$ , while the lowest is 50.7 kJ/kg for  $x(Fe) = 0.40$ . It should be noted that the DSC peaks for  $x(Fe) = 0.40$  are very small, which makes them difficult to analyze. For pure  $Co_3O_4$ , our data is close to the value of 576 kJ/kg obtained by [2] with a similar experimental procedure. As recently discussed in details by Block et al. [22], this kind of DSC measurements, operated in an open reactor at a rather fast heating rate, is not able to reproduce the tabulated enthalpy value, which is commonly reported as 844 kJ/kg [3–6]. To explain the large discrepancy, the authors state that the contribution of a  $Co^{3+}$  spin-state change, associated with an enthalpy of about 222 kJ/kg, is not measured by dynamic techniques.

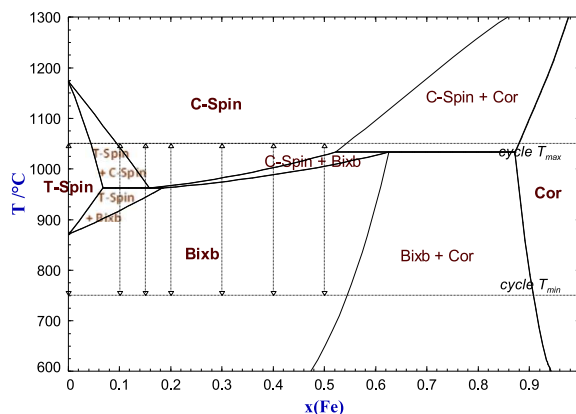
The thermodynamic model used in this study [13], which takes into account the heat capacity anomaly due to spin-state transition of  $Co^{3+}$ , leads to an enthalpy of reaction of 749 kJ/kg for  $x(Fe) = 0$ . This is noticeably lower than the commonly admitted value of 827 kJ/mol [2,22]. For higher Fe contents, the calculations reproduce well the general trend (decrease of  $\Delta_rH$ ) with a systematic gap of about 180 kJ/kg.

In TES application, the enthalpy of the reaction is related to the oxygen storage capacity of the material (the energy stored/released during the reduction/oxidation is related to the reaction extent that corresponds to the quantity of  $O_2$  released/captured). As evidenced by measurements and calculations, the gravimetric energy storage density of mixed oxides is decreased when compared with pure  $Co_3O_4$ , resulting in less storage capacity per gram of material. This observation is in accordance with the work of Block et al. [2], who stated that both pure  $Co_3O_4$  and  $Fe_2O_3$  show higher enthalpies of reaction than any mixture of the two.

In summary, while the  $Co_3O_4/CoO$  redox pair shows very good cycling stability, the addition of iron is shown to slightly affect it and to decrease drastically the overall oxygen storage capacity. According to equilibrium calculations in the Co-Fe-O system, the addition of iron to  $Co_3O_4$  results in a lower amount of  $O_2$  exchanged during cycles and a loss of the reduction reaction enthalpy, due to an incomplete conversion of the spinel phase at 1050 °C and to the formation of a non-stoichiometric monoxide. The addition of iron also increases the reduction and oxidation temperatures, while slightly decreasing the gap in temperature between the reduction and the oxidation step.

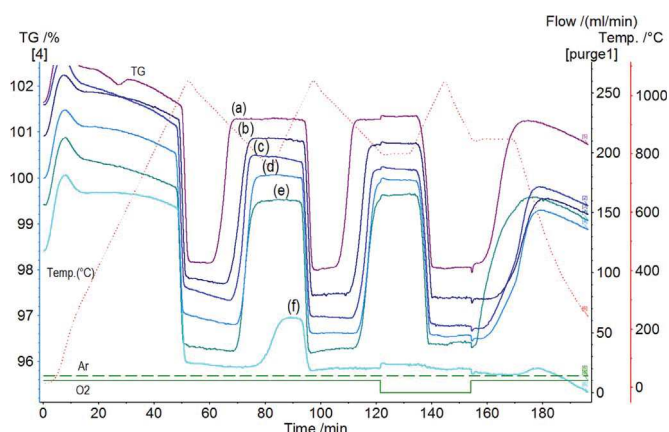
### 3.2. Manganese-based mixed oxides

The calculated Mn-Fe-O phase diagram is presented in Fig. 10, for  $p_{O_2} = 0.20$  atm. Again, the expected behavior of the mixed oxides is strongly dependent on the system composition. At Fe contents above 50%, the requested temperature to reach a full conversion of the initial oxide into a spinel phase is above 1100 °C. At very low Fe contents ( $0 < x(Fe) < 0.05$ ), the stable phase at 1050 °C is the tetragonal spinel. For  $0.05 < x(Fe) < 0.15$ , the transition of bixbyite to cubic spinel goes



**Fig. 10.** Calculated Mn-Fe-O phase diagram at  $p_{O_2} = 0.20$  atm.

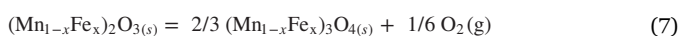




**Fig. 11.** TGA of  $\text{Mn}_2\text{O}_3/\text{Mn}_3\text{O}_4$  with addition of (a) 50 mol% Fe, (b) 40 mol% Fe, (c) 30 mol% Fe, (d) 20 mol% Fe, (e) 15 mol% Fe, and (f) 10 mol% Fe.

through two consecutive two-phase zones (T-Spin+Bixb and T-Spin+C-Spin). Finally, above about 20 mol% Fe, the material transforms almost directly from the bixbyite phase to the cubic spinel.

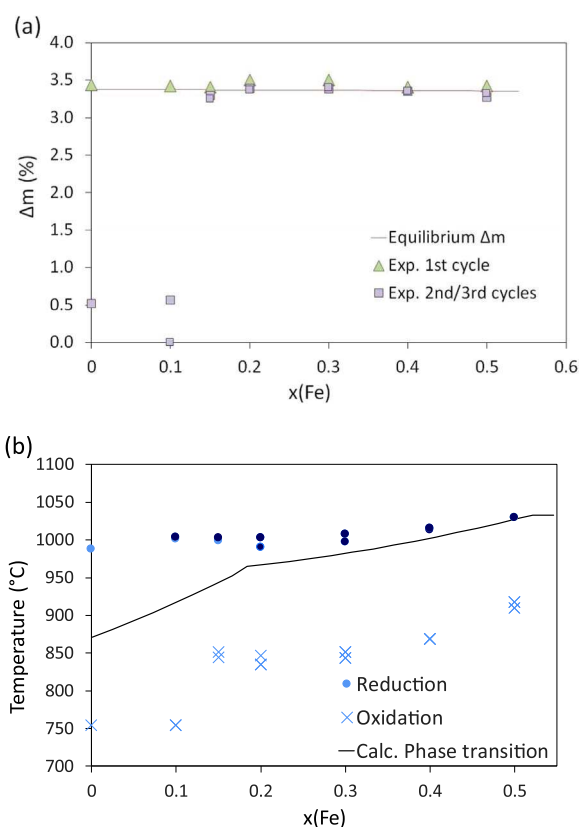
According to the model [15], the non-stoichiometry of the oxide phases should not play a significant role regarding oxygen storage capacity. Indeed, the bixbyite phase ( $\text{Mn}_{1-x}\text{Fe}_x)_2\text{O}_3$  is considered as fully stoichiometric. For the spinel phases T-Spin and C-Spin, a cationic non-stoichiometry is considered in the model, with the presence of cationic vacancies. However, as shown in Fig. S18, the vacancies concentration at 1050 °C is at the most  $1.4 \times 10^{-4}$  mol per mol of Mn + Fe, which leads to a negligible impact on the oxygen storage capacity. In the composition range  $0 < x(\text{Fe}) < 0.5$  considered in this study, the redox cycle is thus represented by:



At equilibrium, according to the model, the theoretical amount of  $\text{O}_2$  exchanged between 750 °C and 1050 °C remains thus the same in the  $0 < x(\text{Fe}) < 0.5$  composition range.

The TGA, presented in Fig. 11, shows that the sample with the composition  $x(\text{Fe}) = 0.10$  is unable to regain its full mass during oxidation, as the mass lost during the first reduction step is not recovered during the re-oxidation step, similarly to the case of pure  $\text{Mn}_2\text{O}_3$  (TGA shown in Fig. S19). Conversely, the other compositions, from 15 mol% Fe to 50 mol% Fe, are regaining their lost mass in a complete reversible way. XRD analysis of Mn-Fe samples after TGA was performed (Fig. S12). The XRD pattern of  $\text{Mn}_2\text{O}_3$  with 10 mol% Fe is identified as a mixture of tetragonal spinel structure and  $\text{Fe}_2\text{O}_3$  (Fig. S12e), which confirms the poor re-oxidation yield of the cycled material. Conversely, the XRD pattern of  $\text{Mn}_2\text{O}_3$  with 20, 30, 40 and 50 mol% Fe after TGA is identified as  $(\text{Mn}_{1-x}\text{Fe}_x)_2\text{O}_3$  (Fig. S12a–d) with  $\text{Fe}_2\text{O}_3$  visible on the sample with the highest amount of Fe added (Fig. S12a), which denotes the complete re-oxidation of the samples after TGA. SEM characterization of the cycled materials compared with the fresh ones reveals sintering regardless of the amount of Fe (Fig. S110), which does not alter the cycling ability of Mn-Fe mixed oxides. Sintering is thus not the cause of the reactivity loss in the case of pure  $\text{Mn}_2\text{O}_3$  and  $\text{Mn}_2\text{O}_3$  mixed with 10 mol% Fe.

Experimental and theoretical mass variations,  $\Delta m$ , were compared. As illustrated in Fig. 12a, all the samples feature the same  $\Delta m$  during the first reduction, in good accordance with the equilibrium calculations summarized by (Eq. (7)). However, pure  $\text{Mn}_2\text{O}_3$  shows cycling stability issues as already evidenced by [8]. This phenomenon is reflected by the drop of the experimental  $\Delta m$  during 2nd and 3rd cycles, showing a decrease of redox activity with redox cycling. Similarly,  $\text{Mn}_2\text{O}_3$  mixed with 10 mol% Fe also loses cycling stability, regaining only 31% of its lost mass (Fig. 11f). From  $x(\text{Fe}) = 0.15$  to 0.50, a great improvement is evidenced, since the experimental  $\Delta m$

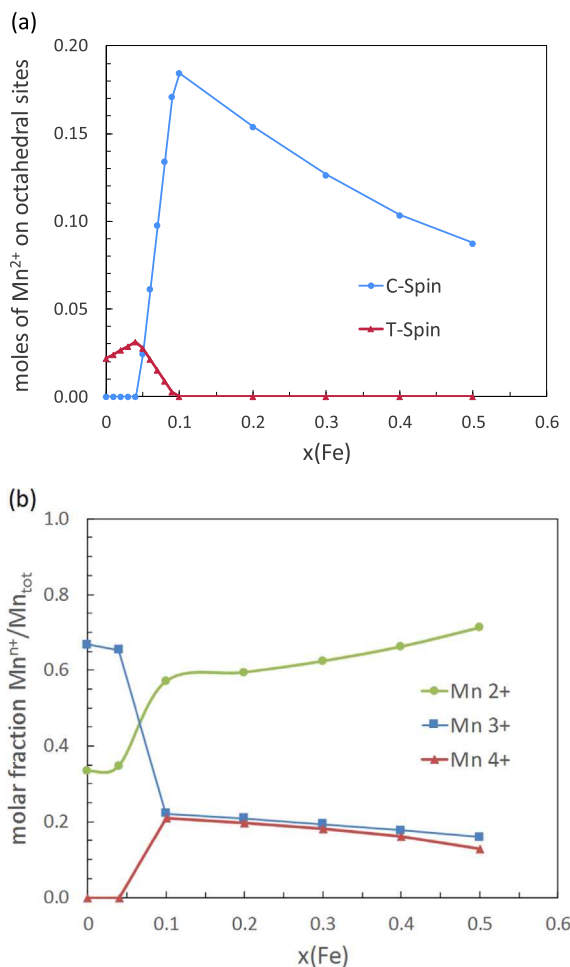


**Fig. 12.** (a) Evolution of experimental  $\Delta m$  (%) during reduction compared to theoretical  $\Delta m$  ( $p\text{O}_2 = 0.20 \text{ atm}$ ), (b) Experimental temperatures at peak reaction rate for manganese-based oxides in 20%  $\text{O}_2/\text{Ar}$  and comparison with the calculated temperature of the Bixb/Spinel transition.

value for each cycle remains close both to the maximum  $\Delta m$  value and to the equilibrium value, which denotes negligible deactivation during redox cycling. The addition of iron to  $\text{Mn}_2\text{O}_3$  thus increases the re-oxidation yield of the material and enhances the cycling stability, as recently observed by Carrillo et al. [11].

Experimental measurements clearly indicate that the minimum Fe content necessary to improve the TES properties of mixed Mn-Fe oxides lies between 10 and 15 mol% Fe. The phase diagram indicates that this corresponds to the formation of the cubic spinel phase only, compared to lower Fe contents, where the tetragonal spinel cannot be reversibly oxidized during cooling. The addition of 20 mol% Fe in  $\text{Mn}_2\text{O}_3$  was previously mentioned as the optimal composition for obtaining the highest enthalpy and most stable re-oxidation yields [11]. However, the authors also obtained full conversion for all their tested samples regardless of the Fe content (especially below 10% Fe), which contrasts sharply with the results of the present study in which pure  $\text{Mn}_2\text{O}_3$  and  $\text{Mn}_2\text{O}_3$  sample with 10 mol% Fe were not able to fully recover the  $\text{O}_2$  lost mass. More recently, an in-depth kinetic and mechanistic study focused on the 20 mol% Fe composition was carried out by the same group [23]. It is stated that the cationic distribution in the spinel structures (cubic and tetragonal) might be sufficiently different to explain the strong variation in the kinetics of the oxidation reaction. The use of the thermodynamic model proposed by Kang and Jung [15] brings support to this explanation. Indeed, as illustrated in Fig. 13a, the calculated cationic distribution evidences that the amount of  $\text{Mn}^{2+}$  on octahedral sites of the spinel strongly increases in the cubic spinel. Furthermore, it has been shown that  $\text{Mn}^{2+}$  on octahedral sites is easier to oxidize than  $\text{Mn}^{2+}$  on tetragonal sites [24]. This difference might very well explain the reason why the cycling properties of the cubic spinel are much better than those of the tetragonal spinel.

Another difference between the two spinel structures is that, in the



**Fig. 13.** (a) Evolution of the amount of Mn<sup>2+</sup> on octahedral sites of the spinel phases with Fe content, at 1050 °C. (b) Evolution of the oxidation number of Mn cations in the spinel phases with Fe content, at 1050 °C.

cubic spinel, a disproportionation reaction takes place according to  $\text{Mn}^{3+} = 1/2 \text{Mn}^{4+} + 1/2 \text{Mn}^{2+}$ , as illustrated in Fig. 13b. The increased amount of Mn<sup>2+</sup> in the cubic spinel, which can be more easily oxidized than Mn<sup>3+</sup> thanks to the favored thermodynamic driving force, may also explain the enhanced re-oxidation ability of the cubic spinel. This result means that pure Mn<sub>2</sub>O<sub>3</sub> (that reduces into pure tetragonal spinel) and mixed Mn-Fe oxides with Fe content below 15% cannot be suitable candidates for achieving reversible reactions because of the poor re-oxidation ability of the tetragonal spinel formed upon reduction.

As for the influence of Fe incorporation in Mn<sub>2</sub>O<sub>3</sub> on the reaction temperatures, a similar tendency as with cobalt oxide is observed. The reduction and oxidation temperatures of Mn<sub>2</sub>O<sub>3</sub> softly increase with increasing amount of added iron (Fig. 12b). According to TGA, an increase of 60 °C is noted between the onset temperatures for reduction (Fig. SI11) of pure Mn<sub>2</sub>O<sub>3</sub> and Mn<sub>2</sub>O<sub>3</sub> with 50 mol% Fe. Concomitantly, a temperature increase of 160 °C is observed for oxidation of Mn<sub>2</sub>O<sub>3</sub> with 50 mol% Fe when compared to Mn<sub>2</sub>O<sub>3</sub> alone. This way, the reaction temperature can be tuned. On top of an increase of the reaction temperature, addition of iron also reduces the temperature gap between the reduction and the oxidation step. A temperature increase was also reported by [11], with 60 °C difference between 0 and 40 mol% Fe added for the reduction, and 236 °C for the oxidation.

Regarding the effect of the gaseous atmosphere composition, the experimental and theoretical  $\Delta m$  values for the reduction in pure Ar atmosphere were found stable with the addition of Fe to manganese

oxide and similar to the  $\Delta m$  measured with 20% O<sub>2</sub>. Again, the reduction temperature increases with the O<sub>2</sub> partial pressure (Fig. SI11). The onset temperature for reduction under inert atmosphere rises with the amount of Fe added to manganese oxide, from about 800 °C for pure Mn<sub>2</sub>O<sub>3</sub> up to 903 °C for x(Fe) = 0.5 (Fig. SI11). As illustrated by the phase diagram (Fig. SI12) calculated at low pO<sub>2</sub> (10<sup>-5</sup> atm), decreasing the oxygen content results in enhancing the tetragonal spinel stability, which is likely to be detrimental to the cycling stability of the materials.

As for the energy storage density, the measured enthalpy for the first reduction step with full conversion of pure Mn<sub>2</sub>O<sub>3</sub> (148 kJ/kg) is smaller than theoretical estimations of 190.1 kJ/kg at turning temperature ( $\Delta G^\circ = 0$ ) of 915 °C [10]. An average of 187.7 kJ/kg is measured for the samples with compositions between 20 and 50 mol% Fe. Increasing the amount of Fe thus slightly improves the energy storage capacity of the material at low Fe contents while it remains unchanged above ~20 mol% Fe (Fig. 9). Accordingly, the thermodynamic calculations indicate that an increase of  $\Delta_r H$  is expected when the Fe content increases from 0 mol% (207 kJ/kg) to 20 mol% (300 kJ/kg), and is stable for higher Fe contents.

In summary, the addition of iron to manganese oxide enhances considerably the cycling stability of the material by improving the re-oxidation yield thanks to the formation of a reactive cubic spinel phase. Also, the higher the amount of Fe added to Mn<sub>2</sub>O<sub>3</sub>, the higher the reaction temperatures. In addition, the gap in temperature between the reduction and the oxidation decreases with higher iron content. The low re-oxidation yield observed for pure Mn<sub>2</sub>O<sub>3</sub> and Mn<sub>2</sub>O<sub>3</sub> with 10 mol% Fe is attributed to the low reactivity of the tetragonal spinel phase. The addition of Fe to Mn<sub>2</sub>O<sub>3</sub> becomes effective for the enhancement of the cycling stability above ~15 mol% Fe, with the suppression of any transition involving this tetragonal spinel phase. The markedly improved reactivity of the cubic spinel featuring reversible reactions is attributed to the increased amount of Mn<sup>2+</sup> cations (resulting from Mn<sup>3+</sup> disproportionation) on octahedral sites of the spinel.

#### 4. Conclusion

The effect of Fe addition in Co and Mn-based oxides was studied experimentally and results were compared with thermodynamic calculations. The calculations were shown to be pertinent since equilibrium is reached at least on the first reduction step of all materials considered in this study. The addition of Fe to Mn<sub>2</sub>O<sub>3</sub> was shown to be beneficial to tune the temperature of redox reactions, to reduce the gap in temperature hysteresis between the reduction and the oxidation step, as well as to enhance the re-oxidation kinetics and cycling stability of the material by countering the deactivation issue of Mn<sub>2</sub>O<sub>3</sub>. Furthermore, a Fe content of ~15 mol% added to Mn<sub>2</sub>O<sub>3</sub> was identified as a minimum threshold for avoiding the formation of a low reactive Mn<sub>3</sub>O<sub>4</sub> tetragonal spinel phase during reduction, which is detrimental to the reaction reversibility because of poor oxidation rate and yield. Noticeably, the Mn<sub>2</sub>O<sub>3</sub> compounds with Fe content in the range 15–50 mol% could be cycled between bixbyite and cubic spinel phases without any reactivity losses during redox reactions. Conversely, the incorporation of Fe to Co<sub>3</sub>O<sub>4</sub> shows adverse effect on the redox performances since both the maximum amount of O<sub>2</sub> exchanged and the reaction enthalpy are lowered when the amount of iron added is increased. The increasing amount of iron added to Co<sub>3</sub>O<sub>4</sub> reduces the maximum oxygen exchange capacity during a redox cycle. The addition of iron to Co and Mn-based oxides also results in an increase of the reaction temperatures, while slightly lowering the gap in temperature between the reduction and oxidation step, which thereby reduces the sensible energy losses during the heating and cooling stages. The comparison of the obtained experimental data with thermodynamic modelling proves that equilibrium calculations bring a strong support for predicting the behavior of mixed oxides since it results in consistent

phase transition temperatures and reliable oxygen storage capacities. It further provided new physical insights into the role of Fe incorporation on the oxidation improvement of Co and Mn-based oxides related to the crystallographic transformations that take place during such redox process depending on Fe content. With the development of new models covering large multi-components systems, it could be further used for selecting other transition metals to enhance the properties of mixed metal oxides for thermochemical energy storage application.

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## Appendix A. Supplementary material

Supplementary data associated with this article can be found in the online version at [doi:10.1016/j.jssc.2017.05.015](https://doi.org/10.1016/j.jssc.2017.05.015).

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