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Optimizing water permeability through the hourglass shape of aquaporins

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The ubiquitous aquaporin channels are able to conduct water across cell membranes, combining the seemingly antagonist functions of a very high selectivity with a remarkable permeability. While molecular details are obvious keys to perform these tasks, the overall efficiency of transport in such nanopores is also strongly limited by viscous dissipation arising at the connection between the nano-constriction and the nearby bulk reservoirs. In this contribution, we focus on these so-called entrance effects and specifically examine whether the characteristic hourglass shape of aquaporins may arise from a geometrical optimum for such hydrodynamic dissipation. Using a combination of finite element calculations and analytical modeling, we show that conical entrances with suitable opening angle can indeed provide a large increase of the overall channel permeability. Moreover, the optimal opening angles that maximize the permeability are found to compare well with the angles measured in a large variety of aquaporins. This suggests that the hourglass shape of aquaporins could be the result of a natural selection process toward optimal hydrodynamic transport. Finally, in a biomimetic perspective, these results provide guidelines to design artificial nanopores with optimal performances.

Aquaporin channels are able to selectively conduct water across cell membranes, with a remarkable efficiency. While molecular details are crucial to the pore performance, permeability is also strongly limited by viscous dissipation at the entrances. Could the hourglass shape of aquaporins optimize such entrance effects? We show that conical entrances with suitable opening angle can indeed provide a large increase of the channel permeability. Strikingly, the optimal opening angles compare well with the angles measured in a large variety of aquaporins, suggesting that their hourglass shape could be the result of a natural selection process toward optimal permeability. This work also provides guidelines to optimize the performances of artificial nanopores, with applications in desalination, ultrafiltration or energy conversion.

nanofluidics | hydrodynamic permeability | biochannels | aquaporin

quaporins (AQP) are water selective channels, ubiquitous in the Aliving world [1, 2]. They are involved in many physiological processes and play a crucial role in water exchanges across membranes, in particular under osmotic gradients. AQP are considered to be excellent water filters, able to achieve contradictory and exquisite tasks: they exhibit high water permeability, while ensuring excellent water selectivity [3, 4]. From a technological point of view, designing artificial systems with similar performances would make a breakthrough with applications in water desalination, ultrafiltration or energy harvesting based on osmotic power. By overcoming the limits of macroscopic transport, novel nanofluidic systems – involving transport of fluids in specifically designed nanochannels – have recently raised great hopes towards the realization of such achievements [5, 6]. One may quote in particular experiments reporting high flow rate of water through carbon nanotube membranes [7, 8], as well as giant osmotic effects in boron nitride nanotubes [9].

Yet, in order to design artificial nanopores with optimized performances, it would be interesting to investigate more closely the solution reached by biological nanochannels to perform similar functionalities. An intriguing aspect of AQP, highlighted in Fig. 1, is the hourglass shape exhibited by the aqueous pathway, with the inner part of the pore connected to the bulk water reservoirs via cone-shaped vestibules. The central pore is of molecular size, and water is transported in this region as a single file [10]. Selectivity is achieved in this molecular scale confinement via a subtle molecular organization of the confining pore [3, 4, 11, 12, 13, 14]. On the other hand, the conical entrances are of much larger size, making a slow transition towards the bulk water. While the inner part of the pore is ruled by one-dimensional molecular transport [15], continuum hydrodynamics should apply to some extent in these cone-shaped vestibules, as it was shown that the Navier-Stokes equation remains valid down to extremely small length scales (typically 1 nm for water) [6, 16]. In this simplifying picture, the central part is the key to ensure the selectivity at the molecular scale, but the overall transport efficiency nonetheless incorporates a priori effects occurring in the conical entrances, that makes the transition to the bulk.

Accordingly, we raise in this paper the question of hydrodynamic entrance effects. Specifically, we study whether the hourglass shape of AQP corresponds to an optimum with respect to hydrodynamic dissipation. As we demonstrate below, the hourglass geometry does indeed display an optimal angle for which entrance effects are minimized, and the resulting gain in overall channel permeability can reach hundreds of percents. Strikingly, geometrical parameters measured on a variety of AQP are found to compare well with these optimal opening angles. In a broader biomimetic perspective, our findings point to general design rules to minimize entrance effects and ensure optimal transport in artificial nanopores.

Hydrodynamic Entrance effects

The question of entrance effects in hydrodynamic flows goes back to the early history of hydrodynamics. In 1891, Sampson obtained the exact solution for the Stokes flow through a circular aperture in an infinitely thin membrane [17] and found that the pressure drop Δp across the membrane was

$$\Delta p = \frac{3\eta}{a^3} \times Q, \tag{1}$$

with a the aperture radius, η the liquid dynamic viscosity and Q the flow rate through the aperture. The pressure drop results from the narrowing of the streamlines over a range a. The scaling results accordingly from Stokes' equation: $\eta\Delta v=\nabla p\Rightarrow \eta v/a^2\sim \Delta p/a$, with $v\sim Q/a^2$ the typical fluid velocity. Extending this estimate to the converging flow into a cylindrical pore, the previous Sampson's

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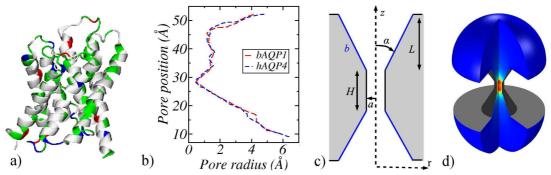


Fig. 1. a) Molecular structure of human aquaporin 4 (hAQP4) obtained from the Protein Data Bank [29]. b) Profiles of two aquaporins collected from Ref. [14]. The pore dimensions were estimated using the HOLE program [30]. c) The biconical channel considered in this work. The central cylinder, where perfect slip is assumed, is connected to two truncated cones of length L, opening angle α and with perfect or finite slip (slip length b, see text). d) Schematic of the system used for the finite element (FE) resolution of the Stokes equation (COMSOL). The channel is connected to half-spherical reservoirs (not to scale). Color represents the magnitude of fluid velocity, from blue (slow flow) to red (fast flow).

formula provides a very good estimate of the access pressure drop [18], as highlighted by an exact calculation [19].

Now, if one consider water transport through a pore, the dissipation occurring in the bulk access regions yields an upper bound to sipation is extremely small (such as carbon nanotubes [7, 8, 20, 21]), entrance effects thus act as the limiting factor for water transport, as shown recently [22, 23, 24], and exemplified by the capillary uptake of water in carbon nanotubes [25]. For AQP, whose dissipation in the inner part has not been fully characterized, a simple estimate nevertheless shows that entrance effects contribute to a large part to the global hydrodynamic resistance. Indeed, the permeabilities of AQP reported in the literature vary typically in the range $p_f=0.5$ to 1.5×10^{-19} m³/s [26]. This is to be compared to a typical order of magnitude for the entrance contribution to the permeability¹, which can be estimated from Sampson's formula², Eq. [1], giving $p_f^{\rm access} = 1.5 \times 10^{-19} \,\mathrm{m}^3/\mathrm{s}$. This estimate shows that entrance effects contribute importantly to the overall AQP permeability and cannot be overlooked. It is therefore interesting to investigate whether regardless of the dissipation occurring in the central, molecular part of the pore -, strategies exist to reduce significantly these entrance effects. Altogether, the global permeability of a pore may be written as two resistances in series,

$$p_{f,tot}^{-1} = p_{f,access}^{-1} + p_{f,central}^{-1}$$
 [2]

where the two contributions in the right hand side stand for the two access resistances and the resistance originating in the central part of the channel. In the following we focus on the first, access part of the permeability, so that our result constitute an upper bound to the total permeability. We show that a conical shape allows to reduce considerably the corresponding entrance dissipation, and thus provides an optimal shape for water transport.

Optimized permeability of hourglass-shaped pores

Inspired by the AQP shape (Fig. 1), we investigate hydrodynamic entrance effects in nanopores with an hourglass shape. We consider a pore made of a central cylinder with radius a and length H, connected to two conical vestibules, with length L and opening angle α (Fig. 1c). This system will be studied at the level of the continuum Stokes equation. Given that aquaporins dimensions are subnanometric, with the pore mouth in the nanometer range down to a central pore diameter $\sim\,0.3\,\mathrm{nm},$ using continuum hydrodynamics may certainly be questioned. However, it is known that Navier-Stokes equation is remarkably robust, remaining valid down to the nanometer scale [6, 16], so that it should apply – at least to some extent – in the entrance regions connecting the pore mouth to the bulk³.

Now, fluid transport inside the central part of the aquaporin belongs to the single-file regime and the physics at play here cannot be captured by a continuum description. However, we are not interested here in the specific selectivity of the AQP – which would indeed require a detailed atomic modeling [11, 12, 13, 14]. In order to focus on entrance effects alone, we consider a simplified view in which all dissipation in the AQP central channel is neglected. This is done by assuming a perfect-slip boundary condition on the pore surface (see Methods), so that surface friction is vanishing in this central part. By doing so, we thus focus on the entrance contribution to the permeability, *i.e.* the first term in Eq.(1). Therefore, our results provide an upper bound to the total permeability of the pore.

Boundary conditions (BC) in the conical regions have also to be prescribed (see Methods). As shown to be relevant for nano-scale flows [31], we assume a partial slip BC on the cones' walls, with the velocity field at the surface obeying $b \partial_n v_t|_{\text{surf}} = v_t|_{\text{surf}}$, where bis the so-called slip length and v_t is the tangential component of the velocity. Interestingly, the molecular structure of the AQP in contact with water is mostly hydrophobic [3, 4, 5] (with hydrophilic patches to ensure that water penetrate through the pore), and in line with recent work on hydrodynamic slippage [31, 6], a slip length in the range of tens of nanometers may typically be expected. This value is large as compared to the other typical length scale of the nanopore, $b \gg a$. Consequently, we will start our discussion by assuming perfect slip BC $(b = \infty)$, and then relax this condition in a second step. The Stokes equation with the above BC is solved numerically, see Methods. We will also present a simple model mimicking the generic aspects of flow in the access regions of AQP, which is able to provide the main features of hydrodynamic entrance effects.

Our main result is illustrated in Fig. 2, which shows the hydrodynamic permeability K of the hourglass channel as a function of the opening angle α . The permeability $K = Q/\Delta p$ provides the flow rate Q for a given pressure drop Δp . As highlighted in this figure,

 $^{^{-1}}$ The permeability p_f is defined in the physiology literature from the flux of water Φ_w (in moles per unit time) resulting from an osmotic pressure difference $\Delta\Pi$ across the pore, as $p_f=\Phi_w\mathcal{R}T/\Delta\Pi$, with \mathcal{R} the gas constant [15]. It is related to the hydrodynamic permeability of the property of the property of the permeability of the permeabil ability K defined as the ratio of the flow rate and pressure drop, as p_f with \mathcal{V}_w the molar volume of water.

² Applying Sampson formula at the subnanometric level may seem a bold approximation. However, in Ref. [27], Suk and Aluru have examined the single-file flow of water through a graphene sheet pierced with a subnanometric hole. Their molecular dynamics simulation leads to a hydrodynamic permeability $K=3\,10^{-27}\,\mathrm{m}^3/\mathrm{(Pa\,s)}$. To compare to Sampson's formula, we need the fluid viscosity and the orifice radius a. The former is, for the SPC/E model at 298 K, $\eta=0.73\,10^{-3}$ Pa's [28]. To estimate the latter consistently with Fig. 1a, we follow the 290 K, $\eta=0.73\,10^{-8}$ Pa's [25]. To estimate the fatter consistently with Fig. 1a, we follow the convention of the HOLE program, i.e. $a=d/2-r_{C,vdW}$, where $d=0.75\,$ nm is the diameter obtained using the center-to-center distance of carbon atoms, and $r_{C,vdW}=0.17\,$ nm is the carbon Van der Waals radius. Equation[1] then yields a hydrodynamic permeability $K=3.9\,10^{-27}\,$ m³/(Pa's). This suggests that Sampson's formula gives the correct order of magnitude even at the subnanometric level, down to the single-file regime.

for any cone length L, the permeability is a *non-monotonic* function of the opening angle of the pore: starting from the cylinder geometry ($\alpha=0$), the permeability starts by increasing very quickly with α , before decreasing slowly for larger angles. There is accordingly an optimal angle $\alpha_{\rm opt}$ which maximizes the channel permeability, *i.e.* yields a maximal flow rate under a given pressure forcing. Compared to the cylindrical case ($\alpha=0$), the optimal geometry ($\alpha=\alpha_{\rm opt}$) yields a very significant increase in permeability, especially for long cones. At L/a=20 for instance, the optimal permeability is 6 times larger than the one of a cylinder. Although it increases for shorter cones, the optimal angle remains small, below 10° for L/a>5. Surprisingly, a tiny departure from the straight cylinder makes for a large effect on entrance dissipation. This is an unexpected result and in order to gain insight into its origins, we now develop a simplified model to rationalize viscous dissipation in the hourglass channel.

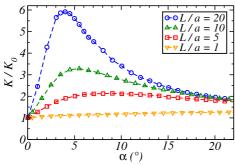


Fig. 2. Hydrodynamic permeability $K=Q/\Delta p$ of the hourglass nanochannel as a function of the opening angle α , obtained from FE calculations. K is normalized by $K_0=K(\alpha=0)$. Perfect slip $(b=\infty)$ is assumed on the cones inner walls. Each curve corresponds to a cone length L.

Towards a simplified analytical model

So far, we assumed in a first step a negligible friction on the cone's surface (perfect slip). In this situation, the dissipation is expected to occur mostly within the two transition regions: from the reservoir to the cone (first entrance), and from the cone to the cylinder (second entrance). This is confirmed by the numerical results, as highlighted in Fig. 3, where we have plotted the local viscous dissipation rate $D=2\eta\Delta:\Delta$, with $\Delta=\left[\nabla\mathbf{v}+\nabla\mathbf{v}^T\right]/2$ the strain rate tensor. The spatial extent of both regions is given by the local radius, with a prefactor close to unity. This figure shows that increasing the opening angle shifts the dissipation from the first entrance to the second. This is to be expected if one realizes that the streamlines have basically to follow the surface of the pore, and that the second angle between the cone and the cylinder increases as the first angle between the wall and the cone decreases (the sum of the two angles being constant due to geometry).

This picture suggests to describe the total hydrodynamic resistance of the pore, $R=K^{-1}=\Delta p/Q$ (the inverse permeability), as the sum of the various contributions (channel entrance, cone region, and cylinder entrance ⁴) in series, as for a resistive circuit:

$$R = R^{\text{ent}} + R^{\text{cone}} + R^{\text{ent,cyl}}.$$
 [3]

For such a decomposition to hold, both the cylinder radius a and the entrance radius $a'=a+L\tan\alpha$ should remain small compared to L, which is valid for large L/a ratio and small opening angle α .

In a cone of infinite extent with arbitrary opening angle and perfect slip at the wall, the Stokes flow is purely radial with a velocity that decreases as $1/r^2$, where r is the distance from the apex. One may then verify that the pressure drop, evaluated from $\nabla p = \eta \Delta \mathbf{v}$, vanishes in this situation. Accordingly, for the case $b = \infty$ that we consider so far, $R^{\rm cone}$ is thus negligible, in agreement with numerical results, see Fig. 3.

Now, to proceed further and estimate the remaining contributions in Eq. [3], we need to estimate entrance hydrodynamic resistance for two configurations: (i) a conical aperture with a finite angle and perfect slip; (ii) a cone-to-cylinder entrance. These are generalized Sampson geometries, which we consider now.

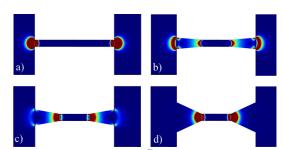


Fig. 3. Local viscous dissipation rate D (see text) inside the nanochannel for different values of the angle α . The color scale, from blue to red, indicates increasing values of local viscous dissipation. Perfect slip boundary condition is imposed on the cone walls. From a) to d), $\alpha=0,5,10$ and 25° .

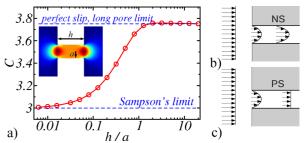


Fig. 4. a) $C=Ra^3/\eta$ (see text) as a function of the pore length h for a perfectly slipping cylindrical channel, obtained with FE calculations (points). The red line is a guide for the eyes. Inset: Velocity field in the considered channel. Color represents the amplitude of the fluid velocity, from blue (slow flow) to red (fast flow). b,c) Schematic profiles of axial velocity in a channel with no slip (NS) and perfect slip (PS) boundary condition. From left to right: outside far field, entry profile and inside far field.

Generalized Sampson formula (i): aperture with perfect slip. To evaluate $R^{\rm ent}$, we build on previous works. We neglect the effect of the conical shape of the aperture and evaluate $R^{\rm ent}$ for the geometry of a flow entering into a cylinder, an approximation valid for long cones with small angle. As quoted above, Sampson calculation was generalized by Dagan et al. to such geometry [19]. However these calculations assumed a no-slip BC at the pore walls and we need first to generalize this result to perfect slip as considered here. On dimensional grounds, the access resistance of the finite tube is expected to write $R = \Delta p/Q = C\eta/a^3$, where C is a numerical prefactor (C=3 in Sampson expression, Eq. [1]). We have computed numerically this prefactor C using FE calculations for a perfectly slipping cylinder of finite length, Fig. 4a. For very short tubes, the BC at the inner wall becomes irrelevant, and Sampson's result for the infinitely thin membrane is recovered with C=3. As the tube gets longer, however, the C coefficient increases up to a plateau value of $C_{\infty} \approx 3.75$, implying that switching from no-slip to perfect slip inside the tube yields a 25% increase in the access resistance. Though counter-intuitive at first sight, this behavior can be qualitatively understood by examining the flow profile at the channel end. In the

⁴Note that the three resistances do not identify with dissipation inside the volume of reservoir, cone and cylinder respectively. For example, the entrance resistance includes dissipation taking place both in the reservoir and in the cone.

no-slip case (Fig. 4b), this "entry" flow profile is, to a very good approximation, halfway between the parabolic profile of Poiseuille flow and the elliptic profile found in Sampson's solution [19]. As a result, the transition to a plain parabolic profile inside the channel involves only a small dissipation. Because the velocity must vanish at the corner, the entry profile in the perfect-slip tube is quite similar to the noslip case, suggesting a comparable amount of viscous losses outside the tube. Now, inside a tube with perfect slip at the boundaries, the transition to a plug profile requires significant reorganization of the streamlines (Fig. 4c), resulting in a higher dissipation, hence a higher C. As a side remark, we find that the BC on the external wall has a negligible impact on the access resistance, presumably because any slip that could happen there is strongly hampered by the vanishing velocity at the corner.

Coming back to the case of the hourglass-shaped pore, we now estimate the hydrodynamic resistance of the first entrance as

$$R^{\mathrm{ent}} = \frac{C_{\infty} \eta}{a'^3}, \quad a' = a + L \tan \alpha,$$
 [4]

with $C_{\infty} = 3.75$.

Generalized Sampson formula (ii): cone-to-cylinder entrance. No prior work seems to have investigated the Stokes flow at the junction between a cone and a cylinder, both with perfect slip ⁵. We could not obtain an analytical solution either for this geometry. However numerical calculations (see Methods) suggest that the hydrodynamic resistance at a cone-to-cylinder transition can be well approximated by

$$R^{\rm ent,cyl} = C_{\infty} \sin \alpha \, \frac{\eta}{a^3},$$
 [5]

with again $C_{\infty}=3.75$. This behavior can be rationalized on the basis of the following "back-of-the-envelope" argument. Far from the junction, streamlines are parallel in the cylinder and radially divergent in the cone. Dissipation occurs only in the vicinity of the junction, where the streamlines change direction by an angle α , so that $\nabla v \sim v_0 \sin \alpha/a$. The pressure drop Δp is then given roughly as $\Delta p \sim \eta \nabla v \approx \eta v_0 \sin \alpha/a$, pointing to the origin of the $\sin \alpha$ dependence for $R^{\rm ent.cyl}$. Now in the case $\alpha=\pi/2$, one should recover the resistance $R^{\rm ent}$ with prefactor C_{∞} , leading to Eq. [5].

Total hydrodynamic resistance. Collecting Eqs. [3], [4] and [5], and remembering that $R^{\rm cone} \approx 0$, yields the total resistance of the hourglass channel in our simplified model:

$$R = \frac{C_{\infty}\eta}{a^3} \left[\left(1 + \frac{L}{a} \tan \alpha \right)^{-3} + \sin \alpha \right].$$
 [6]

This relation exhibits a non-monotonous behavior versus the angle α , as shown in Fig. 5: the first term in the right-hand-side decreases rapidly with α , while the second term steadily increases. Physically, these two terms account for dissipation at the first and second entrance respectively, and their variations confirm the qualitative picture illustrated in Fig. 3. A minimum for the resistance – thus a maximum for the permeability $K=R^{-1}$ – is then found. In particular, for long cones and small angles, $R\approx (\alpha L/a)^{-3}+\alpha$, and the optimal angle decreases with the cone length as $\alpha_{\rm opt}\sim (L/a)^{-3/4}$. More quantitatively, Fig. 5 compares FE calculations and the predictions of our simplified model. While a quantitative agreement is not expected in view of the simplifying assumptions underlying our model, the latter is found to capture the optimization phenomenon. In particular, the variation of the optimal angle $\alpha_{\rm opt}$ versus length L/a is well reproduced, see inset of Fig. 5.

To summarize, there is an optimal angle which maximizes the permeability of an hourglass channel, and minimizes viscous losses. This optimal angle takes rather small values, in the range $\alpha_{\rm opt}\sim5-20^{\circ}$ depending on the length of the conical vestibules, but can

lead to very strong improvements in the permeability. Following Dagan *et al.*, it should be possible to calculate the exact solution for a flow inside a biconical nanochannel [19]. We leave this ambitious work for future dedicated investigations. However, an approximate model is presented in the Supporting Information.

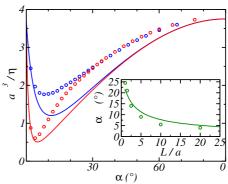


Fig. 5. Pore resistance R versus cone angle α for perfect slip in the cones: comparison between FE calculations (circles) and Eq. **[6]** (lines). Results are presented for two pore lengths: L/a=20 (red) and L/a=5 (blue). Inset: optimal angle α_{opt} , for which the resistance is minimized, as a function of cone length.

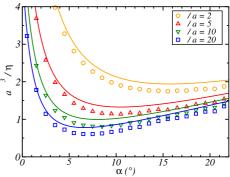


Fig. 6. Pore resistance R versus opening angle α , for various slip lengths b in the conical regions: comparison between FE calculations (symbols) and analytical expression (lines), see text for detail. The cone length is fixed to L/a=20.

Extension to finite friction on the cone surface. Up to now, we assumed a perfect slip BC at the cones' surfaces, corresponding to the limit of large slip lengths compared to transverse dimensions $b/a \to \infty$. We now relax this assumption and consider finite b/a. Figure 6 reports the results of numerical calculations for the hydrodynamic resistance versus opening angle, for various slip lengths b at the cone surface and a fixed cone length, L=20 a (see Methods). As shown in this figure, an optimal angle minimizing the hydrodynamic resistance is still found for finite slip, and its value increases with decreasing slip length, see also Fig. 7a.

Again a simplified model can be built. While we do not expect entrance effects to be radically modified, a supplementary dissipation will now occur due to finite slippage at the cone surface. This contribution, R^{cone} in Eq. [3], can be calculated within lubrication theory, valid for small angles α , as

$$R^{\text{cone}} = 2 \int_0^L dz \, \frac{8\eta}{\pi a(z)^4} \left(1 + \frac{4b}{a(z)} \right)^{-1}, \tag{7}$$

 $^{^5\}mbox{This}$ is not surprising since until recently, the perfect-slip BC was not deemed physically relevant.

with $a(z)=a+z\tan\alpha$ the local radius of the cone. Accordingly, an analytical expression for $R^{\rm cone}$ can be obtained, but its cumbersome expression is not particularly illuminating and we do not report it here. Gathering all contributions in Eq. [3] leads to an analytical expression for the hydrodynamic resistance of the hourglass pore with finite slip length b on the cones. This expression is compared to the numerical calculations in Figs. 6 and 7a. Altogether a good agreement is found and the approximate expression is able to capture both the dependency of $R^{\rm cone}$ with α and b, as well as the order of magnitude of the optimal angle and its variation with b and L/a.

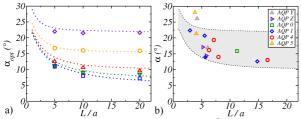


Fig. 7. a) Optimal angle as a function of cone length L for various slip lengths (from top to bottom, b/a=1,2,5,10,20): FE results (circles) and model (lines). b) Angle α evaluated in six aquaporins (see Methods). The gray shaded area corresponds to model predictions for b/a=1 to 5 (as shown in left panel). Data are extracted from Refs. [14, 32, 33, 34, 35, 36, 37].

Discussion

Altogether, our results show that the hourglass geometry, associated with small surface friction, does optimize the permeability by reducing considerably the magnitude of entrance effects. A small opening angle in the range $5-20^\circ$, depending on the precise geometry and boundary conditions, can increase the permeability by a large factor, reaching hundreds of percents for typical parameters.

To conclude, we discuss the relevance of these effects for the shape and the hydrodynamic permeability of aquaporins. As explained in the introduction, AQPs have hourglass shapes resembling the model geometry considered here. Furthermore, due to their mostly hydrophobic inner surface, a small friction, and large slip length, is expected at the cone walls. Overall, they exhibit the main ingredients associated with permeability optimization discussed above. In order to push further the comparison, we have extracted some generic shape parameters of a large variety of AQPs. As illustrated in Fig. 1, and detailed in the method section, we used molecular structures obtained from high-precision X-ray crystallography - which are available for several aquaporins, and obtained the radius profile of the channel, as estimated by the HOLE program [30]. Though irregular, those profiles can be divided into three parts: a central (molecular) constriction, and two vestibules with roughly conical shapes. Although matching an atomically detailed structure to a simplified geometry involves a certain degree of arbitrariness (see Methods), we estimated the L and α parameters of our model for a series of six aquaporins. The results for the opening angle α of the AQPs conical section are displayed in Fig. 7b. Two conclusions can be drawn from this figure: (i) the opening angle keeps rather low values, within the range $10-25^{\circ}$; (ii) the optimal angle decreases as the cone gets longer. It is therefore striking that the adopted global geometry follows the expectations for the hydrodynamic optimization process discussed above to minimize the entrance permeability.

Obviously, some more detailed features of the AQP geometry can not be discussed within the previous results. In particular, the structure and shape selection of AQPs follows from a number of constraints and requirements, many of them from the molecular level and the subtle balances to achieve selectivity and efficient transport in the inner single-file constriction. For instance, aquaporins channels are not symmetric with respect to the membrane half-plane, as the cone

towards the cell exterior is apparently longer and more divergent than the interior cone. Within our model, this could be explained only if the inner and outer cylinders radii were different. While this is often the case, we have considered only the average radius of the central portion, so as to keep a small number of parameters.

Conclusion

The aim of this work was to determine the effect of geometry and boundary conditions on hydrodynamic entrance effects in biconical nanochannels. Using finite element calculations, we have shown that compared to a plain cylindrical pipe, a biconical channel with its optimal angle can provide a spectacular increase in hydrodynamic permeability. A simplified model based on entrance effects and lubrication approximation rationalizes the observed behavior. Although speculative, this could indicate that the hourglass geometry of aquaporins results from a shape optimization, in order to reduce end effects and maximize water permeability.

Among transmembrane proteins, and ionic channels in particular, examples abound where the particular function - ion selectivity for instance- is tied to a specific feature of the molecular architecture. Yet it remains worth wondering, as we have done here, whether generic factors such as viscous dissipation could be the driving force behind the shapes fine-tuned by evolution. Finally, in a more general biomimetic perspective, this work provides guidelines to optimize the performances of artificial nanopores. Hydrodynamic permeability is indeed a crucial property for applications in water desalination, ultrafiltration or energy harvesting from salinity gradients. For those particularly relevant nanochannels whose inner dissipation is extremely low [20, 21], it is of prime importance to reduce entrance effects, because they control the overall permeability of the membrane.

Materials and Methods

Numerical calculations.

We study low-Reynolds numbers flows in two-dimensional axisymmetric geometry. The system of interest includes two reservoirs separated by a membrane containing one biconical nanochannel. We used finite-element method (COMSOL) to solve the Stokes equation

$$\nabla p = \eta \, \Delta \mathbf{v}, \tag{8}$$

where ${\bf v}$ is the fluid velocity, p the pressure and η the fluid viscosity. We imposed a flow rate Q through the channel and measured the pressure drop across the membrane. In order to avoid finite size effects, we chose a reservoir much larger than the pore radius. In this study we have imposed the following hydrodynamic boundary conditions:

- \bullet No-slip boundary condition: This BC supposes that the fluid has zero velocity relative to the boundary, $v_w=0$ at the wall.
- Partial-slip boundary condition: Deviations from the no-slip hypothesis have been predicted theoretically and observed experimentally at the nanometer scale. First, assume that the tangential force per unit area exerted by the liquid on the solid surface is proportional to the slip velocity v_w : $\sigma_{xz} = \lambda v_w$, with λ the friction coefficient, z the normal to the surface, x the direction of the flow. Combining this equation with the constitutive equation for a bulk Newtonian fluid, $\sigma_{xz} = \eta \partial_z v_x$, we obtain the Navier BC: $v_w = \frac{\eta}{\lambda} \partial_z v_x = b \partial_z v_x$ [31]. This equation defines the slip length $b = \eta/\lambda$ as the ratio between the bulk liquid viscosity and the interfacial friction coefficient. The slip length has a simple geometric interpretation, as the depth inside the solid where the linear extrapolation of the velocity profile vanishes.
- Perfect-slip boundary condition: The limit of an infinite slip length, or equivalently a vanishing friction coefficient, is used when the slip length b is much larger than the characteristic length(s) of the system. For simple liquids on smooth surfaces, slip lengths up to a few tens of nanometers have been experimentally measured [31].

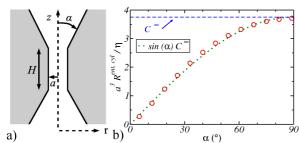


Fig. 8. a) Schematic of the system used to compute the cone-to-cylinder hydrodynamic resistance. b) Cone-to-cylinder resistance $R^{\mathrm{ent,cyl}}$ versus cone angle $\alpha :$ FE calculations (red circles) and analytical approximation by a sine function (dotted line)

Cone to cylinder entrance.

In order to extract the contribution of the cone-cylinder junction to the total resistance of the channel, we performed the following numerical calculations. Reservoir parts are removed to eliminate the outer entrance contribution R^{ent} leaving only a system composed of a central channel and two truncated cones (Fig. 8-a). We imposed perfect slip BC along both the cone and cylinder's walls, and the incoming flow fields is imposed using the far-field exact expression for frictionless cones. We varied the angle lpha and observed that the hydrodynamic resistance of such a junction is to a good approximation proportional to the sine of the angle of the cone α (Fig. 8-b).

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Evaluation of aquaporins' geometrical properties.

We have chosen to divide the aquaporin in three parts; two conical entrances and one central part (see Fig. 9). Each part of the aquaporin was linearly fitted to extract the relevant parameters.

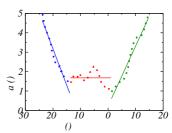


Fig. 9. Profile of an aquaporin (hAQP4 [32], dotted line) and linear curve fitting (solid lines).

The central part of the aquaporin gives us the value of the central radius a.From conical entrances, we extracted both the length L and the angle α . Due to the asymmetry of the aquaporin, we obtained two values of cone length and angle for each aquaporin.

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