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## TRANSIENT REGIME TO FLUIDIZED CHIMNEY WITHIN A GRANULAR BED BY MEANS OF A 2D DEM/LBM MODELING

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**Abstract.** Beyond a given threshold, an upward fluid flow at constant flowrate, injected through a small size section, is able to generate a fluidization along a vertical chimney over the entire height of a granular assembly. Fluidization is first initiated in the immediate vicinity of the injection hole and then the fluidized zone grows gradually until reaching the upper surface of the granular packing. In this work, we present numerical results on the kinetics of chimney fluidization in an immersed granular bed produced with two-dimensional simulations coupling the Discrete Element and Lattice Boltzmann Methods (DEM-LBM). A parametric study is carried out with 11 different sets of physical parameters and analyzed based on spatio-temporal diagrams. Then a dimensional analysis allows finding general scaling laws for both threshold and growth rate of the fluidized zone by use of two dimensionless numbers, namely Reynolds and Archimedes numbers, while quite simple empirical relationships can also be proposed.

## 1 INTRODUCTION

A fluidized state within a granular bed is reached when the upward force exerted by the flow can balance the buoyant weight of the particles. Fluidization is used extensively in industry for drying, mixing and agglomeration processes with many applications as gasification of biomass, ion exchange processes or high efficiency carbon capture. Some among these industrial processes rely more specifically on a localized state of fluidization as is the case for spouted beds [1] and tapered beds [2] which are generated by means of an upward gas flow injected most often at the neck of a conical container. Contrariwise, channelization, i.e. occurrence of such preferential channels of fluidization, is to be absolutely avoided for other types of fluidized bed applications. In sedimentology, some geologic formations of fluid escape structures by localized fluidization through vertical pipe have been specifically examined [3]. A somehow similar situation is encountered in the context of dike safety, when a seepage flow through the foundation of an embankment is susceptible to generate such a local fluidization, commonly called “sandboil”, and possibly initiate a piping process by backward erosion, which is one of the four basic mechanisms identified for soil particles removal by internal erosion [4].

Here the focus is put more restrictively on the development and growth of a local fluidized state within an immersed granular assembly induced at the bottom of the grain bed by an upward fluid flow passing through a small injection hole. Several previous works have studied specifically this configuration and analysed the formation of a vertical chimney of fluidized soil on the basis of either experiments [5, 6] or numerical simulations coupling Discrete Element Method (DEM) with Lattice Boltzmann Method (LBM) [7]. It should be noted, however, that most efforts have been so far dedicated to the steady state rather than to the transitory development of such fluidized chimney [6]. This transient regime of localized fluidization is therefore specifically under the scope of the present study. For this purpose, a numerical model based on a 2D DEM/LBM coupled approach has been implemented to carry out a systematic analysis of the temporal evolution of the fluidized zone, expanding progressively from the injection hole to the top of the granular layer. As will be detailed below, a critical fluid velocity  $U_c$  as well as the growth rate of the fluidized cavity above this threshold can be precisely defined. Using the relevant dimensionless numbers of the problem, a general collapse of the data can be obtained, which permits the proposal of empirical scaling laws both for the critical velocity and for the fluidization growth rate.

The following sections first introduce the numerical approach developed in the present study and then focus specifically on the transient regime to fluidized chimney within an immersed granular bed subject to a localized fluid injection at its base.

## 2 NUMERICAL METHODS

Many numerical methods are developed to simulate fluid-particles interactions at the micro-scale. The crucial point is the approach taken to couple the particles’ dynamics and the interstitial fluid flow. Here we have chosen to tackle this issue by a simultaneous use of the Discrete Element Method (DEM) and of the Lattice Boltzmann Method (LBM). This choice has the advantage to combine the comparative simplicity of DEM with LBM, one of the most efficient computational methods for fluid dynamics. Both methods as well as the coupling strategy are briefly described below.

## 2.1 DEM modeling of the solid phase

In this study, the Discrete Element Method (DEM) is implemented through the Molecular Dynamics modeling, a numerical method originally developed by Cundall and Strack [8] for rock mechanics applications and which quickly became very popular in many other fields of application dealing with interacting solid particles [9]. The Molecular Dynamics method considers the solid material as discrete particles that interact with each other in areas of mutual contact. The particles are assumed to be rigid with possibly a small overlap at the contact while the interactions are modelled by appropriate and physically based laws depending on this overlap. Then, the particles' motion can be directly described by Newton's equations. More details can be found in [10, 11].

## 2.2 LBM modeling of the fluid phase

A classical D2Q9 scheme is used here for LBM describing the fluid flow within the grains, allowing for an explicit finite differences calculation of Boltzmann equation on a Cartesian lattice grid (2D) and using a discrete set of velocity vectors at each grid node (Q9) [12]. The calculation is related to a probability density function, discretized on the lattice, and computed in two successive steps: collision and advection, both assuming specific rules to ensure mass, momentum and energy conservation provided that Mach number is very low or, equivalently, that fluid velocity remains significantly smaller than the lattice speed. With this condition, the fluid flow follows the incompressible Navier-Stokes equations. Note also that, instead of the classical single relaxation time scheme originally proposed by Bhatnagar, Gross, and Krook [12], a multiple relaxation time (MRT) is advantageously implemented here, following the generalized formulation by d'Humières [13, 14]. Further details on this method can also be found in [10, 11].

## 2.3 Solid-fluid coupling

In our modelling, the simple technique proposed by Bouzidi et al. [15] for momentum exchange is implemented to calculate the hydrodynamic forces on each discrete particle and couple this way the fluid and solid phases. This computation is based on a generalized bounce-back condition with a linearly interpolated geometry of the particles boundary inside the fluid lattice. A key parameter for the fluid-solid coupling is the space resolution, i.e. the lattice grid size compared to the minimum particle diameter. It is commonly accepted that a satisfactory result can be obtained with at least 10 grid points per grain diameter, which is the resolution used in the present study for an affordable computational cost. Moreover, as the calculation time is much larger for LBM than DEM, we have used the sub-cycling time integration technique proposed by Feng et al [16] with a number of DEM sub-cycles which is restricted to 2 for each LBM loop, a good compromise to maintain the accuracy of the computed hydrodynamic forces on the solid particles. In order to overcome the fact that a real 2D assembly of discs in contact is an occluded space with a zero permeability value, the LBM calculations are here carried out with a constant reduction of the particles' radius by a factor of 0.8, which provides a realistic permeability value [17] and roughly accounts for lubrication forces [18].

### 3 TRANSIENT REGIME TO FLUIDIZED CHIMNEY

#### 3.1 Configuration and parameters

Based on the coupled DEM-LBM technique described above, a two-dimensional numerical modeling was carried out to simulate an assembly of grains subjected to a localized fluid injection at its base. Grain sizes have a mean value  $d$  and are uniformly distributed from  $0.8d$  to  $1.2d$ . Two different samples have been used with initial height  $H_0$  equal respectively to approximately 86 mm and 54 mm while the overall domain dimensions are  $L = 222$  mm in length and  $H = 160$  mm in height. The bottom boundary is a solid wall except for a filtering orifice of width  $D = 14$  mm at its center which allows the fluid to be injected upwards at a constant velocity  $U$  but remains impassable for the grains. A velocity inlet condition is thus implemented at the injection hole while a periodic condition is set at the top and bottom boundaries of the domain. A no-slip condition is implemented on all other boundaries, considered as solid walls. A sketch of the configuration is shown in Figure 1.

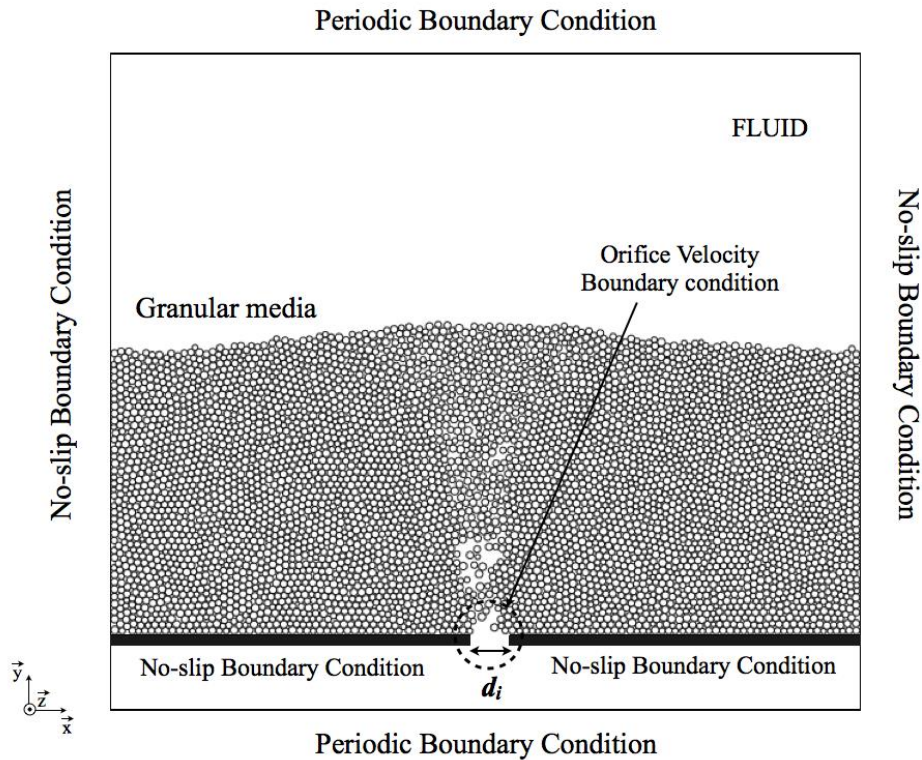


Figure 1: Configuration and boundary conditions of the numerical study.

To reach a fluidized state, the drag forces induced by the interstitial flow must overcome the inter-granular forces within the particles' sample. In the studied conditions of purely frictional interactions between grains, the internal granular stress is solely related to the buoyant weight of the system. Consequently, the physical parameters of the problem are: the diameter of the grains  $d$ , the kinematic viscosity of the fluid  $\nu_f$ , the density of the fluid  $\rho_f$  and

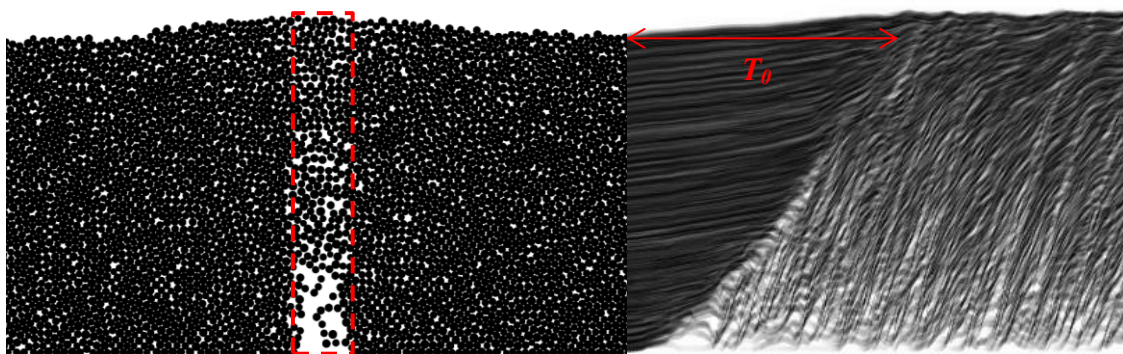
of the grains  $\rho_g$ , and finally the gravity  $g$ . The control parameter used here is the injected fluid velocity  $U$  while the geometry of the system is fixed by the initial height  $H_0$ , the width of the domain  $L$  and the diameter of the injection hole  $D$ . In what follows,  $L$  and  $D$  remain unchanged and, since  $D$  is much smaller than  $L$  ( $D/L \approx 0.06$ ), it can be reasonably considered that  $L$  plays a minor role.

A parametric study has been carried out using 11 different parameter sets (see Table 1) enabling some of the physical parameters to be significantly varied, namely  $v_f$ ,  $\rho_g$ ,  $g$  and  $d$ . Two different values of the initial height  $H_0$  has also been used while the injection diameter  $D$  was kept constant ( $D = 14\text{mm}$ ).

**Table 1:** Sets of parameters

Set number	$v_f$ ( $\text{m}^2 \cdot \text{s}^{-1}$ )	$\rho_g$ ( $\text{kg} \cdot \text{m}^{-3}$ )	$g$ ( $\text{m} \cdot \text{s}^{-2}$ )	$d$ (mm)
1	$5 \cdot 10^{-5}$	2500	9.81	2
2	$1 \cdot 10^{-5}$	2500	9.81	2
3	$5 \cdot 10^{-5}$	2500	1	2
4	$1 \cdot 10^{-5}$	1500	9.81	2
5	$5 \cdot 10^{-5}$	1500	9.81	2
6	$5 \cdot 10^{-5}$	2500	1	2
7	$5 \cdot 10^{-6}$	2500	9.81	2
8	$5 \cdot 10^{-6}$	1500	9.81	2
9	$2 \cdot 10^{-6}$	2500	9.81	2
10	$2 \cdot 10^{-6}$	1500	9.81	2
11	$5 \cdot 10^{-5}$	2500	9.81	4

For all parameter sets, the analysis of the transitory evolution to final fluidized chimney is performed using space-time diagrams constructed at the injection from the different sequences obtained for each successive fluid velocity  $U$  imposed at the injection hole (Figure 2). From these diagrams, it is then possible to determine quite accurately the time  $T_0$  needed for the fluidized zone to expand upwards to a height equal to  $H_0$ .



**Figure 2:** Typical space-time diagram used to determine the duration  $T_0$  of the transient regime and calculated in the rectangular area (in dotted line) located above the injection hole.

### 3.2 Chimney expansion time and growth rate

Plotting the chimney expansion time  $T_0$  as a function of the injection velocity  $U$ , a divergence is observed when  $U$  tends to a threshold value  $U_c$  which can be accurately determined by use of the following power law adjustment of the curve:

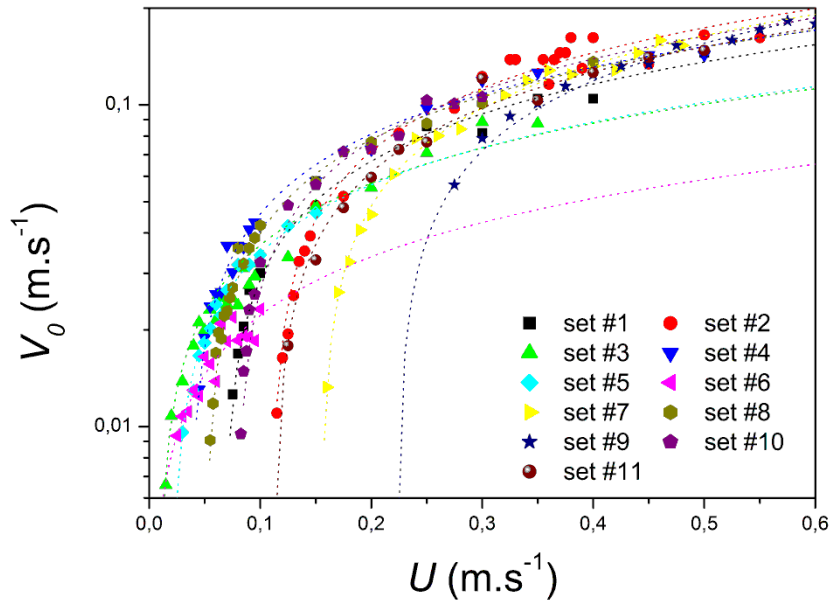
$$T_0(U) = \tau_0(U/U_c - 1)^{-\alpha} \quad (1)$$

where  $\tau_0$  is a constant equal to  $T_0(U = 2U_c)$  and  $\alpha$  is the opposite of the exponent.

The value of  $\alpha$  can be satisfactorily chosen within the range  $0.5 < \alpha < 0.7$  with a small but still significant impact on the threshold velocity  $U_c$ . Of probably greater interest is  $V_0 = H_0/T_0$ , the characteristic growth rate which quantifies the velocity at which the fluidized zone expands upwards. Here again, as shown in Figure 3, a power law can be used with the opposite exponent  $\alpha$ :

$$V_0(U) = \Lambda_0(U/U_c - 1)^\alpha \quad (2)$$

where  $\Lambda_0$  is a constant equal to  $V_0(U = 2U_c)$ .



**Figure 3:** Characteristic growth rate  $V_0$  of the fluidized zone versus fluid injection velocity  $U$  for  $H_0 = 86$  mm. The lines are power law functions given by Equation (2) with  $\alpha = 0.6$ .

It can be noted that in the present study  $\alpha$  has been arbitrarily fixed equal to 0.6 and, depending on the parameters in Table 1, the values obtained for  $U_c$  vary on several orders of magnitude as can be noticed in Figure 3.

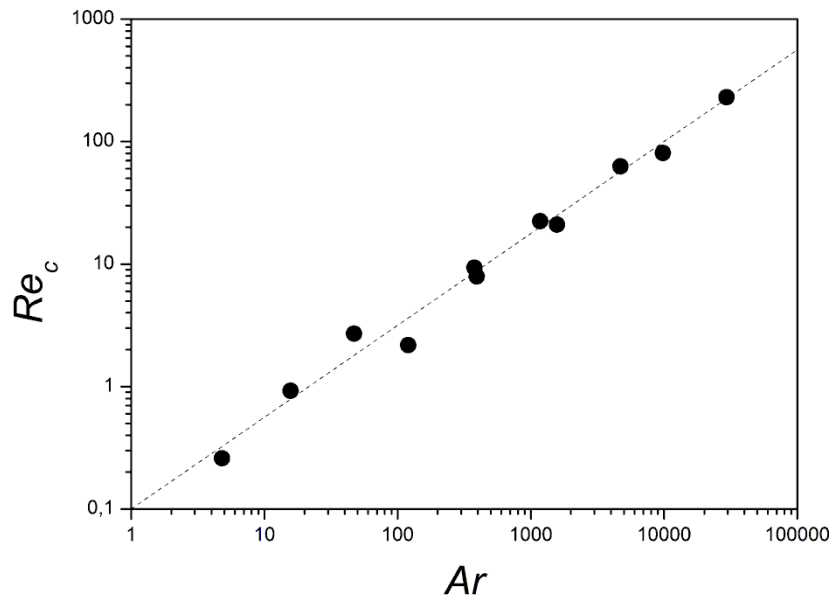
### 3.3 Scaling laws

Accounting for buoyancy, the only relevant physical quantities are the fluid kinematic viscosity  $\nu_f$ , the fluid injection velocity  $U$ , the grain diameter  $d$ , and the resultant buoyant

gravity  $g^* = g(\rho_g / \rho_f - 1)$ . From these magnitudes, two dimensionless numbers can be formed, namely the Reynolds number  $Re = Ud/v_f$  and the Archimedes number  $Ar = g^*d^3/v_f^2$ . And thus, the critical Reynolds number  $Re_c = U_c d/v_f$  should consequently be simply dependent on  $Ar$ . As shown in Figure 4, such a relationship is indeed reasonably well obtained for all values corresponding to the 11 different sets of parameters and a very simple empirical power law relation can be proposed:

$$Re_c \propto Ar^{3/4} \quad (3)$$

Therefore, the dependencies on the geometrical parameters  $H_0$  and  $D$  are completely taken into account by the proportionality factor in Equation (3).



**Figure 4:** The critical Reynolds number  $Re_c$  plotted as a function of Archimedes number  $Ar$  for  $H_0 = 86$  mm. The line corresponds to Equation (3) with a proportionality factor equal to 0.1.

Such a dimensional analysis can be extended beyond the critical value for chimney fluidization to account more broadly for the transient behavior obtained once this threshold is exceeded, i.e. for  $U > U_c$ . For this purpose, we now use the general expression of the Reynolds number,  $Re = Ud/v_f$ , while the characteristic growth rate  $V_0$  is also made dimensionless by introducing a new Reynolds numbers  $Re_0$  defined as follows:

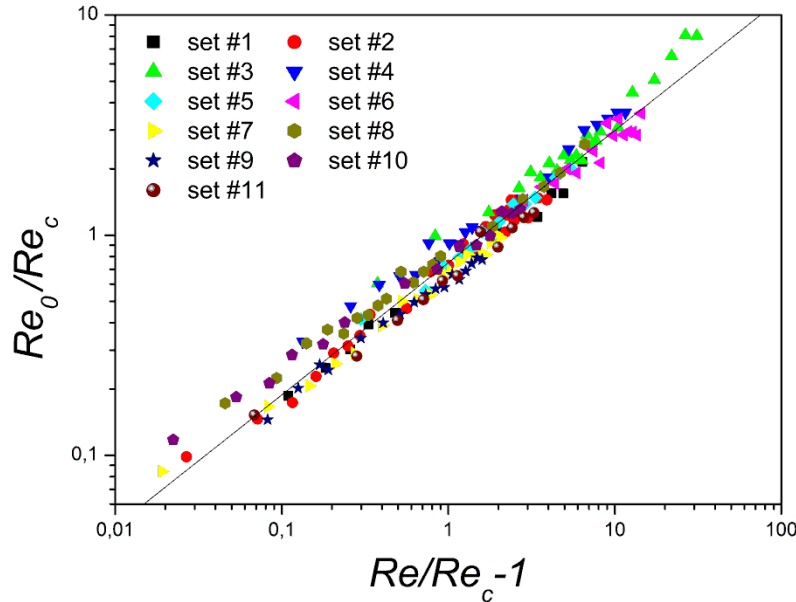
$$Re_0 = V_0 d/v_f \quad (4)$$

Finally, to get rid of the additional dependencies due to the geometry of the system (mainly through the initial height  $H_0$ ),  $Re$  and  $Re_0$  are both divided by the critical Reynolds number  $Re_c$ . This way, as shown in Figure 5, a global collapse of all the data is obtained, confirming the previous analysis. Moreover, following Equation (2), a general empirical scaling law can now be proposed in the form:

$$Re_0 / Re_c \propto (Re / Re_c - 1)^{3/5} \quad (3)$$



Note that the proportionality factors obtained for the two values of  $H_0$  used in this study are indeed rather close although slightly different, equal to 0.75 and 0.95 respectively for  $H_0 = 86$  mm and  $H_0 = 54$  mm.



**Figure 5:** The ratio  $Re_0/Re_c$  plotted versus  $Re/Re_c - 1$  for  $H_0 = 86$  mm. The line stands for Equation (5) with a proportionality factor being equal to 0.75.

#### 4 CONCLUSION

A 2D coupled DEM-LBM model has been implemented to produce a realistic representation of fluid-grains interactions and dynamics. This model has been successfully applied to study the particular phenomenon of development of a fluidized chimney within an immersed granular bed from a small fluid injection hole at the base of a grain assembly. Focusing specifically on the transient regime leading to a steady chimney, a parametric analysis has been undertaken with 11 different sets of the main physical parameters involved in the problem. The first outcome of this study shows that the critical fluid velocity  $U_c$  needed for such a chimney fluidization can be clearly interpreted in terms of dimensionless numbers. The corresponding critical Reynolds  $Re_c = U_c d / \nu_f$  is indeed simply a function of the Archimedes number  $Ar = g(\rho_g / \rho_f - 1) d^3 / \nu_f^2$  which is fairly compatible with an empirical power law relation:  $Re_c \propto Ar^{3/4}$ .

In addition, the characteristic growth rate  $V_0$ , i.e. the upward expansion rate of the fluidized zone, can also be predicted from our dimensional analysis provided that additional Reynolds numbers are formed using the different velocities of the system:  $U$ ,  $U_c$  and  $V_0$ . This way, it is possible to obtain a general collapse of all data from the different parameter sets, allowing the proposal of a very simple empirical law:  $Re_0 / Re_c \propto (Re/Re_c - 1)^{3/5}$ .

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