

REDUCING ENERGY USE IN FOOD MANUFACTURING BY PROCESS FLOWSHEETING

Application to milk concentration by evaporation

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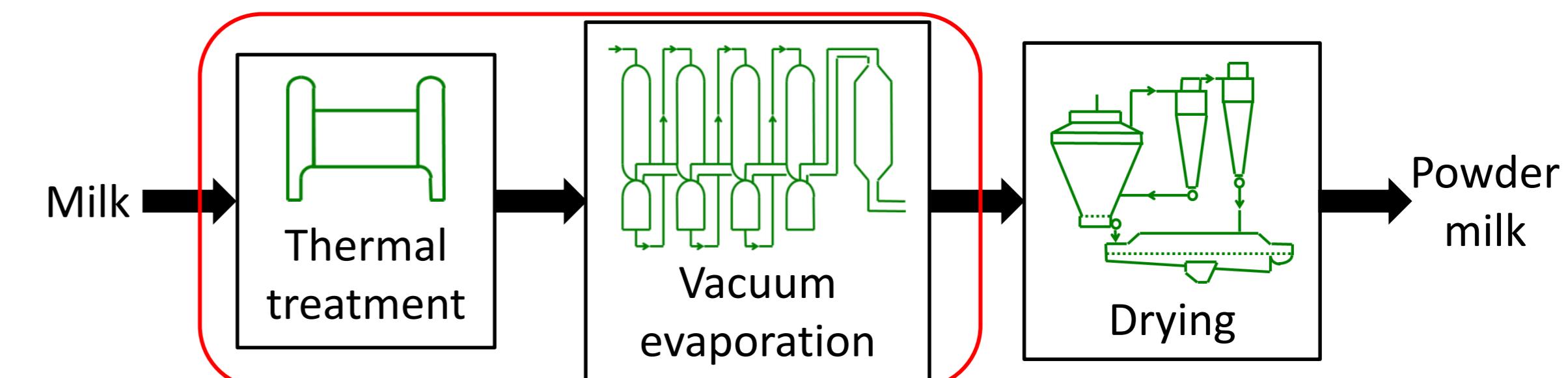
Context

The design and development of **sustainable food processes** constitute a major challenge in a context of transitions that encompass climate change, energy scarcity and energy price increase. A systemic approach combining **process modelling**, **simulation**, and **optimization** can be a sound way of coping with this issue. While the benefit of using computer-aided process engineering tools has long been recognized in the chemical industry, their use is not yet systematic in the development of food processes.

Objective

Develop a process modelling and simulation tool for embedding in a framework for the systemic eco-design of food processes.

Approach: **modelling food products with property models from the literature, directly specified in a chemical process simulator**; applying the tool to the modelling and simulation of dairy concentration processes.



Modelling the properties of liquid food products in a chemical process simulator

1 Definition of milk in the simulator

Water	Component from the simulator database
Fat	
Proteins	
Lactose	
Minerals	User-defined components

Milk behaviour is defined only by liquid mixture property models.

2 Selection of food property models: comparison of existing models and experimental data over a range of temperature and dry matter content

Whole milk concentrate at 28% dry matter

Example of heat capacity

3 Input macroscopic models in Aspen Plus as Fortran programs compiled and linked to Aspen Plus

Validating the selected milk properties models with an industrial and a pilot-scale processes

Industrial process (Ribeiro, 2001)
4-effect plate evaporator

Pilot-scale process (Silveira et al., 2013)
Mono-effect, 3 tubes evaporator

Materials and methods

Results

1 Choice of the milk properties models

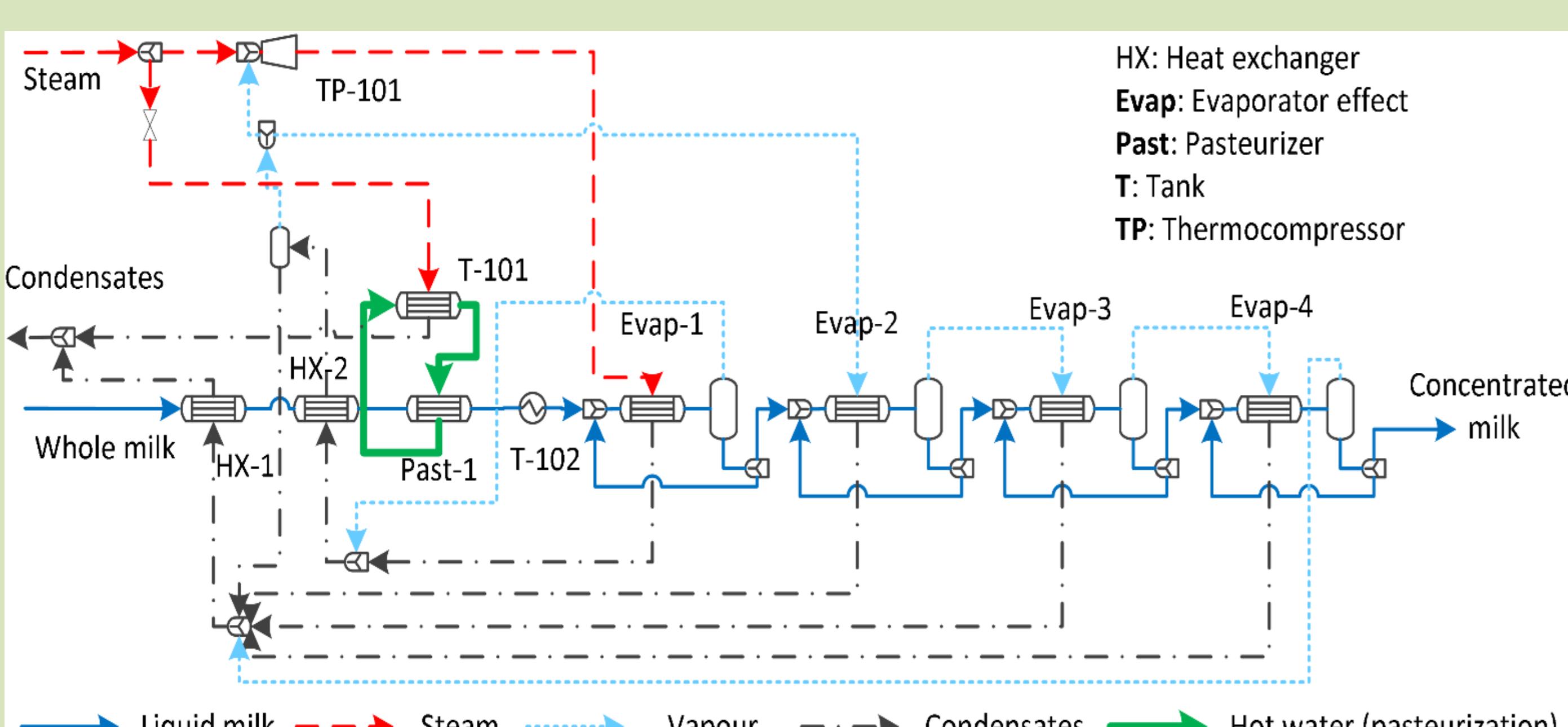
Heat capacity	$C_p = \sum C_{p,i} \times X_i$ With temperature-dependant correlations for fat, protein, carbohydrates and minerals.	Choi and Okos, 1986
Boiling Point Elevation	$\Delta T_{BPE} = \left[\frac{1}{\frac{1}{T_{SAT}} + R \times \ln(1 - x_{SOL})} - T_{SAT} \right]$	Winchester, 2000
Density	$\rho = \frac{1}{\sum X_{W,i} / \rho_i}$ With temperature-dependant correlations for fat, protein, carbohydrates and minerals.	Choi and Okos, 1986
Thermal conductivity	$\lambda = (326.58 + 1.0412 \times T - 3.37 \times 10^{-3} \times T^2) \times (0.46 + 0.54 \times X_{Water}) \times 1.73 \times 10^{-3}$	Riedel, 1949
Viscosity	$\mu = 1000 \times \mu_{Water} \times \exp\left(\frac{\sum A_i \times X_{W,i}}{X_{W,Water}}\right)$ With temperature-dependant coefficients A_i for fat, proteins and carbohydrates.	Morison et al., 2013
Surface tension	General model (whole milk & skim milk): $\sigma = 55.6 - 0.163 \times T + 1.8 \times 10^{-4} \times T^2$	Bertsch, 1983

X_i	Component mass fraction
x_{SOL}	Component molar fraction
T	Temperature (°C)
T_{SAT}	Saturation temperature (°C)
H_{VAP}	Water vaporization enthalpy (J.kg⁻¹)

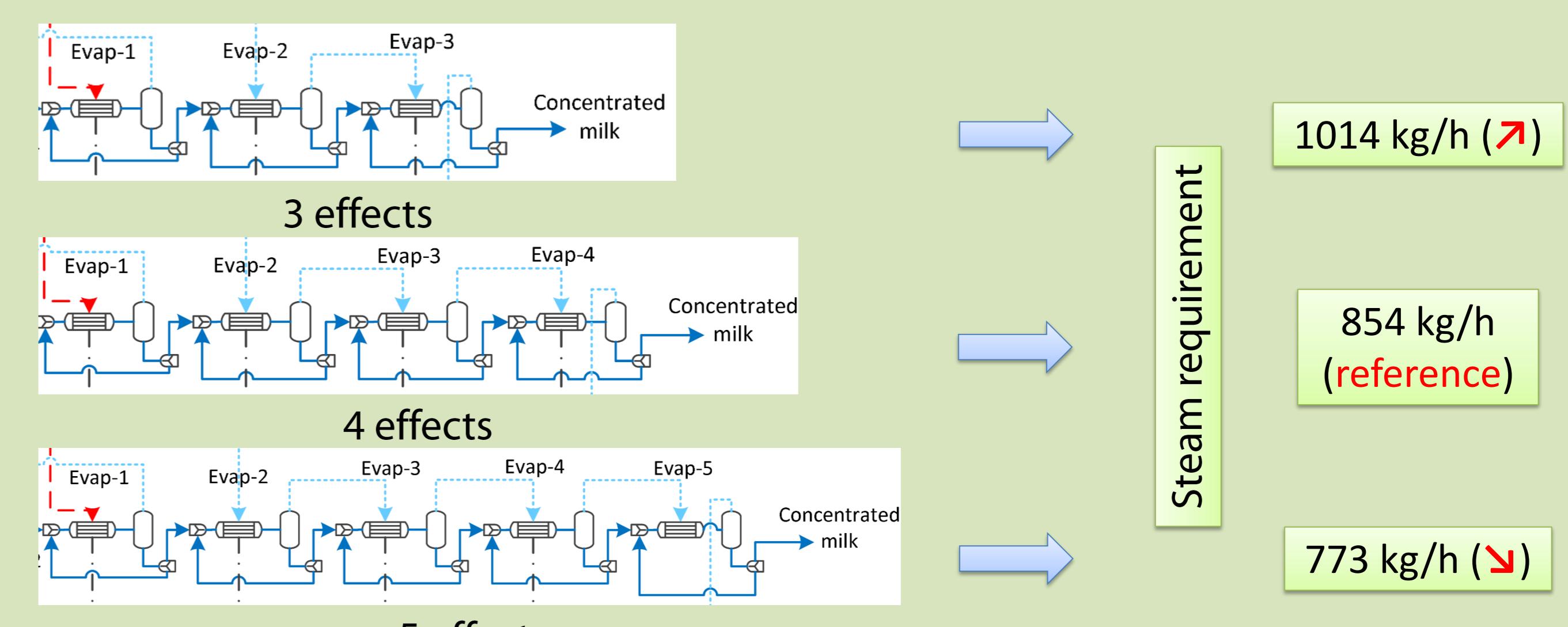
2 Validation of the modelling approach: modelling and simulating milk concentration processes

	Effect 1	Effect 2	Effect 3	Effect 4
Concentrate dry matter	Simulation	20.4%	25.2%	33.0%
Industrial results		20.5%	25.2%	48.0%
Concentrate temperature	Simulation	66.2°C	61.3°C	55.8°C
Industrial results		66.0°C	61.0°C	45.1°C
	Run 10% → 24%	Run 24% → 52%		
Concentrate dry matter	Simulation	21.9%	45.5%	
Pilot-scale process	Experimental results	24.0%	52.0%	
Concentrate temperature	Simulation	60.4°C	61.0°C	
	Experimental results	60.0°C	60.0°C	

3 Computing energy requirements of the industrial process for different evaporator configurations



Evaporator design



1014 kg/h (↗)

854 kg/h (reference)

773 kg/h (↘)

Conclusions and perspectives

- A process flowsheeting simulator has been adapted to the simulation of milk concentration processes by incorporating milk physico-chemical property models retrieved from the literature.
- In order to validate the approach, simulations have been performed on thermal treatments and vacuum evaporation steps, classically carried out prior to spray drying.
- The capabilities of the simulator have been used to study energy reduction scenarios.
- The modelling approach may be applied to different food products (fruit juice, whey...).
- This is a first step towards an eco-design approach combining modelling, cost analysis, environmental analysis and multi-objective optimization.

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