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Steam reforming of methane in a synthesis gas from biomass gasification

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Highlights

- Experimental and modelling study of pyrolysis and of steam reforming of methane
- Investigation of the kinetic effect of gases issued from biomass gasification
- Steam shows little effect on CH₄ conversion but allows the oxidation of products
- CO₂ promotes the reaction while H₂ inhibits it
- High temperature necessary to the reforming favors the formation of soot precursors

Abstract

An experimental and modelling study of the pyrolysis and of the steam reforming of methane in mixtures representative of a gas produced from biomass gasification has been performed. The experimental study has been done in a plug flow reactor under a near atmospheric pressure (1.07 bar), for a residence time of 0.68 s and temperature ranging from 1200 up to 1800 K. Reactants and products were quantified on-line at the exit of the reactor by gas chromatography. The kinetic influence of the different gases present in the synthesis gas (H_2O , H_2 , CO , CO_2) on the methane conversion has been investigated. Water steam has shown a very limited impact on conversion, even at the highest temperature, while hydrogen exhibited a strong inhibiting effect on the reforming reaction. Carbon dioxide promoted slightly the reaction, unlike carbon monoxide, which had no kinetic effect. A temperature as high as 1700 K is necessary in these conditions to convert entirely methane. A model derived from that for the combustion of light hydrocarbons was developed with attention to the reactions of unsaturated species with hydroxyl radical OH, which are responsible for the reforming. The main experimental trends are well reproduced. Carbon reforming occurs mainly by reactions of OH radical with unsaturated C_2 molecules, which are soot precursors. Process conditions necessary for high temperature methane reforming would then be favorable to undesirable soot formation.

Keywords: Steam reforming, pyrolysis, methane, syngas, kinetic modeling

1. Introduction

Environmental concerns, especially greenhouse gases emissions, have led to an increased interest in the use of renewable energies. Biomass is widely used in combustion but can also be involved in more advanced applications such as the production of liquid combustibles (GTL) or the cogeneration by means of a fuel cell [1]. These applications require the production of a high quality synthesis gas (syngas, mixture of CO and H₂). Cellulosic biomass may be a promising feedstock through the gasification processes [2,3]. Wood gasification is a heterogeneous process between a carbon-containing solid and an oxidizer such as O₂, CO₂ or water steam [4,5]. The main products are CO and H₂, but large fractions of hydrocarbons, char and soot, which are undesirable to achieve a high efficiency and avoid fouling, are yielded too. Three phases can be distinguished [6]. The solid phase includes soot and char. The liquid phase involves the condensable intermediates named as tars, while carbon oxides, hydrogen, water, methane and other light hydrocarbons remain in the gas phase. The hot gases from the gasification need to be cleaned drastically to reach the severe specifications of fuel cells or catalytic processes [7]. Catalytic post treatment are usually used to clean the gases at the exhaust of the gasification [8], but the severe conditions, especially the high temperature, lead to a short life time for the catalytic bed. A non catalytic alternative can be a high temperature steam gasification and reforming of a mixture of biomass and methane, which permits to optimize hydrogen yields for downstream liquid fuel synthesis and shows a rather good efficiency over autothermal process [9,10]. Another alternative process would be a homogeneous high temperature reforming of tars (T > 1273 K) and light hydrocarbons at the exhaust of the gasifier. This would allow a cleaning of the gas and an improvement of the global yield by oxidizing the remaining hydrocarbons into CO and H₂ [11]. The technical evaluation of such an alternative is required to know precisely

the kinetics of the hydro reforming of hydrocarbons. These reactions are also involved in other processes proposed for the production of hydrogen, such as solar driven methane [12] or carbonaceous material steam reforming [13,14] or auto-thermal reforming using partial oxidation of hydrocarbons [15–18]. Up to now, modeling of gas phase reforming or water gas shift reaction in thermal processes often relies on thermochemical equilibrium [19] or global stoichiometric equations [20].

Few studies have been devoted to the reaction of hydrocarbons and tars with water steam. Jönsson [21] studied the conversion of methane in a gas obtained from wood pyrolysis, in a tubular reactor. The conversion was found to be maximum at 1523 K (60% conversion) and to be not very sensitive to the amounts of water and oxygen, while hydrogen showed an inhibiting effect. Tijmensen [22] studied the reaction of methane with water between 973 and 1373 K between 10 and 35 bar and proposed a global reaction rate. Valin et al. [23] followed the conversion of methane in a pilot scale tubular reactor in a gas mixture representative of that obtained after the gasification of wood. 90% of the hydrocarbon was oxidized at 1653 K for a residence time of 2s and they noted also the inhibiting effect of hydrogen [24].

Reactions of tars have been also the subject of some studies. At high temperature, tars are mostly composed of aromatic and polyaromatic compounds [6]. The major components are benzene, toluene, indene, naphthalene, and phenol [25]. These compounds could then be used as surrogates for the reactions of tars. Jess [26] studied the steam reforming of benzene, toluene, and naphthalene in a tubular reactor between 973 K and 1673 K under 1,6 bar. Toluene was found to be completely consumed at 1300 K while a temperature of 1700 K was necessary to convert benzene.

Although many detailed kinetic models exist for the thermal decomposition and the combustion of light hydrocarbons, especially for methane [27–37], these models were not

designed to simulate the slow oxidation by water in a reducing atmosphere containing mainly CO and H₂. Reactions at very high temperature in a mixture rich in H₂O, CO, CO₂ and H₂ need further investigations. The present work aimed to go further than the process study by Valin et al. [23] and to investigate the kinetic behavior and interactions of the different compounds in well-defined conditions. An experimental and modelling study of the thermal cracking of methane has been performed at high temperature in a synthetic gas representative of that produced by the gasification of biomass. The effect of temperature and composition has been investigated and is discussed.

2. Experiments

The experimental study has been performed in a continuous flow reactor under a near atmospheric pressure (800 Torr, 1.07 bar). The reactor was a tubular mullite pipe (60 cm length and 2.4 cm internal diameter) of internal volume 271 cm³ involving a S/V ratio of 1.67 cm⁻¹. The mullite, which is an oxide of silicon and aluminum, allows a heating up to 1900 K. Comparisons were made at lower temperature, between 973 and 1273 K, with a fused silica reactor to check that no wall reaction occurs. Results were found identical in the case of the pyrolysis of ethane up to 1273 K. As pyrolytic carbon deposits were formed in the hottest part of the reactor, the effect of reactor aging was checked in another set of experiments. For a fixed temperature, thermal decomposition of methane, ethylene and acetylene was performed in neat and in coked reactors. It appeared that the formation of carbon deposit had a little promoting influence on the consumption of acetylene, without affecting the conversion of methane and other C₂ hydrocarbons. Experiments were then performed in all cases in clean reactors. A horizontal Vecstar oven allowed heating the reactor up to 1870 K. Temperature profiles were measured by a type S thermocouple coated in an alumina pipe. Uncertainty is estimated to ± 20K. Figure 1 presents

temperature profiles. A plateau of 16 cm length was reached at the set point temperature but lower temperature regions cannot be neglected in modeling. The reactor can be considered as a plug flow reactor in the studied conditions between 1000 K and 1800 K. For a residence time of 0.68 s calculated in the 16 cm long hot section of the reactor, the Péclet number lies between 120 and 140 as a function of the temperature, whereas a value above 50 allows to consider the reactor as a plug flow reactor.

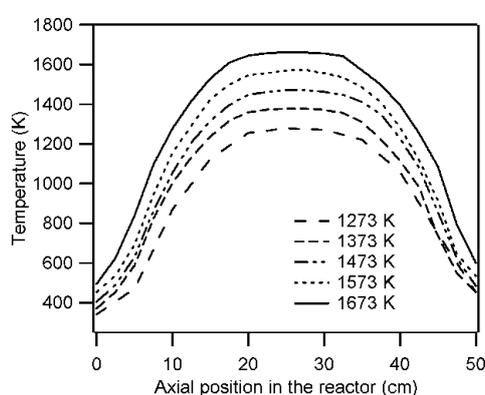


Figure 1: Temperature profiles in the reactor as a function of the oven set point.

Messer and Air Liquide supplied gases, with a purity at least above 99.9 %. Water was added through a Bronkhorst liquid mass flow controller coupled with a controlled evaporator mixer from the same supplier. For all the experiments, residence time was fixed to 0.68 s (in the hot area), pressure was 800 Torr (1,07 bar) and argon was used as diluent in order to make negligible the thermal effect and the volumetric expansion of the flow due to the reaction.

On-line analyses were done by gas chromatography. Permanent gases were quantified by a thermal conductivity detector (TCD) and hydrocarbons by a flame ionization detector (FID). Light species, i.e. H₂, CO, CO₂, methane, ethane, ethylene and acetylene were separated with a Carbosphere packed column. The uncertainties are

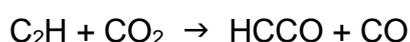
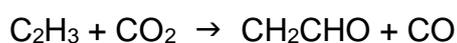
around 5%; the detection threshold is below 1 ppm with FID, it is 30 and 10 ppm for hydrogen and carbon oxides with TCD, respectively. Heavier compounds up to C₄ were separated with a Hayesep D packed column. When C₂ were added in the reacting mixture to test the kinetic effect of the coking of the walls, propene, allene (propadiene), propyne, 1-butene, 1,3-butadiene, vinylacetylene and diacetylene could be detected (not presented here).

3. Modeling

A detailed kinetic mechanism has been developed in order to simulate and analyze the experimental results of steam reforming. It was based on a model for the combustion of C₀-C₂ species, which includes also a reaction base for the reaction of C₃-C₅ unsaturated hydrocarbons validated in flame and shock tube conditions [38,39]. The C₀-C₂ reaction base contains all unimolecular and bimolecular reactions between species involving less than three carbon atoms and was especially validated against experimental results for the combustion of methane and ethane. Pressure dependence is taken into account for reaction of light species when data are available in the literature.

In the mechanism, reactions involving HO₂, H₂O₂ and O₂ were negligible and were removed since molecular oxygen was not present. The enthalpy of reaction of the hydroxyl radical, which is the main species responsible for steam reforming, was updated according to Burcat and Ruscic [40]. Several kinetic parameters were updated in order to include recent recommended values for the sensitive reactions. Data from the review by Baulch et al [41] were used for the H-abstraction by a H-atom and OH radical on methane, by H-atom on methyl radical producing H₂ and CH₂ diradical or the decomposition of vinyl radical to ethylene and H-atom. Special care was given to reactions of methyl radical and unsaturated species with H₂O and OH radical, which can be involved in the reforming

process. Combination of methyl and hydroxyl radical yields numerous products: methanol if the adduct is stabilized [41], or decomposition products such as water and CH₂ diradical [42], formaldehyde and H₂ [43], or methoxy radical and H-atom. Important reactions in the reforming of hydrocarbons are the addition of OH radical on unsaturated hydrocarbons, yielding the first C-O bonds that lead ultimately to the production of CO. These reactions are usually not sensitive in combustion and both rate constants and products are subject to discussion. In the case of the reactions OH+C₂H₄ and OH+C₂H₂, two pathways are possible: the H-atom abstraction and the formation of an adduct, which decomposes. In the case of ethylene, the adduct can decompose through three routes producing CH₃ and HCHO, CH₂CHOH and an H-atom, and CH₃CHO and an H-atom, respectively [41]. The formation of methyl radical and formaldehyde is dominant and the concurrent routes have been neglected. According to the literature, the rate parameters of the H-abstraction and of the addition were supposed to be similar ($k=10^{13}\exp(-5940 \text{ cal mol}^{-1}/RT) \text{ cm}^3 \text{ mol}^{-1} \text{ s}^{-1}$), and their sum equal to the value proposed for the global reaction of OH with ethylene [41]. These choices led to average values in comparison to studies of the literature. In the case of reactions between OH and acetylene, the data for the H-abstraction was taken from Tsang and Hampson [44]. The addition was supposed to produce mainly ketene (CH₂CO) and an H-atom with a rate constant of $1.1 \times 10^{13} \exp(-7174 \text{ cal mol}^{-1}/RT) \text{ cm}^3 \text{ mol}^{-1} \text{ s}^{-1}$ [45]. Carbon dioxide has shown a promoting effect on the steam reforming of hydrocarbons. By analogy with reaction of CH₃ (and C₂H₅) with CO₂, yielding CO and CH₃O (or C₂H₅O, respectively) [46], reactions of C₂H₃ and C₂H radical with CO₂ were added:



The pre-exponential factors were estimated to $10^{13} \text{ cm}^3 \text{ mol}^{-1} \text{ s}^{-1}$, as in the case of the addition of a radical on a double bond [47]. The activation energies were estimated from an Evans-Polanyi plot made with the reference reactions of methyl and ethyl radicals [46], which led to activation energies of 17 kcal mol^{-1} and 0 kcal mol^{-1} , respectively.

Simulations were performed with the CHEMKIN suite [48]. The plug flow reactor was modeled as a cascade of small continuously stirred reactors taking into account the experimental temperature profile.

4. Results and Discussion

4.1. Influence of water steam on methane pyrolysis

The degradation of pure methane has been studied as a function of temperature with and without the addition of water (i.e. pyrolysis condition). The initial fractions of methane and water were 0.63 % and 4.8%, respectively, diluted in argon. The profiles of methane and of the main products are presented in figure 2 in the pyrolysis and the case of the addition of water. An interesting result is that the reactivity of methane is not very sensitive to the addition of water. Its consumption starts around 1400 K in these conditions and the conversion is total around 1700 K with and without water. Both experiments and modeling show that water slightly promotes the reaction below 1523 K but inhibits it above this temperature. Conversely, the addition of water changes dramatically the product distribution: while the pyrolysis leads to large amounts of C_2 , especially acetylene, solid carbon and soot, the steam reforming produces H_2 , CO and CO_2 as major products, but also small amounts of C_2 . Ethylene reaches a maximum of about 60 ppm (mol) at 1423 K (150 ppm in pyrolysis at the same temperature), and acetylene an amount of about 550 ppm (mol) at 1523 K (to compare with a maximum of 2000 ppm at 1500 K in pyrolysis).

The model reproduces fairly well the profiles and the influence of temperature in pyrolysis and in presence of steam. The fraction of final products, i.e. hydrogen and carbon oxides, are well simulated. In pyrolysis, the model tends to overestimate acetylene at the highest temperatures, above 1573 K. The formation of solid carbon at the reactor wall and of soot becomes important in pyrolysis at these temperatures, whereas the gas phase model does not take into account these heterogeneous reactions. Studies on the carbon vapor deposition have shown that acetylene is one of the main precursor of pyrolytic carbon. A rate constant for the global reaction of deposition



was determined in the case of carbon vapor infiltration during propane pyrolysis [49]. The same reaction has been tested in the present mechanism. The pre-exponential factor has been corrected to take into account the change of the surface/volume ratio between both reactors, and multiplied by a factor 2, within the range of uncertainty. The rate constant equals finally $1.6 \times 10^5 \exp(-40\,000 \text{ cal mol}^{-1}/RT) \text{ s}^{-1}$. Hydrogen, ethylene and acetylene profiles obtained in pyrolysis with this modified mechanism are shown in Figure 2 (dotted lines). The heterogeneous reaction allows to reproduce perfectly the experimental profile of hydrogen above 1600 K. The most dramatic effect can be seen on acetylene fraction. Instead of an increase of the concentration to a plateau, acetylene profile reaches a maximum, as observed experimentally, and decreases at high temperature to produce solid carbon. Even if the temperature of the maximum is slightly shifted toward high temperature compared to the experiments, it is important to note that the heterogeneous reaction, determined in another reactor during propane pyrolysis, permits to reproduce the present data without further adjustment. The effect is rather moderate on ethylene profile, even if a better fit of the experimental data is obtained at the highest temperatures.

No effect was found on other species, methane and hydrogen and the reaction was found completely negligible in the case of steam reforming.

The low sensitivity of water on the global reactivity is explained by the low reactivity of water: the initial reaction channels consuming methane remains similar in both cases, i.e. a H-abstraction by a H-atom (or an OH radical when water is added) producing a methyl radical which is not very reactive and leads to bimolecular reactions. Water does not allow a new promoting route even at the highest temperatures. The slight promoting effect of water below 1523 K is due first to the reaction of H-atoms with water to produce H₂ and OH radicals. These latter react faster by H-atom abstraction with methane than H atoms. To a lesser extent, methyl radical reacts with H₂O to produce an H-atom and methanol. This latter molecule, much more reactive than methane, acts somewhat as a degenerate branching agent in unimolecular decompositions, which produce new radicals. When the temperature increases, OH radical reacts more with acetylene to yield an H-atom and ketene. The latter react by addition with an H-atom to form CH₃CO that decompose immediately into CO and a methyl radical. The scheme consists then in replacing an OH radical by a methyl radical, much of which yielding back methane by termination with an H-atom. Furthermore, the highest amount of H₂ in pyrolysis at high temperature inhibits methane conversion, as discussed below.

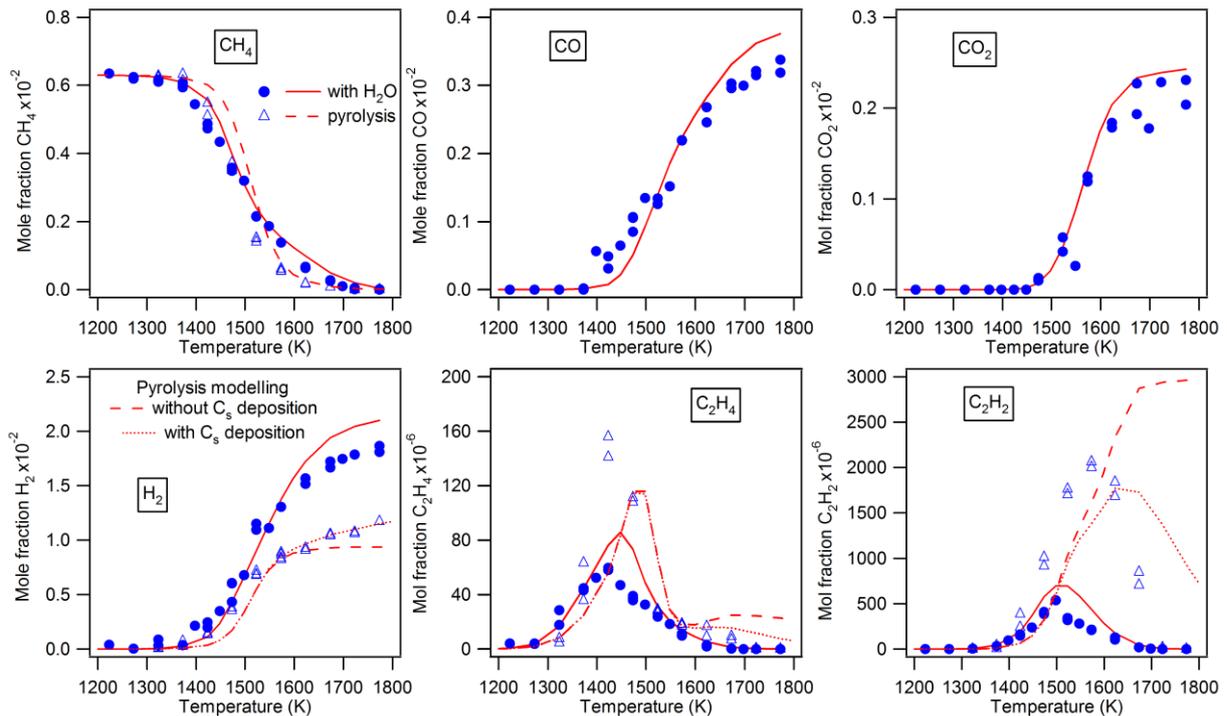


Figure 2: Profiles of species during the steam reforming of methane. In the cases of methane, H₂, and C₂, experimental results in pyrolysis condition without water are also displayed. $X_{CH_4}=0.63\%$, $X_{H_2O}=4.8\%$, diluent argon. Residence time is 0.68s. Points represent experimental results and lines simulations. Dash lines refer to the pyrolysis simulation, dotted lines to the simulation including a reaction of formation of solid carbon.

4.2. Influence of H₂ on methane pyrolysis

The influence of hydrogen in reactants (0-11 %) has been investigated during the pyrolysis of neat methane. Figure 3 displays the amount of methane as a function of the fraction of hydrogen added for two temperatures. At 1523 K, a strong inhibiting effect appears even for amounts of hydrogen as low as 1 %. When amounts larger than 10% are added, the conversion of methane is close to be stopped. The fractions of hydrogen and of C₂ products at the outlet of the reactor at 1523 K are plotted in Figure 4 as a function of H₂ at the inlet of the reactor. A large decrease of the amount of acetylene is observed in both experiments and simulations when hydrogen is added. Conversely, fractions of ethylene and ethane remain almost constant when hydrogen is added. The

model reproduces very well the amount of H₂ produced in addition to that present as reactant. As maximum mole fraction reached by C₂ species are slightly shifted toward higher temperatures (Figure 1), ethylene and acetylene amounts are somewhat overestimated for the lowest additions of hydrogen in figure 4. This is due to the significant uncertainties on reactions of consumption of acetylene with water and OH at high temperatures, but trends are however well predicted. At 1673 K, H₂ keeps an inhibiting effect, but less dramatic (Figure 3): while the conversion of pure methane is close to 99%, the addition of 11% of hydrogen makes it drop to around 70%. Whatever the temperature, the model reproduces very well the experimental observations. Reactions of methyl radicals explain the strong inhibiting effect of H₂. In thermal decomposition, methane yields methyl radicals by initiation (reaction 1) or by H-atom abstraction by another H-atom (reaction 2). CH₃ combines with itself to produce C₂ (reaction 3 and 4), or reacts in the reverse reactions with H or H₂ to yield methane. The addition of H₂ in pyrolysis favors these latter and strongly limit the formation of C₂ and subsequent products.

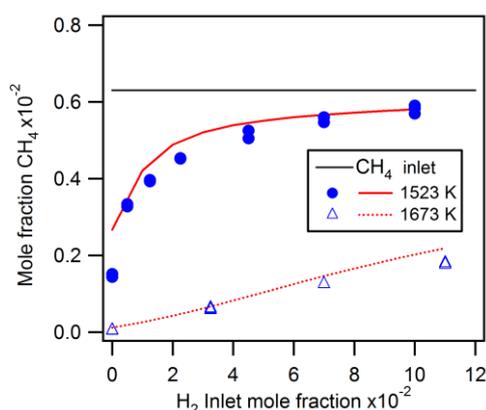
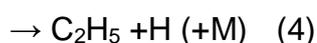
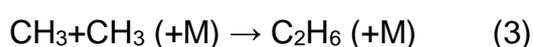
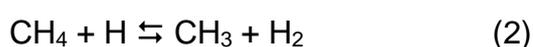
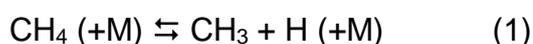


Figure 3: Profiles of methane during its pyrolysis as a function of the fraction of H₂ at 1523 K and 1673 K. Residence time is 0.68 s. Points represent experimental results and line simulations. The horizontal line gives the initial mole fraction of methane.

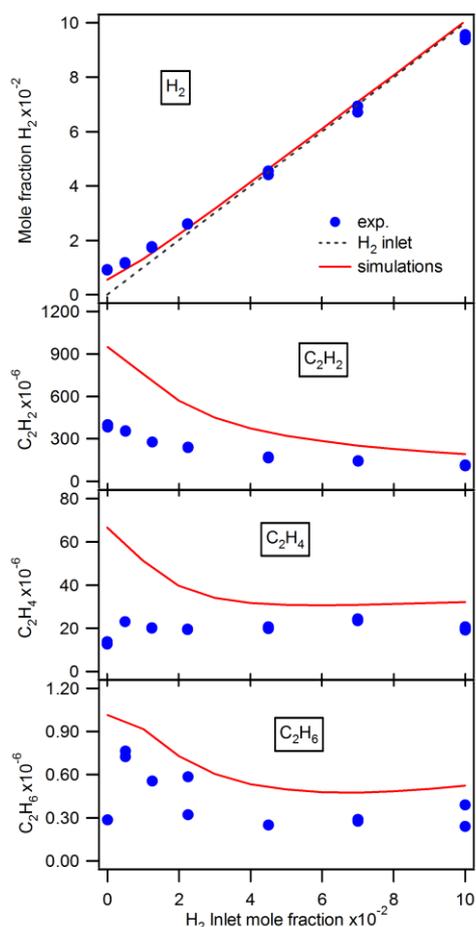


Figure 4: Profiles of hydrogen and products during methane pyrolysis as a function of the fraction of H₂ at 1523 K. Residence time is 0.68 s. Points represent experimental results and line simulations.

4.3. Influence of carbon oxides on methane pyrolysis

A possible kinetic effect of the addition of carbon oxides on the thermal reaction of methane has been also investigated. Carbon monoxide and dioxide are contained in large amounts in gas from biomass or coal gasification. An increasing mole fraction of CO was added to 0.63% of methane, up to 7% at 1523 and up to 10% at 1673 K (Figure 5). Whatever the temperature and the fraction of additive, no change can be observed in methane conversion, which reaches 75% at 1523K and 99.3% at 1673 K (60% and 98% by simulation, respectively). The amount of reaction products; i.e. hydrogen, ethylene,

and acetylene remains also constant at both temperatures whatever the fraction of CO, as illustrated in Figure 5 in the case of hydrogen.

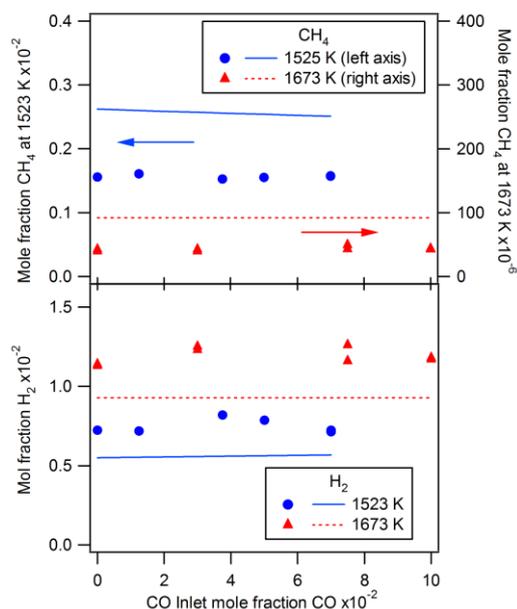


Figure 5: Profiles of methane and hydrogen during methane pyrolysis as a function of the fraction of added CO at 1523 K and 1673 K. Residence time is 0.68 s. Points represent experimental results and line simulations.

Contrariwise, CO₂ addition shows a promoting effect on the reactivity, as displayed in Figure 6. At 1523K, neat methane conversion in pyrolysis reaches 78% experimentally. The conversion increases up to 97% for a 10% mole fraction of carbon dioxide in the reactive mixture. Simultaneously, CO₂ is slightly consumed (experimental points are below the fraction at the reactor inlet in figure 6) and CO appears among the reaction products. The amount of hydrogen and C₂ decreases, as can be seen in the bottom of Figure 6. The model reproduces well the trends, considering the slight underprediction of neat methane conversion at 1523K. In these blends, CO₂ acts as an oxidizer through the reaction $\text{CO}_2 + \text{H} \rightleftharpoons \text{CO} + \text{OH}$. The hydroxyl radicals react hereafter with methane or H₂, reducing the inhibiting influence of this latter. They also can add on unsaturated C₂ to produce oxygenated compound, such as formaldehyde, which decomposes quickly at

this high temperature. Note that the direct reaction between CO_2 and methyl radical to produce CO and methoxy radical, included in the model, remains negligible.

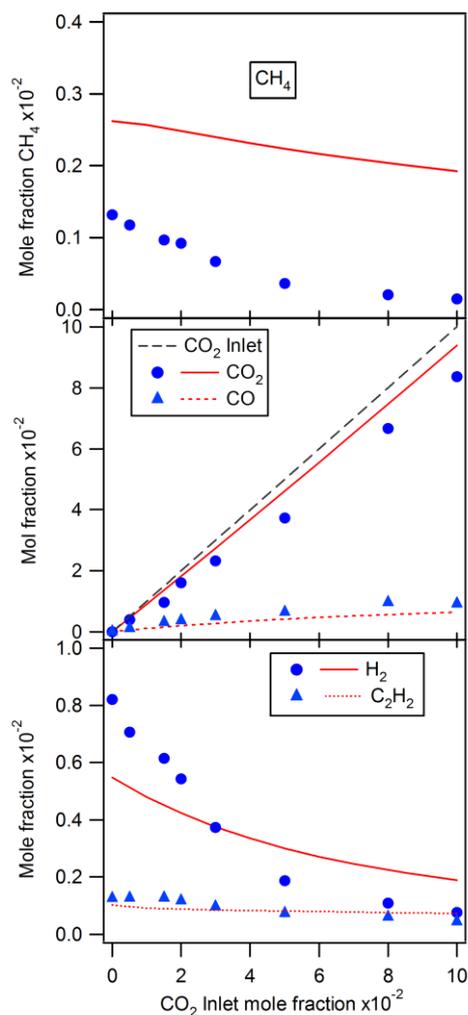


Figure 6: Profiles of methane, CO_2 and products during methane pyrolysis as a function of the fraction of added CO_2 at 1523 K. Residence time is 0.68 s. Points represent experimental results and line simulations.

4.4. Methane reforming in complex mixtures

The reaction of a mixture representative of a gas issued from biomass gasification has also been investigated as a function of the temperature. The blend contained methane (1.26%), CO (5%), H_2 (5%), and H_2O (5%) diluted in argon. Results are presented in figure 7. It appears that the reactivity of the hydrocarbon is lower than in the case of the steam reforming presented in figure 2. The inhibiting effect of hydrogen shifts the reaction

towards higher temperatures. Methane consumption starts around 1423 K (1400K for pure methane) and a temperature higher than 1723 K is necessary to reform completely the hydrocarbon. H₂ and carbon oxides are the major products. CO mole fraction exhibits a V shape profile: it is converted to CO₂ at intermediate temperature by OH radical but at higher temperature, the reverse reduction of CO₂ by H-atom and the reforming of methane to CO make its production predominant. The production of CO₂ is only due to the reaction of CO with OH radicals, which rate constant is well-known. The correct simulation of the amount of CO₂ indicates that the amount of OH radicals is correctly predicted by the model. Ethylene and acetylene are produced in important amounts at intermediate temperatures. Note that if methane concentration is twice that used in the study of the reforming of pure methane, the amount of acetylene reaches a maximum as high as 3500 ppm against 550 in the first conditions. This explains the significant formation of soot and carbon deposit that was observed experimentally. The model reproduces well both reactivity and product distribution, the simulation of the amounts of C₂ compounds is somewhat underestimated.

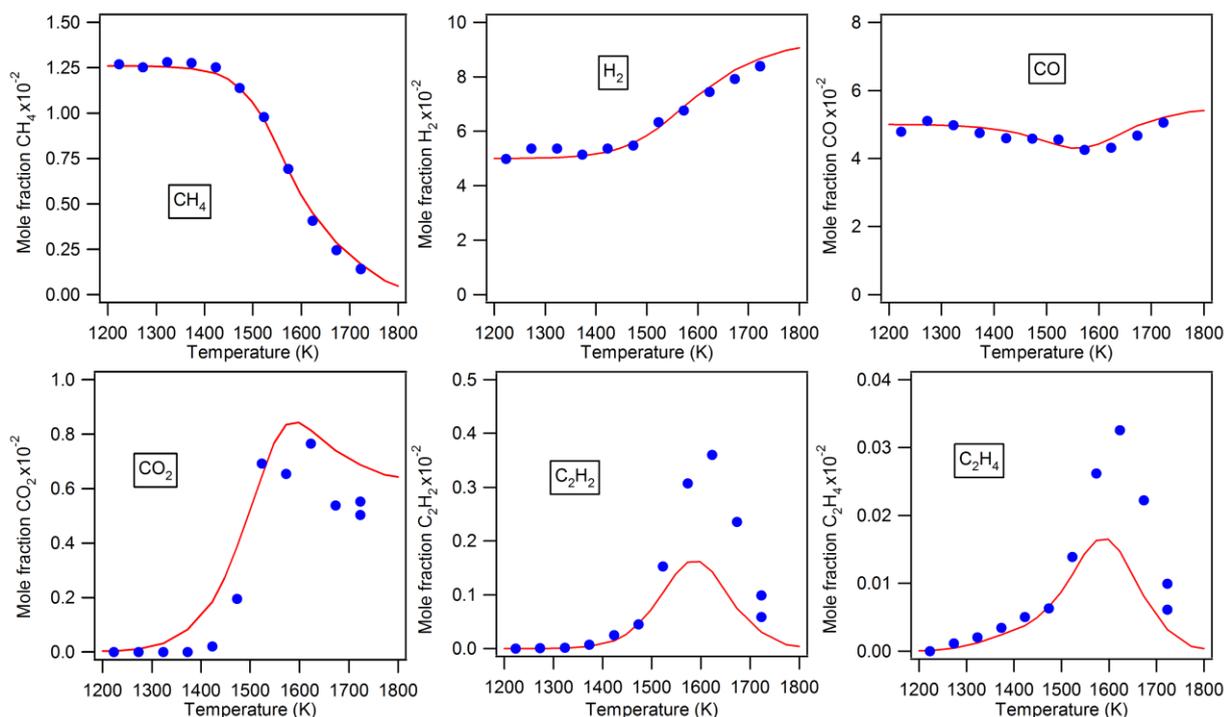


Figure 7: Profiles of species during the reaction of a mixture methane (1.26%), CO (5%), H₂ (5%), H₂O (5%) as a function of temperature. Residence time is 0.68 s. Points represent experimental results and line simulations.

A second mixture representative of a gas issued from biomass gasification has been investigated by replacing carbon monoxide by carbon dioxide. The mixture contained methane (1.26%), CO₂ (5%), H₂ (5%), and H₂O (5%) diluted in argon. Results are displayed in Figure 8 for the reactants and the C₂ products, including ethane, which is produced in very low amounts (maximum 2 ppm) at moderate temperatures. The global behavior looks close to that obtained with the first mixture involving CO, but the addition of CO₂ promotes the reactivity, as observed during neat methane pyrolysis. The profiles of products are also modified. The model simulates well the results. Methane and carbon dioxide consumption are very well represented as functions of the temperature, as CO and H₂ behavior. As in the case of the CO blend, ethylene and acetylene peak values are at the right temperature but are somewhat underestimated. Unlike in steam reforming in which C₂ were a little overestimated by the model (Figure 1), the high fraction of hydrogen in the mixture disadvantage the formation of C₂ by the combination of methyl radicals and

the subsequent dehydrogenation. The model may overvalue this effect at the highest temperatures. Ethane profile is very well reproduced.

Methane consumption starts at lower temperature than in the case of the CO blend. An experimental methane conversion around 6% is achieved at 1423K, whereas the CO-containing mixture does not react. At 1573K, the conversion reaches 60% in the CO₂ blend and 45% in the CO blend, respectively. The amount of the final products from reforming are also modified. In the CO-containing mixture, methane reforming leads to the formation of hydrogen, CO and C₂, which are converted thereafter to CO and H₂. Meanwhile, a small part of CO is oxidized into CO₂. When CO is replaced by CO₂ in the blend, this compound acts as an oxidizer, as discussed above in the case of pure methane pyrolysis. The water gas shift reaction, induced by the reaction of an H-atom with CO₂ yielding CO and an OH radical, leads to the oxidation of H₂ into water. In Figure 8, it appears that half of the CO₂ content is reduced to CO at high temperature, while the profile of H₂ exhibits a V-shape as a function of temperature. At moderate methane conversion, up to 1573 K, hydrogen consumption exceeds the production from the hydrocarbon reforming. When the temperature increases, the hydrogen formation from methane balances the oxidation of H₂ by CO₂. The promoting effect of CO₂ on the reforming reaction is also noticeable on the profiles of ethylene and acetylene. The amounts of unsaturated C₂ are almost the same for both mixture up to 1523 K, but differentiate at higher temperatures. In the case of the CO₂ blend, peak values are reached at a lower temperature and with a lower maximum amount than in the case of the CO blend (2500 ppm of acetylene instead of 3600 ppm, 144 ppm of ethylene instead of 326 ppm). The higher concentration of hydroxyl radical promoted by the reaction of carbon dioxide permits a larger consumption of methyl radical by termination with OH and

furthermore favors ethylene and acetylene consumption, which produces oxygenated species.

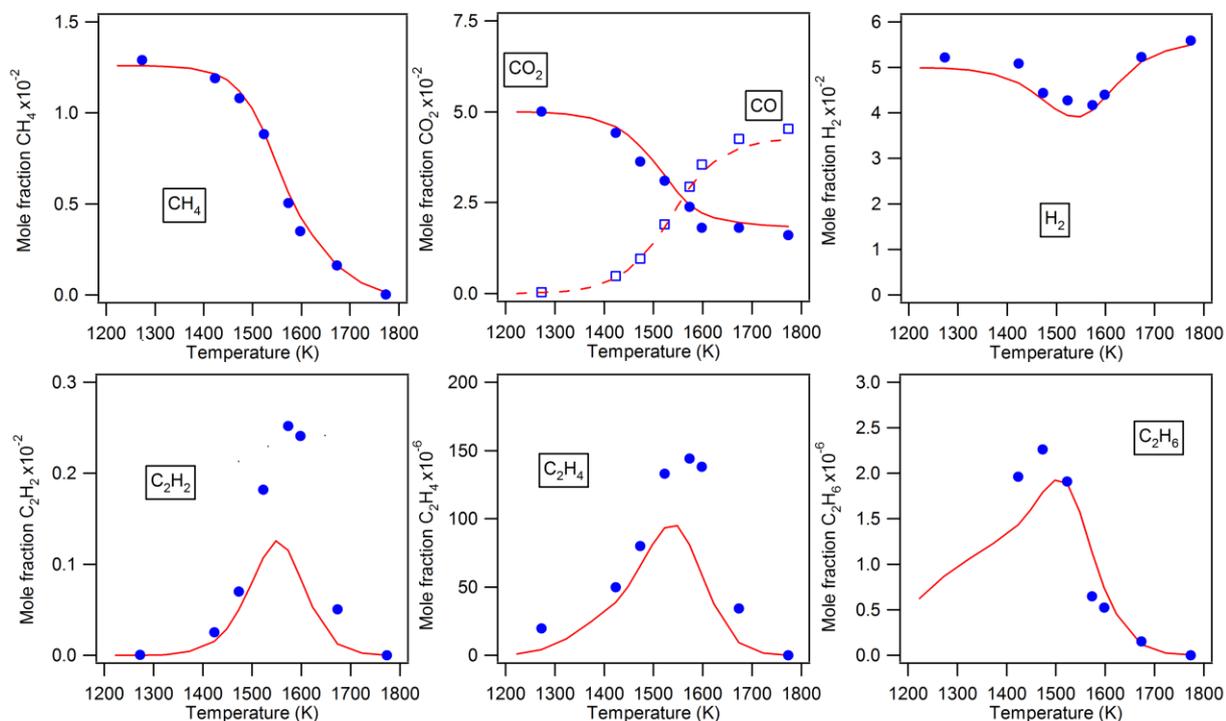


Figure 8: Profiles of species during the reaction of a mixture methane (1.26%), CO₂ (5%), H₂ (5%), H₂O (5%) as a function of temperature. Residence time is 0.68 s. Points represent experimental results and line simulations.

The model shows that in all the conditions studied, the hydrocarbon reforming does not go mainly through direct reactions of molecules or hydrocarbon radicals with water, but by the addition of OH radical on unsaturated bonds, which produced oxygenated species leading ultimately to CO and CO₂. Figure 9 presents the main reaction pathways of the thermal reaction of methane in the presence of water, in the conditions of figure 8 at 1573 K. The analysis is made in the middle of the plug flow reactor, corresponding to a simulated methane conversion of around 24%. It appears that, even if a part of methyl radicals reacts with water or OH radicals yielding methanol or CH₂OH, respectively, these reaction routes account for only 8% of the net flux of consumption of methyl radicals. The

main reaction channel is the combination with another methyl radical yielding C_2H_6 , C_2H_5+H or $C_2H_4+H_2$. The formation of C_2 accounts for 81% of methyl consumption. Remaining reactions consuming methyl radicals are H-atom abstractions on products, such as formaldehyde, which produces methane, and additions to unsaturated molecules, which yield heavier soot precursors. Ethane and ethylene dehydrogenate quickly by pericyclic H_2 eliminations (concerted molecular elimination through a cyclic transition state) or by successive H-atom abstractions and radical decompositions. Large amounts of acetylene, which is more stable, are eventually produced. This latter can react by addition of an OH radical. This reaction is the main channel in these conditions and represents 61% of acetylene consumption. Formation of propyne, a precursor of aromatic rings, accounts for 23% of acetylene consumption, while H-atom abstractions yielding C_2H radicals represents 10% of the flux. Remaining reactions include C_4 formation. Note that in these conditions, very reactive C_2H radicals react mainly with CO_2 to produce CO and HCCO radicals.

Even in presence of a large amount of water, methane reacts mostly as in pyrolysis. The presence of H_2 in the blend inhibits slightly the successive dehydrogenations of the C_2 , but does not really change the main reaction route. Note that in this mixture, the inhibiting effect of H_2 on methane conversion is due to its reactions with methyl radicals, as in pyrolysis, but also to the competition between reaction channels of OH radicals with methane and H_2 ($H_2+OH=H_2O+H$). A major consequence of the pyrolysis-like reaction of methane is that the reforming is enabled by the formation of unsaturated hydrocarbons, which are in the same time soot precursors. Oxygenated compounds are produced by the addition of OH on ethylene, yielding formaldehyde and a methyl radical, and predominantly on acetylene, yielding ketene and an H-atom. These oxygenates, much more reactive than methane at this high temperature, react quickly to produce CO in few

steps. Meanwhile, acetylene reacts with methyl radicals to produce propyne, which leads to propargyl radicals, and then to aromatic rings. There is then a competition between the fast pyrolysis process, which leads ultimately to soot and solid carbon and the somewhat slow reforming producing oxygenated species, which decompose into CO. The high temperature necessary to methane reforming by water in the reducing blend issued from gasification makes unavoidable the formation of heavy unsaturated compounds, soot and carbon deposits.

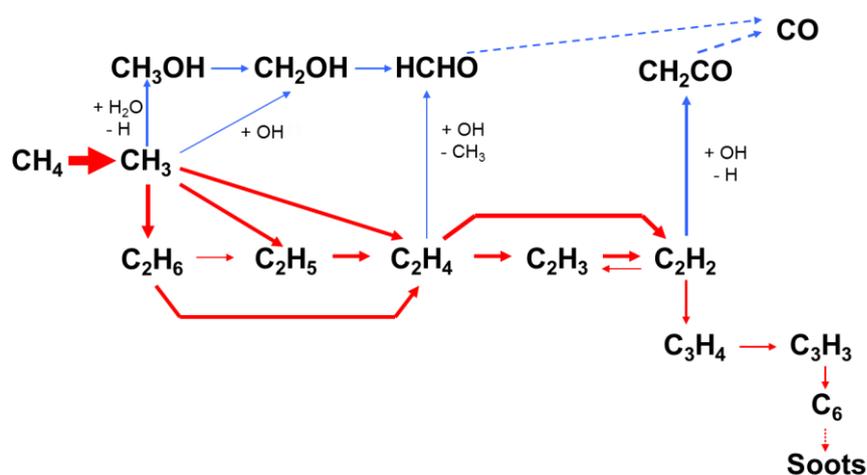


Figure 9: Reaction flux in steam reforming of methane in a mixture $\text{CH}_4/\text{CO}_2/\text{H}_2/\text{H}_2\text{O}$ at 1573 K in condition of Figure 8. Analysis performed in the middle of the flow reactor, corresponding to a simulated conversion of 24%. Arrow thickness is proportional to the net flux. Red arrows represent the pyrolysis channel, blue arrows the reforming one.

5. Conclusion

The pyrolysis and the steam reforming of methane has been studied at high temperature, as well as the behavior of complex mixtures representative of that produced by the gasification of the lignocellulosic biomass. It appears that near atmospheric pressure and for a residence time of 0.68 s, methane starts reacting at temperature below 1400 K and that it is necessary to heat up to more than 1700 K to achieve a complete reforming. The presence of carbon monoxide was found to have no kinetic effect,

whereas carbon dioxide slightly promote the reaction by acting as an oxidizer. While hydrogen has a strong inhibiting effect, water does not influence dramatically the global rate of reaction but the product distribution. Since reaction of methyl radical with water or OH radicals are slow in comparison with the pyrolysis reactions, an important point is that the reforming process implies the formation of unsaturated compounds, on which OH radicals can add, but which are also soot precursors. A limitation of a temperature reforming process could then limit the energetic cost and the soot and carbon deposit formation.

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