A solution to the stick slip problem for an electropneumatic drive

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A SOLUTION TO THE "STICK-SLIP" PROBLEM FOR AN ELECTROPNEUMATIC DRIVE

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Abstract

This paper describes a solution to the problem of «stick-slip» for an electropneumatic system. The phenomenon of «stick-slip» may appear during the mechanical static state when the position is fixed but the pressures continue to evolve in each actuators chambers, until exceeding the dry friction zone. The system is then in partial equilibrium. The idea to avoid this phenomenon is a switching control law between the tracking position control and the pressure regulation.

Keywords: "Stick-slip" phenomenon, electropneumatic system, switching control, experimental results.

1 Introduction

"Stick-slip" refers to the phenomenon of a spontaneous jerking motion that can occur while two objects are sliding over each other. Stick-slip is caused by the surfaces alternating between sticking to each other and sliding over each other, with a corresponding change in the force of friction. Typically, the stiction friction coefficient between two surfaces is larger than the Coulomb friction coefficient. If an applied force is large enough to overcome the stiction friction, then the reduction of the friction to the Coulomb friction can cause a sudden jump in the velocity of the movement. Examples of stick-slip can be heard from hydraulic cylinders, honing machines etc. Special chemicals can be added to the hydraulic fluid or the cooling fluid to overcome or minimize the stick-slip effect. Stick-slip is also experienced in lathes, mill centres and other machinery where something slides on a slideway. Slideway oil typically lists "prevention of stick-slip" as one of its features.

The "stick-slip" phenomenon is a real problem for the industrial development of pneumatic technology. However there are no industrial or scientific research works in the literature which present a solution that can be generalized for certain fields or in every fluid power process to eliminate this phenomenon. Only some specific empirical solutions have been tested in specific contexts to reduce the possibility of the occurrence of the "stick-slip" phenomenon. Cite for example: Control Engineering Staff (2003) have proposed a technological improvement by developing specific valves. Ming-Chang and Shy-I (1995) have used specific control laws to reduce the effect of friction in electropneumatic applications by using, for example, control laws with velocity or acceleration tracking trajectories. Brun, Sesmat, Thomasset and Scavarda (2005) have presented the necessary and sufficient conditions not to have the restarting phenomenon and gave an estimation of the restarting time if the condition is not in effect. Hamiti, Voda-Besançon and Roux-Buisson (1996) have coped with the problem caused by the stick-slip friction in a pneumatic system and propose a method to limit and to be eliminated in a progressive manner the stiction effect by decreasing the integral gain of the PI controllers. PAI and SHIH (2003) have designed a velocity compensator to overcome the stick-slip effect of the pneumatic-driven ultraprecision table while adding directly the velocity compensation signal to the conventional PD and Fuzzy controller. Hägglund has presented a procedure that compensates for static friction (stiction) in pneumatic control valves by adding pulses to the control signal. Renn and Liao (2004) have proposed the fuzzy-sliding mode controller at a low rotational speed of a servo-pneumatic motor with presence of the nonlinear deadband and stick-

slip friction. In all technologies for positioning systems, its well known that the use of an integral action in the control law lead to «stick-slip» occurrence. However it will be explain in this paper that in fluid power systems, the reason of «stick-slip» appearance is fundamentally different and not due to integral action.

In this paper, a solution for the problem of «stick-slip» for an electropneumatic system for tracking position trajectory will be presented. It is organized as follows; in the next section the electropneumatic system is described. Then the main idea result using two switching sets of control laws is developed. Finally experimental results are presented and compared to validate the procedure.

2 Electropneumatic system modeling

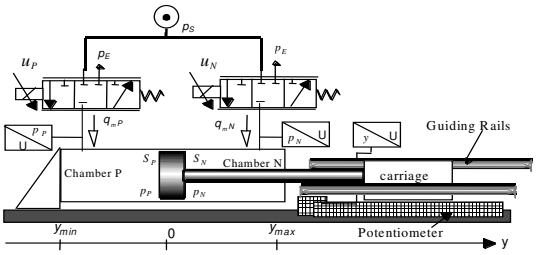

Fig.1: The electropneumatic system

The system under consideration, fig. 1, is a linear inline double acting electropneumatic servo-drive using a single rod controlled by two three-way servodistributors. The actuator rod is connected to one side of the carriage and drives an inertial load on guiding rails. The total moving mass is *17 kg*.

2.1 Physical model

The electropneumatic system model can be obtained using three physical laws, the mass flow rate through a restriction, the pressure behavior in a chamber with variable volume and the fundamental mechanical equation.
The pressure evolution law in a chamber with variable volume is obtained via the following assumptions Shearer (1956):

a) air is a perfect gas and its kinetic energy is negligible;
b) the pressure and the temperature are supposed to be homogeneous in each chamber;
c) the process is polytropic and characterized by the coefficient *k*.

Also the electropneumatic system model is obtained by combining all the previous relations. The two servodistributors are supposed identical and can be decomposed into a dynamic and static part (fig. 2).

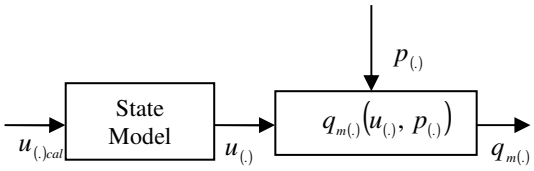

Fig.2: The dynamic and a static part of the servodistributor

In this paper, the results of Sesmat and Scavarda (1996) of the global experimental method giving the static characteristics of the flow stage have been used. The global characterization corresponds to the static measurement of the output mass flow rate $q_{m(.)}$, which depends on the input control $u_{(.)}$ (fig. 3) and the output pressure $p_{(.)}$, for constant source and exhaust pressure.

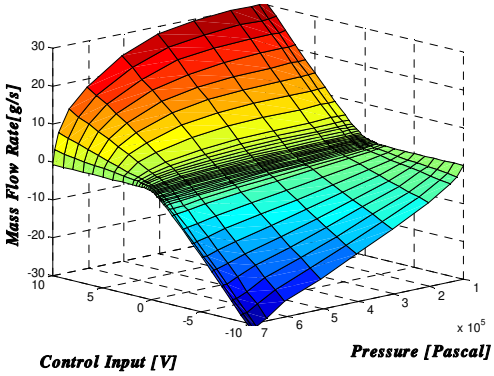

Fig. 3: The mass flow rate

The state model of the two servodistributors is given by:

$$\begin{cases} \dfrac{d\ddot{x}_P}{dt} = -a_{11}\dddot{x}_P - a_{12}\ddot{x}_P - a_{13}\dot{x}_P + k_1 u_{Pcal} \\ \dfrac{d\dot{x}_P}{dt} = \ddot{x}_P \\ \dfrac{dx_P}{dt} = \dot{x}_P \\ u_P = x_P \end{cases} \qquad \begin{cases} \dfrac{d\ddot{x}_N}{dt} = -a_{11}\dddot{x}_N - a_{12}\ddot{x}_N - a_{13}\dot{x}_N + k_1 u_{Pcal} \\ \dfrac{d\dot{x}_N}{dt} = \ddot{x}_N \\ \dfrac{dx_N}{dt} = \dot{x}_N \\ u_N = x_N \end{cases} \tag{1}$$

where $x_{(.)}$ is the slide valve position.

The mechanical equation includes pressure force, viscous friction, dry friction forces and an external constant force due to atmospheric pressure. The following equations give the physical model of the actuator:

$$\begin{cases} \dot{y} & = v \\ \dot{v} & = \dfrac{1}{M}\left[S_P p_P - S_N p_N - bv - F_f(v) - F_{ext} \right] \\ \dot{p}_P & = \dfrac{krT_P}{V_P(y)}\left[q_{m_P}(u_P, p_P) - \dfrac{S_P}{rT_P} p_P v \right] \\ T_P^k p_P^{k-1} & = \text{constant} \\ \dot{p}_N & = \dfrac{krT_N}{V_N(y)}\left[q_{m_N}(u_N, p_N) + \dfrac{S_N}{rT_N} p_N v \right] \\ T_N^k p_N^{k-1} & = \text{constant} \end{cases} \quad (2)$$

where: $\begin{cases} V_P(y) = V_P(0) + S_P y \\ V_N(y) = V_N(0) - S_N y \end{cases}$

with: $\begin{cases} V_p(0) = V_{DP} + S_P \dfrac{l}{2} \\ V_N(0) = V_{DN} + S_N \dfrac{l}{2} \end{cases}$

are the piping volumes of the chambers for the zero position and $V_{D(P\ or\ N)}$ are dead volumes present at each extremity of the cylinder.
The dry friction forces F_f, which act on the moving part in the presence of viscous friction, is a nonlinear model given by several relations, for example Tustin (1947):

$$F_f(v) = \left[F_C + (F_S - F_C)\exp(-c|v|) \right] sign(v) \quad (3)$$

where F_s, F_c and c are the stiction friction, the Coulomb friction and the Stribeck constant effect.

The function $sign(v)$ is defined as follows:

$$\begin{cases} if & v > 0 \ sign(v) = 1 \\ if & v = 0 \ -1 \le sign(v) \le 1 \\ if & v < 0 \ sign(v) = -1 \end{cases} \quad (4)$$

Figure 4 shows the results of the friction model for low velocities. Outside the small velocity region shown this figure, the dry friction is dominated by the constant Coulomb friction value.

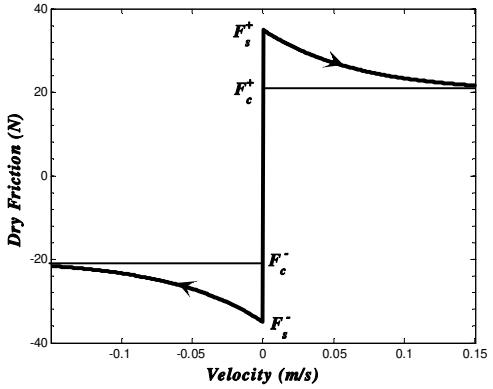

Fig. 4: Dry friction model

2.2 Control model

The actuator bandwith is about $10Hz$ and the servodistributor bandwith is about $200Hz$. Then, and because the local PI controller is used for a slide valve position, the servodistributors model can be reduced to two static relations defining the mass flow rates $q_{m^P}(u_P, p_P)$ and $q_{m^N}(u_N, p_N)$, where $u_P = u_{Pcal}$ and $u_N = u_{Ncal}$.

To establish a mathematical model of the power modulator flow stage, the standard ISO 6538 may be used, see for example Hildebrandt, Kharitonov, Sawdony, Göttert and Hartmann (2005). Another research work of Araki (1981) shows approximations based on physical laws by modeling the geometrical variations of the restriction areas of the servodistributor. Another way proposed by Richard and Scavarda (1996) is based on an experimental characterization model using a Wheatstone bridge representation of the servodistributor. Using the measures of the global experimental method giving the static characteristics of the flow stage, Belgharbi, Thomasset, Scavarda, and Sesmat (1999) has developed analytical models for both simulation and control purposes. For control purposes, the flow stage characteristics were approximated by the following model, affine in control, such that:

$$q_{m(.)} = \varphi(p_{(.)}) + \psi(p_{(.)}, \text{sgn}(u_{(.)}))\, u_{(.)} \quad (5)$$

Where $\varphi(p_{(.)})$ (fig. 5.a) in Eq.5 is a polynomial function of the pressure whose evolution corresponds to the mass flow rate leakage and does not depend of the input control. $\psi(p_{(.)}, \text{sgn}(u_{(.)}))$ is a polynomial function both of the pressure and the sign of the input control because the behavior of the mass flow rate characteristics is clearly different for the inlet $(u_{(.)} > 0)$ (fig. 5.b) and the exhaust $(u_{(.)} < 0)$ (fig. 5.c). The polynomial functions $\varphi(p_{(.)})$, $\psi(p_{(.)}, u_{(.)} > 0)$, $\psi(p_{(.)}, u_{(.)} < 0)$ have been chosen with five equal degrees multi linear regression with R^2 (multiple correlation coefficients) greater than *0.96*.

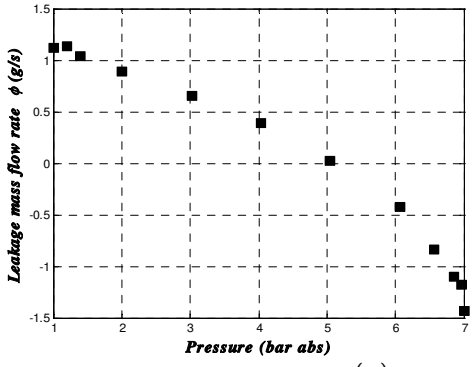

Fig. 5.a: The function $\varphi(p)$

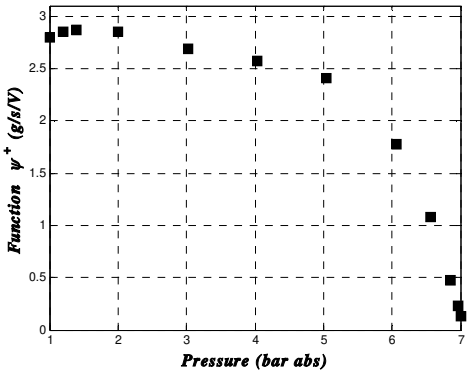

Fig. 5.b: The function $\psi(p, u>0)$

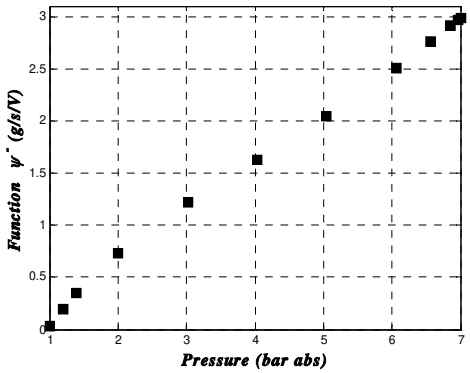

Fig. 5.c: The function $\psi(p, u<0)$

Using Eq.5 and Eq.2 with these two assumptions:

- F_s and F_c are not easily measurable and variable during experimental tests. Thus, only for the control model, the dry friction forces F_f (v) in Eq.3, have been neglected compared to other forces,

- the temperature variation is negligible so the temperature chambers are equal to the supply temperature: $T_P = T_N = T_s$, with the polytropic coefficient $k = 1.2$, see Shearer (1956).

The nonlinear affine model is then given by:

$$\dot{x} = f(x) + g(x)U \tag{6}$$

Where $x = (y, v, p_P, p_N)^T$ and D_φ is its physical domain:

$$D_\varphi = \begin{bmatrix} y_{\min} & y_{\max} \\ v_{\min} & v_{\max} \\ p_{p,\min} & p_{p,\max} \\ p_{n,\min} & p_{n,\max} \end{bmatrix} = \begin{bmatrix} -l/2 & l/2 \\ -v_{\max} & v_{\max} \\ P_E = 10^5 & P_S = 7.10^5 \\ P_E = 10^5 & P_S = 7.10^5 \end{bmatrix} \begin{pmatrix} m \\ m/s \\ Pascal \\ Pascal \end{pmatrix} \tag{7}$$

With

$$f(x) = \begin{pmatrix} v \\ \frac{1}{M}\left[S_P p_P - S_N p_N - bv - F_{ext}\right] \\ \frac{krT_s}{V_P(y)}\left[\varphi(p_P) - \frac{S_P}{rT_s} p_P v\right] \\ \frac{krT_s}{V_N(y)}\left[\varphi(p_N) + \frac{S_N}{rT_s} p_N v\right] \end{pmatrix} \tag{8}$$

$$g(x) = \begin{pmatrix} 0 & 0 \\ 0 & 0 \\ \frac{krT_s}{V_P(y)}\psi(p_P, \mathrm{sgn}(u_P)) & 0 \\ 0 & \frac{krT_s}{V_N(y)}\psi(p_N, \mathrm{sgn}(u_N)) \end{pmatrix} \tag{9}$$

$$U = (u_P, u_N)^T \tag{10}$$

In the next section a solution for the "stick-slip" problem of electropneumatic systems will be proposed.

3 A solution for the "stick-slip" phenomenon of electropneumatic systems

The problem of "stick-slip" was encountered with many other positions tracking control laws already applied to this electropneumatic system. Let us note for example, the backstepping control by Smaoui, Brun and Thomasset (2006a) and sliding mode control by Bouri and Thomasset (2001), Laghrouche, Smaoui, Plestan, and Brun (2006) and Smaoui, Brun and Thomasset (2008).

3.1 Existence Condition of the "stick-slip" phenomenon

When the partial equilibrium is attained ($t=t_{stop}$ in figure 6), the condition (11) is satisfied, but the two pressures continue to evolve:

$$\dot{v} = v = 0 \Rightarrow F_f(0) = S_P p_P - S_N p_N - F_{ext} \tag{11}$$

However, according to Eq. 3:

$$F_f(0) = \left[F_C + (F_S - F_C)\exp(c \times 0)\right] sign(0) \tag{12}$$

With the definition of sign function in Eq.4, the "stick-slip" phenomenon is avoided (fig. 6) when this condition is satisfied:

$$F_S^- \leq F_f(0) \leq F_S^+ \tag{13}$$
$$F_S^- + F_{ext} \leq S_P p_P - S_N p_N \leq F_S^+ + F_{ext}$$

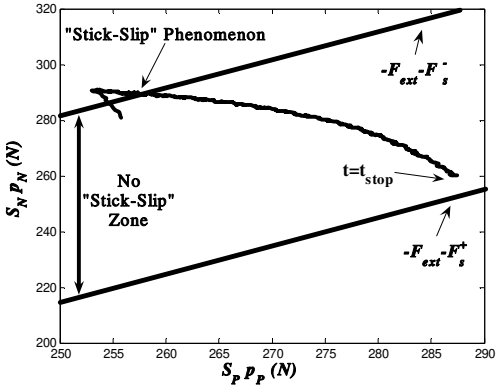

Fig. 6.a: "Stick-Slip" Phenomenon

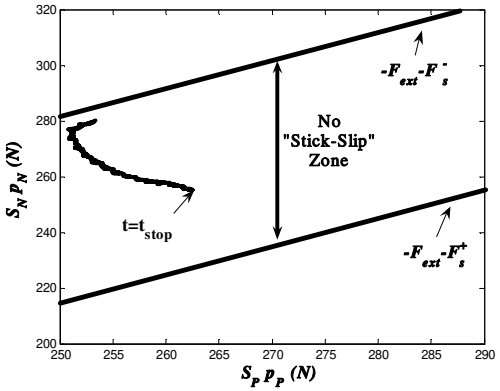

Fig. 6.b: No "Stick-Slip" Phenomenon

3.2 Switching between position control and pressure regulation

The system is controlled in position during the follow-up of trajectory and, if this trajectory contains a static phase, the closed-loop system switches to pressures regulation during this phase, according to the algorithm describes in next paragraph. Figure 7 illustrates the commutation between the control laws.

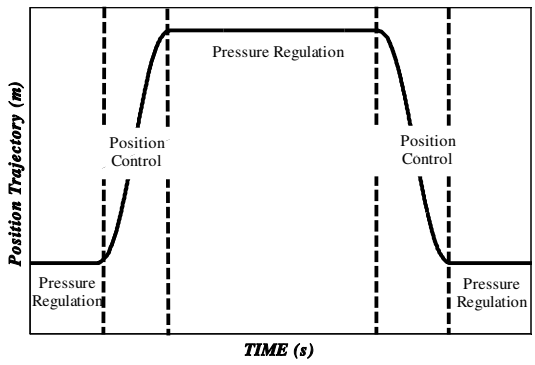

Fig. 7: Commutation between the control laws

The criterion of commutation chosen between these two control laws rests on error position and velocity variation. In fact the commutation of position control to pressure control is when all these conditions are satisfied:

1. $v_d = 0$: the desired velocity is null
2. $\left|y - y_{stop}\right| \le \varepsilon_1$: the position error during the static phase, lower than a value fixed in advance ε_1 .
3. $\left|v\right| \le \varepsilon_2$: the velocity is very small. This last condition is necessary if the variation in the velocity desired trajectory is very important.

Initially the reference inputs of the regulation pressures (p_P^d and p_N^d) are the pressures values in the chamber when the system is at rest. Then, at any commutation, the reference inputs of the regulation pressures (p_P^d and p_N^d) are the pressure values in the chambers (p_P^{stop} and p_N^{stop}) which are maintained constant with these values. Figure 8 shows the time of calculation of the desired pressures and the selected values of its levels.

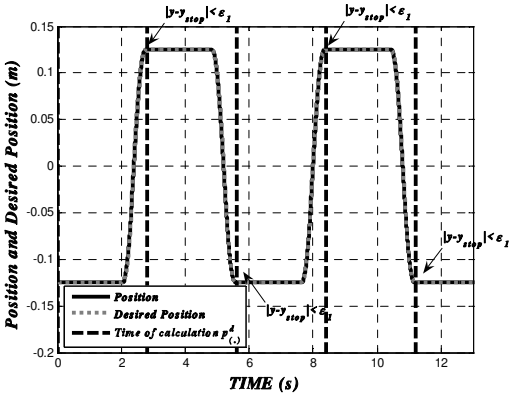

Fig. 8.a : Position & Desired Position (m)

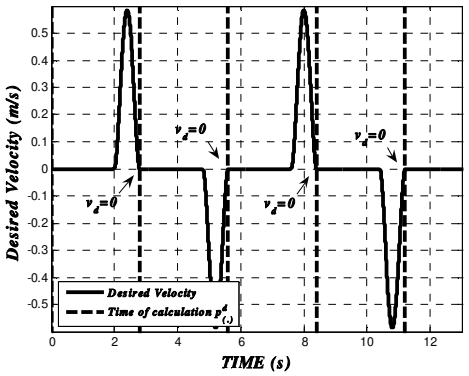

Fig. 8.b : Desired Velocity (m/s)

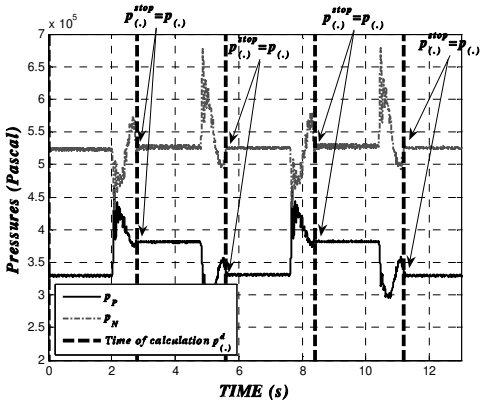

Fig. 8.c : Pressures (Pascal)

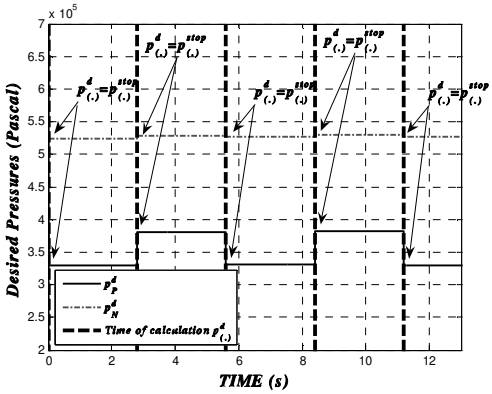

Fig. 8.d : Desired Pressures (Pascal)

For position tracking non linear control law is proposed and for the pressure control, the non linear input/output linearisation method is applied.

3.3 Position control

For the synthesis of the non linear tracking position control law, a diffeomorphism $\left[y\ L_f y\ L_f^2 y\ p_p\right]^T$ is applied and leads to a control model of the form:

$$\begin{cases} \dot{y} &= v \\ \dot{v} &= a \\ \dot{a} &= L_f^3 y + L_g L_f^2 y.u \\ \dot{p}_P &= \dfrac{krT_s}{V_P(y)}\left[\varphi(p_P) - \dfrac{S_P}{rT_s}\, p_P v\right] + \dfrac{krT_s}{V_P(y)}\psi(p_P, \mathrm{sgn}(u))u \end{cases} \tag{14}$$

where :

$$u = u_P = -u_N \tag{15}$$

and

$$L_f^3 y(y,v,a,p_P,p_N) = \frac{S_p k rT_s}{MV_p(y)}\left[\varphi(p_P) - \frac{S_p}{rT_s}\, p_p v\right] - \frac{S_n k rT_s}{MV_n(y)}\left[\varphi(p_n) + \frac{S_n}{rT_s}\, p_n v\right] - \frac{b}{M} a \tag{16.a}$$

$$L_g L_f^2 y(y,p_P,p_N) = \frac{k\,rT_s}{M}\frac{S_p \psi(p_p,\ sign\ (u))}{V_p(y)} + \frac{k\,rT_s}{M}\frac{S_n \psi(p_n,\ sign\ (-u))}{V_n(y)} \tag{16.b}$$

As shown in figure (5.b and 5.c) $\psi_{(.)} > 0$ and $L_g L_f^2 y(y,p_P,p_N) \neq 0$ over the physical domain.

This system in Eq.14 is partially feedback linearizable. It has been shown in Brun, Belgharbi, Sesmat, Thomasset and Scavarda (1999) that the system is minimum phase.

Now create three separate dynamic errors as follow:

$$\begin{cases} e_y = y - y_d \\ e_v = v - v_d \\ e_a = a - a_d \end{cases} \tag{17}$$

And then a new state system:
The choice of input:

$$u = \frac{1}{L_g L_f^2 y}\left[-L_f^3 y + \dot{a}_d - K_a e_a - K_v e_v - K_y e_y\right] \tag{19}$$

leads to a linear closed loop system

$$\begin{bmatrix} \dot{e}_y \\ \dot{e}_v \\ \dot{e}_a \end{bmatrix} = \begin{bmatrix} 0 & 1 & 0 \\ 0 & 0 & 1 \\ -K_y & -K_v & -K_a \end{bmatrix}\begin{bmatrix} e_y \\ e_v \\ e_a \end{bmatrix} \tag{20}$$

where the equilibrium point $\left[e_y = 0\ e_v = 0\ e_a = 0\right]^T$ is exponentially stable $\forall K_y, K_v$ and K_a and ensuring the Hurwitz polynomial $s + K_a s^2 + K_v s + K_y = 0$,see Isidori (1989).

3.4 Pressure control

For the pressure control, the classical non linear multi-input/multi-output linearisation method is used. In static phase, when the partial equilibrium is obtained, this system must be considered:

$$\begin{cases} y &= y_{stop} + \Delta y & |\Delta y| \le \varepsilon_1 \\ v &= \Delta v & |\Delta v| \le \varepsilon_2 \\ \dot{p}_P &= f_P(y,v,p_P) + g_P(y,p_P)\,u_P \\ \dot{p}_N &= f_N(y,v,p_N) + g_N(y,p_N)\,u_N \\ z_P &= \left[p_P\ p_N\right]^T \end{cases} \tag{21}$$

Where ε_1 and ε_2 are small and positive and :

$$\begin{aligned} f_P(y,v,p_P) &= \frac{krT_s}{V_P(y)}\left[\varphi(p_P)-\frac{S_P}{rT_s}p_P v\right] \\ g_P(y,p_P) &= \frac{krT_s}{V_P(y)}\left[\psi(p_p,\mathrm{sgn}(u_P))\right] \\ f_N(y,v,p_N) &= \frac{krT_s}{V_N(y)}\left[\varphi(p_N)+\frac{S_N}{rT_s}p_N v\right] \\ g_N(y,p_N) &= \frac{krT_s}{V_N(y)}\left[\psi(p_N,\mathrm{sgn}(u_N))\right] \end{aligned} \quad (22)$$

The outputs of the system are the two pressures.

Now create 2 separate errors between the pressure and the constant desired pressure:

$$\begin{cases} e_P = p_P - p_P^d \\ e_N = p_N - p_N^d \end{cases} \quad (23)$$

Differentiating each error Eq.23 once gives:

$$\begin{cases} \dot{e}_P = \dot{p}_P = f_P(y,v,p_P)+g_P(y,p_P)u_P \\ \dot{e}_N = \dot{p}_N = f_N(y,v,p_N)+g_N(y,p_N)u_N \end{cases} \quad (24)$$

Define the control inputs of system as:

$$\begin{cases} u_P = \dfrac{1}{g_P(y,p_P)}\left(-f_P(y,v,p_P)-k_P e_P\right) \\ u_N = \dfrac{1}{g_N(y,p_N)}\left(-f_N(y,v,p_N)-k_N e_N\right) \end{cases} \quad (25)$$

And combining Eq.25 into Eq.24:

$$\begin{cases} \dot{e}_P = -k_P e_P \\ \dot{e}_N = -k_N e_N \end{cases} \quad (26)$$

Therefore, since k_p and $k_N > 0$, e_P and e_N converge exponentially to zero.

4 Experimental Results

Before the application on the real electropneumatic system, the method developed above was implemented in co-simulation. The co-simulation consists of using jointly the software developed by the modelling researchers, and the software dedicated for the system control. Thus, the physical model of electropneumatic system, defined in section 2.1, was treated by AMESim (LMS Imagine) and the control laws (Eq.19 and Eq.25), with the criteria of switching and the calculation of the desired pressure, were developed using Simulink Mathworks. In fact the co-simulation enables the parameters of the commutation criterion and the gains of the two control laws to be tested. Satisfactory simulation results are obtained.

Then the control law is implemented using a Dspace 1104 controller board with the dedicated digital signal processor. The controller requires measurements of position, velocity, acceleration and the two pressures. The measured signals, all analog, were run through the signal conditioning unit before being read by the 16 bit analog/digital converter. Two pressure sensors are used, their precision is equal to *700 Pa* (*0.1%* of the extended measurement) and their combined non linearity and hysteresis is equal to *0.1%* of the extended measurement. The cylinder velocity is determined by analogue differentiation and low-pass filtering of the output of the position given by an analogue potentiometer (Its precision and repeatability is equal to *10 μm* and its linearity is *0.05%* of the extended measurement.). The acceleration information is obtained by a robust velocity differentiator, via a high order sliding mode; see Smaoui, Brun and Thomasset (2008).

4.1 An Example of the "stick-slip" phenomenon

For the first part of these experimental results an example of the "stick slip" phenomenon is explained. This is shown on a position tracking system with only one control law (i.e. without commutation between position tracking and pressures regulation).

Figure 9 shows the "stick-slip" phenomenon with the position, the desired position, the position error, the pressure in the chambers P and N, the control input and the "stick-slip" phenomenon. For this position tracking the gains are fixed to $K_y = 96000$, $K_v = 6800$, $K_a = 150$. For a total displacement equal to *250 mm*, the maximum dynamic position tracking error is about *1.5 mm*. In, a steady state, the average position error is about *0.13 mm*. The pressures continue to evolve, during the steady state of the position. The "stick-slip' phenomenon is seen at $t = 31\ s$, $t = 33{,}4\ s$ and $t = 34{,}2\ s$.

On the same experimental set-up and in the same conditions, has been implemented two other non linear control laws:

- a backstepping control in Smaoui, Brun and Thomasset (2006 b) the error in steady sate is about $0.10\ mm$.

- an high order sliding mode controller in Smaoui, Brun and Thomasset (2006 b) the error in steady sate is about $0.11\ mm$.

With these two control laws, the "stick slip" problem also appears. Thus the tracking performances obtained by the control proposed are similar in regard of precedents one.

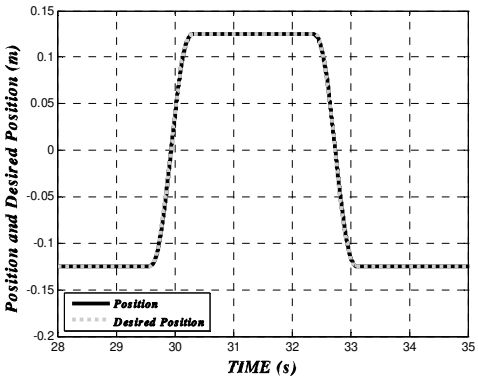

Fig. 9.a :Position & Desired Position (m)

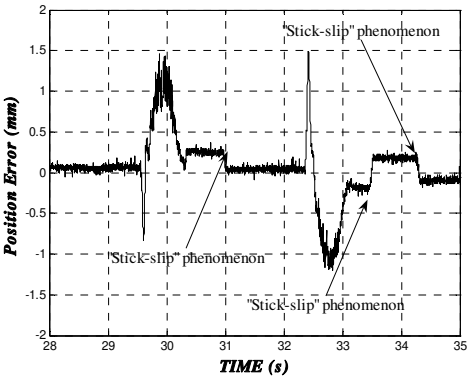

Fig. 9.b : Position Error (mm)

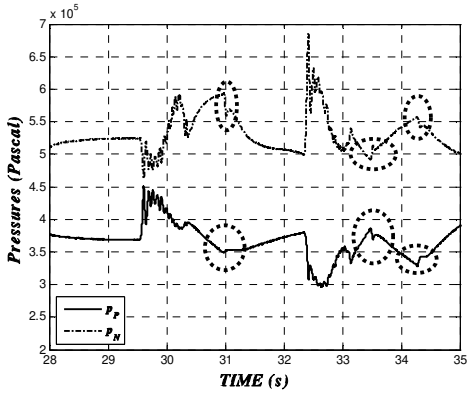

Fig. 9.c : Pressures (Pascal)

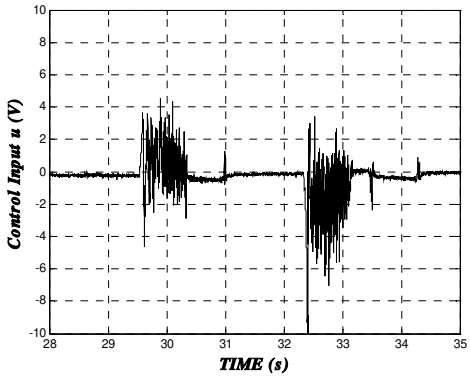

Fig. 9.d : Control input (V)

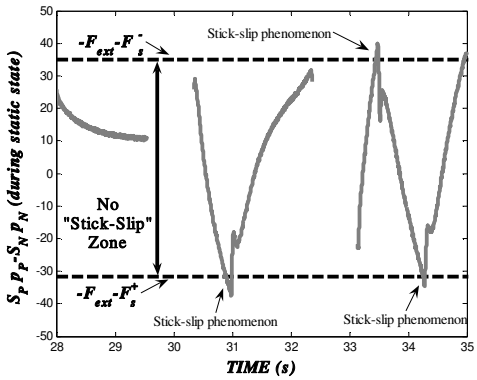

Fig. 9.e : "Stick-slip" phenomenon

4.2 An example of a no "stick-slip" phenomenon

In the second part of this section, the experimental results are presented when the system is controlled by the two control laws developed in section 3.2 and 3.3 with the commutation criteria proposed in section 3.1, position control during the dynamic phase and pressure regulation during the static phase. Thus fig. 10 proves that the solution proposed avoids the "stick-slip" phenomenon.

For the position control the gains tuned are the same that in last section. For the pressure control the gains are fixed to $k_p = k_N = 300$. These values ensure good static and dynamic performances. Some experimental results are provided here to demonstrate the validity of the solution suggested to the problem of "stick-slip".

Figure 10 shows the position, the desired position same that it's shown in fig. 9.a, the position error, the pressure in the chamber P, the pressure in the chamber N, the control inputs u_P and u_N and no "stick-slip" phenomenon. The maximum dynamic position tracking error is about *1.65 mm* . In steady state, the average position error is about *0.18 mm.*

The presence of thresholds on the criteria of commutation degrade a little the performances compared to the preceding case but the pressures are stabilized during this static phase of the position and the phenomenon of "stick-slip" is avoided.

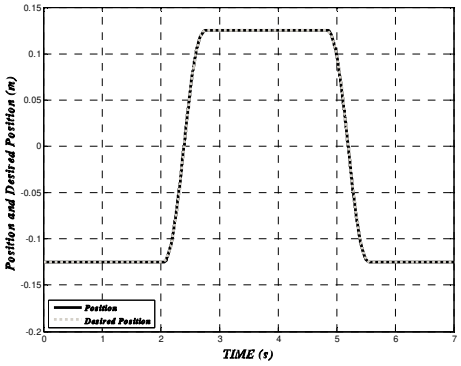

Fig. 10.a :Position & Desired Position (m)

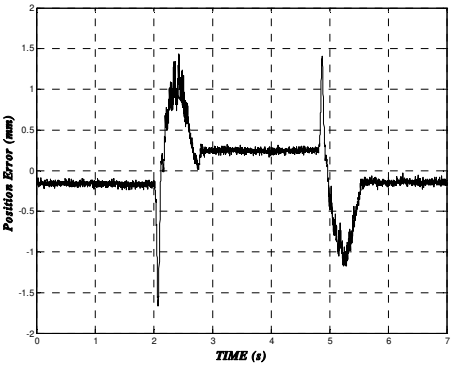

Fig. 10.b : Position Error (mm)

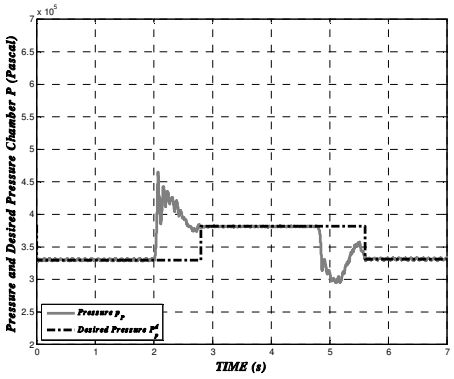

Fig. 10.c : Pressure and desired pressure chamber P (Pascal)

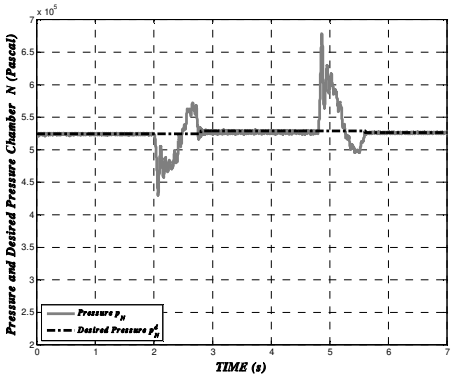

Fig. 10.d : Pressure and desired pressure chamber N (Pascal)

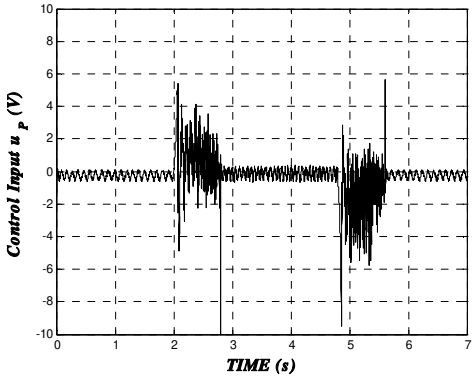

Fig. 12.e : Control input u_P (V)

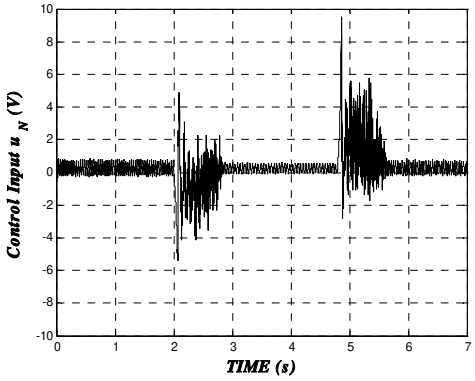

Fig. 12.f : Control input u_N (V)

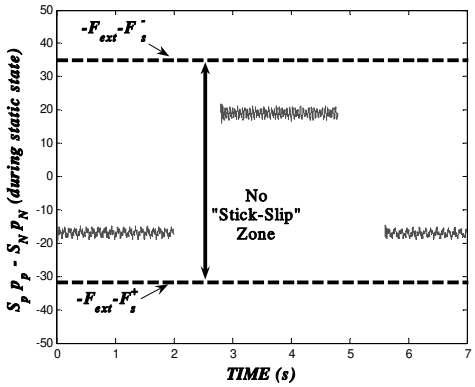

Fig. 10.g : No “stick-slip” phenomenon

5 Conclusion

The contribution of this paper consists of the solution to the “stick-slip” phenomenon for an electropneumatic system with a given desired position trajectory. The system is controlled by two sets of control laws, a non linear control law for the dynamic state of the position then, when the system is in partial equilibrium, the algorithm switches to the pressure regulations obtained with the classical non linear input/output linearization method.

The perspectives are to avoid the “stick-slip” phenomenon, without degrading the performances of tracking position trajectory.

Nomenclature

b	viscous friction coefficient (N/m/s)
k	polytropic constant
M	total load mass (kg)
p	pressure in the cylinder chamber (Pascal)
q_m	mass flow rate provided from servodistributor to cylinder chamber (kg/s)
r	perfect gas constant related to unit mass (J/kg/K)
S	area of the piston cylinder (m^2)
T_s	temperature (K)
V	volume (m^3)
y	position (m)
v	velocity (m/s)
a	acceleration(m/s^2)
$\varphi(.)$	polynomial leakage function (kg/s)
$\psi(.)$	polynomial function (kg/s/V)
l	length of stroke (m)
F_{ext}	External force (N)
F_f	dry friction force (N)
F_c	Coulomb friction (N)
F_s	Stiction friction (N)
c	Stribeck effect constant
x	slide valve position
$u, u_{(.)}$	control input

Subscript and superscript

D	dead volume
N	chamber N
P	chamber P
d	Desired
max	maximum

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