Performance study of a cooling device coupled to a membrane distillation unit

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Outline

- ↘ Context of air-conditioning
- ↘ Experimental bench
- ↘ Simulation model
- ↘ Results
- ↘ Conclusions
- ↘ Perspectives



Refrigeration cycle



Cooling devices







Electricity consumption



Air-conditioning situation

Vakiloroaya V. et al. A review of different strategies for HVAC energy saving, Energy Conversion and Management 77 (2014) 738–754

- In Europe, building = 40 % of energy consumption (in the US, 50 %)
- In India, air-conditioning = 32 % of electricity consumption
- In Hong Kong in 2006, refrigeration and air-conditioning = 33 % of electricity consumption
- In the Middle East, refrigeration and air-conditioning = more than 70 % of energy consumption

Electricity consumption for air-conditioning in buildings



Tendency 2000-2100

Isaac M. et al. Modeling global residential sector energy demand for heating and air conditioning in the context of climate change, Energy Policy 37 (2009) 507–521

> Prospective of energy demand taking into account climate change: -34 % for heating +72 % for air-conditioning



Let's valorize this heat loss!

62 condensers 2 times the front area 2 sides ~3 kW 62 x 2 x 2 x3

= 744 kW thermal

Heat rejected by ~620 refrigerators of 100 l



Membrane Distillation

• T = 25 à 80 °C

Compatible with temperature levels of airconditioning condensers

- Membranes
 - Microporous : pore size ~0,2 μm, porosity 80%
 - Hydrophobic : only vapour transfers
 - <u>Polypropylene</u>, PTFE (Teflon), PVDF, PAN...









Scheme of the coupled system



14



Numerical model 1/2

Heat transfer

•
$$\dot{Q}_h = \dot{Q}_m = \dot{Q}_{ag} = \dot{Q}_{plate} = \dot{Q}_c$$
 (1)

• $\dot{Q}_h = hc_h \left(T_h - T_{hm}\right)$ (2)

•
$$\dot{Q}_m = \frac{1}{R_{mT}} \left(T_{hm} - T_{mg} \right) + J_v \Delta h_{vap}$$
 (3)

•
$$\dot{Q}_{ag} = \frac{1}{R_{ag}} \left(T_{mg} - T_p \right)$$
 (4)

•
$$\dot{Q}_{plate} = \frac{k_p}{\delta_p} \left(T_{pc} - T_p \right) + J_v \Delta h_{cond}$$
 (5)

•
$$\dot{Q}_c = hc_c \left(T_p - T_c\right)$$
 (6)



Numerical model 2/2

Mass transfer

•
$$J_{\nu} = B_{\nu} \cdot \Delta P_{\nu}$$
 (7)

•
$$P_{v} = exp\left(23,1964 - \frac{3816,44}{T-46.13}\right)$$
 (8)

•
$$B_{v} = \frac{\varepsilon M_{v} P D_{ia}}{RT_{m}(\delta_{m}\tau + \delta_{g})|P_{a}|_{ln,a}}$$



(9)







Coefficient of performance



a look back to the scheme...



Gained output ratio



Performance ratio



Exergy efficiency 40 Exergy efficiency (%) 05 05 05 05 0 0.4 0.5 0.6 0.7 0.8 0.9 1 1.1 1.2 1.3 1.4 1.5 1.6 Flow rate (I/min) -15 °C - 30 °C



Conclusions

- Best COP with low temperature and high flow rate
- Maximum GOR over 10
- Maximum PR over 4 kg/MJ
- Optimal exergy efficiency for low water flow rates and high temperature
- Low operating temperatures of MD
- Compatible with a cooling device



Perspective

Coupled prototype MD unit fabricated with a 3D printer



Cold channel



Coupled prototype scheme



27

Let's valorize lost heat !

Model : PR = 3 kg/MJ PR = 10.8 kg/kWh

For 1 apartment : Condenser ~3 kW_{th} 32.4 kg/h

Hyp: 2000 kWh_{elec}/year COP = 3: 6000 kWh_{th}/year

64.8 m³ per year !



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