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INFLUENCE OF NON- ETTING CONDITIONS ON AGGREGATION OF DI IDED SOLIDS IN LIQUID PHASE

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Abstract. e present here the main results of an experimental study of aggregation hich as performed on t o silica granular samples: one is naturally hydrophilic; the other has been made hydrophobic by superficial grafting of hydrophobic groups. Aggregation is studied in ater-ethanol mixtures of variable compositions and follo ed by in situ turbidimetry at different stirring rates. The aggregation behaviours of the t o samples are quite different. Aggregates of hydrophilic particles are small and fragile hereas aggregates of hydrophobic particles are large and particularly solid. Interpretation of these differences is presented; it is based on several elements: modelling of hydrophobic interaction and of aggregate morphology, modelling of the aggregate optical properties and determination of the aggregation and fragmentation rates. Essential modification introduced by non- etting consists of the formation of gas bridges around contact points bet een particles in aggregates.

INTRODUCTION

Aggregation of hydrophilic particles in stirred liquid media can be considered as a relatively ell understood process in spite of the variety and complexity of its aspects: physicochemical, hydrodynamic, morphological [1]; on the contrary, little is kno n about aggregation of hydrophobic particles in aqueous media and more generally about the aggregate structure and properties. This case is met in several industrial situations: suspension, sedimentation and flotation of hydrophobic po ders in aqueous media of course, ho ever also hen solid particles are not etted by liquid media, for instance, alumina inclusions in liquid steel baths [2].

A large number of experimental orks indeed have definitely proved the existence of very strong long range attractive forces bet een hydrophobic surfaces in ater [3-4]. This hydrophobic interaction as quantified from direct force measurements and proved to be, in most cases, much larger than the van der aals forces. Several of the experimental orks mention the existence of gas bridges bet een particles in close interaction [4-6]. In a recent theoretical ork [7], e sho that hydrophobic particles are likely covered by a gas layer hich invades their superficial porosity; e prove too that this gas layer may play an essential part both in the aggregate formation and fragmentation.

To our kno ledge, no systematic study of hydrophobic aggregation exists. The aim of this paper is to present a compared experimental study of aggregation of t o silica samples coming from the same lot: one is naturally hydrophilic; the other has been made hydrophobic by surface chemical processing. The results ill be then interpreted in reference ith classical aggregation models [1,8-9] and ith ne theoretical considerations [7].

EXPERIMENTAL PART

1. Materials and met ods

Original solid samples consist of monodisperse silica spheres (0.5 µm and 1.5 µm in diameter, *Geltech Inc* products). They are poorly soluble in ater and can be made hydrophobic by grafting of carbon chains. Grafting procedure involves an hydroxylation process hich produces highly reactive surface silanol (-SiOH) groups, then a etting step ith a N,N-Dimethyloctadecylaminosilane solution; this results in a surface silanisation reaction, i.e. the grafting of a carbon chain via a strong Si-O-Si bond. Both silica particles, processed or unprocessed, have a zero point charge pH of 3.2.











Aggregation is studied in ater-ethanol solutions of variable composition because hydrophoby (or equivalently non-etting) varies ith the ethanol ratio. etting of a solid is characterized by the contact angle of a liquid drop put on its surface. Perfect etting corresponds to a zero angle hereas non etting begins for angles higher than 90. For our hydrophobized silica, contact angle value is given in Table 1. Starting from 125 in pure ater, it decreases ith ethanol addition; non-etting conditions vanish beyond 15% volume ratio in ethanol.

Table 1. Contact angle versus ethanol volume content in ethanol- ater mixture

EtOH (%)	0	3.45	5	10	15	25
Contact angle ()	125	118	116	105	90	67

Aggregation is studied in a double jacketed 4-baffled 1.45 L pyrex vessel. This reactor is provided ith a atertight cover so that it can be completely filled ith liquid, avoiding in this the presence of a free interface hich could entrap hydrophobic particles. Agitation is ensured by a four bladed 45 Teflon impeller. Temperature is kept constant at 25.00 C. The reactor is fitted ith an optical system to measure in situ the suspension turbidity in the avelength range 350 nm-800 nm. Details can be found in [10].

Each aggregation experiment consists of the follo ing steps:

- i) preliminary dispersion by ultrasounds of 0.246 g of solid sample in an ethanol-rich small volume;
 - ii) filling-up of the reactor ith the ethanol- ater solution;
- iii) injection of the silica suspension and destabilization by nitric acid addition (pH = 2.4). This pH value is very close to the zero point charge and allo s aggregation to take place at significant rate;
- iv) after this injection, aggregation starts and can be follo ed by continuous in situ turbidity measurements [8-9].

2. Principle o exploitation o t e experimental data

Light scattering by solid particles (here aggregates) in suspension results in extinction of an incident light beam of avelength λ_0 , the intensity $I_0(\lambda_0)$ of hich is reduced do n to value $I(\lambda_0)$ after crossing of an optical path of length L_{opt} . Turbidity τ , hich expresses this extinction phenomenon, is defined by:

$$\tau \lambda_0 = \frac{1}{L_{ont}} \ln \frac{I_0 \lambda_0}{I \lambda_0} \tag{1}$$

 τ depends on mean diameter d_p particle density function f according to the integral:

$$\tau \lambda_0 \qquad C_{ext} d_p f d_p dd_p \tag{2}$$

Particle extinction cross-section C_{ext} is derived from the Mie theory [11]; its calculation is relatively easy for spherical, compact, or large particles, ho ever much more delicate for small, non compact aggregates [12].











ith our experimental system, turbidity variation ith time is available over a hole aggregation experiment for several avelengths. Moreover from dynamic models of the process and morphological and physical models of the aggregates, density function $f(d_p)$, thus turbidity can be calculated at any time [8-9]. From comparison bet een experimental and predicted values, the most relevant models can be selected and their unkno n parameters determined. From a more qualitative point of vie , turbidity $\tau(t)$ plot shape can be analysed from t o main characteristics: initial slope, hich is globally proportional to the aggregation rate, final plateau height, hich is significant of dynamic equilibrium bet een aggregation and fragmentation (see Fig. 1 for instance).

3. Experimental results

3.1. Stirring rate influence on aggregation of hydrophilic silica

Stirring rate has a multiple influence on aggregation: collision frequency increase, capture efficiency decrease, aggregate fragmentation increase.

Figure 1 sho s aggregation of 0.5 m non processed (hydrophilic) silica at different stirring rate values. Turbidity increases ith time. For 1.5 m particles, ho ever, turbidity decreases [10]. This behaviour difference is due to light scattering properties hich vary a lot in the investigated size range. From a more quantitative point of vie, aggregation is relatively slo, particularly at lo stirring rate (lo initial slope values) and produces small aggregates, particularly at high stirring rate (lo variation of turbidity bet een initial value and final plateau). These elements ill be integrated later on in a global model.

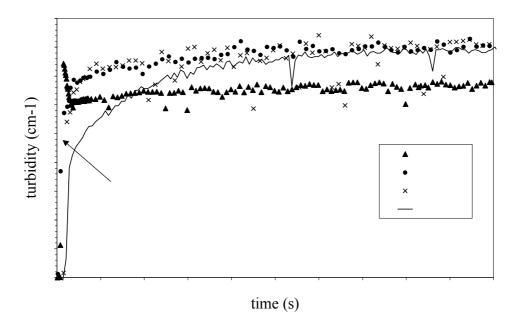


Figure 1. Influence of stirring rate on 0.5 µm hydrophilic silica aggregation

3.2. Stirring rate influence on aggregation of hydrophobic silica

Figure 2 sho s aggregation of 0.5 m hydrophobic silica at different stirring rates. Turbidity decreases contrary to hat as observed previously. This change points to a modification of the aggregate scattering properties probably due to the presence of gas bridges. The same behaviour is observed for 1.5 m particles. The stirring rate effects are globally the same as for hydrophilic silica, ho ever, aggregation is much more rapid and large agglomerates are formed as indicated by the lo final level of turbidity.











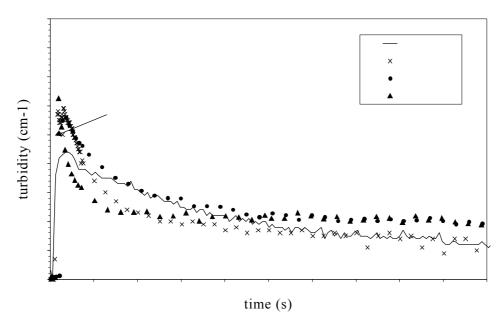


Figure 2. Influence of stirring rate on 0.5 µm hydrophobic silica aggregation

3.3. Influence of the liquid phase composition

Analysis of the turbidity curves in ater-ethanol solutions is delicate, because of the turbidity value offset due to the change in the medium refractive index. In the case of hydrophilic silica, they have the same aspect hatever the composition. In the case of hydrophobic silica, effect of ethanol content is complex (Figure 3). Ho ever, after correction, it seems that in all cases, presence of ethanol decreases the aggregation rate.

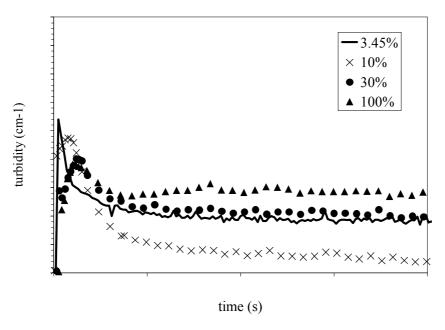


Figure 3. Effect of ethanol volume content on hydrophobic silica aggregate

3.4. Aggregate size and morphology

Photographs of aggregates ithdra n from the medium at late stages of aggregation of 1.5 m particles confirm the presence of small relatively ramified aggregates in the case of hydrophilic silica and of enormous aggregates in the case of hydrophobic silica (Figure 4).











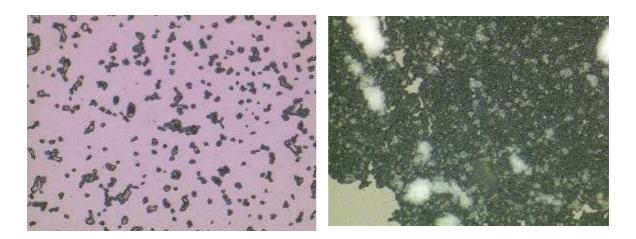


Figure 4. Photographs of 1.5 µm silica particle aggregates (left side: hydrophilic particles; right: hydrophobic particles)

Results interpretation requires on one hand model of hydrophilic silica aggregation, on the other hand understanding of the specific elements brought by hydrophoby.

THEORY

1. Basic elements o modeling

From a general point of vie, aggregation of hydrophilic silica is expected to follo classical theory of turbulent aggregation [13]. Ho ever, some attention should be given to the small size and morphology of the aggregates hich are indeed proved to be ramified and tens of particles at the maximum [10; 12] Classical models, either consist in a fe hydrodynamic or optical, ho ever ere conceived for large aggregates and based on quasifractal morphology. For instance, the concept of fractal dimension cannot be rigorously kept ithout modification for the smallest aggregates. Ho ever, this convenient tool for describing and modelling ramified objects can be generalised for all the aggregate sizes. One of us [12] introduced indeed the notion of ea fractal dimension to represent the aggregates morphology do n to a fe particles. Thanks to this generalization, procedures established for large objects can be applied over the hole range of aggregate size. Moreover, Gruy [12] developed original calculation of the aggregate extinction cross-section C_{ext} . In these conditions, results concerning hydrophilic silica aggregation can be interpreted using the modified models. Fractal dimension of the aggregates ranges bet een 2.4 and 2.5 and may vary ith their size.

In [7], e proved that hen solid particles are immersed in a non-etting liquid, gas or vapour spontaneously fills the pores or the surface anfractuosities (Figure 5). This results in a partial or total coverage of the solid surface ith a gas layer. Consequences are multiple:

- i) hen to particles get in contact, their mutual gas pockets can merge, creating a gas bridge hich ensures strong cohesion bet een them (Figure 6);
- ii) prior to the contact, presence of bubbles at the particle surface may give rise to an additional static attractive force; this force, hich is called *B er nes force* [14] has an hydrodynamic origin and is due to coupled thermal vibrations of the bubbles. Ruckenstein [14] proposes a calculation procedure based on dimensional and experimental considerations, ho ever does not obtain quantitative determinations. e recently re-visited this problem [7], using another approach and correcting some errors. e obtained the order of magnitude of the Bjerknes force and concluded that in several cases they ere not necessarily higher than the van der aals force as Ruckenstein claimed.











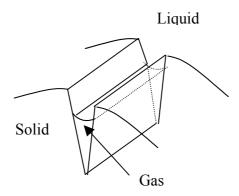


Figure 5. Gas cavity in a crevice in a pore

- iii) existence of a gas-liquid interface(instead of a solid-liquid interface) modifies too the boundary conditions, thus the particle motion in the liquid phase (violation of the no-slip condition); in particular, hen t o particles or aggregates are in close approach, the liquid layer bet een them should be evacuated. This may result in a repulsive force hich reduces the collision rate by a *capture efficiency coefficient* lo er than one. In case of non- etting, e re-calculated the capture efficiency coefficient [7] and proved it as slightly higher than in case of etting, hatever the interaction force (van der aals or Ruckenstein-like) thus aggregation rate is increased.
- iv) the main consequence of non- etting, ho ever, concerns the fragmentation of the aggregates; hydrophilic particle aggregates, indeed, have a eak cohesion, because of the lo value of the van der aals forces hich are responsible for their cohesion; in case of hydrophobic particles, on the contrary, gas bridges bet een particles ensure very strong cohesion forces and considerably reduce the fragmentation possibilities.

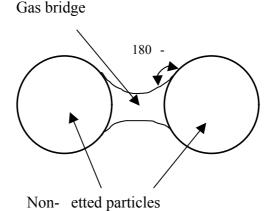


Figure 6. Gas bridge bet een solid particles in non- etting liquid

2. Ne t eoretical aspects

In the text above, e often refer to the presence of gaseous bridges bet een hydrophobic particles and e attribute to this particularity most of the ne behaviours observed in hydrophobic aggregation. This deserves to be verified because observation of the samples is difficult and not conclusive. One of our subjects of interest concerns the ne optical properties of the aggregates and their consequences on turbidity.

2.1. Light scattering by hydrophobic silica aggregates

Refractive indices of silica, ater and gases are respectively 1.44, 1.34 and 1.0. Scattering properties of particles in a medium mainly depends on the index contrast bet een the media











and on the particle size. Presence of gas (air or vapour) in an aggregate may considerably change this contrast and be responsible for the behaviour modification—e noted in Figures 1 and 2. Calculation of the scattering properties of a silica- ater-air aggregate requires assumptions on the three phase location. The t o cases—hich have been envisaged—homogeneous density in the porous particle or surrounding thin layer [10]- give us similar results. Particle extinction section is reduced as expected and gas proportion is found to be equal up to 0.3,—hich—ould correspond to a uniform external layer of 0.05—m in thickness. 2.2. Simulation of turbidity time evolution

Basic simulation equation is the ell-kno n partial derivative equation of Smolucho sky [13]. In case of hydrophilic aggregation, fragmentation is envisaged. Agreement ith experimental turbidity plots is good for fractal dimension of 2.4 (Figure 7). At 200 rpm, the predicted maximum particle number in the aggregates is 68, hereas experiment gives 64 [15]. In case of hydrophobic aggregation, fragmentation is no considered. Fractal dimension is found to be higher (2.7). This is consistent ith the more compact observed aggregates. Aggregates can contain several hundreds of particles. Agreement bet een experimental and theoretical plots is still good as sho n in Figure 8 for stirring rate of 200 rpm.

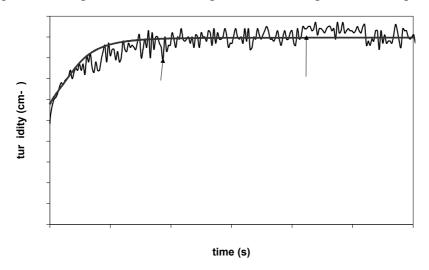


Figure 7. Turbidity variation ith time (experimental and simulated) during aggregation of hydrophilic 0.5 µm silica particles.

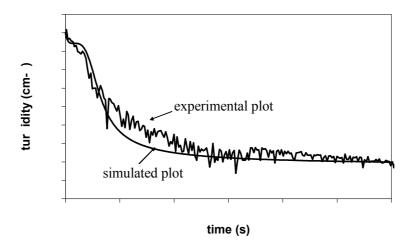


Figure 8. Turbidity variation ith time (experimental and simulated) during aggregation of hydropobic 0.5 µm silica particles.











CONCLUSION

In this ork, e emphasize the main consequences of non- etting on solid particle aggregation in stirred liquid media. In case of non- etting, very large and resistant aggregates are formed. The presence of gas bridges bet een particles is at the origin of the cohesion of the hydrophobic aggregates. Influence of non- etting exists on other aggregation characteristics (interaction forces, capture efficiency), ho ever is less significant. Presence of gas in the aggregates also affects their optical properties; this is an important detail, kno ing that optical methods are the most idespread particle sizing techniques.

The application field of this study is not restricted to the only systems of hydrophobic solid particles in ater, hatever its importance, relatively, for instance to transport, stirring, sedimentation, flotation. Recently e ere faced to the problem of aggregation of alumina inclusions in molten steel baths [2]. Alumina is not etted by steel and observations prove that very large ramified clusters can be formed and heavily affect the mechanical properties of the metal if they are not eliminated at early stages of the process. Present models as ell as analogy ith hydrophobic aggregation can provide ith information about the conditions of formation of these clusters and on their location in the industrial facilities, so that elimination procedures can be operated ith more efficiency.

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