

An experimental study of gas hydrate formation of CH4-C3H8 binary mixture under the non-equilibrium conditions

MAGHSOODLOO Saheb, LE-QUANG Du, BOUILLOT Baptiste, HERRI Jean-Michel



Gas Hydrate Dynamics Centre, Ecole Nationale Superieure des Mines de Saint-Etienne, Centre SPIN-Laboratoire Georges Friedel (UMR 5703)

Abstract

Gas hydrates are a crucial issue in many fields, from oil & gas industry, to carbon capture and storage, air conditioning, or even planetary science. They also have an enormous potential as an energy resource because of the tremendous quantity of methane trapped within them. To understand better the gas hydrates phenomena, understanding of the thermodynamics and the crystallization mechanisms of clathrate hydrates are required. The determination of the hydrate composition and volume is also a technical challenge and we recall in the paper the method used by our laboratory. In this work, several experiments were performed to obtain precious experimental data and the gas compositions in hydrate phase. GasHyDyn group has recently found out that the composition of gas hydrate is sensitive to the crystallization conditions. Hence in this work, it was tried to understand better the relation between the composition of hydrate during the crystallization and final state and crystallization rates. Experiments were performed in a batch reactor and there were an online gas chromatography connected to the experimental setup and an off-line ion-chromatography to measure the gas compositions and liquid compositions, respectively. Based on these data and mass balance, the gas compositions in hydrate phase and hydrate volume can be calculated. During the last decade, our GasHyDyn team has also measured equilibrium data for many gas mixtures, and this document adds new data involving propane. In the present work, the experimental results are discussed after formation following two different experimental protocols: at quick and slow rates of crystallizations. It was observed that, from the same initial conditions, the final pressure and water conversion for two different procedures are slightly different.

Experimental Set-up

For performing the experiments, a system (called SECOHYA) consists of a 2.36 liter autoclave reactor has been used. The reactor is equipped with two vertical stirrers with four blades, one in the liquid and one in the gas. The temperature is controlled by a cryostat. The liquid is injected in the reactor under pressure by using a HPLC pump. Temperature is monitored by two probes, one in the gas phase and the other one in the liquid phase. The pressure is measured with an accuracy of 0.01 MPa. A ROLSI sampler allows to take online sample of gas and to send it into a gas chromatograph. Liquid sample can be taken by a mechanical valve and a capillary tube. The liquid is analyzed off-line by ion chromatography (Fig. 1).

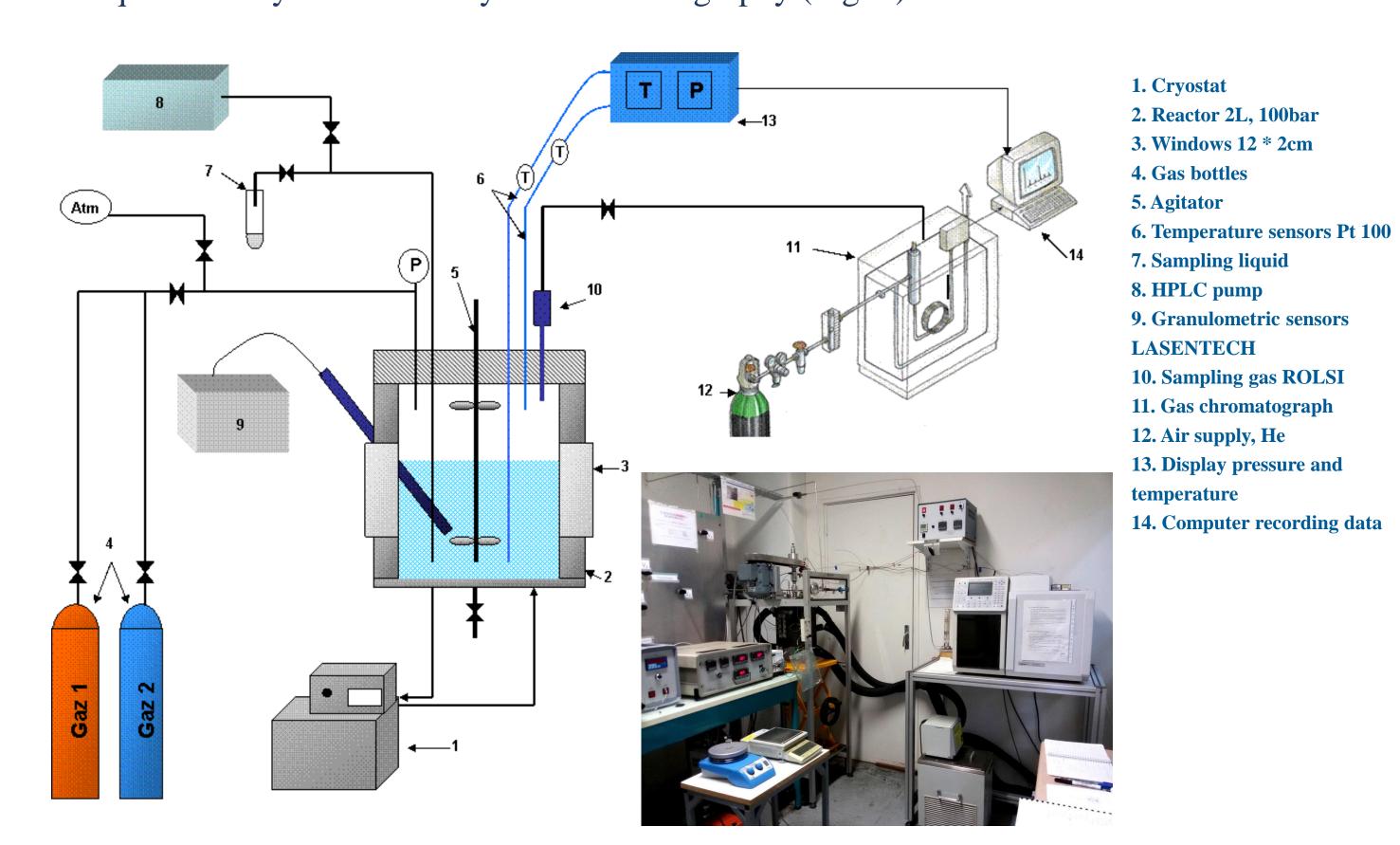
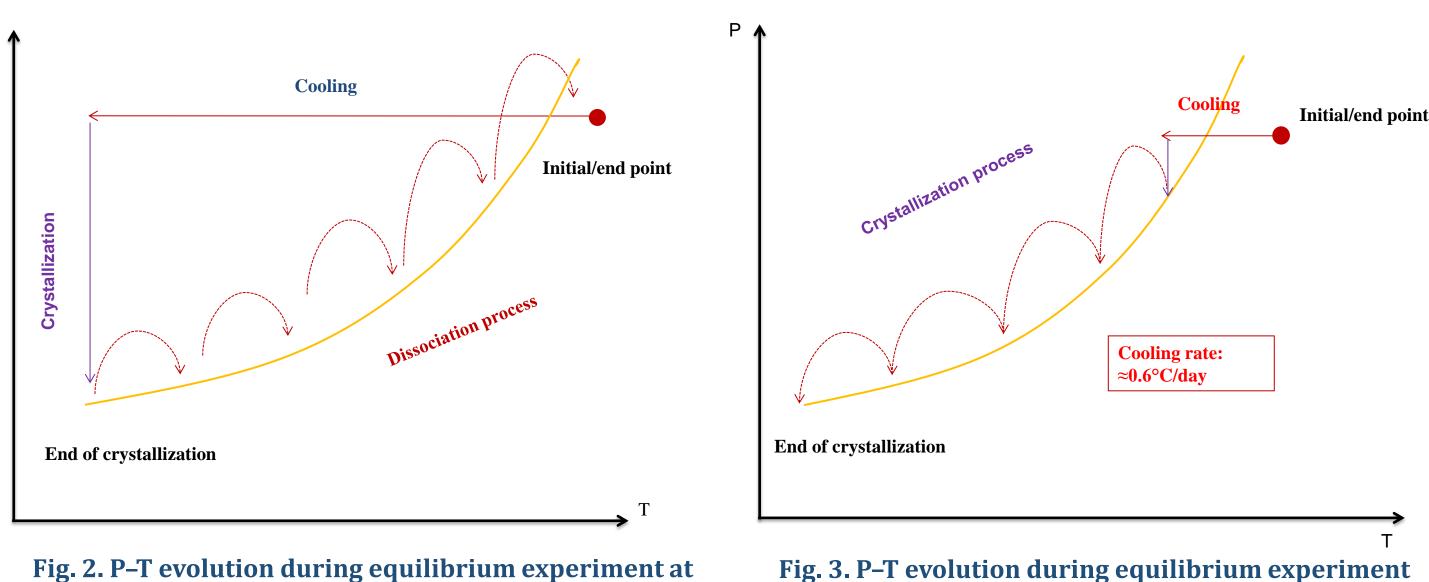


Fig. 1. The schematic diagram of the apparatus

Experimental Procedures

In this work, we have investigated two types of crystallization; quick and slow crystallization rates, which are based on the same initial conditions. The goal is to point out the differences between the initial solution composition and the final solution composition, and to establish a link between the final state and the crystallization rate. In quick procedure, the crystallization occurs at a high supersaturation (Fig.2). But in slow procedure, Instead of decreasing very quickly the temperature to the final state, the temperature is decreased very slowly (Fig. 3). The objective of this procedure is to focus on thermodynamic equilibrium, limiting as much as possible kinetic effects.

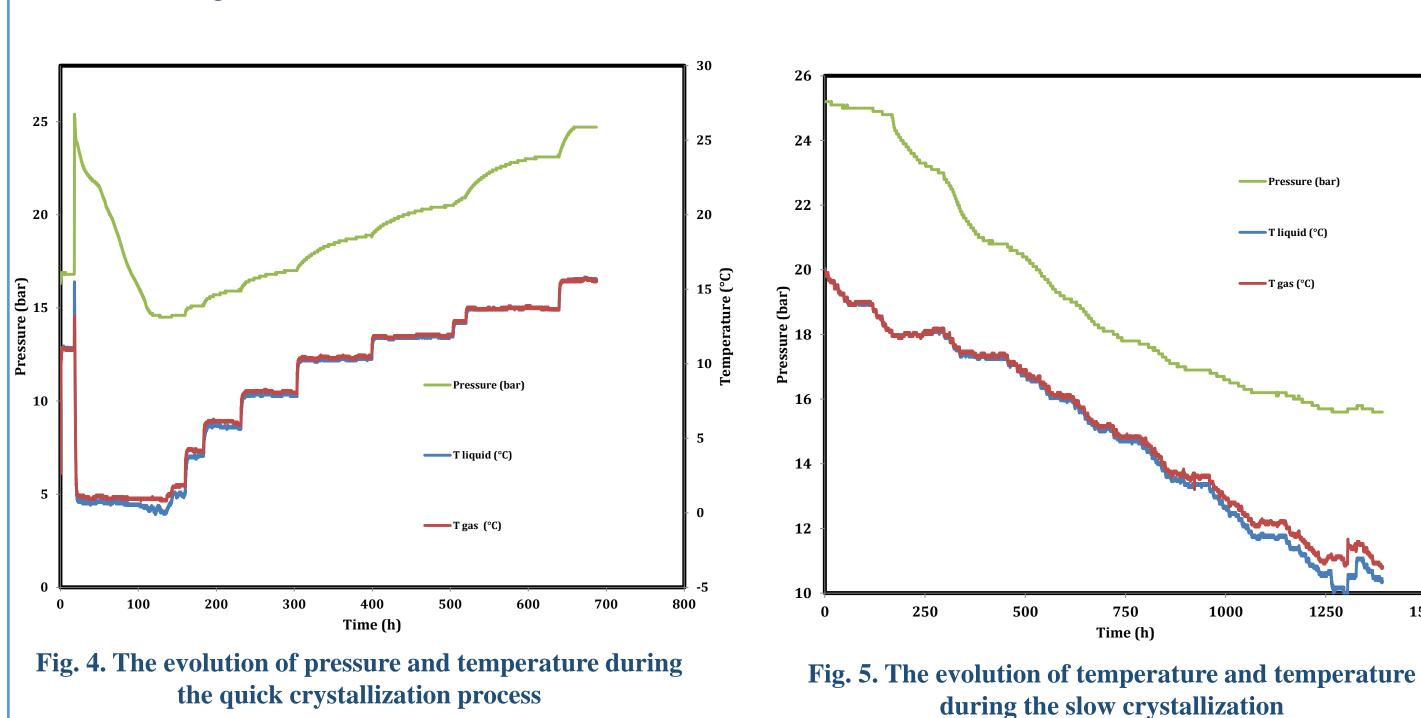


high crystallization rate

Fig. 3. P-T evolution during equilibrium experiment at slow crystallization rate

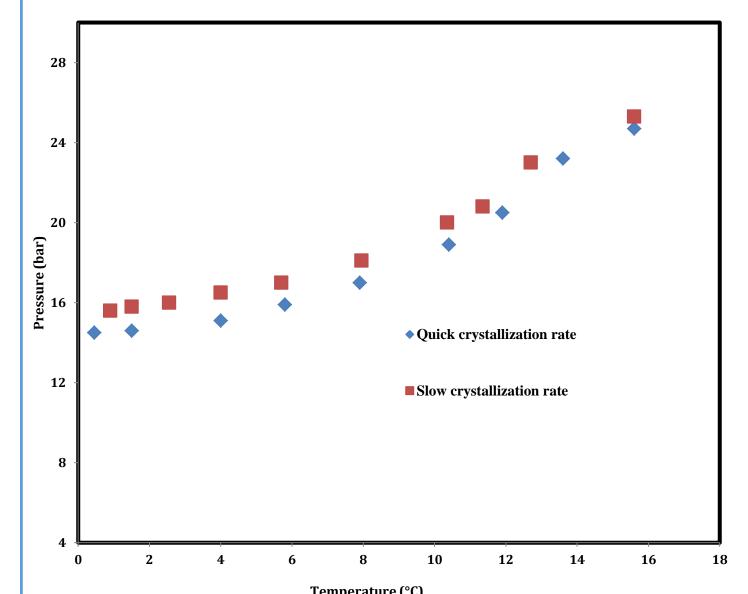
Results and discussions

A set of experimental data on the phase equilibrium of gas hydrates in the presence of binary gas mixture of CH_4 - C_3H_8 in two different approaches on the crystallization rate was obtained and shown in Fig 4 and 5.



The comparison between the results of quick and slow crystallization rates has been shown in Fig. 6. It can be seen that the pressure drop in the case of slow crystallization rate is less than quick crystallization rate. So it means that there was not any leakage in our experimental set-up. Furthermore, the pressure difference at high temperature is less than low temperature. The water conversion and the change of gas composition in hydrate phase during the quick and slow crystallization are brought in Table 1.

Quick crystallization



(bar)	fraction)	fraction)	conversion	(°C)	(bar)	fraction)	fraction)	water conversion
14,5	0,6900	0,3100	20,395	12,7	23	0,4346	0,5654	0,7328
14,6	0,6873	0,3127	16,0229	11,3 5	20,8	0,5659	0,4341	6,2098
15,9	0,6756	0,3244	13,9257	10,3 5	20	0,5777	0,4223	6,0033
17	0,6613	0,3387	12,6243	7,95	18,1	0,6028	0,3972	8,1925
18,9	0,6390	0,3610	11,1133	5,7	17	0,6142	0,3858	8,519
20,5	0,6142	0,3858	9,7432	0,9	15,6	0,6292	0,3708	9,7061
23,2	0,4624	0,5376	7,2548	-	-	-	-	-
	14,5 14,6 15,9 17 18,9 20,5	14,5 0,6900 14,6 0,6873 15,9 0,6756 17 0,6613 18,9 0,6390 20,5 0,6142	14,5 0,6900 0,3100 14,6 0,6873 0,3127 15,9 0,6756 0,3244 17 0,6613 0,3387 18,9 0,6390 0,3610 20,5 0,6142 0,3858	14,5 0,6900 0,3100 20,395 14,6 0,6873 0,3127 16,0229 15,9 0,6756 0,3244 13,9257 17 0,6613 0,3387 12,6243 18,9 0,6390 0,3610 11,1133 20,5 0,6142 0,3858 9,7432	14,5 0,6900 0,3100 20,395 12,7 14,6 0,6873 0,3127 16,0229 11,3 5 15,9 0,6756 0,3244 13,9257 10,3 5 17 0,6613 0,3387 12,6243 7,95 18,9 0,6390 0,3610 11,1133 5,7 20,5 0,6142 0,3858 9,7432 0,9	14,5 0,6900 0,3100 20,395 12,7 23 14,6 0,6873 0,3127 16,0229 11,3 5 20,8 15,9 0,6756 0,3244 13,9257 10,3 5 20 17 0,6613 0,3387 12,6243 7,95 18,1 18,9 0,6390 0,3610 11,1133 5,7 17 20,5 0,6142 0,3858 9,7432 0,9 15,6	14,5 0,6900 0,3100 20,395 12,7 23 0,4346 14,6 0,6873 0,3127 16,0229 11,3 5 5 20,8 0,5659 15,9 0,6756 0,3244 13,9257 10,3 5 5 20 0,5777 17 0,6613 0,3387 12,6243 7,95 18,1 0,6028 18,9 0,6390 0,3610 11,1133 5,7 17 0,6142 20,5 0,6142 0,3858 9,7432 0,9 15,6 0,6292	14,5 0,6900 0,3100 20,395 12,7 23 0,4346 0,5654 14,6 0,6873 0,3127 16,0229 11,3 5 20,8 20,8 20,5659 0,4341 15,9 0,6756 0,3244 13,9257 10,3 5 20 20 20,5777 0,4223 17 0,6613 0,3387 12,6243 7,95 18,1 20,6028 0,3972 18,9 0,6390 0,3610 11,1133 5,7 17 20,6142 0,3858 20,5 0,6142 0,3858 9,7432 0,9 15,6 292 0,3708

Slow crystallization

Fig. 5. The comparison between the results of equilibrium points for quick and slow crystallization rates

Table. Water conversion and the change of gas composition in hydrate phase during quick and slow crystallization

Conclusion

In this work, the influence of crystallization rate on a binary mixture of CH4-C3H8 was studied. The determination of the hydrate composition and volume were also investigated, not only at equilibrium conditions, but also during the crystallization and at non-equilibrium conditions. These parameters are really important studding about the gas mixture, because estimation of the hydrate volume can help us to determine the amount of kinetic inhibitors (KHI) to use in flow-assurance issues, and knowing the gas compositions in hydrate phase can be useful for understanding the gas hydrate phenomena. The results showed that although the initial conditions for two crystallization rates were almost the same, the pressure at final state was a little different. It can be better intercepted based on the results of water conversion. Water conversion for the quick crystallization was more than the slow crystallization. Furthermore he mole number of gases in hydrate for quick crystallization was more than slow crystallization. It means that more gases trapped in hydrate phase, hence the pressure drop must be higher. The gas compositions in hydrate phase were slightly different for both crystallization rates (slow and quick). Based on the results, it was concluded that in slow crystallization rate, the heavier molecules can be trapped in hydrate cages more than the quick crystallization rates.

References

Bouillot, B., Herri, J.-M., 2015. Framework for clathrate hydrate flash calculations and implications on the crystal structure and final equilibrium of mixed hydrates. Fluid Phase Equilibria. 413, 184-195.

Herri, J.-M., Bouchemoua, A., Kwaterski, M., Fezoua, A., Ouabbas, Y., Cameirao, A., 2011. Gas hydrate equilibria for CO2–N2 and CO2–CH4 gas mixtures-Experimental studies and thermodynamic modelling. Fluid Phase Equilibria 301, 171–190.

Le Quang, D., Le Quang, D., Bouillot, B., Herri, J.-M., Glenat, P., Duchet-Suchaux, P., 2015. Experimental procedure and results to measure the composition of gas hydrate, during crystallization and at equilibrium, from N2–CO2–CH4–C2H6–C3H8–C4H10 gas mixtures. Fluid Phase Equilibria. 413, 10-21.

Le Quang, D., Herri, J-M., Ouabbas, Y. A method to calculate the composition of clathrate hydrate of CO2-CH4, at equilibrium and during crystallization. 2013. Energies nouvelles et procédées (104), pp.No 99.

Nixdorf, J., Oellrich, L.R., 1997. Experimental determination of hydrate equilibrium conditions for pure gases, binary and ternary mixtures and natural gases. Fluid Phase Equilibria 139, 325–333.