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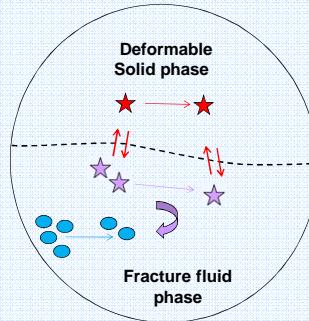
# The importance of local thermal non-equilibrium in the modeling of a fractured hot dry rock reservoir

Rachel Gelet<sup>(1)</sup>, Benjamin Loret<sup>(2)</sup>

**Abstract** Thermal recovery from a HDR reservoir, viewed as a deformable fractured medium, is investigated with a focus on the assumption of local thermal non-equilibrium. The numerical model is used to investigate the coupled thermo-hydro-mechanical behavior of the Fenton Hill site. The time profile of the outlet fluid temperature displays a double-step pattern, a feature which is interpreted as characteristic of established local thermal non-equilibrium.

**The constitutive model** uses a two-phase mixture and accounts for:

- ✓ Generalized diffusion
  - Hydraulic (Darcy) → ●
  - Thermal (Fourier) → ★
- ✓ Thermal convection → ↗
- ✓ Heat transfer → ↔



The significant contribution is  
the local thermal non-equilibrium  
★ ≠ ★

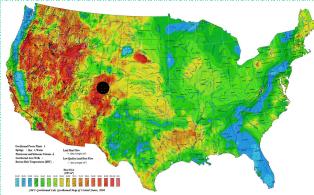
## Characteristic times

$$t_{\text{Fourier,frac.}} < t_{\text{Fourier,solid}} < t_{\text{Convection,frac.}} < t_{\text{Darcy,frac.}}$$

$$10\,000 \text{ years} < 1\,500 \text{ years} < [2 \text{ days} - 7 \text{ years}] < 1 \text{ hour}$$

- Large difference in characteristic times between thermal diffusion in the solid phase and convection in the fluid phase
- Local thermal non-equilibrium is required to accurately represent the overall thermo-hydro-mechanical behavior
- The thermally induced effective stress will trigger thermal shrinkage across the body of the reservoir that may lead to permeability change and fluid loss

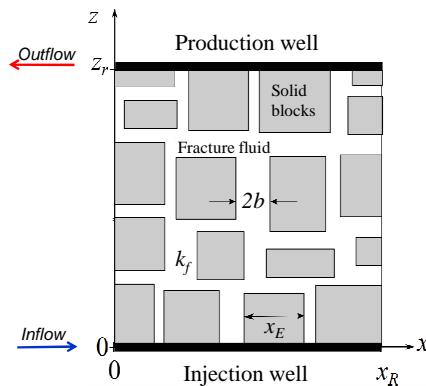
## Site: Fenton Hill (US)



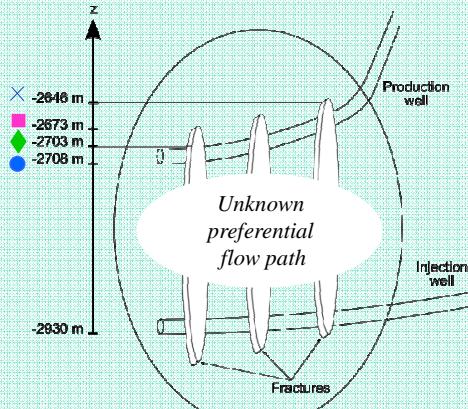
## FE Simulation tools

- SUPG method
- Non-linear analysis treated with a Newton-Raphson algorithm
- Fortran language

## Numerical setup

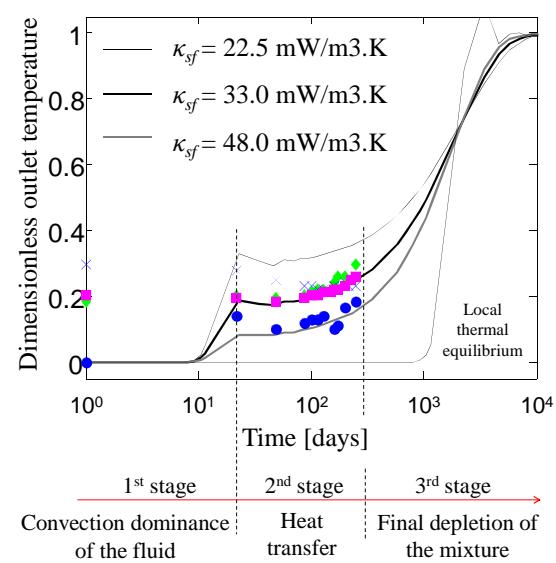


## Compared with experimental data



**THM coupled Results:** relative temperature outlet versus time along the production well:

- Three parameters of the model are calibrated, namely the permeability  $k_f = 8.0 \text{ mD}$ , the porosity  $n_f = 0.005$  and the specific interphase heat transfer coefficient  $\kappa_{sf} = 33.0 \text{ mW/m}^3\text{K}$ .
- Three stages characteristic of local thermal non-equilibrium are identified
- Local thermal non-equilibrium is characterized by a double step curve, while local thermal equilibrium is recognized by a single-step pattern



## Summary

- Numerical results compare well with experimental ones
- The thermal drawdown curve is characterized by three stages, characteristic of local thermal non-equilibrium

## Perspectives

Start experimental CHM and THM measures on real samples (ANR project in development)