Numerical simulation of combined natural convection surface radiation for large temperature gradients

Saber Hamimid, Messaoud Guellal, Madiha Bouafia

Numerical Simulation of Combined Natural Convection Surface Radiation for Large Temperature Gradients

Saber Hamimid* and Messaoud Guellal†
Université Ferhat Abbas, Sétif 19000, Algeria
and
Madiha Bouafia‡
Université d'Évry Val-d'Essonne, 91000 Évry, France

Nomenclature

Cp	=	dimensionless specific heat
F_{ij}	=	geometry view factor
g	=	gravitational acceleration
H	=	dimension of the enclosure
k	=	thermal conductivity
Nr	=	dimensionless parameter of conduction–radiation, $\sigma T_0^4 H/k\Delta T$
Nu	=	convective Nusselt number
Pr	=	Prandtl number, ν/α
p	=	dynamic pressure
p'	=	dynamic perturbed pressure
$\bar{p}$	=	mean thermodynamic pressure
Qr	=	dimensionless net radiative heat flux
R_i	=	radiosity
Ra	=	Rayleigh number, $g\beta\Delta T H^3/(\nu\alpha)$
T	=	temperature
t	=	dimensionless time
U, V	=	dimensionless velocity components
X, Y	=	dimensionless coordinates
α	=	thermal diffusivity, $k/\rho \cdot Cp$
β	=	thermal expansion coefficient
ε_b	=	temperature difference parameter (Boussinesq parameter), $\Delta T/2T_0$
Θ	=	dimensionless radiative temperature, T/T_0
θ	=	dimensionless temperature, $(T-T_0)/(T_h-T_c)$
μ	=	dimensionless dynamic viscosity
ν	=	kinematic viscosity
Π	=	dimensionless pressure, $(p-\bar{p}+\rho_0 g y)/\rho_0(\alpha_0/H)^2$
ρ	=	dimensionless fluid density
σ	=	Stefan–Boltzmann constant

Subscripts

avg	=	average value
BS	=	Boussinesq model
CP	=	constant properties
c	=	cold
h	=	hot
max	=	maximum value
mid	=	midplane
min	=	minimum value
0	=	reference state

*Assistant Professor, Laboratoire de Génie des Procédés Chimiques; sab_hamimid@yahoo.fr (Corresponding Author).
†Professor, Laboratoire de Génie des Procédés Chimiques; messaoud.guellal@gmail.com.
‡Professor, Laboratoire de Mécanique et d'Energétique d'Evry; madiha.bouafia@ufrst.univ-evry.fr.

I. Introduction

Coupled natural convection and radiation transport processes in cavities are interesting topics concerning thermal and mass transport processes involved in various types of engineering systems, such as solar energy collectors, cooling of electronic devices, multilayered walls (facades) and double windows, thermal behavior in nuclear reactors, space technology, and processes involving high temperatures.

In most of the work reported on enclosure (coupling natural convection with surface radiation), the Boussinesq approximation has been invoked. However, for higher overheat ratios, compressibility effects need to be taken into account, since the Boussinesq approximation can become inadequate. Such an approximation leads to an accurate description of convection flows if the temperature difference in the flow domain does not exceed a few degrees. However, in many physical and industrial applications such as thermal insulation systems, chemical vapor deposition reactors [1], atmospheric flows [2,3], and combustion process [4,5], the temperature differences reach tens and hundreds of degrees; all the assumptions used to justify the Boussinesq approximation fail; and a different, more complicated modeling approach is required that accounts for realistic nonlinear fluid properties variations. The low-Mach-number (LMN) approximation suggested by Paolucci [6], and used later by Hamimid et al. [7] for pure natural convection, allows one to take into account arbitrary property variations for a general fluid.

This study illustrates a comparative investigation to analyze the physical differences between numerical simulations obtained with both the Boussinesq and LMN forms of the Navier–Stokes equations for natural convection flow coupled with surface radiation in simple geometries. The purpose of this Note is to study the combined effects of surface radiation and temperature-dependent viscosity and conductivity on the momentum and heat transfer in the enclosure, as well as to quantify how the incompressible flow assumption differs from the compressible form when solving flows driven by gravity acting upon density variations resulting from local temperature gradients.

A complete parametric study is made for different Rayleigh numbers, conductivities and viscosities of the fluid, Boussinesq parameter, and wall emissivity. From these simulations, the selected characterization parameters of the maximum convective and radiative Nusselt number, the average Nusselt number, and the normalized pressure reduction were calculated. Comparisons of these parameters were made with benchmark solutions for air with the ideal gas assumption. Additionally, we generated vertical and horizontal velocities at the midvertical plane and midhorizontal planes, respectively, streamlines, and isotherms distributions to provide a basis for further analysis.

II. Problem Formulation

We consider a bidimensional square cavity of side H (Fig. 1) filled with a variable-property Newtonian fluid of density ρ, molecular viscosity μ, thermal conductivity k, and temperature T. The natural convection problem is described by two vertically heated walls with

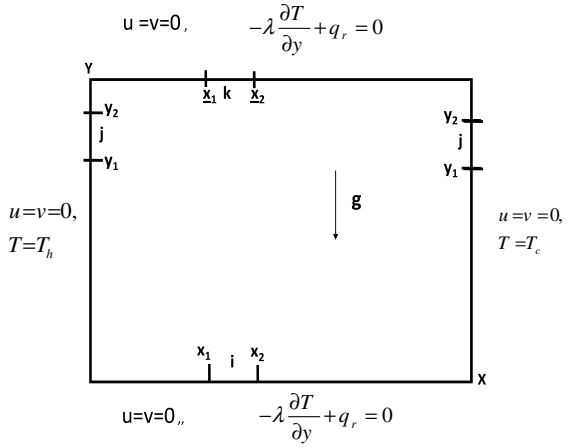

Fig. 1 Flow configuration and coordinate system.

prescribed temperatures T_h and T_c ($T_h \succ T_c$), which are the "hot" and "cold" wall temperatures, respectively. We assume that the horizontal surfaces are under the combined action of the convective and radiative contributions such as $-k\frac{\partial T}{\partial y}+q_r=0$. All four walls have no-slip zero-mass flux boundary conditions ($\boldsymbol{V}=0$) and have the same emissivity value, ε. A Cartesian (x, y) coordinate system is selected with y pointing vertical and x horizontal; thus, the gravitational vector $\boldsymbol{g}$ is applied on the y coordinate. Initial conditions are composed of constant distributions of reference pressure and temperature, p_0 and T_0, and stationary flow ($\boldsymbol{V}=0$). The reference temperature T_0 is defined as $T_0=(T_h+T_c)/2$. Using the mean temperature and the temperature difference between the hot and cold walls ($\Delta T=T_h-T_c$), we introduce the Boussinesq ratio $\varepsilon_b=\Delta T/2T_0$. The inner surfaces, in contact with the fluid, are assumed to be gray, diffuse emitters and reflectors of radiation with identical emissivity.

In addition to assuming a Newtonian fluid, another assumption must be made in order to obtain the usual compressible Navier–Stokes equations. This assumption has to do with the relationship between the dynamic and bulk viscosity coefficients (μ and λ) that relate the strain rate and the stress: $\lambda+\frac{2}{3}\mu=0$.

A low-Mach-number [8–14] flow model is used to describe the dynamics of the heated cavity. In this limit, the complete Navier–Stokes equations are expanded in powers of a small parameter M^2 (where M is the Mach number), and the total pressure P is decomposed into the mean thermodynamic pressure $\bar{p}(t)$ and the dynamic pressure P'.

A. Governing Equations

Since we are interested in the case of large temperature differences, the low-Mach-number equations are adopted in order to describe such a flow. The equations are made nondimensional by the use of the nondimensional variables:

$$\frac{x}{H},\quad \frac{y}{H},\quad \frac{uH}{\alpha_0},\quad \frac{vH}{\alpha_0},\quad \frac{t}{H^2/\alpha_0},\quad \frac{pH^2}{\rho_0\alpha_0^2},\quad \frac{(T-T_0)}{(T_h-T_c)},\quad \text{and}$$

$$\prod=\frac{\pi}{\rho_0(\alpha_0/H)^2}=\frac{p-\bar{p}+\rho_0 gy}{\rho_0(\alpha_0/H)^2}$$

The thermophysical properties (density, dynamic viscosity, thermal conductivity, and thermal diffusivity) are scaled by ρ_0, μ_0, k_0, and α_0, where the subscript 0 denotes values at the reference temperature T_0. The influence of the temperature on the specific heat is assumed to be negligible so that $C_p/C_{p0}=1$ [15].

The system Navier–Stokes equations are expressed in nondimensional conservative form [7] as

$$\frac{\partial\rho}{\partial t}+\frac{\partial\rho U}{\partial X}+\frac{\partial\rho V}{\partial Y}=0 \tag{1}$$

$$\rho\left(\frac{\partial U}{\partial t}+U\frac{\partial U}{\partial X}+V\frac{\partial U}{\partial Y}\right)=-\frac{\partial\Pi}{\partial X}+Pr\left\{\frac{\partial}{\partial X}\left(\mu\frac{\partial U}{\partial X}\right)+\frac{\partial}{\partial Y}\left(\mu\frac{\partial U}{\partial Y}\right)+\frac{1}{3}\nabla\mu\nabla.\boldsymbol{V}\right\} \tag{2}$$

$$\rho\left(\frac{\partial V}{\partial t}+U\frac{\partial V}{\partial X}+V\frac{\partial V}{\partial Y}\right)=-\frac{\partial\Pi}{\partial Y}-RaPr\frac{\rho-1}{2\varepsilon_b}+Pr\left\{\frac{\partial}{\partial X}\left(\mu\frac{\partial V}{\partial X}\right)+\frac{\partial}{\partial Y}\left(\mu\frac{\partial V}{\partial Y}\right)+\frac{1}{3}\nabla\mu\nabla\cdot\boldsymbol{V}\right\} \tag{3}$$

$$\rho c_p\left(\frac{\partial\theta}{\partial t}+U\frac{\partial\theta}{\partial X}+V\frac{\partial\theta}{\partial Y}\right)=\frac{\partial}{\partial X}\left(k\frac{\partial\theta}{\partial X}\right)+\frac{\partial}{\partial Y}\left(k\frac{\partial\theta}{\partial Y}\right)+\frac{\gamma-1}{2\varepsilon_b\gamma}\frac{\mathrm{d}\bar{P}}{\mathrm{d}t} \tag{4}$$

$$\rho=\frac{\bar{P}}{(2\varepsilon_b T+1)} \tag{5}$$

Additional equations are needed to calculate the mean thermodynamic pressure $\bar{p}(t)$ and its derivate:

$$\frac{\mathrm{d}\bar{P}}{\mathrm{d}t}=2\varepsilon_b\gamma\cdot\frac{1}{\int_\Omega \mathrm{d}\Omega}\cdot\int_S k\frac{\partial T}{\partial n}\,\mathrm{d}S \tag{6}$$

$$\bar{P}=\frac{\int_\Omega \mathrm{d}\Omega}{\int_\Omega[1/(2\varepsilon_b\theta+1)]\,\mathrm{d}\Omega} \tag{7}$$

In this study, the fluid (air) is considered as a perfect gas at reference temperature $T_o=300\,\mathrm{K}$ (we set in this case $T_h=480$ K and $T_c=120$ K) and the transport coefficients $\mu(T)$ and $k(T)$ are given by Sutherland's law:

$$\mu=(2\varepsilon_b T+1)^{3/2}\frac{(1+S_\mu/T_0)}{2\varepsilon_b T+1+S_\mu/T_0} \tag{8}$$

Where $S_\mu=110.4$ [16]. The conductivity is given by

$$k(T)=\frac{\mu(T)}{Pr} \tag{9}$$

B. Radiative Analysis

When surface radiation transfer is considered in the analysis, the temperature boundary condition at the top and bottom adiabatic walls of the square cavity must be changed. Thus, one assumes that the solid surfaces are in thermal equilibrium under the combined action of the convective and radiative contributions, which give

$$\left.\frac{\partial\theta}{\partial Y}\right|_{Y=0,1}-NrQ_r=0 \tag{10}$$

where $Nr=\sigma T_0^4 H/k\Delta T$ is the dimensionless parameter of conduction–radiation, and $Q_r=q_r/\sigma T_0^4$ is the dimensionless net radiative heat flux on the corresponding insulated wall expressed as

$$Q_{r,i}=R_i-\sum_{j=1}^{N}R_j F_{i-j} \tag{11}$$

where R_i is the dimensionless radiosity of surface A_i, obtained by resolving the following system:

$$\sum_{j=1}^{N}(\delta_{ij}-(1-\varepsilon_i)F_{i-j})R_j=\varepsilon_i\Theta_i^4 \tag{12}$$

where the dimensionless radiative temperature Θ_i is given by

$$\Theta_i = \frac{T_i}{T_0} = [(T_h - T_c)\theta_i + T_0]/T_0 = \theta_i \frac{\Delta T}{T_0} + 1 = \frac{\theta_i}{\theta_0} + 1 \quad (13)$$

C. Heat Transfer Parameters

The nondimensional heat transfer rate in terms of convective and radiative Nusselt numbers, Nu_c and Nu_r, on the heated vertical surface are given by

$$Nu_c = -\left.\frac{\partial\theta}{\partial X}\right|_{Y=0,1} \quad (14)$$

$$Nu_r = N_r Q_r|_{Y=0,1} \quad (15)$$

The average convective Nusselt number was calculated by integrating the temperature gradient over the vertical wall as

$$Nu_{c_{\text{avg}}} = \frac{1}{A}\int_0^A -\frac{\partial\theta}{\partial X}\,\mathrm{d}X \quad (16)$$

The average radiative Nusselt number is obtained by integrating the net radiative flux

$$Nu_{r_{\text{avg}}} = N_r \frac{1}{A}\int_0^A Q_r\,\mathrm{d}X \quad (17)$$

The total average Nusselt number is calculated by summing the average values of convective and radiative Nusselt numbers [17]:

$$Nu_{\text{avg}} = \frac{1}{A}\int_0^A \left(-\left.\frac{\partial\theta}{\partial X}\right|_{0,Y} + N_r Q_r(0,Y)\right)\mathrm{d}Y \quad (18)$$

D. Numerical Modeling

The numerical solution of the governing differential equations for the velocity, pressure, and temperature fields is obtained by using a finite volume technique. A power scheme was also used in approximating advection–diffusion terms. The SIMPLER algorithm, for which the details can be found in work by Patankar [18], with a staggered grid is employed to solve the coupling between pressure and velocity. The radiosities of the elemental wall surfaces are expressed as a function of elemental wall surface temperature, emissivity, and the view factors. The radiosity R_i and temperature θ_i are connected by a matrix of the type

$$[A_{i,j}]\{R_i\} = \{\sigma\theta_i^4\} \quad (19)$$

The inverse of the matrix $[A_{i,j}]$ is determined (only once) by the Gauss elimination method. The coefficients of $[A]$ are constants and depend only on the emissivity and view factors.

In a two-dimensional formulation, the view factors are analytic [19]:

$$F_{ij} = \frac{-1}{2(x_2 - x_1)}\left[\sqrt{x_2^2 + y^2}\Big|_{y_1}^{y_2} - \sqrt{x_2^2 + y^2}\Big|_{y_1}^{y_2}\right] \quad (20)$$

$$F_{i-k} = -\frac{1}{2(x_2 - x_1)}\left[\sqrt{(x_2 - x)^2 + H^2}\Big|_{x=x_1}^{x=x_2} - \sqrt{(x_1 - x)^2 + H^2}\Big|_{x=x_1}^{x=x_2}\right] \quad (21)$$

For the most computations reported in this study, 242×242 grid points were chosen to optimize the relation between the accuracy required and the computing time; nevertheless, in the case of variable properties, a 322×322 grid was used. The grid is nonuniform and very fine in the *near-wall* region.

III. Verification

The validity of the solution procedure described previously is demonstrated in this section by presenting a solution in the classical case of natural convection and surface thermal radiation in a Boussinesq approximation. A good agreement was found between the present calculations and those reported in the work of [20] (Table 1).

IV. Results and Discussion

In this section, the low-Mach-number code is applied to analyze the effect of the Boussinesq parameter ε_b, temperature-dependent fluid properties, and surface radiation on heat transfer and fluid flow in steady-state conditions.

The fixed parameters of simulation are $Pr = 0.71$, $T_0 = 300$ K, $A = 1$, and ε. However, to examine the effect of the Boussinesq parameter and emissivity, we consider different values of $\varepsilon_b(0 \ldots 0,6)$ and $\varepsilon(0 \ldots 1)$.

When the radiation exchange is taken into account, the characteristic dimension of the cavity may be calculated for a specific Rayleigh number ($H = 0.097$ in the case $Ra = 10^6$). For the Boussinesq solution, the difference temperature ΔT is fixed to 10 K. Substituting values of H and ΔT into the expression of Nr gives

$$Nr = \frac{\sigma T_0^4}{k\Delta T}\left(\frac{\nu\alpha}{g\beta\Delta T}\right)^{1/3} Ra^{1/3}$$

A. Effect of Boussinesq Parameter ε_b

Figures 2–10 allow comparison of the results obtained from Boussinesq, weak non-Boussinesq, and strong non-Boussinesq cases

Table 1 Nusselt number at active walls obtained with $T_0 = 293.5$ K and $\Delta t = 10$ K[a,b]

			Wang et al. [20]						Present work					
			Hot wall			Cold wall			Hot wall			Cold wall		
Ra	H	ε	Nu_c	Nu_r	Nu_t	Nu_c	Nu_r	Nu_t	Nu_c	Nu_r	Nu_t	Nu_c	Nu_r	Nu_t
10^4	0.021	0	2.246	0	2.246	2.246	0	2.246	2.246	0	2.246	2.246	0	2.246
10^4	0.021	0.2	2.260	0.507	2.767	2.268	0.499	2.767	2.262	0.507	2.769	2.271	0.498	2.769
10^4	0.021	0.8	2.249	2.401	4.650	2.278	2.372	4.650	2.255	2.401	4.656	2.284	2.371	4.656
10^5	0.045	0	4.540	0	4.540	4.540	0	4.540	4.532	0	4.532	4.532	0	4.532
10^5	0.045	0.2	4.394	1.090	5.484	4.411	1.073	5.484	4.398	1.090	5.489	4.417	1.072	5.489
10^5	0.045	0.8	4.189	5.196	9.385	4.247	5.137	9.384	4.200	5.196	9.397	4.261	5.136	9.397
10^6	0.097	0	8.852	0	8.852	8.852	0	8.852	8.863	0	8.863	8.863	0	8.863
10^6	0.097	0.2	8.381	2.355	10.736	8.417	2.319	10.736	8.379	2.355	10.734	8.416	2.318	10.734
10^6	0.097	0.8	7.815	11.265	19.080	7.930	11.150	19.078	7.861	11.265	19.126	7.971	11.151	19.126

[a] $Nu_t = Nu_c + Nu_r$.

[b] Comparison with values published in [20].

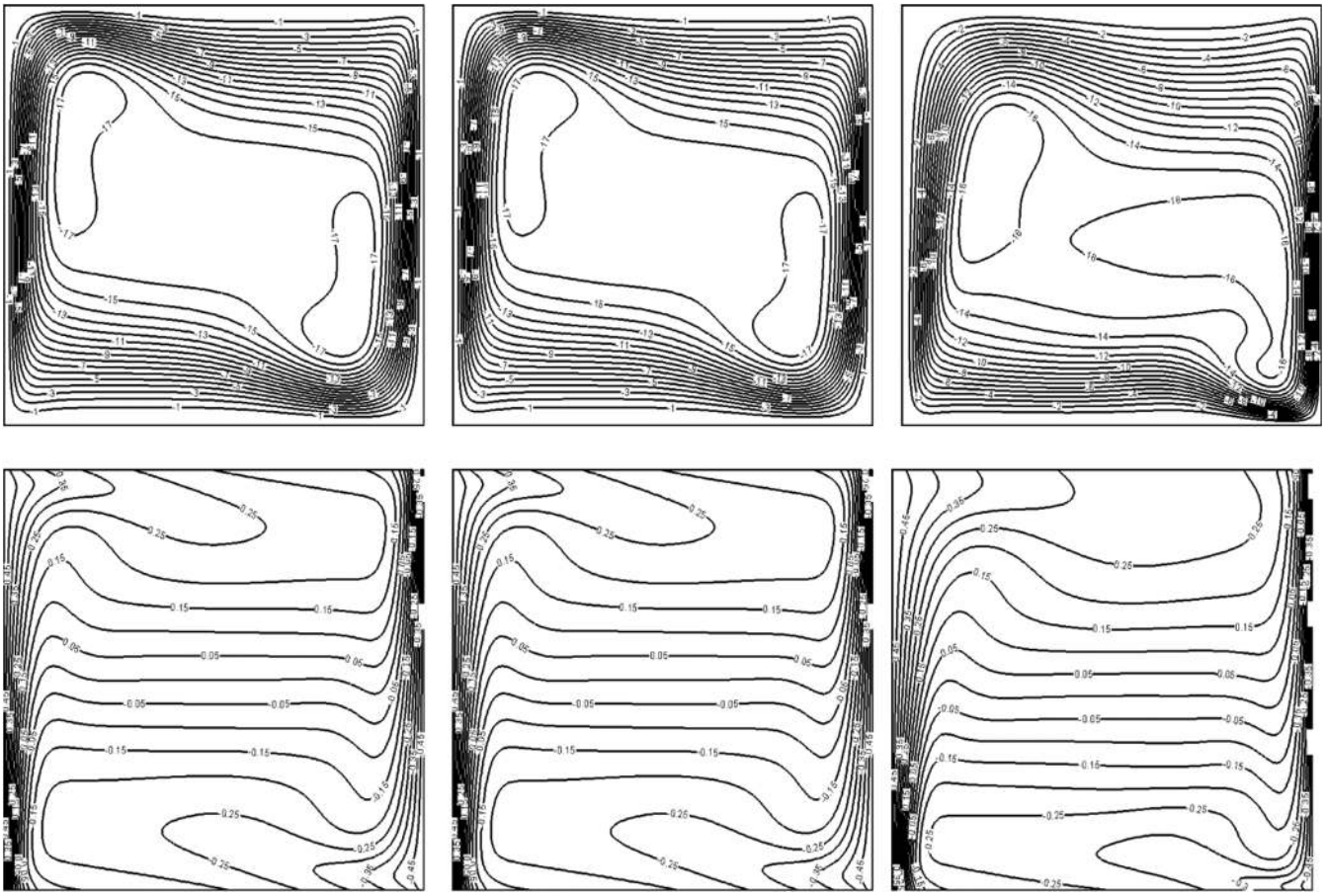

Fig. 2 Streamlines (top) and temperature contours (bottom) at $Ra = 10^6$ and $\varepsilon = 0.2$. From left to right, Boussinesq model (BS), $\varepsilon_b = 0.017$, and $\varepsilon_b = 0.6$.

at $Ra = 10^6$ in the presence of radiation with a wall emissivity of $\varepsilon = 0.2$. The properties are assumed to be variable.

From a general point of view, it can be seen that, for a low temperature difference ($\varepsilon = 0.017$), the solutions for compressible and incompressible models did not differ significantly. Isotherms and streamlines (Fig. 2) indicate a symmetric structure with respect to the cavity center with the presence of two secondary flows *symmetrically arranged at the cavity center.* At the horizontal walls, the isotherms show the existence of temperature gradients due to radiative exchange.

For a large temperature difference ($\varepsilon_b = 0.6$), the symmetric nature of the flow is broken. A rapid look in Fig. 2 allows us to note that the isotherms' slopes near the lower wall are different from those of the upper wall; moreover, the secondary rolls inside the primary flow are no longer symmetric.

Considering the convective heat transfer along the hot and cold walls, there is a remarkable change in their profiles according to the parameter ε_b (Fig. 3). This behavior is especially observed at the bottom, where the Nusselt number for $\varepsilon_b = 0.6$ is larger than for $\varepsilon_b = 0.017$ on the hot wall. An opposed comportment is noticed on the cold wall.

Profiles of the local radiative Nusselt number on the vertical walls are depicted on Fig. 4. The quasi-linear character of these profiles reflects a uniform temperature on each side. Note, however, that the difference between $Nu_r(h)$ and $Nu_r(c)$ is even more important, as the parameter ε_b is small. This remark is also observed on the horizontal walls (Fig. 5). The shape of these profiles reflects the temperature evolution on the top and bottom walls, which results from a balance between convective and radiative exchanges. Temperature profiles on the horizontal walls are plotted in Fig. 6. With increasing ε_b, the bottom wall is cooling while the top wall is heating.

Horizontal profiles of air temperature at the midheight of the cavity are displayed in Fig. 7. One can see that, for $\varepsilon_b = 0.6$, the thermal boundary layer gets thicker near the hot wall and thinner near the cold

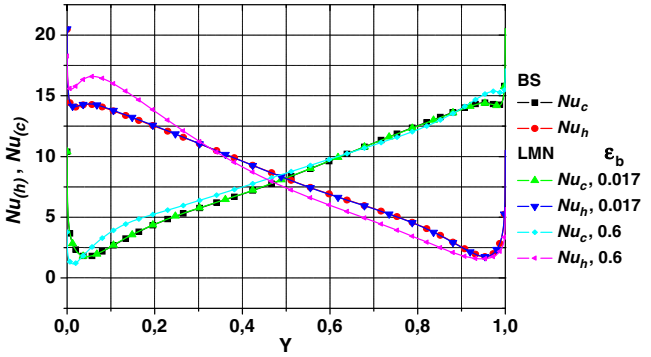

Fig. 3 Distributions of local Nusselt numbers on the hot and cold walls at $Ra = 10^6$ and $\varepsilon = 0.2$.

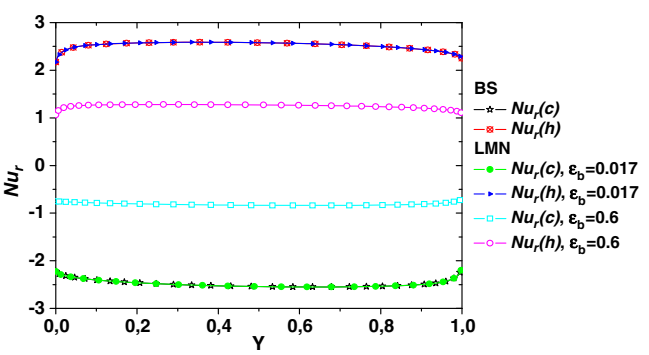

Fig. 4 Distribution of the local radiative Nusselt number on vertical walls at $Ra = 10^6$ and $\varepsilon = 0.2$.

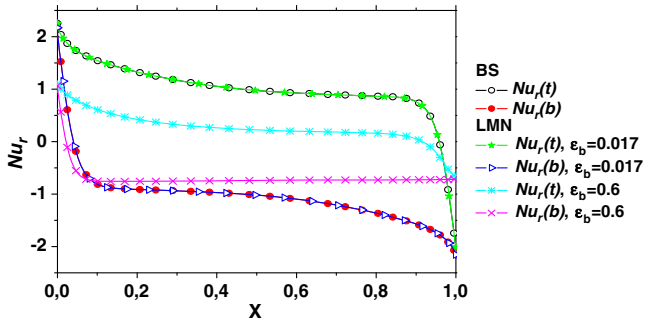

Fig. 5 Radiative Nusselt number distribution on the horizontal walls at $Ra = 10^6$ and $\varepsilon = 0.2$.

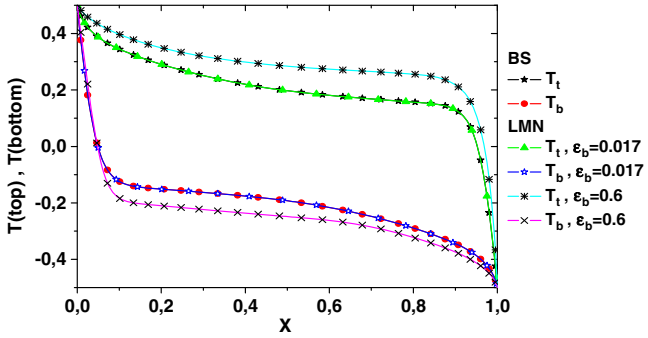

Fig. 6 Distributions of upper and lower wall temperatures for $Ra = 10^6$ and $\varepsilon = 0.2$.

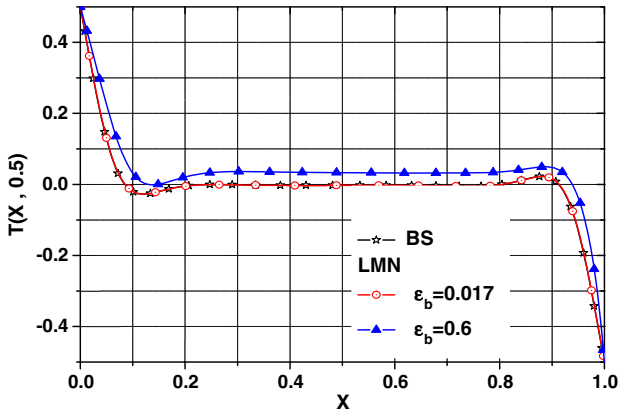

Fig. 7 Cross-section of the temperature at midheight cavity for $Ra = 10^6$ and $\varepsilon = 0.2$.

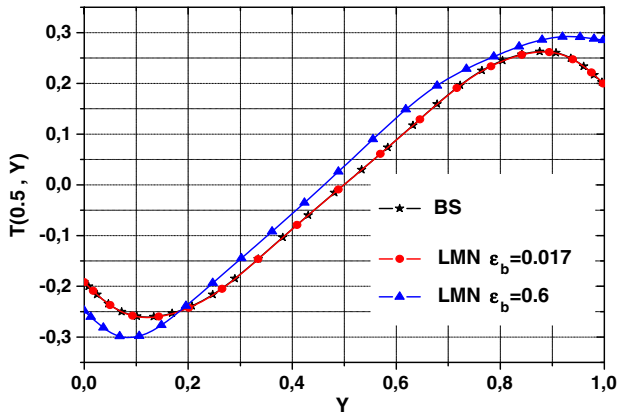

Fig. 8 Cross section of the temperature at $x = 0.5$ for $Ra = 10^6$ and $\varepsilon = 0.2$.

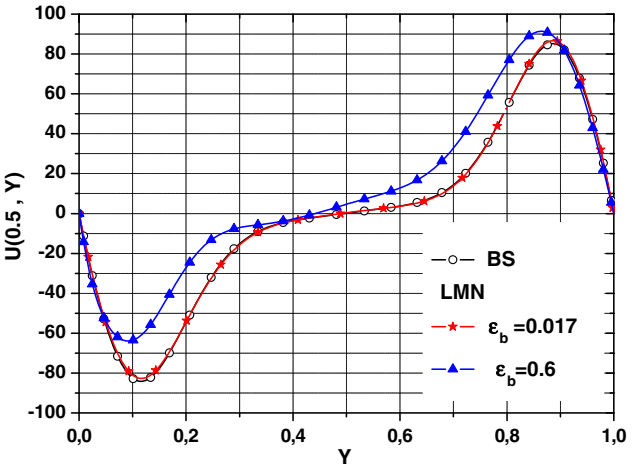

Fig. 9 Horizontal velocity at the vertical cross section at $x = 0.5$ for $Ra = 10^6$ and $\varepsilon = 0.2$.

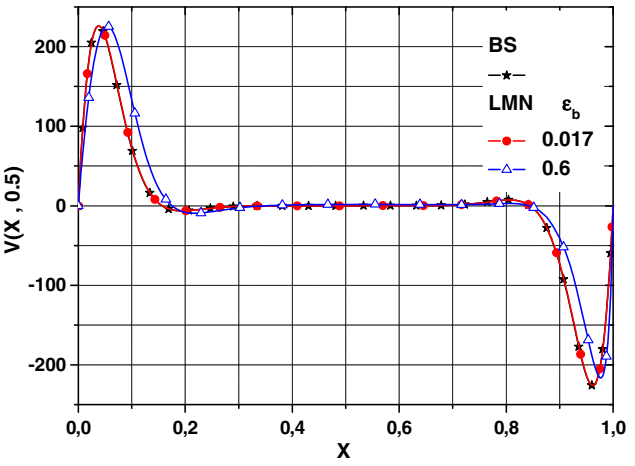

Fig. 10 Vertical velocity at the horizontal cross section at $y = 0.5$ for $Ra = 10^6$ and $\varepsilon = 0.2$.

wall, showing a deflection of peaks toward the cold wall. This behavior is due entirely to non-Boussinesq effects. In the center region, the fluid heats up with increasing ε_b and the stratification decreases, as shown in Fig. 8.

The effect of the parameter ε_b on the flow is presented in Figs. 9 and 10, where horizontal and vertical velocity components are plotted at $x = 0.5$ and $y = 0.5$, respectively. Compared to the case with a low value ($\varepsilon_b = 0.017$), profiles of the U component show that the boundary layer contracts in the vicinity of the bottom wall and

Table 2 Variation of thermophysical properties as a function of Boussinesq parameter

ε_b	ΔT	$\Delta\rho$, %	Δk, %	$\Delta\mu$, %
0.0083	5	1.59	1.19	1.26
0.017	10	3.24	2.57	2.50
0.025	15	4.87	3.73	3.87
0.033	20	6.47	4.98	4.95
0.042	25	8.05	6.20	6.28
0.05	30	9.59	7.42	7.46
0.058	35	11.02	8.62	8.50
0.083	50	15.48	12.04	12.05
0.167	100	28.61	22.89	22.84
0.25	150	40.00	32.74	32.78
0.33	200	49.97	41.84	41.87
0.417	250	58.81	50.39	50.44
0.5	300	66.67	58.59	58.53
0.6	360	75.01	67.95	67.97

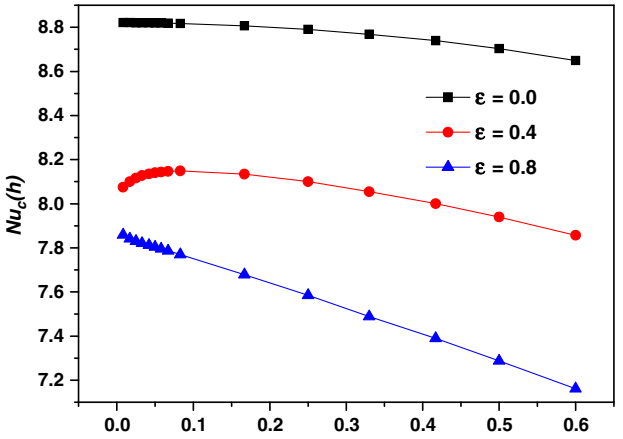

Fig. 11 Variation of the average convection Nusselt number on the hot wall as a function of Boussinesq parameter.

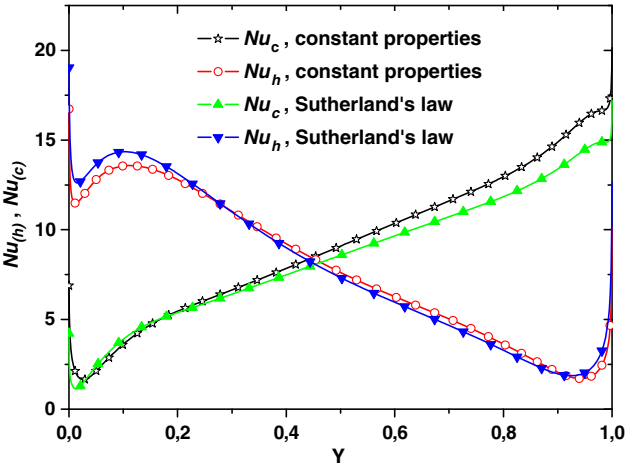

Fig. 13 Distributions of local convective Nusselt numbers on the hot and cold walls for $Ra = 10^6$ and $\varepsilon = 0.5$.

expands near the opposite wall. The same trend is observed for the V component near the vertical walls but not in the same proportions. It is interesting to note that, in the stratified region, the flow remains invariant for the component V, and the peak value near the cold vertical wall is slightly lower for $\varepsilon_b = 0.6$ than for $\varepsilon_b = 0.017$.

In Fig. 11, the low variations of Nusselt number for the weak values of the Boussinesq parameterε_b show that, under the condition $\varepsilon_b \leq 0.05$, the incompressible model based on the Boussinesq approximation can be used to simulate both pure natural convection ($\varepsilon = 0$) and combined natural convection surface radiation ($\varepsilon > 0$). Furthermore, one may note that this interval of Boussinesq parameter corresponds to a temperature difference $\Delta T \leq 30°C$ and maximal variations of thermophysical properties less than 9.5% for the density and 7.5% for the conductivity and viscosity (see Table 2). It is also interesting to note that Gray and Giorgini [21] showed in their study that, for air, the Boussinesq approximation is valid for $\Delta T \leq 28.6\,°C$ corresponding to the density variation of 10%.

B. Effect of Conductivity and Viscosity Variations

Another aim of this study is to examine the effect of fluid properties on the flow and heat transfer in the case of large temperature gradient. Simulation parameters for the compressible model are $\varepsilon_b = 0.6$, $Ra = 10^6$, $\varepsilon = 0.5$, and a reference temperature $T_0 = 300$ K.

A comparison between results obtained with constant and variable properties is first illustrated by isotherms and streamlines plotted in Fig. 12. The most visible effect on isotherms occurs at the top wall.

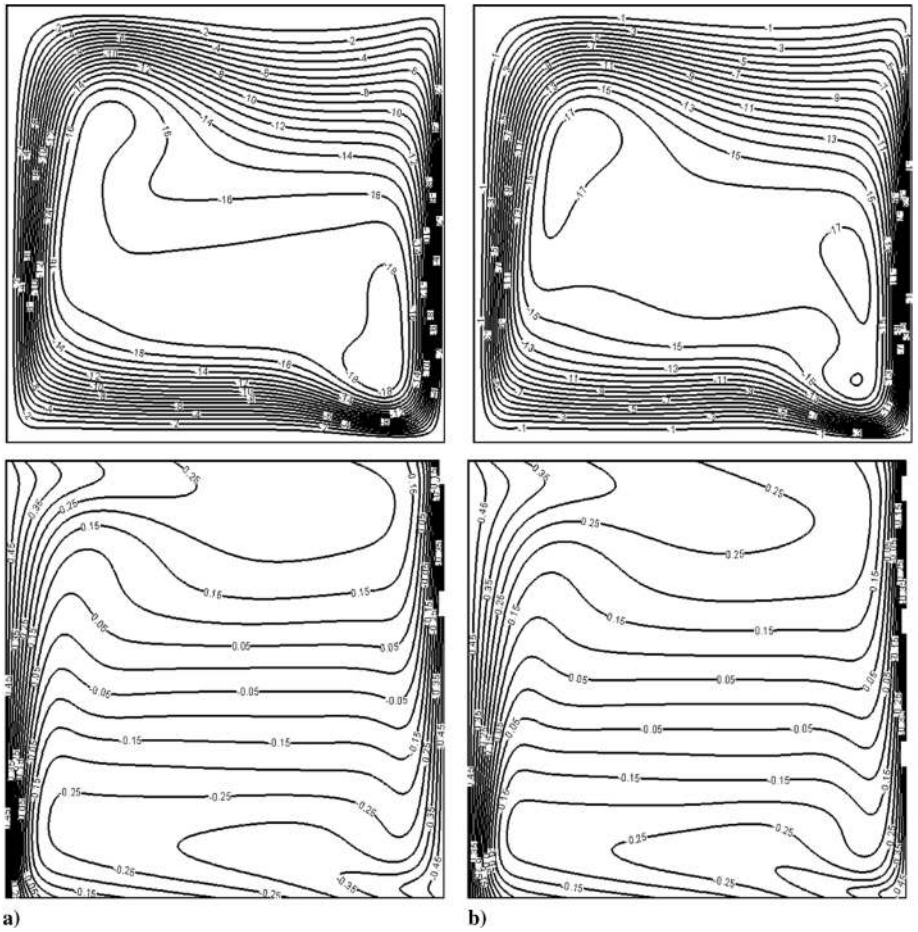

Fig. 12 Streamlines (top) and temperature contours (bottom) for $Ra = 10^6$ and $\varepsilon = 0.5$: a) constant properties, and b) Sutherland's law.

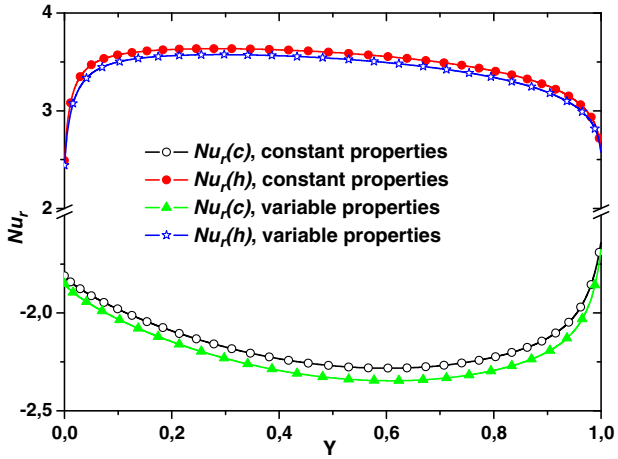

Fig. 14 Distributions of local radiative Nusselt numbers on the vertical walls for $Ra = 10^6$ and $\varepsilon = 0.5$.

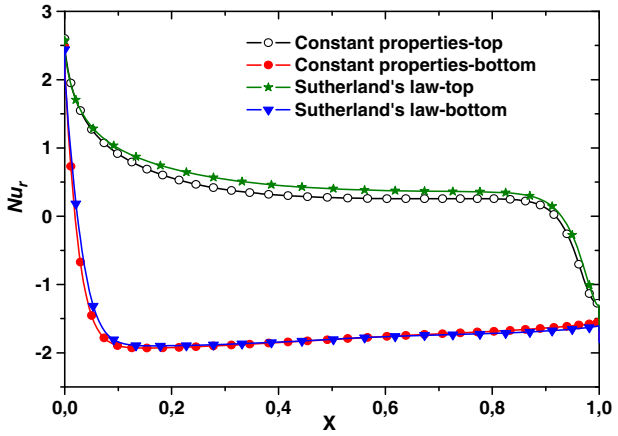

Fig. 15 Radiative Nusselt number distribution on the horizontal walls for $Ra = 10^6$ and $\varepsilon = 0.5$.

The center region of the cavity is marked by a sensible change in the fluid flow. Note that the symmetrical nature of the flow is strongly broken in the case of the constant.

Distributions of convective and radiative Nusselt numbers along the vertical walls are displayed in Figs. 13 and 14. By taking into account variable properties, the most noted change concerns the decrease of the convective Nusselt number on the cold wall at the upper part of the cavity. Unlike convection, Nu_r profiles undergo a weak translation, showing a slight decrease of radiative heat transfer for variable properties. On the horizontal walls, the fluid properties weakly affect the radiative exchanges for which the effects are more visible on the upper wall (Fig. 15). Consideration of variable properties slightly enhances the radiative exchange at the top wall. The temperature profiles on the horizontal walls are higher for variable properties than for constant properties (Fig. 16).

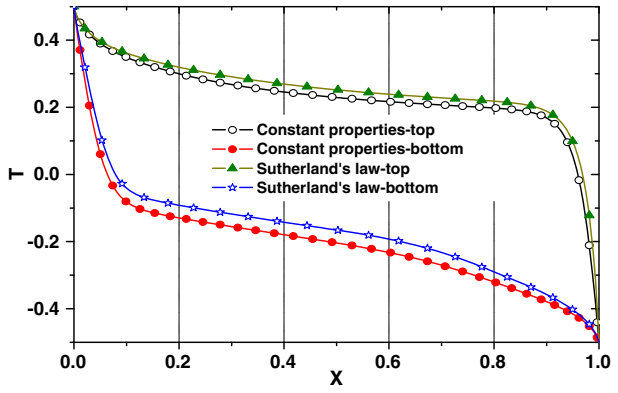

Fig. 16 Distributions of upper and lower wall temperatures for $Ra = 10^6$ and $\varepsilon = 0.5$.

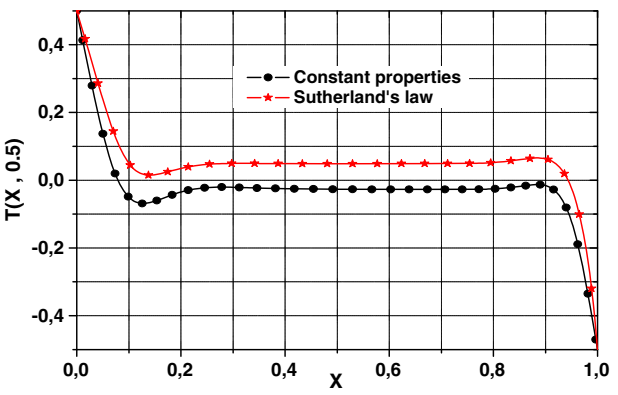

Fig. 17 Cross section of the temperature at midheight cavity for $Ra = 10^6$ and $\varepsilon = 0.5$.

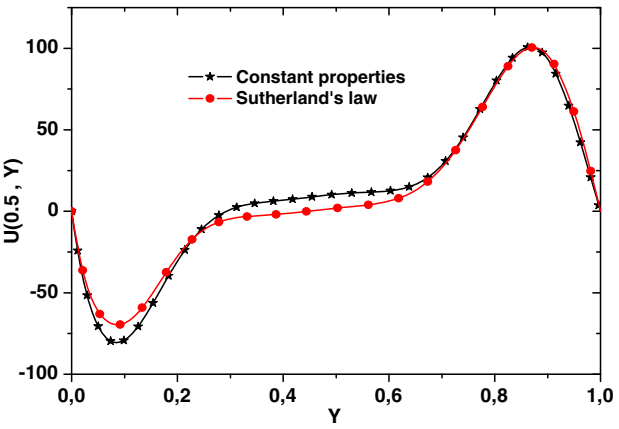

Fig. 18 Horizontal velocity at the vertical cross section at $x = 0.5$ for $Ra = 10^6$ and $\varepsilon = 0.5$..

The effect of fluid properties on the air temperature is evidenced in Fig. 17. By assuming variable properties, the temperature considerably increases in both boundary layers and at the core cavity. For the velocity components, the influence of fluid properties essentially appears near the bottom wall, at the cavity center for U, and near the hot wall for V. Variable properties lead to a decrease of the magnitude of both components, as seen in Figs. 18 and 19. It is interesting to note that the boundary layers near the hot wall remain thicker for both cases (constant or variable properties), reflecting that this behavior is mainly due to the nonlinear density variation.

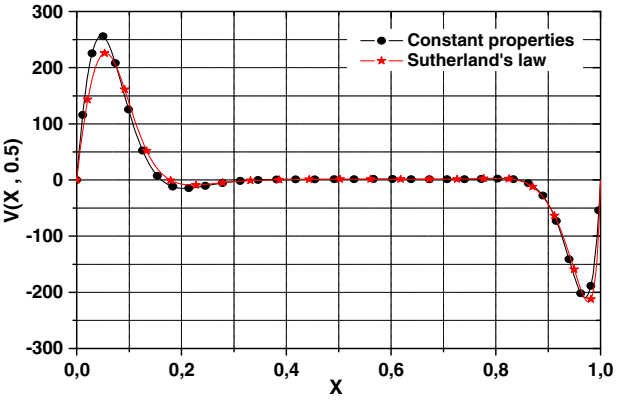

Fig. 19 Vertical velocity at the horizontal cross section at $y = 0.5$ for $Ra = 10^6$ and $\varepsilon = 0.5$.

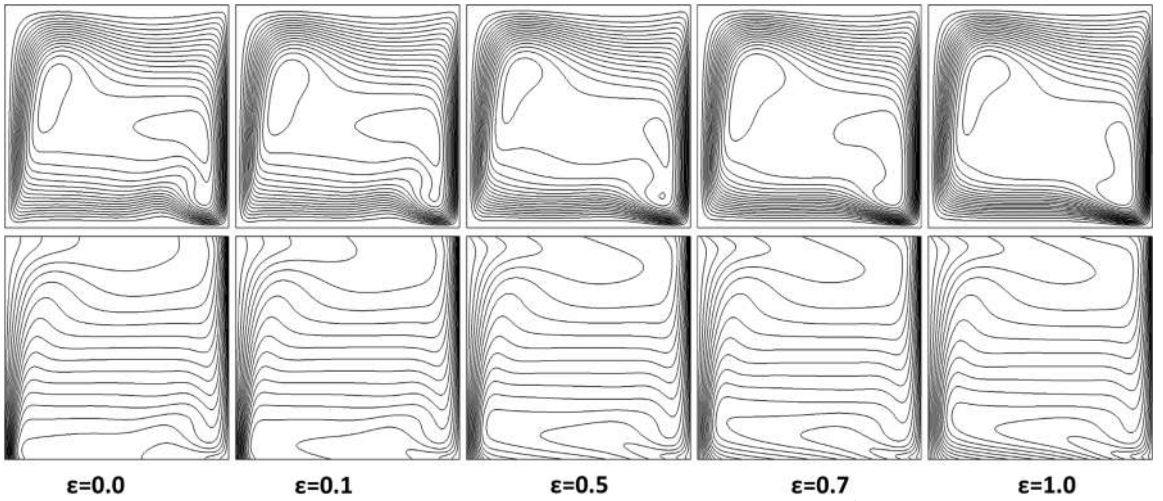

Fig. 20 Streamlines (top) and temperature contours (bottom) for $Ra = 10^6$ and $\varepsilon_b = 0.6$.

C. Effect of Surface Radiation

In this section, computations are carried out for different values of emissivity ($0.1 \le \varepsilon \le 1.0$), $Ra = 10^6$, $\varepsilon_b = 0.6$, and $T_0 = 300$ K. The properties are assumed to be variable according to Sutherland's law.

Typical isotherms and streamlines are plotted in Fig. 20 for different values of emissivity. Compared to the case without radiation, the temperature contours show the existence of temperature gradients near the top and bottom walls due to the radiative exchange. At the center region, the stratification is changed and the flow is modified but remains globally with the same structure: a primary flow along the walls and inside two asymmetrical secondary flows.

Figure 21 shows the variations of local convective Nusselt numbers on the vertical walls as a function of emissivity ε. Convective exchanges on the hot wall are greatly influenced by the wall radiation, especially on the lower part of the hot wall. Increasing the wall emissivity ε produces a decreasing of Nu_h, whereas it is less significant for Nu_c. For the local radiative exchange, an opposite trend is observed. Increasing ε leads to an increase of Nu_r on the hot wall and a decrease on the cold wall (see Fig. 22). On the horizontal walls, it is clearly seen that an increase of the wall emissivity leads to the cooling of the top wall and the heating of the bottom wall (Fig. 23). This behavior is explained by the fact that the top wall loses heat while the bottom wall receives heat. The distribution of the radiative Nusselt number on the top and bottom walls, presented in Fig. 24, shows that the net radiative heat flux is essentially positive at the top and negative at the bottom. Vertical profiles of air temperature

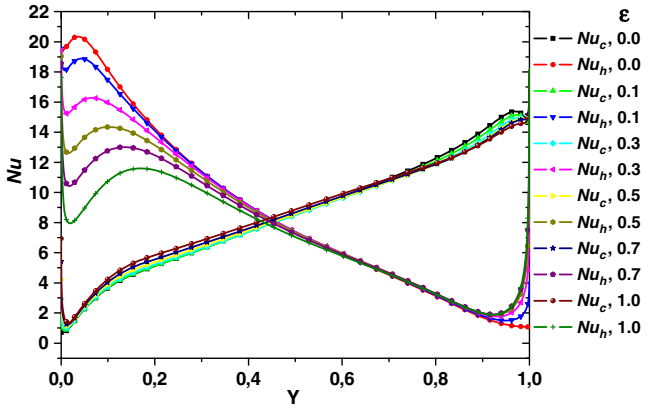

Fig. 21 Variations of convective Nusselt numbers at the hot and cold walls.

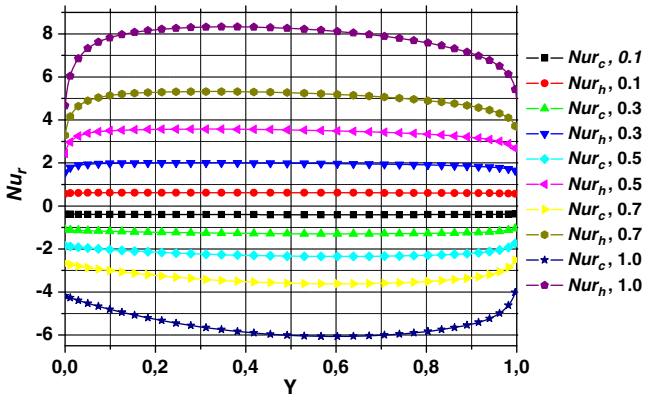

Fig. 22 Variations of radiative Nusselt number at the hot and cold walls.

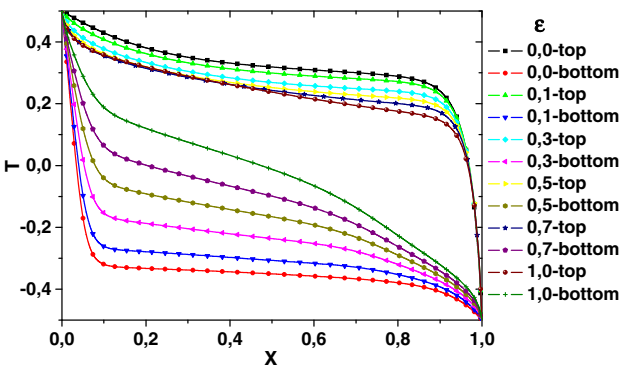

Fig. 23 Distribution of upper and lower wall temperatures for $Ra = 10^6$ and $\varepsilon_b = 0.6$.

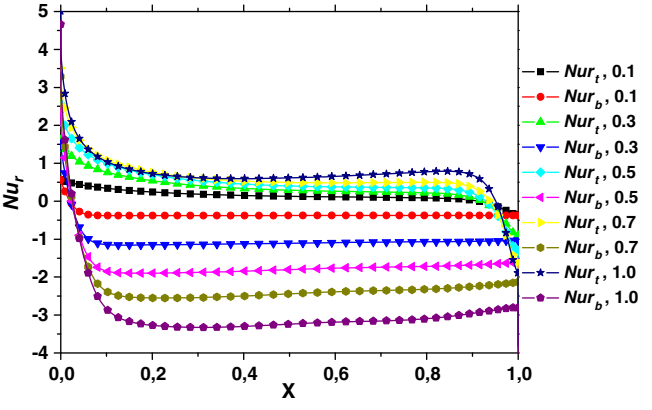

Fig. 24 Distribution of radiative Nusselt number on upper and lower walls for $Ra = 10^6$ and $\varepsilon_b = 0.6$.

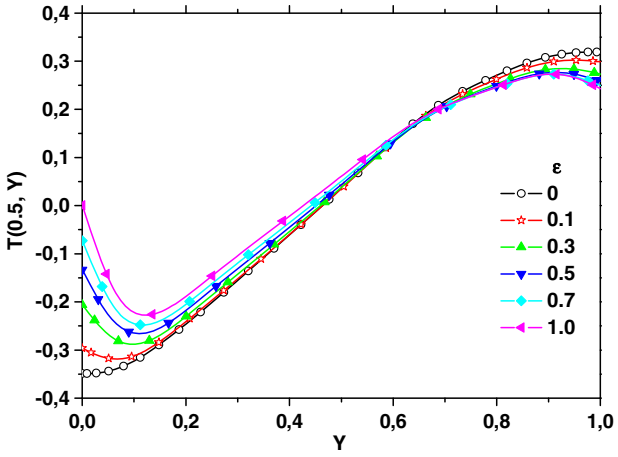

Fig. 25 Cross section of the temperature at $x = 0.5$ for $Ra = 10^6$ and $\varepsilon_b = 0.6$.

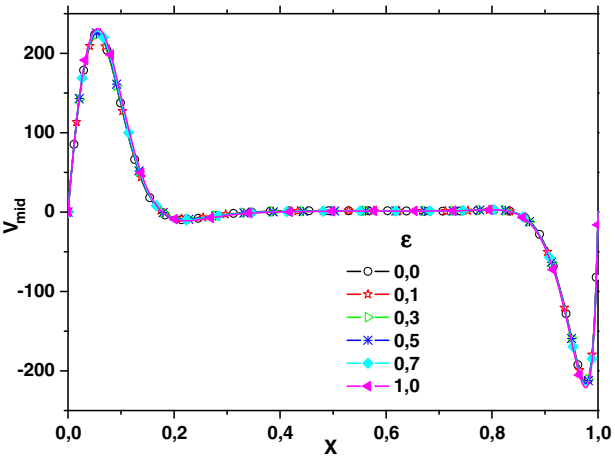

Fig. 27 Vertical velocity at $y = 0.5$ for $Ra = 10^6$ and $\varepsilon_b = 0.6$.

show that the emissivity reduces the stratification in the core (Fig. 25).

Figure 26 shows the variations of the average convective and radiative Nusselt numbers (Nuc_{avg}, Nur_{avg}) according to the emissivity for $Ra = 10^5$, 10^6, and 10^7. With increasing of the wall emissivity ε, the radiative Nusselt number on the hot wall increases and the convective Nusselt number Nuc_{avg} decreases. On the cold wall, an opposite trend is observed for the radiative Nusselt number, whereas the convective Nusselt number keeps the same shape of variation.

Velocity components are plotted in Figs. 27 and 28 across the midplanes. Unlike the vertical velocity where ε has almost no effect, the influence of the wall emissivity on the horizontal component indicates that the flow is intensified near the horizontal walls and the stratified region is almost at rest.

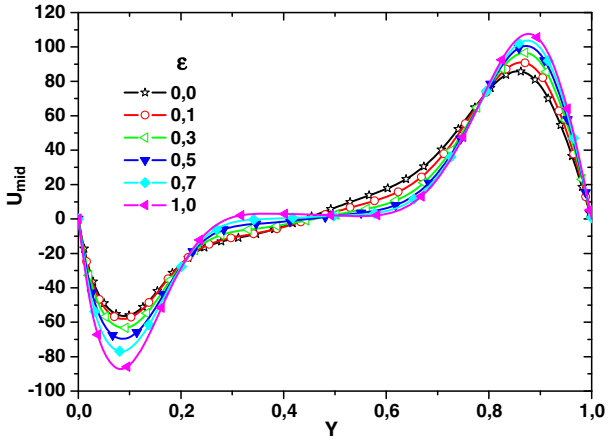

Fig. 28 Horizontal velocity at $x = 0.5$ for $Ra = 10^6$ and $\varepsilon_b = 0.6$.

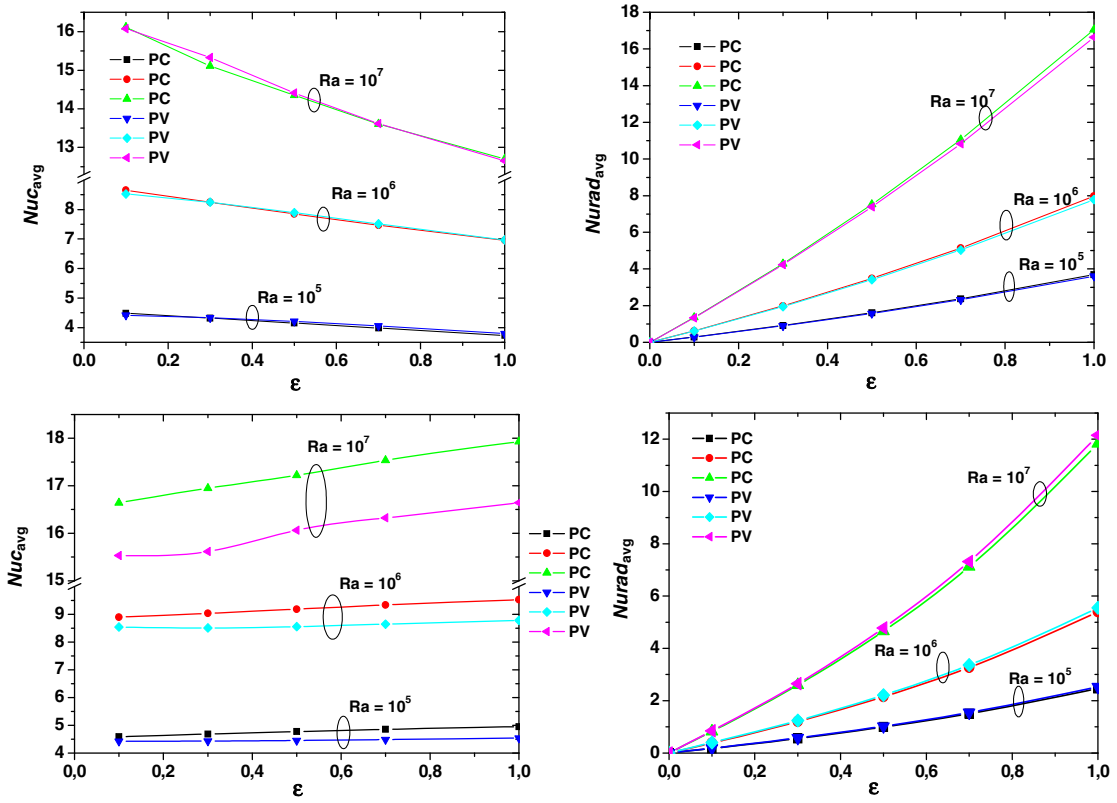

Fig. 26 Variation of the average convection and radiation Nusselt numbers on hot (top) and cold (bottom) walls as a function of emissivity (PC: constant properties, PV: variable properties).

V. Conclusions

In this Note, computations have been made in the context of a low-Mach-number formulation to study the combined natural convection and surface radiation in a square enclosure using a control volume approach. The present study shows the effects of the temperature difference parameter, surface emissivity, and temperature-dependent fluid properties on the flow and heat transfer. In view of the results presented, the main points can be summarized as follows:

1) Under non-Boussinesq conditions, and when the temperature difference increases, a significant variation between incompressible and compressible solutions is observed. In this case, the compressible model based on a low-Mach-number approximation can be used with a sufficient accuracy to simulate the combined natural convective surface radiation.

2) The variation of thermophysical properties could put a significant influence on the convective and radiative heat transfer and on the fluid flow.

3) The radiation exchange reduces the stratification at the cavity center and intensifies the flow at the horizontal walls.

4) The presence of radiation increases the temperatures of the fluid, and it considerably modifies the fluid flow and temperature distribution.

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