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New patterns in high-speed granular flows

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We report on new patterns in high-speed flows of granular materials obtained by means of extensive numerical simulations. These patterns emerge from the destabilization of unidirectional flows upon increase of mass holdup and inclination angle, and are characterized by complex internal structures including secondary flows, heterogeneous particle volume fraction, symmetry breaking and dynamically maintained order. In particular, we evidenced steady and fully developed "supported" flows, which consist of a dense core surrounded by a highly energetic granular gas. Interestingly, despite their overall diversity, these regimes are shown to obey a scaling law for the mass flow rate as a function of the mass holdup. This unique set of 3D flow regimes raises new challenges for extending the scope of current granular rheological models.

Key words:

1. Introduction

Granular gravity-driven flows are very common in industrial and geophysical processes. These flows are generally dense and can be confined by lateral walls or levees (due to self-channeling). The scientific community has paid particular attention to these flows over the last thirty years. However, their modeling is still an open issue. The complexity comes from grain/grain interactions that include both collisions and long lasting frictional contacts. Identifying regions of the flow where one type of interaction prevails over the other is part of the issue to be resolved.

One of the most studied configurations is the inclined plane geometry. Partly because it is a simple and good model for many common situations, but also because it may be seen as a rheological test with constant friction. Indeed, if sidewall friction is negligible, for steady and fully developed (SFD) flows, the tangential and normal forces on the base correspond exactly to the components of the flow weight. Their ratio, which is nothing but the apparent friction μ , is equal to the tangent of the angle of inclination θ . To date, experiments and simulations have focused mainly on flows with moderate inclination, leading to fairly simple unidirectional SFD flows (GDR-MiDi 2004; Delannay *et al.* 2007). However, more complex SFD flows with spanwise vortices were obtained for higher angles (Börzsönyi *et al.* 2009). One therefore expects that upon further increase of the inclination angle more and more complex flow features should emerge.

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In the case of flows running on a flat frictional base, the ratio of the tangential to the normal component of the contact force acting on a grain in contact with the base has an upper bound which is the microscopic friction coefficient μ_m . Thereby, the effective friction $\mu = \tan \theta$ is also bounded by μ_m . For definite and realistic values of μ_m , this automatically limits the possible angles for SFD flows. In the case of a bumpy base, there is also a limit, which depends in a complex and intricate manner on the microscopic friction coefficient, the bumpiness and the coefficient of restitution e (GDR-MiDi 2004). In particular, a small restitution coefficient allows SFD flows at high angles of incline. However, these flows seem to be unstable (Taberlet *et al.* 2007), which makes them difficult to study. The easiest way to obtain SFD flows at high angles is to introduce frictional side walls. This is what we have done in the present work. If the grain/wall friction coefficient is high enough, one may expect that the base friction supplemented by the side wall friction will be able to balance the driving component of the weight.

We have conducted simulations of granular flows down flat and steep inclines with frictional side walls using a discrete element model (DEM). The principle of DEM simulations is to treat each grain as a sphere (of diameter D) subject to gravity and contact forces with both the other grains and the basal and lateral walls. These contact forces are characterized by a coefficient of restitution $e_g = 0.972$, a coefficient of friction $\mu_g = 0.33$ for interactions between grains, with $e_m = 0.8$ and $\mu_m = 0.596$ for grain/wall interactions (values taken from (Louge & Keast 2001)). Newton's second law is applied to calculate the motion of each individual particle. This method, which has successfully been used to simulate granular flows (Cundall & Strack 1979; Silbert *et al.* 2001; Luding 2008), has been optimized to obtain three-dimensional SFD flows within a reasonable computation time.

We used periodic boundary conditions in the streamwise direction, while walls constrain the flow in lateral directions (see Fig. 1). The periodic cell had a length $L = 20D$ and width $W = 68D$. We used a relative large cell width to allow for the development of transverse instabilities (Börzsönyi *et al.* 2009). It is worth mentioning that most simulations in the literature used lateral periodic boundary conditions with a small width (typically $W = 20D$), preventing three-dimensional patterns to develop.

The mass hold-up is a measure of the mass of particles per unit basal surface within the simulation cell: $\tilde{m} = \sum_g m_g/A$, where m_g is the mass of a grain g and $A = L \times W$ is the basal area of the cell. For ease of interpretation, we choose to express the mass hold-up in terms of an equivalent grain height \tilde{H} by dividing \tilde{m} by the particle density ρ : $\tilde{H} = \tilde{m}/(\rho D)$. \tilde{H} is thus the height of a dense block with the same volume as the grains. This quantity is a control parameter which simply specifies the amount of particles within the system, irrespectively of their spatial repartition. For each value of the control parameters θ and \tilde{H} , the simulations were run up to a stabilization of the total kinetic energy of the system, see (Brodu *et al.* 2013) for details as we reused the same configuration and simulation

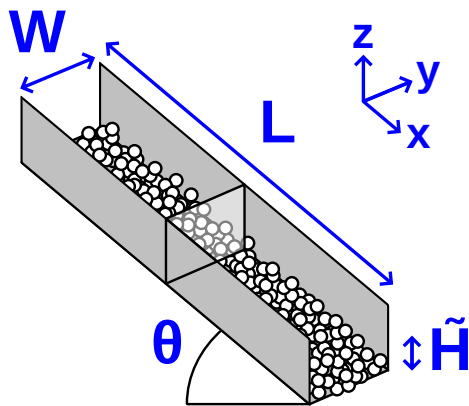


FIGURE 1. Geometry of the system. The grains flow on an inclined plane (length L) and between two side walls separated by a gap W . Periodic boundary conditions are used in the x -direction. The variations of the mass holdup \tilde{H} and of the angle of inclination θ lead to the observation of new SFD flow regimes.

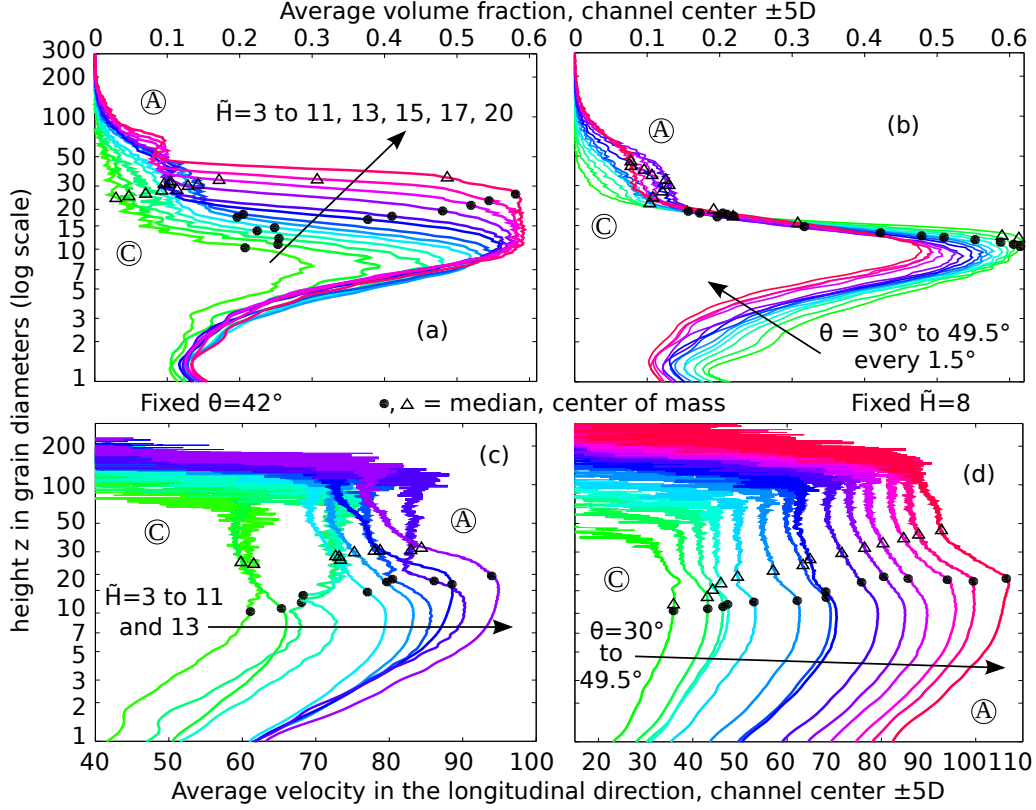


FIGURE 2. Vertical profiles of the volume fraction of the flow ((a) and (b)), of the velocity in the main flow direction X ((c) and (d)). All quantities are measured at the center of the channel and are averaged over $10D$ in the transverse direction Y. The curves reported in the right column are for a fixed mass holdup $\tilde{H} = 8$ and for different angles of inclination. Those reported in the left are for a fixed angle of inclination $\theta = 42^\circ$ and for different values of mass holdup. Circles and triangles respectively indicate the vertical position of the median and center of mass, which increases both with the mass holdup and the angle of inclination.

parameters. We obtained SFD flows for all the flow configurations we have investigated, varying extensively the inclination angle θ between 0 and 50° and the mass hold-up \tilde{H} between 0 and 20 . We also tested much larger values of the angle of inclination (see Supplementary Figure 2), but we always reached SFD flows after a transient which duration increases with the angle.

Our simulations reveal the existence of many SFD regimes which have very different characteristics: coexistence of order and disorder phases, symmetry breaking, oscillations, intermittency, stacked granular "convection" rolls, polyphasic flows, etc. These new regimes emerge from the destabilization of SFD unidirectional flows upon increase of the mass holdup and the slope. In a previous work (Brodu *et al.* 2013) flows corresponding to $\tilde{H} = 4$ and $\theta < 23^\circ$ were studied. We thus focus more specifically here on large inclination flows ($\theta > 30^\circ$) and on the effect produced by an increasing mass holdup. The next section gives details on supported regimes, observed for $\theta > 30^\circ$. Section 3 gives an overview of the different regimes we obtained by exploring the parameter space, and reports their domain of existence. Section 4 reveals that, despite the very different characteristics of the observed regimes, they show common features. Concluding remarks are

given in section 5.

2. Supported regimes

We identified at high angle ($\theta > 30^\circ$) a new flow regime, referred to as "supported flows". This regime is drastically different from those reported in the literature and, in particular, from the "rolls" regime investigated in several recent works (Forterre & Pouliquen 2002; Börzsönyi *et al.* 2009; Brodu *et al.* 2013). Dense unidirectional flows destabilize upon increase of the inclination angle (typically between 20° and 30°) and then exhibit longitudinal rolls. The above references provide evidence that, with these rolls, the particle volume fraction becomes lower at the base than in the midst of the flow. Density inverted profiles are also predicted by the granular kinetic theory (Jenkins & Askari 1999). However, in these regimes with rolls, the depletion of particles is moderate and located at the flow base. The geometric structure remains that of a slab of grains occupying the whole width of the channel, together with the associated secondary circulation pattern. Upon further increase of the angle, $\theta > 30^\circ$, a strongly sheared, dilute and agitated layer spontaneously appears at the base of the flow (see Fig. 3).

Such a layer is able to support a dense packing of grains moving as a whole. Additional granular gas layers separate that dense core from the side walls. This geometric structure is clearly distinct from that of the dense slab with secondary rolls, as can be seen on the bottom line of snapshots of Fig. 6 (see also Supplementary Figure 2), which also shows their transition. In particular, the packing fraction in the core of the supported regimes is higher than within the dense slab with the secondary rolls. This high unexpected volume fraction is not seen in density inverted profiles obtained from the kinetic theory of granular gas (Jenkins & Askari 1999). These supported regimes have been

already mentioned in the literature as a possible explanation for the unexpected high mobility of granular avalanches. Campbell (1989) indeed suggested that the existence of a layer of highly agitated particles at low concentration beneath a densely packed main body could reduce the apparent basal friction and allow the flow to reach long runouts. However, DEM simulations were unable up to now to reproduce these flow regimes as steady and stable states. They were only observed as transient states in decelerated flows (Campbell 1989) or as a steady but unstable state at a unique value of the inclination angle (Taberlet *et al.* 2007). In contrast, the supported regimes reported here are steady and fully developed, stable and, thanks to sidewall friction, were obtained within a large range of inclination angles.

The existence of a stabilized dense core within a very agitated and dilute region is probably a direct consequence of the clustering instability occurring in granular gas (McNamara & Young 1994). It is also worth noting that this flow regime bears a strong resemblance with that observed experimentally by Holyoake and McElwaine (Holyoake & McElwaine 2012) on steep slopes with a "depletion layer" at the walls. The structure

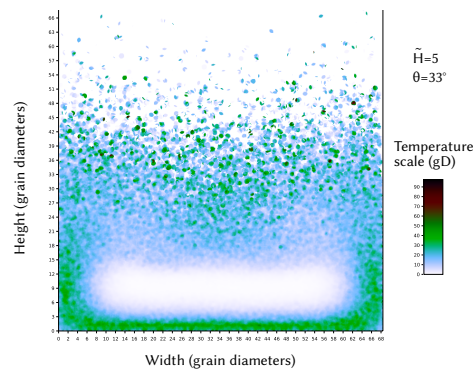


FIGURE 3. Map of the granular "temperature" for $\tilde{H} = 5$ and $\theta = 33^\circ$, the same situation as for the bottom-right snapshot in Fig. 5. This clearly shows a much less agitated dense core than the surrounding "hot" basal and side layers of gas.

of supported flows may also bear some resemblance to vibrated beds (Eshuis *et al.* 2013). Gravity-driven flows can be seen as the superposition of two solicitations: A shearing, induced by gravity; and collisions with the boundaries, which can be seen as either energy sources or sinks depending on their nature (e.g. loose base comprised of other mobile grains). In our situation, the base behaves as an energy source, which resembles the situation for vibrated media. Motion along the flow, mainly driven by gravity, could be more or less independent from motion in the transverse direction which, according to this hypothesis, would be mainly driven by the interactions of the grains with the boundaries. This would explain a similarity with some regimes observed in vibrated media. However, even if similarities may occur, a major difference is that in our case there is a volumic source of momentum, which induces shearing, while in the vibrated case, momentum is only transferred to the granular medium through the boundaries. It would nevertheless be interesting to use a hydrodynamic-like model (Eshuis *et al.* 2013) to study the stability of the usual unidirectional flow when the control parameters increase, and the patterns which could result from the destabilisation.

Fig. 2 shows typical volume fraction and velocity profiles for SFD supported regimes in the vertical (x,z) symmetry plane. They present a dense core, moving at a fast and almost uniform speed, floating above a highly agitated granular gaseous phase, and topped by a dilute "atmosphere" which spans over a great distance over the dense core. Due to this heterogeneous mass distribution, the center of mass is located just on top of the core. The median of mass is unaffected by the distance of small contributions high in the dilute "atmosphere". By definition, the median separates half of the mass beneath and half above, so it arguably better corresponds to the intuition for where is the "middle" of the flow. We plot both quantities in Fig. 2. When the mass holdup increases the core lifts up and densifies (see Fig. 2a). Its lateral width decreases with increasing \tilde{H} because the lateral pressure pushes the grains toward the central core (see Fig. 6). This core can reach very high values of the volume fraction up to 0.6 at large mass holdup, while the volume fraction in the supporting basal gaseous layer is below 0.2.

Above the dense core, the volume fraction is well described by a decreasing exponential: $\nu(z) \propto \exp(-z/H_C)$, where H_C represents the characteristic height of the atmosphere (see Supplementary Figure 1). The core slowly "evaporates" as the angle increases for a gradual transition to granular gas at larger angles (see Supplementary Figures 2 and 3). Surprisingly, when the angle θ increases, the altitude of the core remains nearly constant (see Fig. 2b). However, the center of mass of the flow lifts up and the core thickness decreases as a non-negligible part of the material is transferred into the top granular gaseous phase. The vertical expansion of the flow is necessary to increase its friction on the lateral boundaries and to balance the driving force, which increases with the inclination angle. The basal friction cannot exceed $\mu_m M g \cos \theta$, where $\mu_m = 0.596$ is the microscopic friction value used in the simulations (Brodu *et al.* 2013) and M is the mass of the grains. Thus, for large angles, a large part of the friction comes from the lateral walls as discussed in more details below.

The effective friction coefficients respectively at the base μ_b and at the walls μ_w are computed as the ratio of tangential to normal stresses. Fig. 4a shows the dependency of μ_b and μ_w on θ and \tilde{H} . Both coefficients increase and saturate at high inclination angles as they are upper-bounded by μ_m . In contrast, they decrease with the mass holdup: for a given angle, the basal friction reduces as more matter is added in the flow. This reduction of basal friction with increasing mass hold-up has never been reported before and may be a clue for explaining the long run-out for large rock avalanches (Campbell 1989).

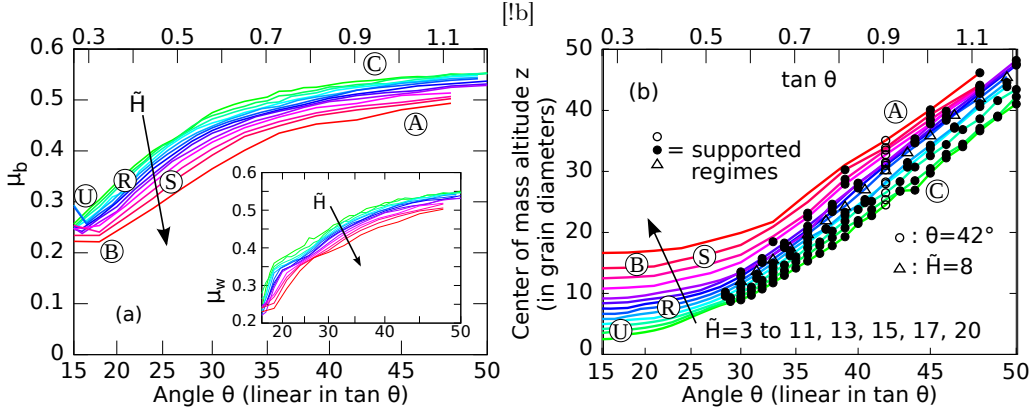


FIGURE 4. (a) Effective friction coefficients on the base μ_b and the wall μ_w (inset) as a function of the inclination angle θ . Both coefficients increase with θ but show a reduction for increasing mass hold-up. (b) Altitude of the center of mass C_M as a function of θ for various mass hold-up. Markers indicate the states corresponding to the supported flow regimes for which C_M exhibits a linear increase with $\tan \theta$. Labels U, R, C, A, S and B refer to the different flow regimes defined in Fig. 6.

In the vertical direction however, friction on the walls do not significantly contribute to supporting the weight of the grains. As the center of mass lifts up (Figs. 2 and 4b), the normal component of the integrated stress on the lateral walls is increased. The zone below the core then reaches a high pressure as it must sustain the flow weight. We have computed the ratio between the vertical component of the force exerted by the grains on the walls, to the vertical component of the force exerted by the grains on the base. This ratio is below 1.3% in the non-supported regimes, with negative values in the supported ones (see Fig. 5). Indeed, in these cases, grains escaping the high pressure gaseous region below the core rebound upward on the wall. Grains circulate slowly downward within the dense core to compensate. The very weak Janssen effect that is observed in the non-supported regimes is thus negated by the convection in the supported ones.

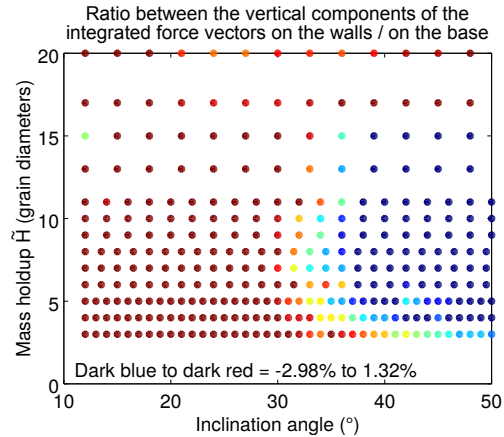


FIGURE 5. Proportion of the effective weight retained by side walls. Positive values of the ratio are when the walls push up the grains, or equivalently when the grains push down on the side walls, since the base always pushes up. This is the case for the non-supported regimes, a Janssen effect that disappears in the supported regimes.

At the same time, the presence of a granular gas at the base lowers the friction compared to the dense regimes, hence larger velocities are reached in steady state. These large velocities are partially due to large sliding velocities and, for the rest, to large gradients, at the base (see Fig. 2c and 2d). The top layer of gas only contributes marginally to this picture as it does not go faster than the core. However, as mentioned earlier, the vertical extent of the flow is a key feature to understand the balance between the gravitational driving force and side walls friction. The position C_M of the center of mass of the flow

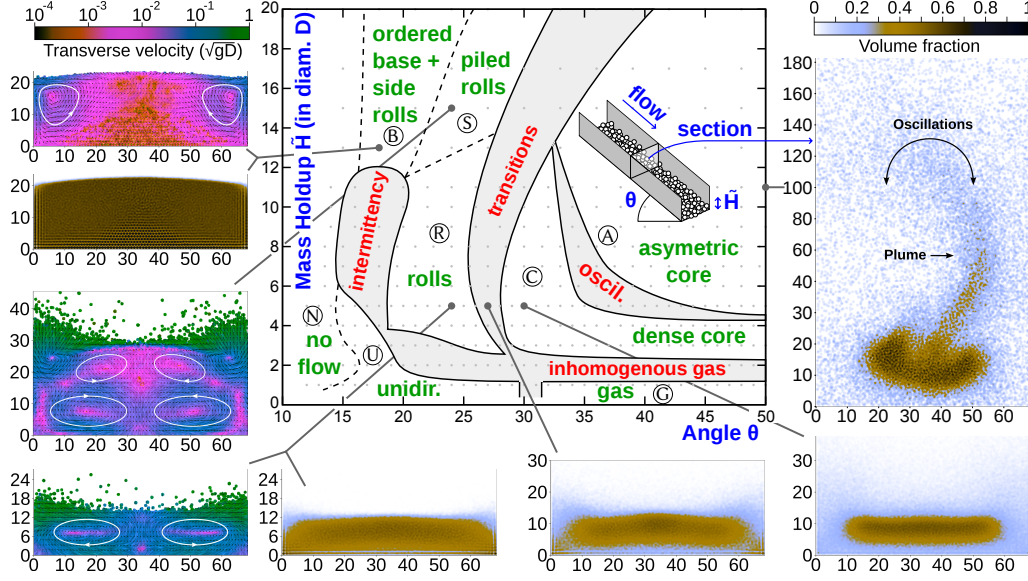


FIGURE 6. Phase diagram in the *mass holdup - angle of inclination* space. \textcircled{U} : Unidirectional flows; \textcircled{R} : flows with Rolls; \textcircled{C} : flows with dense Core (i.e., supported flows); \textcircled{A} : supported flows with Asymmetric core; \textcircled{S} : flows with Superposed rolls; \textcircled{B} : flows with a Basal ordered layer topped by rolls. The 385 gray dots are the sampling points in the phase space where we performed a simulation (also visible in Fig. 5). The phase diagram is supplemented with 2D maps representing the velocity in the transverse direction (left panels) and the particle volume fraction (middle and right panels). These data are averaged over the periodic direction X and over $500\sqrt{D/g}$ time units, which is much larger than a typical oscillation in regime \textcircled{A} . The snapshot on the right is thus averaged only in X and taken at a single time $t = 2000\sqrt{D/g}$. The transition regions in the phase diagram are conservatively defined from the structure of the flow (e.g. bottom right middle snapshot) as well as from the evolution of the kinetic energy over time (e.g. oscillations).

is a simple and interesting indicator which is shown in Fig. 4b. For the supported flows (indicated by dots in the Figure), C_M increases linearly with $\tan\theta$: $C_M = a \tan\theta + b$, where the slope $a = 54.6D$ is independent of the mass holdup. Using a simple force balance, it can be shown that the slope is simply given by $a \approx W/2\mu_m$ (see Appendix). In contrast, the parameter b increases with mass holdup and reflects the corresponding increase of the core thickness with \tilde{H} described in Fig. 2a.

3. Phase Diagram

In addition to the supported flows, we have discovered other new regimes by exploring extensively and systematically the parameter space (θ, \tilde{H}) . We report in Fig. 6 the domain of existence of the different regimes. These were identified using a combination of the flow structure (i.e., the concentration and the velocity fields) together with the evolution of the kinetic energy over time. We have decided to use large grayed-out transition bands for intermediate situations, together with dashed lines for transitions that appear sharp at our resolution, but which may not be so at a lower resolution. Some transitions are also visible in Fig. 5. The regime identifiers are labeled by circled letters and are briefly described below:

- Regime \textcircled{U} corresponds to classical Unidirectional dense flows.

- Regime \textcircled{R} corresponds to flows with Rolls previously reported in experimental and numerical works (Forterre & Pouliquen 2002; Börzsönyi *et al.* 2009; Brodu *et al.* 2013).
- Regime \textcircled{C} stands for the supported regime described in section 2.
- Regime \textcircled{S} corresponds to the Superposed rolls and appears at larger mass holdups \tilde{H} than regime \textcircled{R} . An example is shown in the snapshots of Fig. 6.
- Regime \textcircled{B} is characterized by the presence of a Basal layered structure. The observed order (see snapshots of Fig. 6) is dynamically maintained by collisions and cage effects. The layers are sheared and not static. Rolls are present in the disordered zone on the top of the basal layers and are localized close to the lateral walls.

All these regimes have distributions of mass and of velocities which are symmetric relatively to the central vertical plane: $Y = W/2$. At large inclination angles, this symmetry is broken as the mass holdup increases.

- Regime \textcircled{A} denotes the supported regime with asymmetric core. The dense core swings back and forth from left to right. For larger \tilde{H} and θ , a plume eventually forms on top of the core, as shown in the snapshots of Fig. 6. The symmetry is recovered when averaging over one oscillation cycle, and this average is stationary.

These different flow regimes open many perspectives to test the relevance of granular rheological models. For example, our results may be interpreted in the framework of the second-order fluid model proposed in (McElwaine *et al.* 2012) which predicts that shallow flows develop curved surface, as seen for regimes \textcircled{B} and \textcircled{C} .

4. Scaling behavior

Although these flow regimes exhibit marked difference in terms of structural organization, they surprisingly show common features. First, the transient regime necessary to reach the steady state is well described by a simple exponential saturation for any value of the inclination angle and mass hold-up: $V(t) = V_L - (V_L - V_0) \exp(-t/\tau)$, where $V(t)$ is the average streamwise flow velocity at time t , V_0 the initial flow velocity, and V_L the limit velocity (see Fig. 7a). The characteristic time τ is an increasing function of the mass hold-up and has a non-monotonic variation with the inclination angle (see Supplementary Figure 4a). This exponential velocity saturation, observed in all the regimes, suggests that the flow experiences a viscous-like drag force proportional to the velocity (see Supplementary Figure 4b).

Second, we identify a simple dependency of the limit velocity on the mass hold-up and inclination angle. At any fixed angle, the velocity follows a power law \tilde{H}^α , with an exponent α weakly dependent of θ but close to 0.25. Figure 7b, reports the limit velocity V_L rescaled by $\tilde{H}^{1/4}$ versus the inclination angle θ for various mass holdups. The observed collapse is remarkable given the large diversity of the flow regimes. In steady state, the mass flow rate is simply given by $Q = V_L \tilde{H}$ such that $Q \propto \tilde{H}^{5/4}$. In the configuration of regime \textcircled{U} , (Louge & Keast 2001) have experimentally measured an exponent $Q \propto \tilde{H}^{3/2}$, which is within the range of exponents shown in Figure 7b.

5. Conclusion

Using a simple flow configuration with flat lateral and basal boundaries, we have discovered, by increasing the inclination angle and mass holdup, steady and fully developed regimes which present non-trivial features including heterogeneous volume fraction, secondary flows, symmetry breaking and dynamically maintained order. Despite the diver-

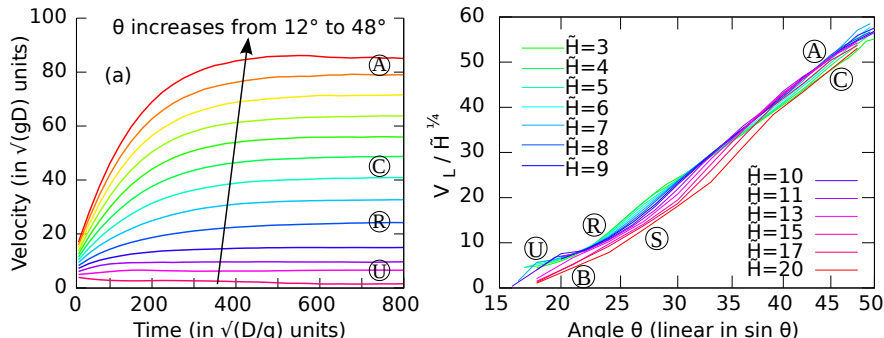


FIGURE 7. (a) Typical temporal evolution of the mean flow velocity, for $\tilde{H} = 5$ and $\theta = 12^\circ$ to $\theta = 48^\circ$ every 3° . All the flows reach a steady state via an exponential saturation. We ran the simulations up to $2000\sqrt{D/g}$ time units. (b) Rescaled steady state velocity $V_L/\tilde{H}^{1/4}$ as a function of $\sin\theta$ for various mass hold-up. The collapse is remarkable given the wide diversity of regimes. The scaling law simply reads: $V_L/\tilde{H}^{1/4} \approx A \sin\theta + B$, with $A \approx 122$ and $B \approx -37$. These parameters may or not depend on the channel width W , the coefficients of friction and elasticity, etc.

sity of the features of these states, we have highlighted that the mass flow rate obeys a scaling law in terms of \tilde{H} . Explaining these regularities is a challenging issue, as they suggest a unified underlying model.

A crucial question is to which extent these regimes and their features are specific to the material parameters and the confined geometry we have considered. Additional simulations, where we have varied the material parameters (friction and restitution coefficient) and the basal conditions (flat or bumpy), lead to similar regimes as long as grain/wall friction prevails on grain/grain friction. Side walls play of course an important role regarding the friction and allow SFD flows for any value of the chute inclination. Without side walls, at least for flat bases, flows at large angle would not be steady but accelerated. Despite of this, analog flow regimes appear but as transient state (see Supplementary Figure 5).

These results provide a unique set of very complex granular flow regimes for testing theoretical and rheological models. These regimes surprisingly appear in a configuration, the inclined channel, that was previously considered boring and well-studied. We have however only explored a small portion of the full high-dimensional phase diagram consisting of the variations of all influential parameters. It is thus very likely that more regimes exist, especially in the wide range of conditions found in nature and in industry. We hope that our study will encourage such investigations of granular flows, in particular for wider channels and higher mass holdup values.

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Appendix. Derivation of the position of the center of mass of the flow as a function of the inclination angle

The linear variation of the center of mass C_M of the flow as a function of the tangent of the inclination angle can be interpreted by considering a simple force balance. In a stationary regime, we have : $Mg \sin\theta = 2\mu_w L \int_0^\infty N_w(z) dz + \mu_b N_b W L$, with $N_w(z)$ and N_b the normal stress at side-walls and at the base respectively. The first term of

the right-hand side is the friction of the wall on the flow, and the second one is the friction at the base. Both μ_w and μ_b saturate in the supported regimes (see Fig. 2a), so they can be considered as constant in a first order approximation. Using the fact that $Mg \cos \theta = N_b W L$, we end up with: $2 \int_0^\infty N_w(z) dz / N_b = \frac{W}{\mu_w} (\tan \theta - \mu_b)$. The term of the right-hand side represents a characteristic height of the flow, denoted later on by H_p (if the pressure was purely hydrostatic, H_p would correspond exactly to the height of the flow). The derived relation expresses the fact that the characteristic height of the flow H_p varies linearly with $\tan \theta$. This explains why the position C_M of the center of mass, which is of the order of the half characteristic height of the flow, evolves linearly with $\tan \theta$. Remarkably, we find here a slope $a \approx W / (2\mu_m)$ in agreement with the hypothesis that $C_M \approx H_p / 2$. We also find that the "atmospheric height" H_C increases linearly with $\tan \theta$ in the supported regimes. The slope here is about two third of W / μ_w , corresponding to $H_c \approx 3H_p / 2$.

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