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An assessment of methods of moments for the simulation of population dynamics in large-scale bioreactors

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Abstract

A predictive modelling for the simulation of bioreactors must account for both the biological and hydrodynamics complexities. Population balance models (PBM) are the best approach to conjointly describe these complexities, by accounting for the adaptation of inner metabolism for microorganisms that travel in a large-scale heterogeneous bioreactor. While being accurate for solving the PBM, the Class and Monte-Carlo methods are expensive in terms of calculation and memory use. Here, we apply Methods of Moments to solve a population balance equation describing the dynamic adaptation of a biological population to its environment. The use of quadrature methods (Maximum Entropy, QMOM or EQMOM) is required for a good integration of the metabolic behavior over the population. We then compare the accuracy provided by these methods against the class method which serves as a reference. We found that the use of 5 moments to describe a distribution of growth-rate over the population gives satisfactory accuracy against a simulation with a hundred classes. Thus, all methods of moments allow a significant decrease of memory usage in simulations. In terms of stability, QMOM and EQMOM performed far better than the Maximum Entropy method. The much lower memory impact of the methods of moments offers promising perspectives for the coupling of biological models with a fine hydrodynamics depiction.

Keywords: Biological dynamics, Population Balance Model, Method of classes, Method of moments, (E)QMOM, Maximum entropy

1. Introduction

The large-scale simulation of bioreactors is currently a challenging issue. Such simulations must account for both (i) the (multiphase) hydrodynamics and (ii) the metabolic behaviour of the biological population carried by the fluid. The first can be achieved through the use of widespread CFD softwares, which themselves already require quite important computation power. The most advanced cell models, which result from community efforts in

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7 integrating genome-scale reconstructions of a strain metabolic network, depict thousands of
8 intracellular reactions and metabolite concentrations. Examples are the iJO1366 model for
9 *Escherichia coli* (Orth et al., 2011) and the consensus YEAST model for *Saccharomyces*
10 *cerevisiae* (Heavner et al., 2012, 2013). These models describe state of the art knowledge
11 of a cell functioning, however their implementations require to solve either cumbersome op-
12 timization problems to access a steady-state cell-functioning, or to solve dynamically the
13 metabolite concentrations in a cell that experiences exogeneous perturbations.

14 Even though the computation power increased significantly over the past few decades,
15 coupling the CFD approach with a biological modelling that fully embraces the biological
16 complexity –by solving the intracellular concentrations for each cell in a bioreactor with an
17 Euler-Lagrange framework– is still not possible. Such an approach is numerically untractable.
18 Usual solutions are either to neglect the spatial heterogeneity and solve a complex metabolic
19 model in homogeneous batch or chemostat cultures (Meadows et al., 2010; Matsuoka and
20 Shimizu, 2013) by assuming that all cells are identical; or to describe the hydrodynamic com-
21 plexity jointly with a simplified biological approach such as either structured or unstructured
22 kinetic models (Bezzo et al., 2003; Elqotbi et al., 2013; Lu et al., 2015).

23 As concentration gradients are known to be responsible for metabolic dysfunctions in
24 large-scale reactors (Enfors et al., 2001), we should avoid the first approach and describe the
25 spatial heterogeneities. However, the use of kinetic models should be discarded too. Indeed,
26 from the point of view of a cell travelling in these heterogeneous concentrations fields, the
27 concentration signal is fluctuating (Linkès et al., 2014; Haringa et al., 2016) which constitutes
28 transient conditions, while kinetic models are often based on the Monod kinetics law which
29 reflects a steady-state equilibrium between a population and its environment. By making
30 use of a Monod law, the kinetic models have “been over simplified by allowing instantaneous
31 adaptation of the cell to the abiotic environment” (Silveston et al., 2008).

32 In previous work (Pigou and Morchain, 2015), we stepped back in both the hydrody-
33 namic description by using a Compartment Model Approach (Cui et al., 1996; Mayr et al.,
34 1993; Vrabel et al., 2000, 2001) and in the metabolic description of *E. coli* by simplify-
35 ing the key reactions of the central carbon metabolism into a 6 reactions model derived
36 from the model proposed by Xu et al. (1999). More importantly, we introduced the use
37 of a Population Balance Model (PBM) as a key modelling tool that allows describing si-
38 multaneously both (i) the concentration gradients, (ii) a dynamic adaptation of cells to the
39 fluctuating conditions they experience along their trajectories and (iii) the metabolic impact
40 of a disequilibrium between a cell and its local environment. This approach has been suc-
41 cessfully challenged against experimental data in lab-scale batch culture and industrial-scale
42 heterogeneous fedbatch culture. More recently, we improved the PBM to account for an
43 experimentally observed stochastic diversity related to cell-division (Morchain et al., 2016).

44 Until now, we solved the PBM using a class method (also known as fixed pivot method,
45 Kumar and Ramkrishna (1996a); Mantzaris et al. (2001)) with at least 60 classes to span
46 the entire range of possible values for the chosen variable (i.e. the maximum growth-rate
47 achievable by a cell provided enough nutrients are available). Each class represents a scalar
48 that must be transported by the hydrodynamic framework. While transporting a hundred
49 classes within a 70 compartments model (Pigou and Morchain, 2015) was perfectly feasible,
50 doing the same in a CFD simulation would be prohibitively expensive.

51 The current paper thus focuses on improving the numerical tractability of the PBM,
52 through the use of Methods of Moments (MOM), in order to increase back the allowed level
53 of spatial accuracy. Instead of doing a direct resolution of the population balance equation,
54 MOM describe the evolution of the first moments of a Number Density Function (NDF).
55 However, it will be of interest to perform a reverse operation and to recover an approximation
56 of the NDF from a finite set of its moments; this is known as a truncated moment problem
57 (Abramov, 2007).

58 Many methods are available to tackle this problem. A review of such methods is available
59 (John et al., 2007) though new methods or improvements are available since its publication.
60 More recently, Lebaz et al. (2016) compared the most common approaches which are Ker-
61 nel Density Element Method (KDEM), Spline-based method, and the Maximum Entropy
62 method applied to the case of a depolymerization process. The KDEM approximates the
63 unknown NDF as the sum of weighted Kernel Density Functions (KDF); the identification
64 of the weights is performed through a constrained minimization procedure, which requires
65 a high number of moments to prevent an underdetermined problem and the multiplicity of
66 solutions. The spline method (John et al., 2007) leads to a piece-wise polynomial reconstruc-
67 tion, but the resulting reconstruction is highly dependent on numerical parameters, and can
68 lead to negative values of the reconstructed NDF. For these reasons, the KDEM and spline
69 methods will be discarded in the current work.

70 The Maximum Entropy method (MaxEnt, Mead and Papanicolaou (1984); Tagliani
71 (1999)) was point out as efficient and accurate, even with a low number of moments, by
72 Lebaz et al. (2016). It is however ill-conditioned at the boundaries of moment space (Massot
73 et al., 2010), but this can be handled provided some adjustments of the method (Vié et al.,
74 2013). Finally, we consider the recent EQMOM method (Chalons et al., 2010; Yuan et al.,
75 2012; Marchisio and Fox, 2013) which constitutes a clever fusion of KDEM with the QMOM
76 approach (Marchisio et al., 2003a,b,c). This method has proven to be stable and efficient,
77 in particular near the moment-space frontier where MaxEnt is ill-conditioned, but requires
78 to make assumptions over the shape of the reconstruction.

79 The current work is focused on assessing the methods QMOM, EQMOM and MaxEnt
80 against the already used class method, in the perspective of running predictive, and nu-
81 merically tractable, bioreactor simulations. All these methods will be implemented for the
82 simulation of a homogeneous chemostat culture stressed with a dilution rate shift (Kätterer
83 et al., 1986). After a first comparison of their numerical efficiency, their accuracy, and their
84 stability when facing such a sudden perturbation, we will reproduce the results from Pigou
85 and Morchain (2015) using these Methods of Moments, in a heterogeneous case based on the
86 Compartment Model from Vrábek et al. (1999, 2000), and compare once again their results
87 against the class method.

88 **2. Models and Methods**

89 *2.1. Local mass balance*

90 The basis in the modelling of bioreactors is the formulation of local mass balances. They
91 describe the evolution of local concentrations as a consequence of (i) transport by the carrying
92 fluid and (ii) consumption or production by the biological phase. As in previous work (Pigou

93 and Morchain, 2015), we will hereafter describe the hydrodynamics using Compartment
 94 Model Approach (CMA). Let \mathbf{C}_n ($kg.m^{-3}$) be the vector of mass concentrations within the
 95 n -th compartment, V_n the volume (m^3) of that compartment, and $Q_{n,m}$ ($m^3.h^{-1}$) the volume
 96 flow rate going from the n -th to the m -th compartment. The total number of compartments
 97 is N_c . Then, the mass balance equation in compartment n is given as:

$$\frac{\partial V_n \mathbf{C}_n}{\partial t} + \mathbf{C}_n \sum_{m=1}^{N_c} (Q_{n,m}) - \sum_{m=1}^{N_c} (Q_{m,n} \mathbf{C}_m) = V_n \mathbf{R}(\mathbf{C}_n) \quad (1)$$

98 Our contribution is to express the vector of biological reaction rates $\mathbf{R}(\mathbf{C})$ ($kg.m^{-3}.h^{-1}$) as
 99 the sum of the substrate uptake rates, or product production rates, due to all cells considering
 100 their individual physiological states. Let μ (h^{-1}) be the biological growth capability of a
 101 cell (i.e. the growth rate they can achieve if permitted by the nutrient availability), we will
 102 distinguish each individual upon this value. Different cells, having different values of μ in a
 103 similar environment, will exhibit different metabolic behaviours. Then, in order to express
 104 the bioreaction rates at the scale of the biological population, one must know the statistical
 105 distribution of the property μ over that population, and integrate the uptake or production
 106 rates over that distribution:

$$R_i(\mathbf{C}_n) = \int_0^{+\infty} n(\mu) \Phi_i(\mu, \mathbf{C}_n) d\mu \quad (2)$$

107 where $n(\mu)$ is the NDF defining the fraction of the biological phase whose specific growth
 108 rate is μ . The first two moments of this NDF are defined as following:

$$\int_0^{+\infty} n(\mu) d\mu = X \quad (3)$$

$$\int_0^{+\infty} \mu n(\mu) d\mu = \tilde{\mu} X \quad (4)$$

109 with X the total biomass concentration ($kg.m^{-3}$) and $\tilde{\mu}$ the population mean growth rate
 110 (h^{-1}). In the current work, we consider the metabolic behaviour of *Escherichia coli* and
 111 the vector \mathbf{C} actually consists in a vector of Glucose (G), Acetate (A) and Oxygen (O)
 112 concentrations.

$$\mathbf{C} = \begin{bmatrix} C_G \\ C_A \\ C_O \end{bmatrix} \quad (5)$$

113 We will also consider scalar variables to transport information about the distribution
 114 $n(\mu)$ as explained afterwards.

115 Therefore, the glucose uptake rate $\Phi_G(\mu, \mathbf{C})$, the oxygen uptake rate $\Phi_O(\mu, \mathbf{C})$ and the
 116 acetate uptake/production rate $\Phi_A(\mu, \mathbf{C})$ will be outcomes of the metabolic model calculation
 117 procedure. The later uses as inputs (i) the specific potential growth rate of individual, μ ; (ii)
 118 the vector of concentrations in the liquid phase \mathbf{C} , and (iii) the equilibrium law $\mu^* = f(\mathbf{C})$.
 119 The growth rate at equilibrium μ^* is the growth rate that cells would exhibit at steady state

120 in an environment defined by the vector of concentrations \mathbf{C} . Such expressions are known
 121 from chemostat experiments and typically take the form of a multi-component Monod-Law,
 122 taking here into account the inhibitory effect of acetate:

$$\mu^* = \mu_{\max} \frac{C_G}{C_G + K_G} \frac{C_O}{C_O + K_O} \frac{K_{i,A}}{C_A + K_{i,A}} \quad (6)$$

123 with K_G and K_O the affinity constants ($kg.m^{-3}$) of the biomass toward glucose and oxygen,
 124 and $K_{i,A}$ the inhibitory constant of growth by acetate.

125 A noticeable point is that the substrate uptake rate is not algebraically related to the
 126 specific growth rate as it cannot be assumed in general that cells are at equilibrium with
 127 their environment (Ferenci, 1996). Therefore, our approach is consistent with theoretical
 128 considerations (Perret, 1960) and experimental observations (Abulesz and Lyberatos, 1989;
 129 Li, 1982; Silveston et al., 2008) indicating that the growth and uptake rates are decoupled
 130 in the dynamic regime whilst an algebraic relation exists between them at steady state.

131 The second point in terms of modelling resides in the calculation of the NDF $n(\mu)$ that
 132 defines the concentration of biomass whose potential growth rate is μ . This calculation will
 133 be addressed in a dedicated paragraph.

134 2.2. Calculation procedure for the metabolic reaction rates

135 The procedure is almost identical to that presented in a previous paper (Pigou and Mor-
 136 chain, 2015), therefore, only the key features of the metabolic model, and the few differences
 137 of the calculation procedure are detailed here.

138 The first step of that procedure is to compute the actual growth rate of each cell, by
 139 taking into account its growth capabilities (see section 2.3), and a potential limitation re-
 140 lated to nutrient availability. In the previous work, we defined this actual growth rate of a
 141 cell, μ_a , as the minimum between its biological growth capability, μ , and the environment
 142 equilibrium growth rate μ^* (given by the Monod law, Eq. 6): $\mu_a = \min(\mu^*, \mu)$. However,
 143 we recently shifted this formulation toward a more meaningful and physical one, based on
 144 a limitation by the micromixing, which proved to be consistent with experimental studies
 145 of membrane transporters at limiting nutrient concentrations (Ferenci, 1996, 1999). The
 146 detailed explanation for this change is given in Morchain et al. (2016).

147 We then defined a threshold glucose concentration, C_{G_T} , around which micromixing will
 148 start to be a limiting factor. As long as the bulk substrate concentration is significantly
 149 higher than this threshold concentration, cells will be fed enough by micromixing to be able
 150 to achieve their potential growth rate.

$$C_{G_T} = R_G \times 17 \left(\frac{\nu}{\varepsilon} \right)^{0.5} \quad (7)$$

151 The term $17\sqrt{\nu/\varepsilon}$ is proposed by Baldyga and Bourne (1999) to evaluate the micro-
 152 mixing time-scale, and depends on the fluid viscosity, ν (m^2/s), and the turbulent energy
 153 dissipation rate, ε (, whose value usually ranges from 0.5 to 10W/kg depending on the
 154 bioreactor stirring.

155 As R_G is an output of the metabolic calculation procedure (Eq. 2), which itself depends
 156 on μ_a , and considering that we only need the order of magnitude of the limiting concentration,
 157 we provide the following rough approximation of R_G for the estimation of C_{G_T} :

$$R_G \approx \frac{M_G}{Y_{XG}M_X} \int_0^{+\infty} \mu n(\mu) d\mu \quad (8)$$

158 With Y_{XG} the molar yield of glucose to cell conversion ($mol_X \cdot mol_G^{-1}$), M_X the molar
 159 mass of biomass ($M_X = 113.1g_X \cdot mol_X^{-1}$ considering the typical chemical formula $C_5H_7NO_2$)
 160 and M_G the molar mass of glucose ($M_G = 180.2g_G \cdot mol_G^{-1}$).

Now, following Morchain et al. (2016), the actual growth rate is given by:

$$\mu_a = \Psi \mu \quad (9)$$

where the coefficient Ψ reads:

$$\Psi = 1 - e^{-C_G/C_{G_T}} \quad (10)$$

161 As a recall, the estimation of μ_a along with the calculation of μ^* is the very first step of
 162 the calculation procedure of the metabolic model, as detailed in Pigou and Morchain (2015)
 163 which explains why the choice of μ_a formulation is of importance. After estimating the
 164 actual -effectively achieved- growth rate of a cell, the calculation procedure of the metabolic
 165 model is exactly the one described in the previous work.

166 This metabolic model roughly describes the central metabolism of *Escherichia coli*, it
 167 accounts for:

- 168 • Anabolism based on either glucose or acetate as a carbon source, leading to the for-
 169 mation of new cells,
- 170 • Oxidative catabolism on both substrates for energy production,
- 171 • Fermentative catabolism of glucose, leading to the production of energy, and acetate
 172 as a by-product,
- 173 • Overflow metabolism, leading to production of acetate when glucose is over-consumed.

174 Each pathway is simplified into the following set of reactions:



175 G: Glucose, E: Energy, A: Acetate, O: Oxygen, X: Biomass. Y_{BA} is the stoichiometric
 176 molar coefficient in mol_B/mol_A . q_α^G and q_α^A are the specific reaction rates for reactions
 177 respectively based on glucose ($mol_G \cdot g_X^{-1} \cdot h^{-1}$) and on acetate ($mol_A \cdot g_X^{-1} \cdot h^{-1}$).

178 The calculation procedure gives access to the specific reaction rates, and is based on:

- 179 • The growth capability of a cell (μ), whose evolution is described by the Population
 180 Balance Model (see section 2.3),
- 181 • The environmental conditions (G, A and O concentrations) and the Ψ coefficient,
- 182 • An assumption of non-accumulation within the cytoplasm. In particular, the rate of
 183 energy production is balanced by the rate of energy consumption.

184 2.3. Population Balance Model

185 External and intrinsic perturbations are known to produce heterogeneity among the cell
 186 population. In order to track this diversity, the usual mathematical approach is to refer to a
 187 population balance model. The originality of our approach resides in that the discriminating
 188 factor is the specific growth rate of individuals. Recent observations have proved that this
 189 variable is actually distributed in a cell population (Yasuda, 2011). This formulation is
 190 advantageous since the relationship between the growth rate and the metabolic reaction rates
 191 is much more natural than when the size or mass of the cell is chosen as the discriminating
 192 parameter (Pigou and Morchain, 2015; Morchain et al., 2016). The Population Balance
 193 Equation (PBE) for the specific growth rate distribution $n(\mu)$ is here given for a homogeneous
 194 case; terms accounting for the transport might be added on the left hand side depending on
 195 the hydrodynamic framework:

$$\frac{\partial n(\mu)}{\partial t} = -\frac{\partial}{\partial \mu} [n(\mu)\zeta(\mu)] + \int_0^{+\infty} \beta(\mu, \mu')n(\mu')\Psi\mu' d\mu' \quad (11)$$

196 The first term in the right-hand side of equation 11 is a convection term in the μ -space
 197 instead of the physical space. It describes the fact that individuals are able to adapt their
 198 specific growth rate in response to insufficient or excessive substrate concentrations. We
 199 refer to this term as the adaptation term. In the adaptation term, $\zeta(\mu)$ refers to a velocity in
 200 the μ -space or equivalently to the rate of change of μ over time. This velocity can be either
 201 positive or negative depending on whether the environment is respectively rich or poor in
 202 nutrients, compared to what a cell is used to. In previous work, a general form for $\zeta(\mu)$ was
 203 proposed and validated against experimental data sets:

$$\zeta(\mu) = \left(\frac{1}{T} + \mu \right) (\mu^* - \mu) \quad (12)$$

204 The second term of equation 11 is often referred to as the birth and death term in PBM.
 205 $\beta(\mu, \mu')$ is a Probability Density function (PDF) which defines the probability that a mother
 206 cell having a specific growth rate μ' produces a daughter cell whose specific growth rate is
 207 μ . The analysis of recent experimental data revealed that β can be modeled using a skew-
 208 normal distribution (Yasuda, 2011; Morchain et al., 2016) whose parameters are given in
 209 Appendix A.

210 Instead of looking for an analytic solution for the PBE (Eq. 11), we will try to solve that
 211 equation numerically. The most straightforward method simply consists in a discretization
 212 of the μ -space using either fixed (Kumar and Ramkrishna, 1996a) or moving (Kumar and
 213 Ramkrishna, 1996b) meshes. These methods tend to be expensive as soon as heterogeneous
 214 systems are considered. However, they accurately describe the solution distribution of the
 215 PBE and allow an easy coupling with the transport and reaction parts of the modelling
 216 (Eq. 1). We used to apply these fixed mesh (also known as Methods of Classes, MOC),
 217 as detailed in previous papers (Morchain et al., 2013; Pigou and Morchain, 2015). We will
 218 here focus on applying methods of moments and challenging their results against the already
 219 validated MOC. Knowing the law for the evolution of the distribution (Eq. 11), the first
 220 step to apply moment methods is to transform the PBE so that it expresses the evolution of
 221 the distribution's moments. The k -th order moment of the distribution $n(\mu)$ is defined as:

$$m_k = \int_0^{+\infty} \mu^k n(\mu) d\mu \quad (13)$$

222 The Appendix A details how this definition and the PBE lead to the following law of
 223 moments evolution:

$$\frac{\partial m_k}{\partial t} = k \left(\frac{\mu^*}{T} m_{k-1} + \left(\mu^* - \frac{1}{T} \right) m_k - m_{k+1} \right) + \Psi m_1 B_k(\tilde{\mu}) \quad (14)$$

- 224 • B_k is the k -th order moment of the PDF $\beta(\mu, \mu')$ whose formulation is also given in
 225 Appendix A.
- 226 • $\tilde{\mu}$ is the population mean growth rate, defined in terms of moments by:

$$\tilde{\mu} = \frac{\int_0^{+\infty} \mu n(\mu) d\mu}{\int_0^{+\infty} n(\mu) d\mu} = \frac{m_1}{m_0} \quad (15)$$

227 $\frac{\partial m_k}{\partial t}$ depends on m_{k+1} which leads to an unclosed formulation. To tackle this issue,
 228 McGraw (1997) introduced the Quadrature Method of Moments (QMOM) which is based
 229 on a Gaussian quadrature whose nodes and weights are chosen so that the N first moments
 230 of the PDF are well computed by the quadrature:

$$m_k = \sum_{i=1}^O w_i L_i^k \quad \forall k \in \{0, \dots, N-1\} \quad (16)$$

231 O is here the order of the method, which deals with $N = 2 * O$ number of moments. The
 232 core of the method lies in the identification of weights w_i and abscissas L_i of the Gaussian
 233 quadrature. These parameters allow an exact computation of moments of order ranging
 234 from 0 to $N-1$ and usually give satisfactory approximation of higher order moments. This
 235 method then allows closing the formulation given by Eq. 14.

236 We introduce here one refinement of the PBE compared to the one described in Pigou
 237 and Morchain (2015). The moment formulation of the PBE (eq. 14) is correct only if the
 238 time constant T is not dependent on μ . However, we used in Pigou and Morchain (2015)

239 one time constant $T_u = 1.9h$ for individuals that are moving upward in the μ -space, and a
 240 different time constant $T_d = 6.7h$ for individuals moving downward. This formulation implies
 241 that the decrease of growth capabilities in poor environments is slower than the increase of
 242 these capabilities in rich environments, and this fact is required to allow a good fitting of
 243 experimental data. In the current work, and in order to make use the moment formulation of
 244 the PBE given in eq. 14, we define the time constant T_m as the mean value of the functional
 245 $T(\mu)$ that we used previously:

$$T(\mu) = \begin{cases} T_u & \text{if } \mu < \mu^* \\ T_d & \text{otherwise} \end{cases} \quad (17)$$

$$T_m = m_0^{-1} \int_{\Omega\mu} T(\mu)n(\mu)d\mu \quad (18)$$

$$= \alpha T_u + (1 - \alpha)T_d \quad \text{with } \alpha = m_0^{-1} \int_0^{\mu^*} n(\mu)d\mu \quad (19)$$

246 We then actually make use of the PBE given in eq. 20 to describe the evolution of
 247 moments. Similarly, we use the time constant T_m to describe the evolution of the distribution
 248 in the class method in order to have consistent formulations between methods.

$$\frac{\partial m_k}{\partial t} = k \left(\frac{\mu^*}{T_m} m_{k-1} + \left(\mu^* - \frac{1}{T_m} \right) m_k - m_{k+1} \right) + \Psi m_1 B_k(\tilde{\mu}) \quad (20)$$

249 2.4. Reconstruction methods

Population balance equation: $\frac{\partial n(\mu)}{\partial t} = -\frac{\partial}{\partial \mu} [n(\mu)\zeta(\mu)] + \int_0^{+\infty} \beta(\mu, \mu')n(\mu')\psi\mu' d\mu'$				
	Method of classes $X_j, j \in \{0, \dots, NC\}$	Method of Moments $m_k, k \in \{0, \dots, N-1\}$		
		QMOM	EQMOM*	MaxEnt*
NDF approximation $\hat{n}(\mu)$	$\sum_{j=1}^{NC} \frac{X_j}{\delta\mu} \delta(\mu - \mu_j)$	$\sum_{i=1}^{N/2} w_i \delta(\mu - L_i)$	$\sum_{i=1}^{\lfloor N/2 \rfloor} w_i \kappa(\mu, L_i, \sigma)$	$\exp\left(\sum_{i=0}^{N-1} \varphi_i \mu^i\right)$
m_{N+1} formulation	\emptyset	$\sum_{i=1}^{N/2} w_i L_i^{N+1}$	$\int \hat{n}(\mu) \mu^{N+1} d\mu$	$\int \hat{n}(\mu) \mu^{N+1} d\mu$
Source term (eq. 2)	$\sum_j X_j \Phi(\mu_j)$	$\sum_{i=1}^{N/2} w_i \Phi(L_i)$	$\int \hat{n}(\mu) \Phi(\mu) d\mu$	$\int \hat{n}(\mu) \Phi(\mu) d\mu$
Number ODE	NC	N	N	N

Figure 1: Summary of applied methods to couple the population balance with transport and reaction.
 *Numerically expensive methods.

250 In the present case, and it seems very likely that this would extend to many biological
 251 applications, the calculation of the integral reaction term in equation 2 cannot be expressed

252 in terms of moments of $n(\mu)$, at least because the uptake rates $\Phi_i(\mu, \mathbf{C})$ are not continuously
 253 differentiable with respect to μ . To tackle this issue, we must construct a suited quadrature
 254 rule that will be used to approximate all integrals of the following form:

$$\int_{\Omega_\mu} f(\mu)n(\mu)d\mu \approx \sum_i w_i f(L_i) \quad (21)$$

255 where \mathbf{w} and \mathbf{L} are the weights and abscissas of the quadrature rule.

256 Different methods exist to provide a quadrature rule with the constraint that this rule
 257 does compute accurately the known N moments of the distribution:

$$\int_{\Omega_\mu} \mu^k n(\mu)d\mu = \sum_i w_i L_i^k \quad k \in \{0, \dots, N-1\} \quad (22)$$

258 Each method formulates some assumptions about the properties of the NDF $n(\mu)$, and
 259 identify a unique NDF $\hat{n}(\mu)$ that matches the set of known moments and the formulated
 260 assumptions. We will refer to $\hat{n}(\mu)$ as a reconstruction –or approximation– of $n(\mu)$. Knowing
 261 the properties of $\hat{n}(\mu)$, obtaining the quadrature rule \mathbf{w} and \mathbf{L} will be quite straightforward.

262 We will then use this rule to perform the estimation of higher order unknown moments
 263 (Eq. 14) as well as the numerical computation of unclosed integral terms (Eq. 2 and 19).

264 2.4.1. The QMOM method

265 The QMOM method is the easiest method to implement. It makes the assumption that
 266 the moment set is at the frontier of the moment space, which implies that the distribution
 267 $\hat{n}(\mu)$ is a sum of $O = N/2$ weighted Dirac distributions. The reconstructed NDF is then
 268 given by:

$$\hat{n}(\mu) = \sum_{i=1}^O w_i \delta(\mu - L_i) \quad (23)$$

269 Thus the reaction term (Eq. 2) can be approximated by:

$$R(\mathbf{C}) \approx \sum_{i=1}^O w_i \Phi(L_i, \mathbf{C}) \quad (24)$$

270 Due to the complexity of the function $\Phi(\mu, \mathbf{C})$, a high order quadrature will be required,
 271 which implies the need of a high number of resolved moments to correctly approximate the
 272 integral term in Eq. 2.

273 The computation of the weights w_i and abscissas L_i of the quadrature nodes is performed
 274 using either the Product-Difference Algorithm (PDA) or the Wheeler Algorithm (WA) as
 275 implemented by Marchisio and Fox (2013), with some code tuning to improve efficiency.

276 2.4.2. The EQMOM method

277 Yuan et al. (2012) introduced the Extended Quadrature Method of Moments (EQMOM)
 278 which consists in coupling QMOM with the Kernel Density Element Method (KDEM) in
 279 which the NDF is reconstructed as the weighted sum of Kernel Density Functions.

280 The reconstructed NDF, using a O -nodes EQMOM reconstruction, has the following
 281 expression:

$$\hat{n}(\mu) = \sum_{i=1}^O w_i \kappa(\mu, L_i, \sigma) \quad (25)$$

282 This method then requires the first $N = 2O + 1$ moments of the NDF, in order to identify
 283 uniquely the value of w_i , L_i and σ . The following kernels are known to be compatible with the
 284 EQMOM procedure: Gaussian κ_G (Chalons et al., 2010), Log-Normal κ_L (Madadi-Kandjani
 285 and Passalacqua, 2015), Beta κ_β of Gamma κ_Γ (Athanassoulis and Gavriiadis, 2002; Yuan
 286 et al., 2012) kernels. We tested each of these kernels but we will only focus on the Gaussian
 287 kernel in this paper. Its expression is given hereafter:

$$\kappa_G(\mu, L, \sigma) = \frac{1}{\sigma\sqrt{2\pi}} e^{-\frac{(\mu-L)^2}{2\sigma^2}} \quad (26)$$

288 This method relies on the Wheeler algorithm (Marchisio and Fox, 2013), in order to
 289 identify the values of \mathbf{w} and \mathbf{L} . On top of that, a non-linear solver must identify the unique
 290 value of σ which leads to a reconstructed distribution whose moments match the expected
 291 values. We implemented a bisection method to find numerically the root of the objective
 292 function that quantify the good agreement of the reconstruction with the set of known
 293 moments. We also implemented analytical solutions for $O = 1$ and $O = 2$ as described by
 294 Marchisio and Fox (2013).

295 The integration of the metabolic behaviour over the population (Eq. 2) is performed
 296 by using a 10-nodes Gauss-Hermite quadrature for each node of the Gaussian EQMOM
 297 reconstruction as suggested by Yuan et al. (2012).

298 2.4.3. The Maximum Entropy method

299 Given a finite realizable set of N moments, there exists an infinite set of NDF with the
 300 same set of first N moments (Mead and Papanicolaou, 1984). Therefore, the goal of any
 301 reconstruction method is to choose one plausible NDF out of this infinite set of possibilities.
 302 While the EQMOM method enforces the expected shape of the reconstruction by choosing
 303 arbitrarily a specific kernel, the Maximum Entropy method aims to find, out of all possible
 304 reconstructions, the one that maximizes the Shannon Entropy defined for any PDF f as:

$$H[f] = - \int_{-\infty}^{+\infty} f(x) \ln(f(x)) dx \quad (27)$$

305 Tagliani (1999) describes the application of this method for the specific case of a positive
 306 PDF defined on the closed support $x \in [0, 1]$. This method can be extended to any finite
 307 support $[a, b]$ without loss of generality by a mere linear change of variable.

The reconstructed distribution whose Shannon entropy is the highest takes the following
 form (Mead and Papanicolaou, 1984; Tagliani, 1999):

$$\hat{n}(\mu) = \exp \left(- \sum_{i=0}^M \varphi_i \mu^i \right) \quad (28)$$

308 With $M = N - 1$ the highest order of known moments.

309 The key issue is to identify the values of the polynomial coefficients φ_i , which is achieved
 310 through the minimization of the following function (Kapur, 1989; Mead and Papanicolaou,
 311 1984):

$$\Gamma(\varphi_1, \dots, \varphi_M) = \sum_{k=1}^M \varphi_k \frac{m_k}{m_0} + \ln \left(\int_0^1 \exp \left(- \sum_{k=1}^M \varphi_k \mu^k \right) d\mu \right) \quad (29)$$

312 The Γ function is both convex and smooth which makes its minimization possible through
 313 an iterative Newton-Raphson procedure, with the necessary and sufficient condition that the
 314 moment sequence is realizable and not too close of the frontier of the moment space, otherwise
 315 the Hessian matrix will be ill-conditioned.

316 The Jacobian and Hessian matrices of this function are easily expressed, but they require
 317 the numerical computation of the following integrals:

$$\hat{m}_k = \int_0^1 \mu^k \exp \left(- \sum_{i=0}^M \varphi_i \mu^i \right) d\mu \quad k \in \{0, \dots, 2M\} \quad (30)$$

318 These integrals must be evaluated numerically as no analytic form exists as soon as
 319 $M > 2$, which is done using the adaptative support quadrature proposed by Vié et al.
 320 (2013). The fact that such integrals must be numerically computed, at each step of the
 321 Newton-Raphson procedure, which itself is called at each time-step, explains why we marked
 322 that method as computationally intensive on Figure 1. However as moments evolve in a
 323 continuous way over time, the φ_i will also evolve continuously, and the initial guess of the
 324 Newton-Raphson procedure is set as the solution of the previous time-step, leading to a fast
 325 convergence.

326 The number of nodes for the resulting quadrature rule actually depends on the results of
 327 the procedure described by Vié et al. (2013). We used a 15 nodes Gauss-Legendre quadrature
 328 for each sub-intervals identified by their procedure.

329 Finally, in our following simulations, we did encounter cases where the moment set was
 330 too close from the frontier of the moment space which led to ill-conditioned Hessian matrices.
 331 We first performed the reconstruction on the support $[0; K * \mu_{\max}]$ with $K = 1.5$, however
 332 we observed that our distributions only span a tiny fraction of this interval at each time.
 333 This often led to moment sets whose last moment were close to their upper or lower bounds
 334 in the moment space (we underlined this by calculating the canonical moments using the
 335 QD algorithm from Dette and Studden (1997)). We then decided to adapt dynamically the
 336 value of K between 0 and 2 in order to stretch the support of the reconstruction so that the
 337 moments of the distribution are always far enough from the frontier of the moment space,
 338 which then allows a fast and accurate convergence of the MaxEnt method.

339 The rules for the evolution of K , from time step (n) to timestep ($n + 1$) are based
 340 on the value of the last canonical moments p_M computed from the set of known moments
 341 m_0, \dots, m_M :

- 342 • If $p_M^{(n)} < 0.4$: $K^{(n+1)} = 0.96 * K^{(n)}$
- 343 • If $p_M^{(n)} > 0.6$: $K^{(n+1)} = 1.04 * K^{(n)}$

344 This proposition is most probably not universal and might only work in our specific
345 application cases.

346 2.5. Simulation software

347 All following simulations are performed using ADENON, a user-friendly simulation soft-
348 ware we developed using the environment provided by MATLAB R2016a. This software is
349 mainly focused on the simulation of bioreactors, by applying our PBM/Metabolic biological
350 models within a hydrodynamic framework (compartment models, plug-flow reactors, batch
351 or fedbatch cultures as well as accelerostat cultures). Population balances can be solved
352 using either class or moment methods, with all core routines –for moment quadrature or
353 distribution reconstruction– built into this software.

354 Following the case configuration provided by the user, this tool formulates the corre-
355 sponding ODE in terms of mass and volume balances. This set of ODE is then solved using
356 an explicit scheme for time integration, either the Runge-Kutta 2,3 pair of Bogacki and
357 Shampine (1989) or a simple first-order Euler scheme. The specificities of our solver com-
358 pared to the built-in “ode23” function are (i) its capability of running in parallel (multi-core)
359 mode by distributing the resolved variables and the reconstruction computing across CPU
360 cores, and (ii) the fact that it enforces the consistency of resolved variables (mainly their
361 non-negativity) in a more stringent way.

362 We used the simple explicit Euler scheme for all simulations, and choose a timestep δt
363 tiny enough to make the solution independent from this timestep.

364 3. Results

365 3.1. Stressed chemostat culture

366 In a first attempt of applying the method of moments with reconstruction of the NDF,
367 we chose to reproduce numerically the experimental results from Kätterer et al. (1986). We
368 simulate a homogeneous chemostat culture with a constant initial dilution rate $D = 0.1h^{-1}$
369 for $30h$ in order to reach a steady-state, we then apply a sudden shift in dilution rate toward
370 $D' = 0.42h^{-1}$ in order to analyse 15 hours of the transient-state.

371 As the original experiments were conducted using *Candida tropicalis* instead of *E. coli*,
372 we adjusted the parameters of our metabolic model to fit quantitatively the biomass and
373 substrate curves provided by Kätterer et al. (1986). It is however obvious that the metabolic
374 behaviours of the yeast *C. tropicalis* and the bacteria *E. coli* are quite different and a mere
375 parameter adjustment of a *E. coli* metabolic model will not produce a model exhibiting the
376 metabolic behaviour of *C. tropicalis*. Here, we are only interested in the analysis of the
377 population balance part of the model. We shall investigate each reconstruction method in
378 terms of stability, computation time, and accuracy of the reconstruction. The shape of the
379 reconstruction will have a metabolic impact in terms of acetate production, and we will only
380 compare these productions between class and moment methods, not against experimental
381 results.

382 The Figure 2 shows simulation results for each method, with different orders or resolution.
383 We applied QMOM with order ranging from $O = 2$ to $O = 5$ ($N = 2O$), EQMOM with
384 order ranging from $O = 1$ to $O = 3$ ($N = 2O + 1$) and MaxEnt with N ranging from 3 to 7.

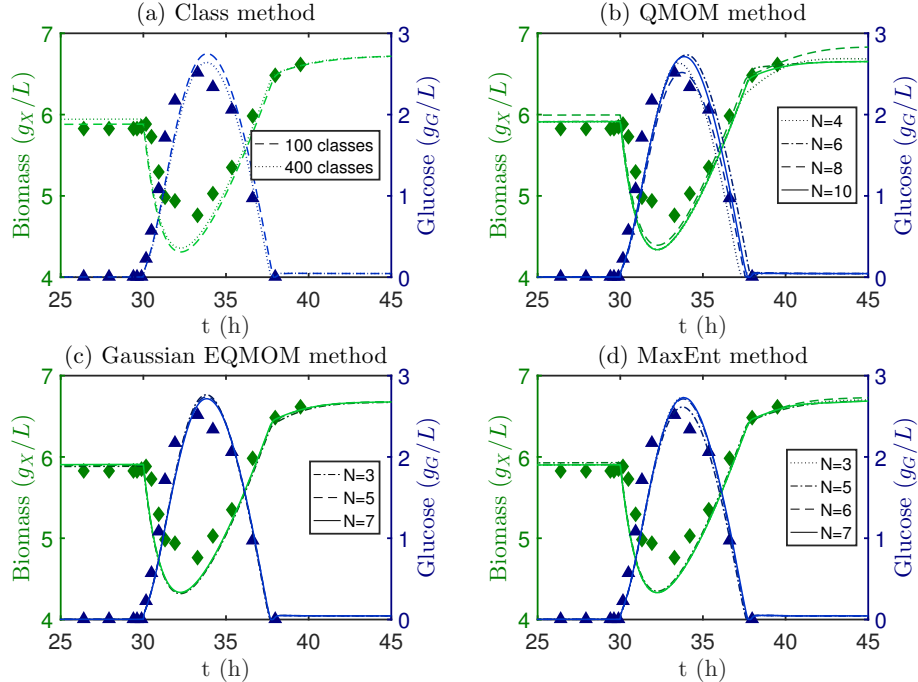


Figure 2: Simulation results for each method, compared with experimental data from Kätterer et al. (1986).

385 The overall dynamics are well reproduced by each method, even with as few as two nodes
 386 with QMOM, even though that last method gives noticeably different results depending
 387 on its order. As explained before, the overall dynamics does not depend directly on the
 388 redistribution term of the PBE (Eq. 11) but mainly on the adaptation term. The moment
 389 formulation of this term needs a closure method to estimate the next unsolved moment, so
 390 as long as this estimation is reasonably accurate, the dynamics should be well reproduced.

391 We then assessed the error on the estimation of the next unknown moment for each
 392 method and order by comparing them to the moments calculated with 400 classes. Full data
 393 set is provided as supplementary data. It is shown that the error is mainly kept under 0.2%.

394 In terms of shape of the reconstruction, we can use the same data set to compare the
 395 original distribution solved with the class method to the reconstructions as illustrated on
 396 Figure 3.

397 The shape of the reconstruction has two main effects. It affects the biomass concentration
 398 at steady-state due to the Pirt law which changes the yield of substrate conversion to biomass
 399 depending on the property μ of each individual. The population mean conversion yield will
 400 then depend on that shape, which explains why steady-state biomass concentrations are
 401 order-dependent for QMOM (Figure 2b). However, as the resulting reconstructions are
 402 quite similar with EQMOM and MaxEnt (Figure 3), no matter the order of the method,
 403 they always predict similar steady-state biomass concentrations.

404 The second effect is the metabolic behaviour. As stated before, our metabolic model
 405 does not represent the actual metabolic behaviour of *Candida tropicalis*, however, it describe
 406 the overflow metabolism existing in *E. coli* which leads to acetate production in a way that
 407 depends on the shape of the distribution. Figure 4 illustrates these different acetate produc-

408 tions depending on the chosen method. Once again, QMOM exhibits different behaviours
 409 depending on the order of the method, while EQMOM and MaxEnt lead to predictions close
 410 to the class method.

411 Acetate production is slightly overestimated by all moment methods, due to the fact that
 412 they do not account for the narrow peak of the distribution (see Figure 3b,c,d). This slightly
 413 overestimates the disequilibrium between the individuals and their environment, which is
 414 a key point in our modelling: the disequilibrium between the cell uptake of substrate and
 415 its requirements for growth determines the intensity of the overflow metabolism (i.e the
 416 production of by-products, here the acetate).

417 In terms of simulation performances, the Figure 5 details the mean computation time
 418 spent on each time-step of the simulation. A blank simulation –ran without computing
 419 the terms related to bioreaction or population balance– is shown in order to estimate and
 420 distinguish the actual models computation time from the time spent on other tasks in the
 421 software.

422 The class method is a direct one, the computation time is mainly spent on (i) computing
 423 the metabolic model from Pigou and Morchain (2015) for each class and (ii) computing the
 424 redistribution term of the PBE as detailed in Morchain et al. (2016) for each class, which
 425 implies computing $NC + 1$ values of the Owen’s T function using 10-nodes Gauss-Legendre
 426 quadratures (with NC the number of classes).

427 All method of moments must compute the first N moments of the skewnormal distri-
 428 bution which is not expensive considering that their expressions are available. The major
 429 computational cost then comes from (i) establishing the quadrature rule and (ii) computing
 430 the metabolic model for each node of the quadrature.

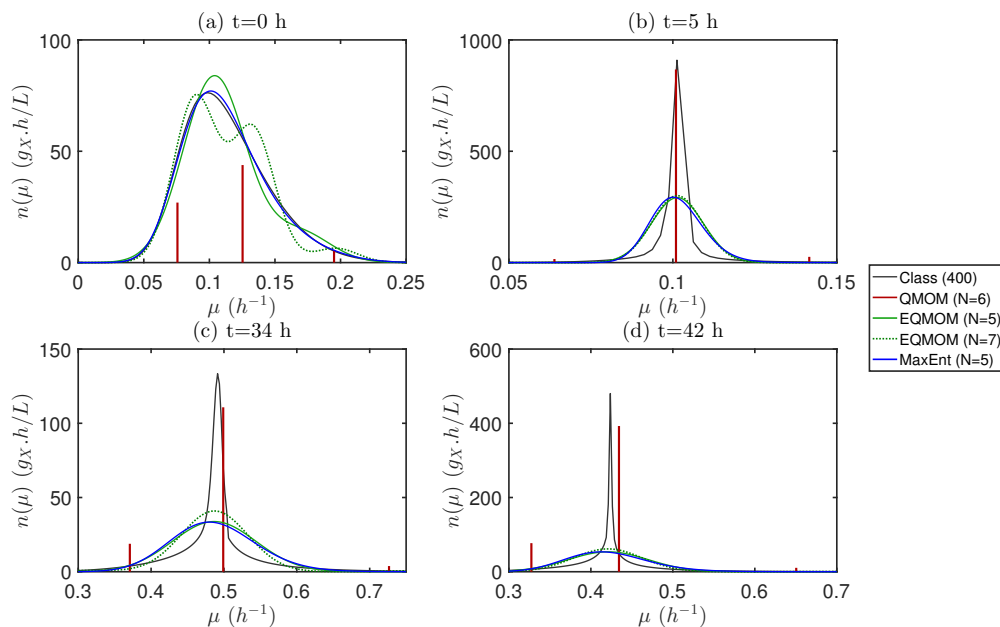


Figure 3: Comparison of reconstructed distributions against distribution resolved by class. An arbitrary scale is used for the Dirac distribution (QMOM).

431 In this regard, QMOM is the least expensive method: the quadrature rule is computed
 432 using directly either the Product-Difference Algorithm (PDA) or the Wheeler Algorithm
 433 (WA), both consisting in computing the eigenvalues and eigenvectors of a particular $N/2 \times$
 434 $N/2$ matrix, and computing the metabolic model for $N/2$ nodes. The WA seems to be
 435 slightly faster than the PDA.

436 In order to establish a quadrature rule with the EQMOM method, Marchisio and Fox
 437 (2013) detail the analytical solution for $N = 3$ and a solution whose cost is hardly higher
 438 than a 2 nodes QMOM for $N = 5$, which explains the low computation times for these
 439 two orders of resolution. The case $N = 7$ needs an iterative algorithm to find the suited
 440 quadrature rule, based on a dichotomic method. We speed-up that method by making use

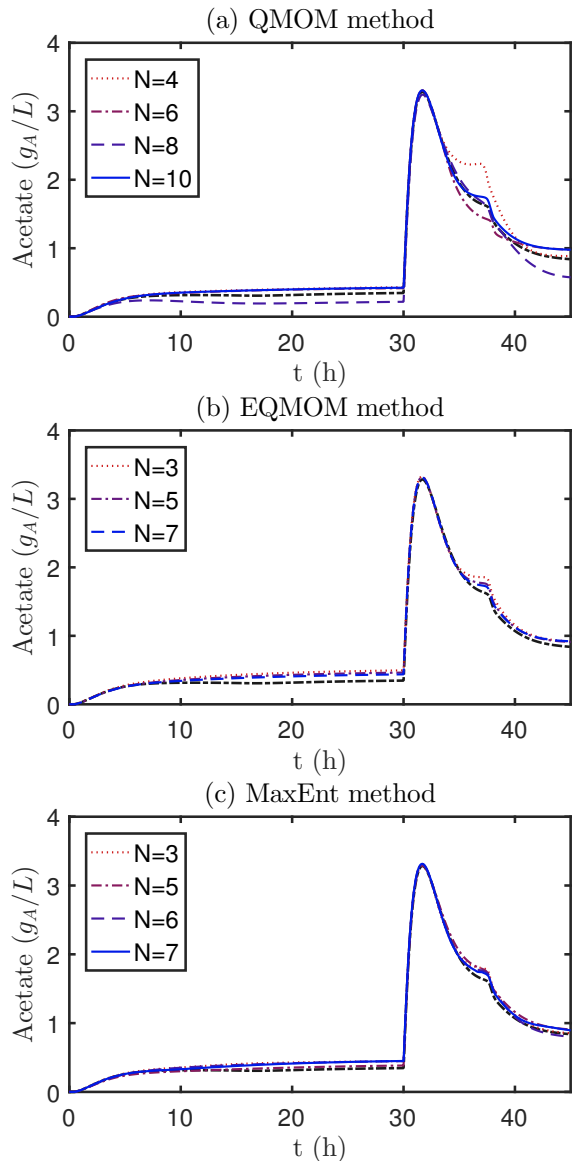


Figure 4: Evolution of acetate concentrations as predicted by the *E. coli* metabolic model. Black dash-dotted line: results from class method.

441 of the result from the previous timestep, the dichotomic algorithm then converges most of
 442 the time in 3 to 6 evaluation of the objective function, each of which requiring a single call
 443 to the WA.

444 Finally, MaxEnt is the most expensive method. It is actually as fast as QMOM and
 445 EQMOM when the moment set is far from the frontier of the moment space, but our model
 446 often produces moment sets near the frontier. Then, we slow down the method by using
 447 different tweaks in order to stabilise it: (i) the adaptive quadrature proposed by (Vié et al.,
 448 2013), (ii) the dynamic adaptation of the distribution’s support and (iii) the computation
 449 of canonical moments to check realizability of the moment set. The underlying Newton-
 450 Raphson procedure often converges in 0 to 1 iterations, but this number increases up to 10
 451 for many time-steps after the dilution rate shift, so simulating the next few hours following
 452 this shift is actually as long as computing the rest of the time range.

453 3.2. Fedbatch culture - Vrabel et al.

454 We simulated the very same fedbatch culture described with a 70 compartments hydro-
 455 dynamic model by Vrabel et al. (2001) but using our own biological modelling as detailed
 456 in Pigou and Morchain (2015). Here, we reproduce these simulations, by using the methods
 457 of moments to solve the population balance model. The QMOM method is applied with 5
 458 nodes (N=10) as this seemed to be required to produce the same results than the EQMOM
 459 and MaxEnt methods (Figures 2 and 4). The MaxEnt method is used with N=5 moments as
 460 we did not manage to increase the number of moments up to 7 in this setup due to stability
 461 issues and also because, surprisingly, the prediction of acetate production was actually better
 462 with 5 moments than with 7 moments (see Figure 4c). Finally, EQMOM was also applied
 463 with N=5 moments as going up to 7 moments did not increase the precision drastically
 464 (Figure 4b) but did increase significantly the computation time (Figure 5). This will also
 465 make the comparison between MaxEnt and EQMOM more relevant.

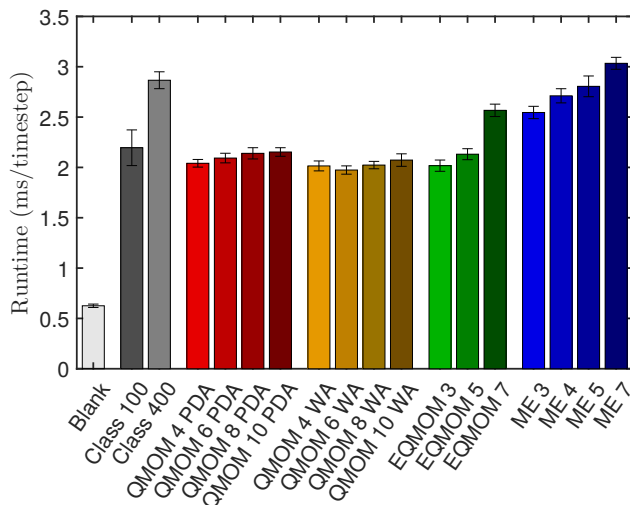


Figure 5: Mean run-time per timestep for each method and different orders (ms/ts) (\pm standard deviation measured on 20 simulations per method and order)

466 In order to enforce the consistency of numerical results, we limit the maximum value of
 467 the time-step to the minimum compartment mean-residence-time:

$$\delta t_{\max} = \min_{n=1}^{N_c} \left(\frac{V_n}{\sum_{m=1}^{N_c} Q_{n,m}} \right) \quad (31)$$

468 The value of the maximum time-step for the compartment model shown in Figure 6 is
 469 $\delta t_{\max} = 1.47 \cdot 10^{-5} h$.

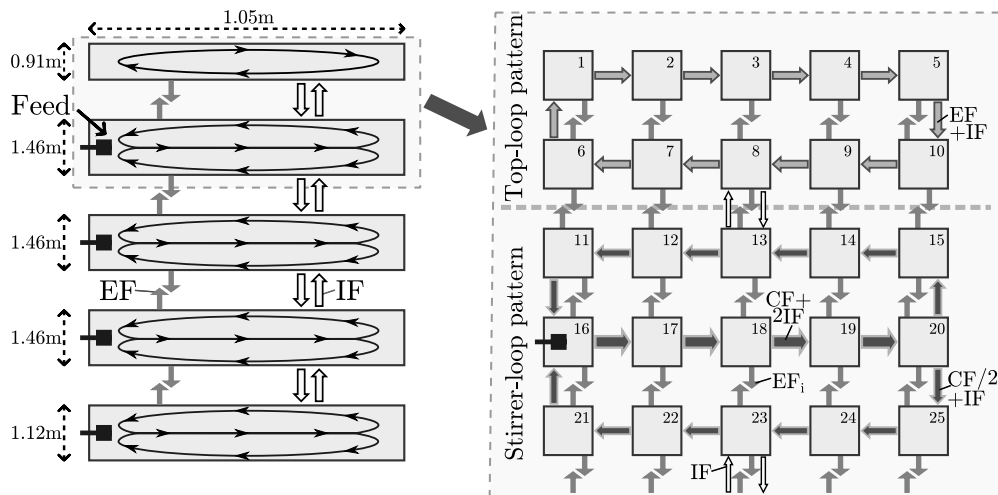


Figure 6: Representation of the macroscopic flow patterns in the fedbatch reactor (left) and details of its compartmentalization and specific flows for the top of the reactor (right). Values for the flow rates CF, IF and EF are given in Pigou and Morchain (2015), appendix B.

470 The Figure 7 gathers the results in term of glucose, total biomass and acetate concen-
 471 trations as well as mean population reaction rates. The plotted values are mean values at
 472 different heights (volumetric mean value over compartments of the same row). The three
 473 heights (top, middle and bottom) correspond to the following compartments (see Figure 6
 474 for numbering):

- 475 • top: compartments 11 to 15
- 476 • middle: compartments 36 to 40
- 477 • bottom: compartments 61 to 65

478 The good agreements between the methods is related to the fact that, in the heteroge-
 479 neous large-scale reactor, the distribution is continuously perturbed by external fluctuations
 480 which prevent the apparition of the narrow distribution seen previously (Figure 3). The
 481 expected distribution has a smoother shape which is well reconstructed by MaxEnt and
 482 EQMOM as shown in Figure 8.

483 Finally, we ran 5 times the first hour of simulation in order to gather statistics about
 484 simulation runtimes in the heterogeneous case with different orders of resolution. The results
 485 are shown in Figure 9.

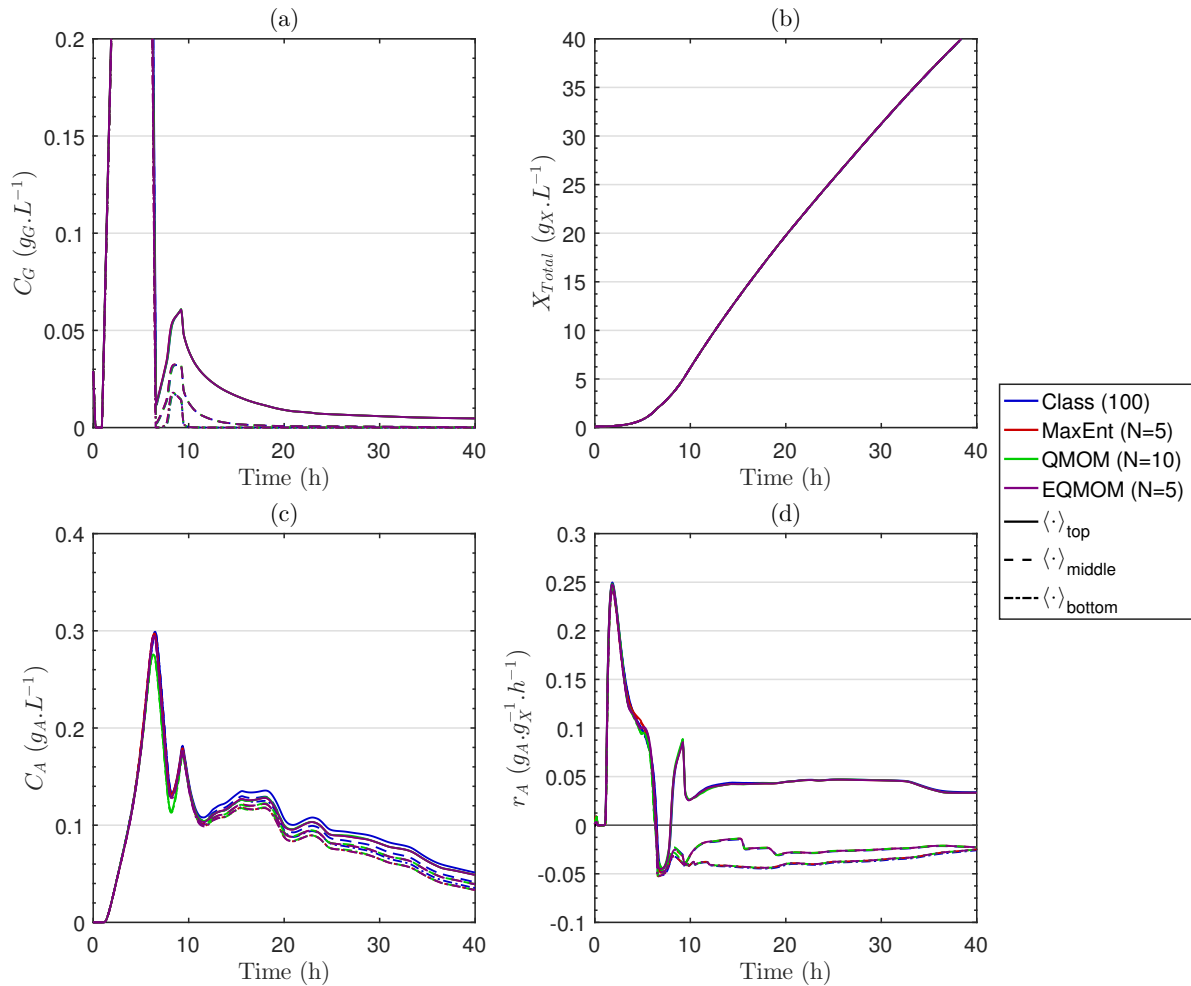


Figure 7: Simulation results for the different population balance methods in the heterogeneous fedbatch culture. (a) Glucose concentration, (b) Total biomass concentration, (c) Acetate concentration and (d) Acetate specific production rate.

486 Each CPU core had to perform calculations for 14 compartments in figure 9 while a single
 487 compartment was considered in figure 5 which explains the overall higher computation times.
 488 However, the previous analysis about the comparison of the complexity of each method
 489 remains the same, and the observations on the heterogeneous case are the same than in the
 490 homogeneous case : QMOM maintains a constant computation time, EQMOM is as fast as
 491 QMOM as long as $N \leq 5$ and MaxEnt is slower than other methods due to the stabilisation
 492 of the method.

493 4. Discussion

494 Dealing with a biological phase naturally leads to the use of the “population” semantic
 495 field due to the individual nature of cells, each of which having its own set of properties and

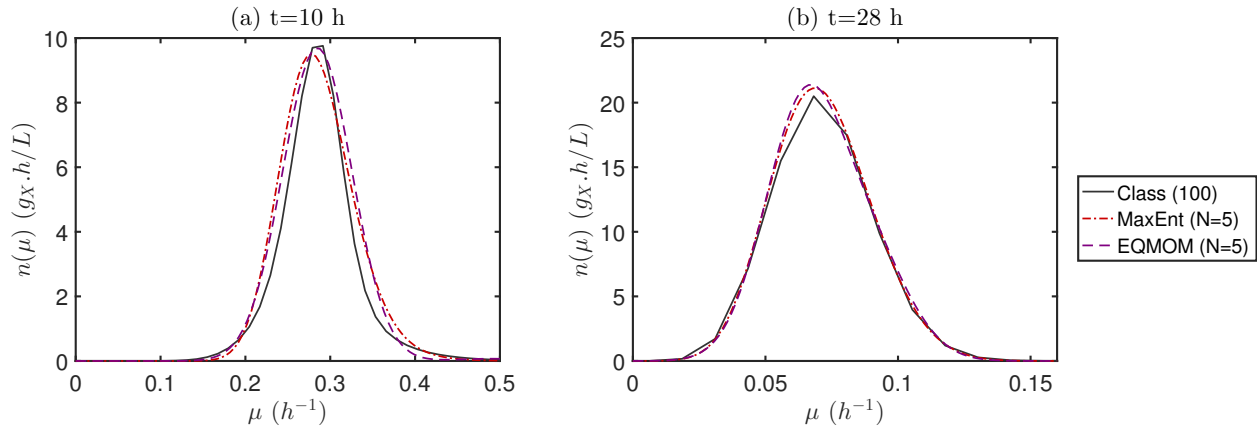


Figure 8: Comparison of distribution shapes as resolved by the class method and reconstructed by the EQMOM and MaxEnt methods both with $N = 5$ moments.

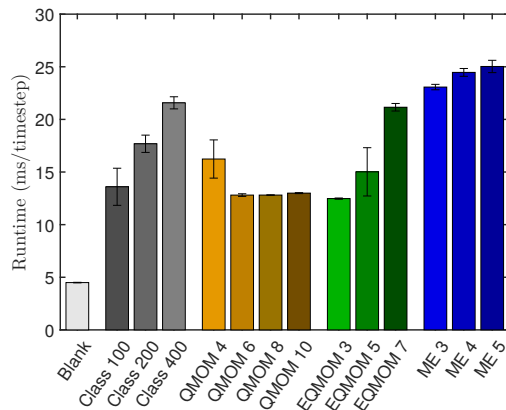


Figure 9: Comparison of simulation runtimes for each method (ms/ts) (\pm standard deviation measured on 5 simulations per method and order). Simulations performed using 5 CPU cores.

496 its own “memory”. Hence, the use of a Population Balance Model to describe a biological
 497 population seems to be obvious, almost axiomatic.

498 The most natural way to solve a PBM is the class method, which constitutes a direct
 499 resolution of the equations. However, its accuracy comes with the price of a high memory
 500 cost. Unpublished data show that for simple batch and chemostat simulations, the results
 501 are dependent on the number of classes up to 60 classes, and we can even notice differences
 502 between 100 and 400 classes in figure 2a. This number of classes is needed to span the entire
 503 property space with sufficient accuracy, however simulations clearly show that most of the
 504 time a large fraction of classes are nearly empty. This means that we allocate memory for
 505 variables that most of the time carry almost no information, but still happen sometime to
 506 be used, depending on the state of the population.

507 This explains why we are shifting toward methods of moments. They resolve basic prop-
 508 erties of the distribution (total number, mean, variance, skewness, flatness, ...) which all
 509 contain useful information no matter the state of the population. Moments gather higher

510 entropy about the distribution than classes, in the sense of information theory. This sig-
511 nificantly reduces the required number of resolved variables, from more than 60, to half a
512 dozen.

513 For some applications, each equation of the model can be formulated in terms of moments
514 (Hulburt and Katz, 1964; McGraw, 1997) leading to closed formulations or easy closure
515 through the used of quadrature based methods. In these cases, the accuracy of the methods
516 of moments poses no question –and is even better than a class method considering that
517 the latter induces numerical diffusion in the parameter space– for a smaller memory and
518 computational cost.

519 Unfortunately, we deal here with a metabolic complexity that offers no model formulation
520 in terms of moments. We tackle this issue by using reconstruction methods, namely QMOM,
521 EQMOM and MaxEnt methods; but these methods introduce quadrature inaccuracy as well
522 as extra computational cost, which we tried to quantify in our simulations.

523 The results in terms of concentration fields are really promising, as the biomass, glucose
524 and acetate concentrations were well reproduced both in the homogeneous and the heteroge-
525 neous cases. We mainly noticed slight errors consisting in an over-production of acetate with
526 moment methods in the Katterer case (see Figure 4) due to difficulties in reconstructing a
527 narrow distribution with a wide base (similar to a Laplace distribution). However, we are
528 shifting toward moment methods only to perform large-scale simulations at low memory cost:
529 the class method performs just fine enough for homogeneous cases. The crucial comparison
530 must then be made on the large-scale simulation.

531 In Figure 7, we observe a surprisingly good agreement between the class method and the
532 moment methods. The only noticeable difference is seen on acetate curves for the moment
533 methods which slightly underestimate the acetate production for $t \approx 10h$ which induces
534 a persistent shift along time when compared to the class method. On this regard, the
535 accuracy for variables whose value is of importance (substrate and product concentrations)
536 is satisfactory for all methods.

537 In terms of computational cost, which we evaluate through the simulation time, Yuan
538 et al. (2012) already performed a comparison of EQMOM and the MaxEnt methods. They
539 observed that EQMOM was a hundred times faster than MaxEnt for the reconstruction
540 of two NDF. However, we do not feel that their comparison is fair: the slow convergence
541 of MaxEnt is only due to a bad initialization of the Newton-Raphson procedure, similar to
542 what we observe in our simulations for the very first time-step. We want to supplement their
543 observations by pointing out that when used in time resolved simulations, which happens
544 to be our specific application for these methods, the MaxEnt method performs only slightly
545 slower than EQMOM (see Figures 5 and 9) due to different adjustments made in order to
546 improve stability.

547 We do not develop nor try to promote a specific reconstruction method, but only want
548 to draw general guidelines about which method should be used for the simulation of large-
549 scale bioreactors. We then did our best to keep the comparison of the methods as fair as
550 possible. On the basis of our results, here are the key observations we made about the
551 different methods.

552 EQMOM is a stable method: it behaves well near the moment space frontier and we
553 did not notice any particular difficulty when increasing the number of resolved moments.

554 When used on monomodal distribution, it can be applied at a low computational cost with
555 3 or 5 moments, thanks to analytical solutions (Marchisio and Fox, 2013). The possibility
556 of increasing the number of resolved moments means that this method is also well suited
557 to reconstruct multi-modal distributions, this will be useful when tracking fast population
558 dynamics in heterogeneous systems. Moreover, the method embeds the principle of nested
559 quadratures: a relevant Gauss-Hermite quadrature can be constructed on each Gaussian node
560 of the EQMOM reconstruction, which helps performing efficiently the integration of Eq. 2.
561 This can be an important advantage of this method if the metabolic model (computation of
562 Φ) is computationally expensive. Here, the metabolic model was easy enough to compute,
563 which hide this salient feature of EQMOM reconstructions.

564 The same level of accuracy than EQMOM with 5 moments could be reached with QMOM
565 using 10 moments with a similar computation time, but with less calls to the metabolic model.
566 Both methods can then be used similarly, based on whether we try to reduce the memory
567 usage or the number of calls to a potentially complex metabolic model.

568 MaxEnt is known to be ill-conditioned near the boundaries of the moment space (Massot
569 et al., 2010) or when the number of resolved moments increases (Gzyl and Tagliani, 2010),
570 in particular we did not manage to perform simulations using this method and more than 7
571 resolved moments, or even 5 moments in the heterogeneous case. This comes from the fact
572 that we describe quite narrow distributions on a large support, which naturally correspond to
573 moments near the frontier of the moment space. When the method is working, it might give a
574 better reconstruction with 5 moments than EQMOM with 7 moments (Figure 3a), however,
575 using this reconstruction to construct a relevant quadrature rule is more difficult than for
576 EQMOM. We then recommend its use when assessing slow dynamics (preserving mono-
577 modal distribution in heterogeneous systems) for simulations where the time-step is negligible
578 compared to the characteristic time of moment evolution (to ensure a good initialization),
579 and only if a method can be designed to form a set of moment far enough from the frontier
580 of the moment space. These are quite restrictive conditions which do not make this method
581 the more advisable.

582 Finally, in terms of memory footprint, we managed to reduce the number of resolved
583 variables to describe the population from about a hundred (class method) to about only
584 5 variables which will be significant when moving toward CFD simulations of bioreactors.
585 However, it should be noted that for MaxEnt, memory registers must be allocated both for
586 the transported moments and for the vector of polynomial coefficients φ which serves as ini-
587 tial value for the Newton-Raphson procedure. MaxEnt then requires twice as much memory
588 space than QMOM and EQMOM methods for equivalent number of resolved moments.

589 The significant improvements in terms of memory usage will be even more significant
590 when we will shift toward multivariate population balance models. For a bivariate distribu-
591 tion, the number of classes or moments will roughly be squared leading to about 10^4 classes
592 opposed to 25 moments in each geometrical mesh.

593 5. Conclusions

594 The point of applying population balance based modelling for the predictive simulation
595 of heterogeneous bioreactors is now well established (Morchain et al., 2014, 2016; Pigou and

596 Morchain, 2015; Heins et al., 2015; Bertuccio et al., 2015; Fredrickson and Mantzaris, 2002).
597 This paper is more focused on numerical methods to solve the population balance model,
598 in order to shift from a class method to moment based methods. In our modelling, the
599 reconstruction methods of a NDF from a finite set of moments is required for the computa-
600 tion of the population metabolic behaviour. We then implemented QMOM, EQMOM and
601 Maximum Entropy methods, and challenged them in terms of stability, memory footprint,
602 computational cost and accuracy against class method results.

603 At equivalent number of resolved moments, QMOM is noticeably less accurate than
604 EQMOM and MaxEnt. However, increasing the number of moments for QMOM does not
605 increase significantly the computation time, which make this method competitive with the
606 others when looking only at accuracy and simulation runtime.

607 If reducing the memory footprint is the main concern, EQMOM actually reaches the
608 same accuracy than QMOM with half the number of resolved moments. However, its com-
609 putational cost increases significantly between 5 and 7 resolved moments, due to the need of
610 an iterative procedure rather than an analytical or direct solution.

611 Depending on the use case, MaxEnt has often been reported as an interesting method
612 (Massot et al., 2010; Vié et al., 2013; Lebaz et al., 2016), however, we will tend to discard it for
613 our future works. Indeed, even when the method is well-conditioned, it is not particularly
614 competitive with EQMOM in terms of computation time and accuracy, but comes with
615 twice the memory usage of EQMOM. Moreover, the method tends to be quickly unstable if
616 moments are near the limit of realizability. This poses problem for our modelling as the lack of
617 experimental data about the dynamics of internal biological properties will make us formulate
618 models which tend toward narrow distributions until data are available. An example of that
619 is the PBM from Pigou and Morchain (2015) which led to a Dirac distribution in steady-state
620 homogeneous systems until experimental data from Nobs and Maerkl (2014); Yasuda (2011)
621 allowed us to improve the PBM and add an experimentally justified redistribution term as
622 explained in Morchain et al. (2016).

623 Overall, the QMOM and EQMOM methods have shown to be accurate and stable enough
624 for the simulation of a large scale bioreactor with a significantly reduced memory impact
625 and a simulation time of the same order of magnitude than the class method.

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629 **Notation**

630 *Roman*

C : Concentration ($kg.m^{-3}$)
 H : Shannon entropy
 K : Biological affinity constant ($kg.m^{-3}$)
 L : Quadrature node abscissae (h^{-1})
 m : Moment of distribution n ($kg.m^{-3}.h^{-k}$)
 n : Number density function ($h.kg_X.m^{-3}$)
 N : Number of resolved moments
 NC : Number of classes
 N_c : Number of compartments
 O : Order of (E)QMOM method
 q : Specific reaction rate ($mol.kg_X^{-1}.h^{-1}$)
 Q : Flow rate ($m^3.h^{-1}$)
 R : Reaction rate ($kg.m^{-3}.h^{-1}$)
 T : Time constant of adaptation (h)
 V : Compartment volume (m^3)
 w : Quadrature node weight ($kg_X.m^{-3}$)
 Y : Stoichiometric molar coefficient ($mol.mol^{-1}$)

631 *Subscript and Superscript*

\tilde{x} : Population mean value
 x^* : Equilibrium value
 x_a : Achieved value
 x_A : Acetate
 x_G : Glucose
 x_i : Inhibition
 x_k : Moment order
 x_m : Compartment index
 x_n : Compartment index
 x_O : Oxygen
 x_T : Threshold value

ε : Turbulent energy dissipation rate ($W.kg^{-1}$)

κ : PDF Kernel

μ : Growth rate ($g_X.g_X^{-1}.h^{-1}$)

ν : Kinematic viscosity ($m^2.s^{-1}$)

φ : Polynomial coefficient

Φ : Specific uptake rate ($g.g_X^{-1}.h^{-1}$)

Ψ : Environmental limitation coefficient

σ : Standard deviation (h^{-1})

ζ : rate of change of specific growth rate (h^{-2})

633 Literature Cited

- 634 Abramov, R.V., 2007. An improved algorithm for the multidimensional moment-constrained
635 maximum entropy problem. *Journal of Computational Physics* 226, 621–644. doi:10.1016/
636 j.jcp.2007.04.026.
- 637 Abulesz, E.M., Lyberatos, G., 1989. Periodic operation of a continuous culture of baker's
638 yeast. *Biotechnology and Bioengineering* 34, 741–749. doi:10.1002/bit.260340603.
- 639 Athanassoulis, G., Gavriliadis, P., 2002. The truncated hausdorff moment problem solved by
640 using kernel density functions. *Probabilistic Engineering Mechanics* 17, 273–291. doi:10.
641 1016/S0266-8920(02)00012-7.
- 642 Baldyga, J., Bourne, J.R., 1999. *Turbulent Mixing and Chemical Reactions*. John Wiley
643 and Sons.
- 644 Bertucco, A., Sforza, E., Fiorenzato, V., Strumendo, M., 2015. Population balance mod-
645 eling of a microalgal culture in photobioreactors: Comparison between experiments and
646 simulations. *AIChE Journal* 61, 2702–2710. doi:10.1002/aic.14893.
- 647 Bezzo, F., Macchietto, S., Pantelides, C.C., 2003. General hybrid multizonal/CFD approach
648 for bioreactor modeling. *AIChE Journal* 49, 2133–2148. doi:10.1002/aic.690490821.
- 649 Bogacki, P., Shampine, L., 1989. A 3(2) pair of Runge-Kutta formulas. *Applied Mathematics*
650 *Letters* 2, 321–325. doi:10.1016/0893-9659(89)90079-7.
- 651 Chalons, C., Fox, R.O., Massot, M., 2010. A multi-Gaussian quadrature method of moments
652 for gas-particle flows in a LES framework, in: *Proceedings of the 2010 Summer Program,*
653 *Center for turbulence Research*. Stanford University. pp. 347–358.
- 654 Cui, Y.Q., van der Lans, R.G., Noorman, H.J., Luyben, K.C.A.M., 1996. Compartment
655 mixing model for stirred reactors with multiple impellers. *Chemical Engineering Research*
656 *and Design* 74, 261–271.

- 657 Dette, H., Studden, W.J., 1997. The theory of canonical moments with applications in
658 statistics, probability, and analysis. John Wiley & Sons, New York; Chichester.
- 659 Elqotbi, M., Vlaev, S., Montastruc, L., Nikov, I., 2013. CFD modelling of two-phase stirred
660 bioreaction systems by segregated solution of the euler-euler model. Computers & Chem-
661 ical Engineering 48, 113–120. doi:10.1016/j.compchemeng.2012.08.005.
- 662 Enfors, S.O., Jahic, M., Rozkov, A., Xu, B., Hecker, M., Jürgen, B., Krüger, E., Schweder,
663 T., Hamer, G., O’Beirne, D., Noisommit-Rizzi, N., Reuss, M., Boone, L., Hewitt, C.,
664 McFarlane, C., Nienow, A., Kovacs, T., Trägårdh, C., Fuchs, L., Revstedt, J., Friberg,
665 P., Hjertager, B., Blomsten, G., Skogman, H., Hjort, S., Hoeks, F., Lin, H.Y., Neubauer,
666 P., van der Lans, R., Luyben, K., Vrábel, P., Å. Manelius, 2001. Physiological responses
667 to mixing in large scale bioreactors. Journal of Biotechnology 85, 175–185. doi:10.1016/
668 S0168-1656(00)00365-5. twenty years of the European Federation of Biotechnology.
- 669 Ferenci, T., 1996. Adaptation to life at micromolar nutrient levels: the regulation of *Es-*
670 *cherichia coli* glucose transport by endoinduction and cAMP. FEMS Microbiol Rev 18,
671 301–317. doi:10.1111/j.1574-6976.1996.tb00246.x.
- 672 Ferenci, T., 1999. Regulation by nutrient limitation. Curr Opin Microbiol 2, 208–213.
673 doi:10.1016/S1369-5274(99)80036-8.
- 674 Fredrickson, A., Mantzaris, N.V., 2002. A new set of population balance equations for
675 microbial and cell cultures. Chemical Engineering Science 57, 2265 – 2278. doi:10.1016/
676 S0009-2509(02)00116-1.
- 677 Gzyl, H., Tagliani, A., 2010. Hausdorff moment problem and fractional moments. Applied
678 Mathematics and Computation 216, 3319–3328. doi:10.1016/j.amc.2010.04.059.
- 679 Haringa, C., Tang, W., Deshmukh, A.T., Xia, J., Reuss, M., Heijnen, J.J., Mudde, R.F.,
680 Noorman, H.J., 2016. Euler-Lagrange computational fluid dynamics for (bio)reactor scale
681 down: An analysis of organism lifelines. Engineering in Life Sciences doi:10.1002/elsc.
682 201600061.
- 683 Heavner, B.D., Smallbone, K., Barker, B., Mendes, P., Walker, L.P., 2012. Yeast 5 - an ex-
684 expanded reconstruction of the *Saccharomyces cerevisiae* metabolic network. BMC Systems
685 Biology 6. doi:10.1186/1752-0509-6-55.
- 686 Heavner, B.D., Smallbone, K., Price, N.D., Walker, L.P., 2013. Version 6 of the consensus
687 yeast metabolic network refines biochemical coverage and improves model performance.
688 Database 2013. doi:10.1093/database/bat059.
- 689 Heins, A.L., Fernandes, R.L., Gernaey, K.V., Lantz, A.E., 2015. Experimental and in silico
690 investigation of population heterogeneity in continuous *Saccharomyces cerevisiae* scale-
691 down fermentation in a two-compartment setup. Journal of Chemical Technology and
692 Biotechnology 90, 324–340. doi:10.1002/jctb.4532.

- 693 Hulburt, H., Katz, S., 1964. Some problems in particle technology: A statistical mechanical
694 formulation. *Chemical Engineering Science* 19, 555–574. doi:10.1016/0009-2509(64)
695 85047-8.
- 696 John, V., Angelov, I., Öncül, A., Thévenin, D., 2007. Techniques for the reconstruction of
697 a distribution from a finite number of its moments. *Chemical Engineering Science* 62,
698 2890–2904. doi:10.1016/j.ces.2007.02.041.
- 699 Kapur, J., 1989. *Maximum-entropy Models in Science and Engineering*. Wiley.
- 700 Kätterer, L., Allemann, H., Käppeli, O., Fiechter, A., 1986. Transient responses of contin-
701 uously growing yeast cultures to dilution rate shifts: A sensitive means to analyze biol-
702 ogy and the performance of equipment. *Biotechnology and Bioengineering* 28, 146–150.
703 doi:10.1002/bit.260280126.
- 704 Kumar, S., Ramkrishna, D., 1996a. On the solution of population balance equations by
705 discretization - I. A fixed pivot technique. *Chemical Engineering Science* 51, 1311–1332.
706 doi:10.1016/0009-2509(96)88489-2.
- 707 Kumar, S., Ramkrishna, D., 1996b. On the solution of population balance equations by
708 discretization - II. A moving pivot technique. *Chemical Engineering Science* 51, 1333–
709 1342. doi:10.1016/0009-2509(95)00355-X.
- 710 Lebaz, N., Cockx, A., Spérandio, M., Morchain, J., 2016. Reconstruction of a distribution
711 from a finite number of its moments: A comparative study in the case of depolymerization
712 process. *Computers & Chemical Engineering* 84, 326–337. doi:10.1016/j.compchemeng.
713 2015.09.008.
- 714 Li, W., 1982. Estimating heterotrophic bacterial productivity by inorganic radiocarbon
715 uptake: importance of establishing time courses of uptake. *Deep Sea Research Part B.*
716 *Oceanographic Literature Review* 29, 167–172. doi:10.1016/0198-0254(82)90325-9.
- 717 Linkès, M., Fede, P., Morchain, J., Schmitz, P., 2014. Numerical investigation of subgrid
718 mixing effects on the calculation of biological reaction rates. *Chemical Engineering Science*
719 116, 473–485. doi:10.1016/j.ces.2014.05.005.
- 720 Lu, H., Li, C., Tang, W., Wang, Z., Xia, J., Zhang, S., Zhuang, Y., Chu, J., Noor-
721 man, H., 2015. Dependence of fungal characteristics on seed morphology and shear
722 stress in bioreactors. *Bioprocess and Biosystems Engineering* 38, 917–928. doi:10.1007/
723 s00449-014-1337-8.
- 724 Madadi-Kandjani, E., Passalacqua, A., 2015. An extended quadrature-based moment
725 method with log-normal kernel density functions. *Chemical Engineering Science* 131,
726 323–339. doi:10.1016/j.ces.2015.04.005.
- 727 Mantzaris, N.V., Daoutidis, P., Sreenc, F., 2001. Numerical solution of multi-variable cell
728 population balance models: I. finite difference methods. *Computers & Chemical Engineer-*
729 *ing* 25, 1411–1440. doi:10.1016/S0098-1354(01)00709-8.

- 730 Marchisio, D., Fox, R., 2013. Computational Models for Polydisperse Particulate and Multi-
731 phase Systems. Cambridge Series in Chemical Engineering, Cambridge University Press.
- 732 Marchisio, D.L., Piktorna, J.T., Fox, R.O., Vigil, R.D., Barresi, A.A., 2003a. Quadrature
733 method of moments for population-balance equations. *AIChE Journal* 49, 1266–1276.
734 doi:10.1002/aic.690490517.
- 735 Marchisio, D.L., Vigil, R., Fox, R.O., 2003b. Quadrature method of moments for aggregation-
736 breakage processes. *Journal of Colloid and Interface Science* 258, 322–334. doi:10.1016/
737 S0021-9797(02)00054-1.
- 738 Marchisio, D.L., Vigil, R.D., Fox, R.O., 2003c. Implementation of the quadrature method of
739 moments in CFD codes for aggregation-breakage problems. *Chemical Engineering Science*
740 58, 3337–3351. doi:10.1016/S0009-2509(03)00211-2.
- 741 Massot, M., Laurent, F., Kah, D., De Chaisemartin, S., 2010. A robust moment method
742 for evaluation of the disappearance rate of evaporating sprays. *SIAM Journal on Applied*
743 *Mathematics* 70, 3203–3234. doi:10.1137/080740027.
- 744 Matsuoka, Y., Shimizu, K., 2013. Catabolite regulation analysis of *Escherichia coli* for
745 acetate overflow mechanism and co-consumption of multiple sugars based on systems
746 biology approach using computer simulation. *Journal of Biotechnology* 168, 155–173.
747 doi:10.1016/j.jbiotec.2013.06.023. special issue: Biotechnology for a healthy and
748 green world.
- 749 Mayr, B., Horvat, P., Nagy, E., Moser, A., 1993. Mixing-models applied to industrial batch
750 bioreactors. *Bioprocess Engineering* 9, 1–12. doi:10.1007/BF00389534.
- 751 McGraw, R., 1997. Description of aerosol dynamics by the quadrature method of moments.
752 *Aerosol Science and Technology* 27, 255–265. doi:10.1080/02786829708965471.
- 753 Mead, L.R., Papanicolaou, N., 1984. Maximum entropy in the problem of moments. *Journal*
754 *of Mathematical Physics* 25, 2404–2417.
- 755 Meadows, A.L., Karnik, R., Lam, H., Forestell, S., Snedecor, B., 2010. Application of
756 dynamic flux balance analysis to an industrial *Escherichia coli* fermentation. *Metabolic*
757 *Engineering* 12, 150–160. doi:10.1016/j.ymben.2009.07.006. metabolic Flux Analysis
758 for Pharmaceutical Production Special Issue.
- 759 Morchain, J., Gabelle, J.C., Cockx, A., 2013. Coupling of biokinetic and population balance
760 models to account for biological heterogeneity in bioreactors. *AIChE Journal* 59, 369–379.
761 doi:10.1002/aic.13820.
- 762 Morchain, J., Gabelle, J.C., Cockx, A., 2014. A coupled population balance model and CFD
763 approach for the simulation of mixing issues in lab-scale and industrial bioreactors. *AIChE*
764 *Journal* 60, 27–40. doi:10.1002/aic.14238.

- 765 Morchain, J., Pigou, M., Lebaz, N., 2016. A population balance model for bioreactors com-
766 bining interdivision time distributions and micromixing concepts. *Biochemical Engineering*
767 *Journal* , In press doi:10.1016/j.bej.2016.09.005.
- 768 Nobs, J.B., Maerkl, S.J., 2014. Long-term single cell analysis of *S. pombe* on a microfluidic
769 microchemostat array. *PLoS ONE* 9. doi:10.1371/journal.pone.0093466.
- 770 Orth, J.D., Conrad, T.M., Na, J., Lerman, J.A., Nam, H., Feist, A.M., Palsson, B.O., 2011.
771 A comprehensive genome-scale reconstruction of *Escherichia coli* metabolism. *Molecular*
772 *Systems Biology* 7. doi:10.1186/1752-0509-6-55.
- 773 Perret, C.J., 1960. A new kinetic model of a growing bacterial population. *Microbiology* 22,
774 589–617. doi:10.1099/00221287-22-3-589.
- 775 Pigou, M., Morchain, J., 2015. Investigating the interactions between physical and biolog-
776 ical heterogeneities in bioreactors using compartment, population balance and metabolic
777 models. *Chemical Engineering Science* 126, 267–282. doi:10.1016/j.ces.2014.11.035.
- 778 Silveston, P., Budman, H., Jervis, E., 2008. Forced modulation of biological processes:
779 A review. *Chemical Engineering Science* 63, 5089–5105. doi:10.1016/j.ces.2008.06.
780 017. 5TH Unsteady-State Processes in Catalysis: a Special Issue of *Chemical Engineering*
781 *Science*.
- 782 Tagliani, A., 1999. Hausdorff moment problem and maximum entropy: A unified approach.
783 *Applied Mathematics and Computation* 105, 291–305. doi:10.1016/S0096-3003(98)
784 10084-X.
- 785 Vié, A., Laurent, F., Massot, M., 2013. Size-velocity correlations in hybrid high order
786 moment/multi-fluid methods for polydisperse evaporating sprays: Modeling and numerical
787 issues. *Journal of Computational Physics* 237, 177–210. doi:10.1016/j.jcp.2012.11.043.
- 788 Vrábel, P., van der Lans, R.G., Luyben, K.C., Boon, L., Nienow, A.W., 2000. Mixing in
789 large-scale vessels stirred with multiple radial or radial and axial up-pumping impellers:
790 modelling and measurements. *Chemical Engineering Science* 55, 5881–5896. doi:10.1016/
791 S0009-2509(00)00175-5.
- 792 Vrábel, P., van der Lans, R.G., van der Schot, F.N., Luyben, K.C., Xu, B., Enfors, S.O.,
793 2001. CMA: integration of fluid dynamics and microbial kinetics in modelling of large-scale
794 fermentations. *Chemical Engineering Journal* 84, 463–474. doi:10.1016/S1385-8947(00)
795 00271-0.
- 796 Vrábel, P., der Lans, R.V., Cui, Y., Luyben, K., 1999. Compartment model approach:
797 Mixing in large scale aerated reactors with multiple impellers. *Chemical Engineering*
798 *Research and Design* 77, 291–302. doi:10.1205/026387699526223.
- 799 Xu, B., Jahic, M., Enfors, S.O., 1999. Modeling of overflow metabolism in batch and
800 fed-batch cultures of *Escherichia coli*. *Biotechnology Progress* 15, 81–90. doi:10.1021/
801 bp9801087.

- 802 Yasuda, K., 2011. Algebraic and geometric understanding of cells: Epigenetic inheritance of
803 phenotypes between generations, in: Müller, S., Bley, T. (Eds.), High Resolution Microbial
804 Single Cell Analytics. Springer Berlin Heidelberg. volume 124 of *Advances in Biochemical*
805 *Engineering / Biotechnology*, pp. 55–81. doi:10.1007/10_2010_97.
- 806 Yuan, C., Laurent, F., Fox, R., 2012. An extended quadrature method of moments for popu-
807 lation balance equations. *Journal of Aerosol Science* 51, 1–23. doi:10.1016/j.jaerosci.
808 2012.04.003.

809 **Appendix A. Moment formulation of the PBE**

810 As a recall, the population balance equation is defined as

$$\frac{\partial n(\mu)}{\partial t} = -\frac{\partial}{\partial \mu} [n(\mu)\zeta(\mu)] + \int_0^{+\infty} \beta(\mu, \mu')n(\mu')\Psi\mu'd\mu' \quad (\text{A.1})$$

811 and the k -th order moment of the distribution $n(\mu)$ is defined by

$$m_k = \int_0^{+\infty} \mu^k n(\mu) d\mu \quad (\text{A.2})$$

812 We want to formulate the law of moments evolution, as the sum of contributions from
813 an adaptation term $\left(\frac{\partial m_{a,k}(t)}{\partial t}\right)$, and a growth term $\left(\frac{\partial m_{g,k}(t)}{\partial t}\right)$:

$$\frac{\partial m_k(t)}{\partial t} = \frac{\partial m_{a,k}(t)}{\partial t} + \frac{\partial m_{g,k}(t)}{\partial t} \quad (\text{A.3})$$

814 The formulation of $\frac{\partial m_{a,k}(t)}{\partial t}$ comes by multiplying the first RHS term of Eq. A.1 by μ^k
815 and integrating by part with respect to μ :

$$\frac{\partial m_{a,k}(t)}{\partial t} = - \int_{\Omega\mu} \mu^k \frac{\partial}{\partial \mu} (n(\mu, t) \cdot \zeta(\mu)) d\mu \quad (\text{A.4})$$

$$= \int_{\Omega\mu} k\mu^{k-1}n(\mu, t)\zeta(\mu)d\mu - [\mu^k n(\mu, t)\zeta(\mu)]_{\partial\Omega\mu} \quad (\text{A.5})$$

816 Considering that the adaptation will not allow individuals to cross the frontier of the μ -
817 space ($\partial\Omega\mu$), the second term of Eq. A.5 is necessarily null. By expanding the formulation of
818 $\zeta(\mu) = (T^{-1} + \mu)(\mu^* - \mu)$, the formulation of $\frac{\partial m_{a,k}(t)}{\partial t}$ in terms of moments of the distribution
819 is trivial:

$$\frac{\partial m_{a,k}(t)}{\partial t} = k \left(\frac{\mu^*}{T} m_{k-1}(t) + \left(\mu^* - \frac{1}{T} \right) m_k(t) - m_{k+1}(t) \right) \quad (\text{A.6})$$

820 The contribution of the growth term to the moment evolution strongly depends on the
821 choice of a closure for the redistribution model. In Morchain et al. (2016), we identified
822 the following probability density function as a good model for experimental data from the
823 literature (Nobs and Maerkl, 2014; Yasuda, 2011):

$$\beta(\mu, \mu') = \beta(\mu, \tilde{\mu}) = \frac{2}{\sigma} \phi \left(\frac{\mu - l}{\sigma} \right) \Phi \left(\alpha \times \frac{\mu - l}{\sigma} \right) \quad (\text{A.7})$$

824 with:

- 825 • $\phi(x) = \frac{1}{\sqrt{2\pi}} e^{-\frac{x^2}{2}}$
- 826 • $\Phi(x) = \frac{1}{2} \left(1 + \operatorname{erf} \left(\frac{x}{\sqrt{2}} \right) \right)$

827 The redistribution law is a skew-normal distribution whose parameters depend on the
 828 population mean growth rate $\tilde{\mu}$ but not on the growth rate of the mother cell:

$$\tilde{\mu} = \frac{m_1(t)}{m_0(t)} \quad (\text{A.8})$$

$$l = k_l \tilde{\mu} \quad (\text{A.9})$$

$$\sigma = k_\sigma \tilde{\mu} \quad (\text{A.10})$$

$$\alpha = 3.65 \quad (\text{A.11})$$

829 The constants k_l and k_σ were chosen so that the PDF $\beta(\mu, \mu')$ fits experimental data,
 830 but also with the constraint that the first moment of this PDF is equal to $\tilde{\mu}$ so that the
 831 redistribution term will have no impact on the population mean growth rate. The used
 832 values are:

$$k_l = 0.651836690282903 \quad (\text{A.12})$$

$$k_\sigma = 0.452438435252710 \quad (\text{A.13})$$

833 Then, the growth related evolution of the distribution moments is easily expressed in
 834 terms of moments of $\beta(\mu)$:

$$\frac{\partial m_{g,k}(t)}{\partial t} = \int_{\Omega_\mu} \left[\mu^k \int_{\Omega_\mu} \beta(\mu, \tilde{\mu}) \Psi \mu' n(\mu') d\mu' \right] d\mu \quad (\text{A.14})$$

$$= \Psi \int_{\Omega_\mu} \mu^k \beta(\mu, \tilde{\mu}) \left[\int_{\Omega_\mu} \mu' n(\mu') d\mu' \right] d\mu \quad (\text{A.15})$$

$$= \Psi \int_{\Omega_\mu} \mu^k \beta(\mu, \tilde{\mu}) m_1(t) d\mu \quad (\text{A.16})$$

$$= \Psi m_1(t) B_k \quad (\text{A.17})$$

$$(\text{A.18})$$

835 B_k is the k -th order moment of the PDF $\beta(\mu, \tilde{\mu})$ which happens to only depend on $\tilde{\mu}$
 836 whose value is accessible using the first two moments of the distribution (Eq. A.8). The
 837 moments B_k can be determined analytically using the Moment Generating Function of the
 838 skew-normal distribution:

$$B_k = \frac{\partial^k M}{\partial t^k}(0) \quad (\text{A.19})$$

$$M(t) = \exp\left(lt + \frac{\sigma^2 t^2}{2}\right) \left(1 + \operatorname{erf}\left(\frac{\sigma \alpha t}{\sqrt{1 + \alpha^2}}\right)\right) \quad (\text{A.20})$$

839 We used the MATLAB Symbolic Toolbox to pre-compute the expressions of $B_k, \forall k \in$
 840 $\{0, \dots, 9\}$.