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An innovative efficient oxygen electrode for SOFC: Pr₆O₁₁ infiltrated into Gd-doped ceria backbone

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Abstract: The praseodymium oxide, Pr_6O_{11} , is regarded as a potential electrocatalyst for the oxygen reduction reaction. Its mixed conductivity properties are characterized. At 600 °C the oxygen diffusion coefficient value is as high as 3.4×10^{-8} cm² s⁻¹, and that of the surface exchange coefficient is 5.4×10^{-7} cm s⁻¹, which supposes excellent electrocatalytic properties. The measured electronic conductivity is high enough for using this material as a SOFC cathode. Herein, praseodymium nitrate is infiltrated into Gd doped ceria (GDC) backbone and fired at 600 °C to form a composite oxygen electrode Pr_6O_{11}/GDC . Electrochemical measurements show very low polarization resistance, $Rp = 0.028 \ \Omega \ cm^2$ at 600 °C. A single cell made of a commercial Ni-YSZ/YSZ half cell and of the infiltrated cathode is able to deliver a maximum power density of 825 mW cm⁻² at 600 °C. Ageing of this cell for 840 h, at 600 °C and 0.5 A cm⁻², shows a degradation rate lower than 1%.

Keywords: Solid oxide fuel cells / Composite cathodes / Praseodymium oxide / Infiltration process / Ageing SOFC test.

Introduction

Mixed electronic and ionic conductors are good candidates for improving the oxygen reduction reaction (ORR) at the cathode side in solid oxide fuel cells (SOFC) [1], [2]. Most of them contain alkaline-earth elements such as strontium or barium, cations that easily diffuse, segregate or react with other cells components as well as with CO₂. In a recent review, Chen et al. [3] claimed that searching for alkaline earth-free electrode materials is highly desirable with respect to these issues.

Among novel cathode materials, those containing Pr cations show good electrocatalytic properties as for instance, the Ruddlesden-Popper (RP) phase Pr₂NiO_{4+δ}. It exhibits high oxygen diffusion and oxygen surface exchange coefficients, as well as a good electronic conductivity [4]. However, it has recently been evidenced that this compound decomposes when held at intermediate temperatures such as those targeted by the SOFC application (600–800 °C), forming the n = 3 RP term, Pr₄Ni₃O_{10+δ}, the perovskite PrNiO_{3-δ}, as well as the simple oxide Pr₆O₁₁ [5], [6]. While for most materials, such a decomposition is detrimental with regard to the electrocatalytic efficiency, for Pr₂NiO_{4+δ}, it was reported that the polarization resistance of the electrode at $i_{dc} = 0$ remains quite stable with time [6]. More recently, we studied a cathode made of Gd (gadolinium) doped ceria (GDC) infiltrated with Pr₂NiO_{4+δ} that showed polarization resistances as low as 0.075 Ω cm² at 600 °C, while the presence of Pr₆O₁₁ as secondary phase was also noticed [7].

It is also interesting to note that few recent studies have reported an improvement of the electrochemical performance when using Pr_6O_{11} as additive in composite electrodes made for instance of LNF (LaNi_{0.6}Fe_{0.4}O₃₋₈) or LSM (La_{0.8}Sr_{0.2}MnO₃)-GDC, either mixed or infiltrated with Pr_6O_{11} [8], [9], [10], [11]. Then, with respect to these features, it becomes mandatory to examine the exact role played by this simple oxide from an electrochemical viewpoint.

In the praseodymium – oxygen phase diagram, six PrO_x phases with various oxygen stoichiometries, belonging to the series Pr_nO_{2n-2} (n = 4, 7, 9 10, 11, 12, ∞), have been evidenced [12]. Except PrO_2 , all exhibit two oxidation states (3+ and 4+); the stable oxide at room temperature is Pr_6O_{11} (n = 12) and only a few studies have been concerned with its properties [12], [13], [14].

In this work, we aim to study Pr_6O_{11} as a potential electrocatalyst of the oxygen reduction reaction (ORR) for a SOFC cathode. Due to phase transitions upon increasing temperature, this oxide undergoes volume changes that may induce cracks and delamination in screen-printed electrodes during sintering. Herein, Pr_6O_{11} will be infiltrated into GDC backbones to form composite electrodes, as the infiltration technique is known to be able to solve such issues [15]. From an application viewpoint, this process is simple and low cost, and has been reported for a large variety of materials to yield highly efficient electrodes [15], [16], [17].

1. Experimental

Sample preparation

The praseodymium oxide, Pr_6O_{11} , was prepared by a glycine - nitrate process (GNP), starting from a commercial praseodymium nitrate (Aldrich), which led to an oxide powder of fine granulometry (<0.2 µm) that favors the densification. The GNP powder was uniaxially pressed, then sintered at 1350 °C for 10 h, in oxygen, with heating and cooling ramps of 3 °C min⁻¹. This protocol significantly reduced the formation of cracks, leading to 95% dense pellets with a diameter $\emptyset = 5.5$ mm. The density of the pellets was determined by the Archimede's method.

Electrical and oxygen diffusivity measurements

The electrical conductivity was measured on dense pellets by the four probe technique, in air, between room temperature and 800 °C. The oxygen diffusivity was determined using the isotopic exchange depth profiling (IEDP) technique as previously reported [4]. Dense pellets were first abraded with silicon carbide papers of successive grades and then polished with an alumina paste (0.3 Am). Then, they equilibrated at 600 °C in a ¹⁶O pressure of 210 mbar, and then quenched down to room temperature. The ¹⁶O was pumped out of the setup and replaced by the ¹⁸O diffusion tracer at the same pressure. The sample was put again at the same temperature for a controlled time to partly exchange ¹⁶O with ¹⁸O. Finally, the diffusion profile was recorded with a Cameca IMS 6F secondary ion mass spectrometer (SIMS) with a Cs⁺ source.

Electrochemical measurements

The electrochemical characterizations were carried out on symmetrical cells. They were prepared starting from commercial membranes (kindly provided by ECN (The Netherlands)) made of 3% yttria stabilized zirconia (TZ3Y) of around 100 μ m thickness and 25 mm diameter, on which a porous backbone of Gd-doped ceria (GDC) (diameter 15 mm) was prepared as follows: a commercial GDC powder (Rhodia) was attrited with zirconia balls in ethanol, for 3 h, then mixed with a pore forming agent (carbon super p), terpineol, and ethyl cellulose to form an ink which was screen printed on both sides of the TZ3Y membrane. A LaNi0.6Fe0.4O3-8 (LNF) collecting layer was also screen printed on the backbone prior to sintering. The assembly was heated at 1150 °C for 1 h to provide a good mechanical resistance of the backbone. Then, both Gd-doped ceria backbone (7 or 14 μ m thick) and LNF (10 μ m thick) were infiltrated with solutions of Pr nitrate (≈ 2 M). An infiltration step consisted in:

i) applying a drop of solution on the backbone, *ii)* putting the sample under primary vacuum for 2 min, *iii)* wiping the solution excess with an absorbing paper, *iv)* firing the infiltrate at 450 °C for 20 min. This infiltration step was repeated till the infiltrate amount reaches 30 wt. % of the backbone (3–4 times). The annealing step was operated in the impedance measurement setup at low temperature, *i.e.* 600 °C for 2 h.

The symmetrical cells were placed between two gold grids supported by channeled ceramics that enhance the gas diffusion toward active sites of the electrodes. Impedance spectroscopy diagrams were recorded every 50 °C between 600 °C and 400 °C at $i_{dc} = 0$ with a Solartron Modulab frequency response analyzer. The frequency range was 1 MHz–10 mHz for 400 °C and 450 °C, above (500– 600 °C) the low frequency limit was 100 mHz. The Kramer–Kronig test was carried out to validate the good quality of the measurements and to withdrawn the part of the diagrams (usually at high frequency) where the KK test was not satisfactory. The AC amplitude was 50 mV. The impedance diagrams were fitted using in-house software (CANELEIS). Single cells were made starting from commercial Ni-YSZ/YSZ half-cells (diameter $\emptyset = 50$ mm); the cathode was prepared using the same protocol as for symmetrical cells, for both the backbone and the infiltration process (diameter $\emptyset = 16$ mm). Then, they were mounted in a measurement setup for single cells with Ni foam as anode current collector, gold grid as cathode current collector, and with air and hydrogen gas supply at each side of the cell. The setup was not sealed for gas tightness, the excess of gas being burnt at the edges.

Microstructure characterization

Images of the microstructure were recorded with a field emission scanning electron microscope Jeol JSM 6700 F at an acceleration voltage of 1 kV. Prior to analyses the samples were covered with a thin sputtered palladium layer to avoid electron charging. Then, the samples were fractured and images were taken on the cross section.

2. Results and discussions

Transport properties

In a first step, electrical conductivity measurements were carried out on Pr_6O_{11} dense pellets from room temperature up to 800 °C. Fig. 1 shows the thermal variation of the electrical conductivity. Even though Pr_6O_{11} has praseodymium with a mixed valence 3+/4+, the electrical conductivity is rather low (1.3 S cm⁻¹ at 600 °C and 3.7 S cm⁻¹ at 800 °C). The conduction behavior is of semi-conductor type over the whole temperature range and is in agreement with a study previously reported by Thangadurai et al. [13]. Rao et al. [18] suggested that the band width in rare earth oxides is narrow, and that the electronic conduction mechanism in Pr_6O_{11} is a small polaron-type. Additionally, one can note that the activation energy decreases around 470 °C, which could be related to the order/disorder transition of oxygen vacancies reported by Hyde et al. [12].



Fig. 1. Thermal variation of the electrical conductivity of Pr₆O₁₁ as a function of temperature.



Fig. 2. Normalized ¹⁸O diffusion profile recorded for Pr_6O_{11} after ¹⁶O/¹⁸O exchange at 600 °C for 13 min 30 s.

The oxygen diffusion and surface exchange coefficients were then determined after ${}^{16}\text{O}/{}^{18}\text{O}$ exchange carried out at 600 °C, for 13 min 30 s on a dense Pr₆O₁₁ pellet. The ${}^{18}\text{O}$ diffusion profile measured by Secondary Ion Mass Spectroscopy is shown in Fig. 2. The ${}^{18}\text{O}$ diffused on roughly 200 µm into the pellet, and the profile can be fitted using the Crank's solution of the Fick second law for diffusion in semi-infinite media [19] (equation (1)):

$$C1(x) = erfc\left(\frac{x}{2\sqrt{D^{*}t}}\right) - exp\left(\frac{k^{*}}{D^{*}}x + \left(\frac{k^{*}}{D^{*}}\right)^{2}t\right) \times erfc\left\{\left(\frac{x}{2\sqrt{D^{*}t}}\right) + \left(\frac{k^{*}}{D^{*}}\sqrt{D^{*}t}\right)\right\} + Aexp(-Zx^{6/5})$$
(1)

where C1(x) is the O^{18} concentration as a function of x, the depth, D^* is the oxygen diffusion coefficient, k^* the surface exchange coefficient, is the exchange time, and A and Z are parameters

related to the grain boundary diffusion. The fit gives the following values: $D^* = 3.4 \times 10^{-8} \pm 0.1 \times 10^{-8} \text{ cm}^2 \text{ s}^{-1}$ and $k^* = 5.4 \times 10^{-7} \pm 0.1 \times 10^{-7} \text{ cm s}^{-1}$. It is the first time that such an experiment is carried out on Pr₆O₁₁ and D^* and k^* values are of the same order of magnitude as those previously reported for Pr₂NiO₄₊₈ that is currently one of the best SOFC cathode materials [4], [20].

 Pr_6O_{11} has a cubic fluorite-type structure, typical of that of well-known good ionic conductors such as yttria doped zirconia (YSZ) or GDC. The unit formula at room temperature, $PrO_{1.83}$, means that the oxygen vacancy content is 0.17. This oxide loses oxygen as the temperature increases [12], which creates additional vacancies and induces oxygen mobility, especially in the disordered state (T > 470 °C). In addition, Pr_6O_{11} oxide exhibits a high surface exchange coefficient, likely resulting from the ease of praseodymium to change its valence state between 3+ and 4+. Its poor electronic conductivity (nevertheless two orders of magnitude larger than the ionic conductivity of the GDC backbone) seems not to be a limiting factor for the oxygen reduction reaction.

Electrochemical measurements on symmetrical cells

Next step was to characterize the infiltrated electrodes using electrochemical impedance spectroscopy.

Fig. 3 shows SEM images of the GDC backbone before and after infiltration with Pr_6O_{11} annealed at 600 °C. Such a low annealing temperature results in very fine Pr_6O_{11} nanoparticles dispersed on the surface of GDC grains.

The electrochemical impedance of infiltrated electrodes was first measured in a symmetrical cell configuration on three infiltrated samples as follows: in earlier works [7], [21], the infiltration of $Pr_2NiO_{4+\delta}$ into $La_{0.9}Sr_{0.1}Ga_{0.8}Mg_{0.2}O_{3-\delta}$ or GDC led to very efficient electrodes, even though the presence of Pr_6O_{11} and NiO additional phases was suspected to play a role in the electrochemical behavior of the electrode [7]. To clarify this role, it was therefore interesting to compare the former results of $Pr_2NiO_{4+\delta}$ infiltrated into GDC backbone with a Pr_6O_{11} infiltrated electrode as well as with one infiltrated only with NiO.

The thermal variation of the polarization resistances of these three infiltrated samples is reported in Fig. 4. When the electrode is only infiltrated with NiO the polarization resistance is high, *i.e.* $1.4 \Omega \text{ cm}^2$ at 600 °C. The cell infiltrated only with a praseodymium solution, however, yields an extraordinary low polarization resistance, even lower than the results previously obtained for the Pr₂NiO₄₊₈ infiltrated electrode, reaching 0.028 $\Omega \text{ cm}^2$ at 600 °C, 0.14 $\Omega \text{ cm}^2$ at 500 °C, and 3.5 $\Omega \text{ cm}^2$ at 400 °C. It is worth noting that it is the first time an electrode material without 3d cations is considered. Indeed, up to now, materials for oxygen electrodes showing good electrocatalytic properties are based on mixed valences of 3d cations such as Mn, Fe or Co [2]. Here, it is assumed that the mixed valence of the praseodymium cations in Pr₆O₁₁ is likely to be responsible for such a high efficiency toward the oxygen reduction reaction. Previous works [8], [9], [10] reported the beneficial effect of Pr₆O₁₁ as additive in oxygen electrode but all these results did not lead to polarization resistances as low as those measured here.



Fig. 3. SEM cross-section image of the GDC backbone prior to infiltration (a) and infiltrated with 30 wt. % of Pr_6O_{11} , annealed at 600 °C for 2 h (b).



Fig. 4. Arrhenius plots of the polarization resistance of Gd-doped ceria backbones infiltrated with Pr_6O_{11} , compared with results for electrodes infiltrated with NiO and $Pr_2NiO_{4+\delta}$, and reported results for $La_2NiO_{4+\delta}$ infiltrated into GDC [22], $Sm_{0.5}Sr_{0.5}CoO_{3-\delta}$ infiltrated into SDC [23], and $La_{0.6}Sr_{0.4}CoO_{3-\delta}$ infiltrated into GDC [24].

In addition, one can compare our results with similar infiltrated electrodes reported in the literature. An electrode of La₂NiO_{4+ δ} infiltrated into GDC prepared in the same conditions led to a polarization resistance value of 0.15 Ω cm² at 600 °C [22]. Nicholas and Barnett [23] reached a value of

 $0.10 \ \Omega \ cm^2$ at 600 °C for Sm_{0.5}Sr_{0.5}CoO₃₋₈ infiltrated into Sm-doped ceria backbones. Samson et al. [24] prepared La_{0.6}Sr_{0.4}CoO₃₋₈ infiltrated into GDC electrodes and measured a polarization resistance of 0.044 $\Omega \ cm^2$ at 600 °C.

The polarization resistance values measured here with Pr_6O_{11} are lower than those of most wellknown cathode materials prepared with similar protocols (infiltration into ceria based backbones), which clearly demonstrates that Pr_6O_{11} is a very promising material for SOFC cathodes.

For collecting the current, a LaNi_{0.6}Fe_{0.4}O_{3- δ} layer is screen printed on the GDC backbone. As it is also infiltrated with Pr₆O₁₁, one can wonder about the role of this infiltrated LNF layer in the electrochemical response of the electrode. Thus, the next step was to determine the electrochemical contribution of the current collector. In this way, using the same process, backbones of LNF or of platinum (as reference for an electronic conductor) were both infiltrated with Pr₆O₁₁. The thermal variations of the polarization resistances of both infiltrated backbones (Fig. 5) are quite similar. At 600 °C, the value of the polarization resistance is rather low, $R_p = 0.072 \ \Omega \ \text{cm}^2$, however, it is more than twice as high as that of the GDC backbone.



Fig. 5. Arrhenius plots of the polarization resistance of Pt, LNF and GDC backbones infiltrated with Pr6O11.

In addition, two GDC backbones with different thicknesses (7 and 14 μ m) were infiltrated with Pr₆O₁₁. As shown in Fig. 5, they lead to exactly the same polarization resistance values. It proves that above a thickness of 7 μ m the polarization resistance does not depend on the thickness of the GDC backbone and that the electrochemical reaction occurs within a layer thickness equal or lower than 7 μ m.

As a consequence of these results, one can conclude that the upper LNF layer strictly plays the role of a current collector. This is corroborated by the values of the diffusion length calculated from the fit of the impedance diagrams.

Fig. 6 shows the impedance diagrams measured at 400, 500, and 600 °C along with their fits. The oxygen electrode reaction (OER), can be fitted with a finite length Gerischer impedance proposed by Nielsen et al. [25] to model composite oxygen electrodes (equation (2)):

$$Z = R_0 \frac{\coth\left((L/\lambda_0)\sqrt{1+iw/k_0}\right)}{\sqrt{1+iw/k_0}}$$
(2)

where R_0 is homogeneous to a resistance, L the electrode thickness, the diffusion length that represents the thickness λ_0 of electrode where the reaction takes place and k_0 a rate constant related to the surface exchange reaction. The polarization resistance R_p corresponds to the DC limit of this impedance, *i.e.* when $i_{\omega} \rightarrow 0$, which is:

$$R_p = R_0 \times \operatorname{coth}(L/\lambda_0)$$

Compared to the typical Gerischer impedance, the finite length Gerischer takes into account the relationship between electrode thickness and diffusion length. If the thickness is much higher than the diffusion length the hyperbolic cotangent term reduces to 1 and the equation becomes similar to that of the typical Gerischer impedance.



Fig. 6. Impedance diagrams recorded at 400, 500 and 600 °C, for an electrode of Pr_6O_{11} infiltrated into GDC backbone with LNF collecting layer, annealed at 600 °C for 2 h.

At 600 °C the diagram is fitted with an equivalent circuit constituted of a series resistance for the electrolyte (Rs), an induction element (L) to take the wires of the measurement set up into consideration, the finite length Gerischer impedance (*FLG*) for the oxygen electrode reaction and a Warburg impedance (W) for the gas diffusion [25], [26], which yields the equivalent circuit: R_s -*L*-*FLG-W*. At 500 °C the induction element is no longer needed as wires do not create inductive effect

strong enough to affect the electrode response. At 400 °C only the series resistance and the finite length Gerischer remain, because the contribution related to gas diffusion is not detected, being too small compared to the contribution of the electrode reaction. The fit leads to the ratio between *L* the electrode thickness and λ_0 the diffusion length, (L/λ_0) , equal to 1.5 for the measurement at 400 °C, meaning that the electrode is thick enough (14 µm) not to limit the electrode performance. This analysis has also been applied to the cell with a 7 µm thick GDC backbone (not shown) and the (L/λ_0) ratio was also higher than 1 over the whole temperature range, which further proves that the reaction only occurs within the GDC layer and does not extend to the LNF collecting layer. When the temperature increases the diffusion length decreases and the typical Gerischer impedance is sufficient to describe the contribution of the oxygen reduction reaction. The diagram recorded at 600 °C is not well defined as the associated resistances are very small, the corresponding fits being not as good as those obtained for diagrams recorded at lower temperatures.

Electrochemical characterization of a single cell

Finally, the praseodymium oxide infiltrated Gd-doped ceria cathode was prepared on a Ni-YSZ/YSZ half-cell and measured in a single cell configuration. Fig. 7a shows the voltage and power density of the single cell as a function of the current density. Measurements were performed at 600 °C under two different gas flow rates (H₂: air): 60:120 NmL·min⁻¹ and 125:250 NmL·min⁻¹. At low current densities, the voltage of the cell is almost independent of this flow rate, but it has a significant impact at higher current densities, where the cell voltage is mainly controlled by the concentration overpotential. It means that the concentration overpotential is in this case governed by the supply of reactants rather than the removal of products. The maximum power density is shifted by 65 mW cm⁻² depending on the flow rates, with a maximum value for (H₂: air): 125:250 NmL·min⁻¹ reaching 825 mW cm⁻². Achieving such a high power density at 600 °C is quite unusual and very promising for the Pr₆O₁₁ infiltrated electrode. Indeed, this result can be compared with the power density of the commercial cell using a lanthanum cobaltite cathode or with that of La2NiO4+8 infiltrated into Gddoped ceria cathode [27], both prepared using the same commercial Ni-YSZ/YSZ half-cell. Maximum power densities of 400 and 250 mW cm⁻², respectively, are measured. They are 2 or 3 times lower than our single cell and only dependent on the infiltrated phase of the cathode, which clearly points out that Pr₆O₁₁ is a very efficient catalyst for the oxygen reduction reaction.

Then, this single cell was aged at 600 °C. The current density was set at 0.5 A cm⁻² with flow rates of reactants at (H₂: air): 60:120 NmL min⁻¹ in H₂ and air. Fig. 7b shows the variation of the cell voltage versus time. The cell potential remains fairly stable at around 0.82 V during the whole experiment (840 h), the extrapolated degradation rate over 1000 h being lower than 1%, which proves that the infiltrated electrode keeps its high electrocatalytic activity even after long time operation.



Fig. 7. (a) i-V and power density curves of a single cell with Pr_6O_{11} infiltrated cathode, measured at 600 °C, for two different gas flow rates; (b) Cell voltage measured at 600 °C and 0.5 A cm⁻² for 840 h. The characteristics of a commercial cell from Elcogen have been measured in a (H₂:air) flow rate = 60:120 Nml min⁻¹.

Such a result is encouraging for infiltrated electrodes that are often believed, as the catalyst is nanoscaled, to be subject to Oswald ripening issues that decrease the specific surface area [28]. These phenomena are often observed when the cell is aged at higher temperatures, and 600 °C might be low enough to prevent it. One can point out that, this catalyst being a simple oxide; it cannot be subject to decomposition as it can occur in perovskites or RP phases [5], [6]. In addition, Pr₆O₁₁ electrodes do not contain Sr cations, and all concerns related to the presence of Sr such as reactivity with Cr from interconnects that forms insulating SrCrO₄ [3], [29], [30], or surface segregation [31], [32] that affects the cell durability, are avoided, which constitutes a strong advantage for the cell durability.

Conclusion

Praseodymium oxide, Pr_6O_{11} , was investigated as a potential electrocatalyst for the oxygen reduction reaction for fuel cell application. Its electrical conductivity is sufficient with regard to the prerequisite of a SOFC cathode. The oxygen diffusion and the surface exchange coefficients have been measured at 600 °C and are quite similar to those of $Pr_2NiO_{4+\delta}$, known for its very high D^* and k^* values.

The composite electrodes were prepared by infiltration of praseodymium nitrate into a Gd-doped ceria backbone and fired at 600 °C. The impedance spectroscopy measurements on symmetrical cells showed values of polarization resistance as low as 0.028 Ω cm² at 600 °C, which is among the lowest R_p ever reported at this temperature. Such an electrode was then prepared on Ni-YSZ/YSZ

commercial half-cell to make a single cell. A remarkable maximum power density of 0.825 W cm⁻² was measured at 600 °C. At a current load of 0.5 A cm⁻², the cell voltage remained stable for 840 h, with a degradation rate lower than 1% per 1000 h.

Up to now, Pr_6O_{11} has only been considered as an improvement of other electrode materials such as $LaNi_{0.6}Fe_{0.4}O_{3-\delta}$ (LNF). In this study, we demonstrate for the first time that this oxide, free of 3d cations, can be used alone as an excellent electrocatalyst for the oxygen reduction reaction in SOFC. As the active material is a simple oxide, there are no decomposition issues that could affect the cell performance, and as it is Sr-free, all issues related to Sr migration and reactivity with other cell components are avoided as well.

To conclude, Pr₆O₁₁ is a very promising electrode material for SOFC applications thanks to its high electrocatalytic activity and stability.

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