



Synthesis of Polyacrylic/Silica Nanocomposite Latexes using Static Mixer

Gholamali Farzi, Elodie Bourgeat-Lami, Timothy Mckenna

► To cite this version:

Gholamali Farzi, Elodie Bourgeat-Lami, Timothy Mckenna. Synthesis of Polyacrylic/Silica Nanocomposite Latexes using Static Mixer. *Macromolecular Symposia*, 2010, 289, pp.129-134. <10.1002/masy.200900015>. <hal-00723802>

HAL Id: hal-00723802

<https://hal.science/hal-00723802v1>

Submitted on 8 Oct 2021

HAL is a multi-disciplinary open access archive for the deposit and dissemination of scientific research documents, whether they are published or not. The documents may come from teaching and research institutions in France or abroad, or from public or private research centers.

L'archive ouverte pluridisciplinaire **HAL**, est destinée au dépôt et à la diffusion de documents scientifiques de niveau recherche, publiés ou non, émanant des établissements d'enseignement et de recherche français ou étrangers, des laboratoires publics ou privés.



HAL Authorization

Synthesis of polyacrylic/silica nanocomposite latexes using static mixer

*G.A.Farzi¹, E. Bourgeat-Lami, T.F.L. McKenna², **

CCPP/CPE UMR 5265, 43 Bd du 11 Nov. 1918, BP 2077, 69616 Villeurbanne Cedex, France, e-mail: *tim.mckenna@chee.queensu.ca

Summary. Static mixers (Sulzer Chemtech; SMX) were used to prepare silica/ MMA-co-BA miniemulsions that were polymerized to produce nanocomposite latexes. Acceptable conditions for the formulation of polymerizable nanodroplets were found. and subsequently used to produce silica/poly(MMA-co-BA) nanocomposites by introducing silica-loaded monomers and preparation of silica-loaded miniemulsions. The droplet size distribution of the resulting miniemulsions was narrow enough that it could be successfully polymerized. It was found that the droplet size depends on the silica content and increases with increasing the silica concentration. It was also shown that there is a relationship between the droplet size and the viscosity of the dispersed phase. The majority of droplets were nucleated upon polymerization when less than 15% silica was used. However, when the silica content exceeded 15%, the ratio of the number of particles in the final latex to the number of droplets (N_p/N_d) increased to value much higher than 1 indicating the occurrence of homogeneous nucleation.

Keywords: silica, nanocomposite, miniemulsion, static mixer, droplet size, particle size.

Introduction

Emulsion polymerization is widely used as a means of making a numerous commercially important products, but does not always offer the necessary flexibility in terms of particle generation needed to produce a range of composite materials. Beginning in the 1970's, researchers began to understand that if the monomer droplets were small enough, they could also capture free radicals and thus polymerize.¹ This was the beginning of miniemulsion polymerization, which has now evolved as an alternative to conventional emulsion polymerization. The ingredients of a miniemulsion system are similar to a conventional system, with the addition of a hydrophobic agent. The main difference between conventional and

¹ Current address: Department of polymer engineering, Amirkabir University of Technology, Tehran, Iran

² Current address: Department of Chemical Engineering, Queen's University, Kingston, ON, Canada

mini-emulsion polymerization is the mechanism of particle creation.³⁻⁵ In commercial emulsion polymerization processes, micellar nucleation is the main method of particle formation. In contrast to a conventional system, monomer droplets are much smaller (50-500nm), and are created by some type of intensive mixing process. If they are small enough, and if there are no micelles present in the reactor they will be the main locus of polymerization. In an ideal mini-emulsion, we will obtain one polymer particle per initial droplet (i.e. $N_p/N_d = 1$). These droplets are stabilized by a two component system: the surfactant (similar to those used for conventional emulsion polymerization) and the hydrophobe.² The surfactant provides the steric and/or electrostatic stabilization, and the hydrophobic agent retards Ostwald ripening; that is to say the degradation of smaller droplets at the expense of larger droplets.

In mini-emulsion polymerization, the droplets (which need to be small enough to capture free radicals at a significant rate) behave as individual reactors, and since they are formed by mechanical agitation this offers certain advantages over conventional emulsion processes in that oil soluble compounds can be directly integrated into the polymer particle “ab initio” to make hybrid or composite materials (or even be used as initiators to limit water-phase reactions).

As we mentioned above, mini-emulsification necessarily involves an intensive mechanical agitation step. Ultrasound (US) is traditionally used on the lab scale, but its use is limited for industrial application. For this reason, the use of more industrially efficient homogenizers such as static mixers (SMs), high pressure homogenizers or rotor-stator (RS) mixers is desirable. There are many reports concerning the use of SM for mixing two immiscible fluids, but its use for a mini-emulsification process has not been well investigated and understood.

Ouzineb *et al.*^{6, 7} and Farzi *et al.*⁸ studied the use of SM's for the mini-emulsification of single monomer systems like styrene (ST), butyl methacrylate (BMA) and methylmethacrylate (MMA). They showed that it is possible to make stable mini-emulsion droplets by SM. In the latter study, we showed that it is possible to homogenize MMA with an SM assembly and to polymerize the resulting nanodroplets. It was also found that higher flow rates and well-defined mixer geometries are needed to emulsify mixtures of MMA and BA. In the current work we will build on these results, first to identify acceptable conditions for the mini-emulsification of a 50/50 wt% mixture of MMA/BA. Subsequently a silica-loaded monomer was emulsified to create nanodroplets containing silica nanoparticles. These droplets were consequently polymerized using mini-emulsion polymerization technique.

Experimental Details

Materials

The aqueous silica suspension used in this study was graciously supplied by Clariant (France). The main characteristics of this suspension, referred to as GEN33 are shown in Table 1. The specific surface area of silica particles was determined from nitrogen adsorption isotherms using the Brunauer, Emmett, Teller (BET) method. The diameter of the silica particles and polydispersity index (PI) were determined by DLS using a Malvern Autosizer.

Table 1 Characterization of supplied silica particles in water

	GEN 33
Specific surface area (S_{spec} , m ² /g)	50.5
Particle diameter (DSiO ₂ , nm)	78
Polydispersity index (PI)	0.020
Solid content (SC, %)	27
Suspension pH	9.57

γ -methacryloxy propyl trimethoxysilane (γ -MPS, Acros organics) was used as coupling agent through this work.

Absolute ethyl alcohol (99.8%) and methyl alcohol (99.9%) were obtained from Carlo Erba, and used as received. MMA and BA and Sodium dodecyl sulphate (SDS) were obtained from Acros and used as received.

Miniemulsification procedure

As mentioned before, it was shown in our previous work⁸ that it is possible to create stable miniemulsion of one single monomer like MMA using a set-up of 8 mm diameter SMX static mixer shown schematically in Figure 1. The SM set-up consisted of 7 elements of 0.7 cm (these were 8mm elements machined down to 7 mm in order to fit in the tube) placed in a polytetrafluoroethylene (PTFE) housing. This housing was attached to a longer nylon tube with the same diameter, through which the liquid phase was recycled during homogenization. A pump with a theoretical pressure loss of 8.7 bar and maximum flowrate of 133 ml/s of emulsion was used to recirculate the fluid.

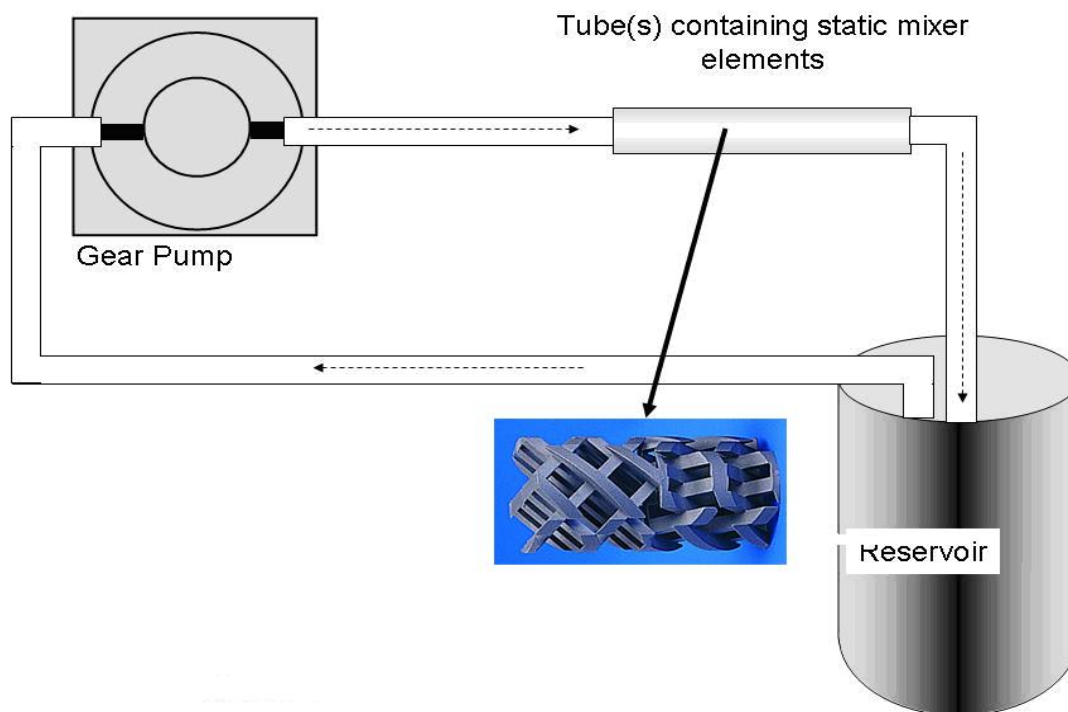


Figure 1. Static mixer homogenisation set-up.

Results and discussions

Formation of mixed monomer droplets

The objective of this initial section is to find acceptable conditions for the formation of nanodroplets and polymerization of a 50/50 MMA/BA mixture. For this purpose, the droplets need to be small enough so that they may successfully compete for free radicals and monomodal enough that they can be polymerized successfully.^{1,9} The mixed monomer system (MMA/BA 50/50 wt %) was homogenized using the SMX mixing elements according to the recipe given in Table 2. The flow rate of the pump was varied from 114 ml/s to 133 ml/s and breakage of droplets was studied. Figure 2 shows the evolution of droplet diameter of miniemulsions as a function of recycle time for increasing flow rates. It can be seen from this figure that regardless of the flow rates, the droplet diameter decreases with increasing homogenization time and then reaches a plateau. As expected, Figure 2 also shows that smaller droplets are obtained at higher flow rates.

Table 2 Miniemulsion recipe

Water	Monomer	Hydrophobic agent	Surfactant	Initiator
69.35 g	28.1 g	2g (ODA)	0.17g TA, 0.26g TN	0.12g APS

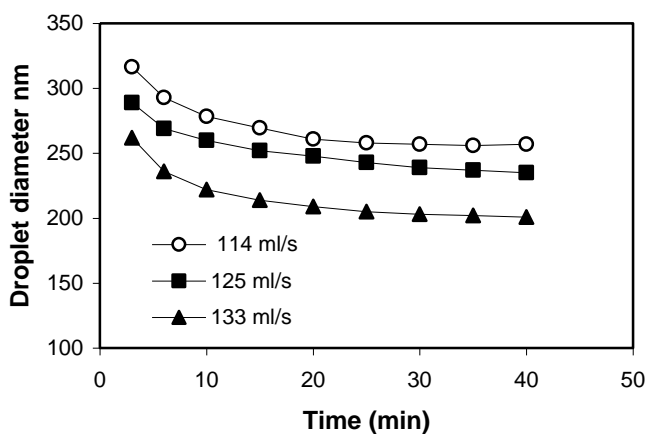


Figure 2. Evolution of droplet diameter as a function of recycle time.

The polydispersity indices (value reported by Malvern Software. A value of less than 0.1 is considered to be monodisperse) of miniemulsions thus created is shown in Figure 3. As can be seen, the polydispersity index of the miniemulsion created at higher flow rate is the smallest.

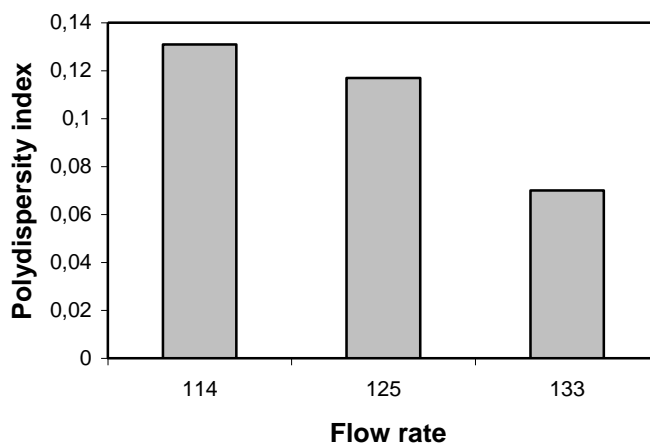


Figure 3. Polydispersity of miniemulsions after 30 minutes homogenization.

These dispersions were polymerized according to the recipe in Table 3 via a batch process in a cylindrical glass reactor (150 ml) with a nitrogen inlet. Droplet diameters of miniemulsions after 30 minutes of homogenization, conversion of polymerization reaction after

120 minutes, particle size and polydispersity index of latexes and also N_p/N_d are given in Table 4 for different flow rates.

Table 3. Effect of flow rate on characteristics of samples

Flow rate	D_d	Conversion	D_p	PI	N_p/N_d
114	257	0.95	181	0.082	2.39
125	235	0.97	183	0.076	1.76
133	201	0.96	189	0.056	1.11

The highest flow rate gave the narrowest DSD, which in turn could be polymerized to yield a narrow PSD with N_p/N_d closest to unity, indicating efficient nucleation of the nanodroplets.¹⁰ The best condition that we obtained corresponds to the flow rate of 133 ml/s. Therefore, this condition was used in the following experiments.

Droplet formation of silica loaded monomer

Miniemulsions with different silica contents were prepared from a master batch of a relatively high concentrated dispersion of silica in monomer (35 wt % silica relative to MMA/BA 50/50 by weight), which were diluted to the desired concentration of silica by adding monomer(s) prior to homogenization.

Stable miniemulsions were created by homogenization of silica-containing monomers in aqueous solution of surfactants using the set-up in Figure 1 and the recipes given in Table 2, using different amounts of silica varying from 0 to 20% w/w relative to total monomer. Droplet size is illustrated in Figure 4 as a function of homogenization time for different silica contents. As can be seen, droplet size decreases as a function of homogenization time as in the case of the unloaded dispersions shown in Figure 2. The results also show that droplet size increased with increasing silica content. At 20 wt % silica content droplet size is very close to that of 15 wt % silica content. This could be due to the fact that when silica content reaches to 15% the viscosity of dispersed phase is relatively high and the energy dissipated by SM might not be enough to break up the droplets as much as samples other samples with lower silica content. General forms of these curves are similar to those obtained for silica-free system; however the presence of silica particles slightly changes the behaviour of system. It worth mentioning that this phenomenon has

reported in literature both for silica particles¹¹ and titanium dioxide.¹²⁻¹⁴ The increasing monomer droplet size containing titanium dioxide has been contributed to the lower adsorption of surfactant on the droplets in the presence of hydrophobic titanium dioxide particles.¹³ We did not found any publications that discussing this topic in depth for silica particles.

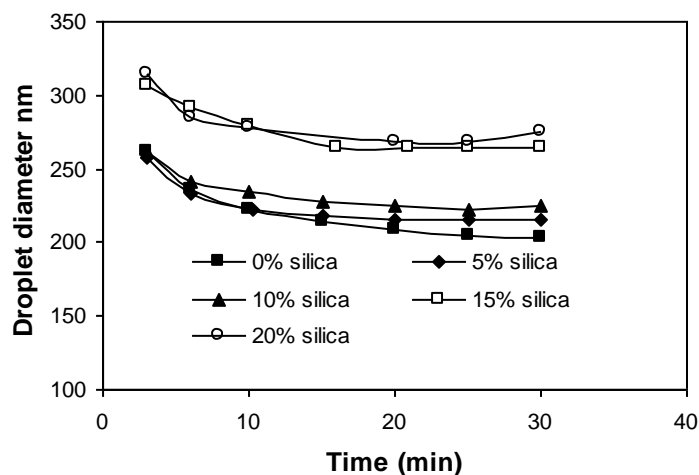


Figure 4. Evolution of droplet diameter versus homogenization time.

The evolution of the polydispersity index for miniemulsions as a function of silica content is plotted in Figure 5. As can be seen here it increases as the silica content is increased. This could be due to the distribution of silica particles in the droplets. Silica particles form a circular configuration at the interface of monomer/water and create some large droplets. This may increase the variance of droplet size in miniemulsion.

Effect of the silica particles on polymerization

The conversion of reaction for silica contents varying from 0 to 20 % versus time is shown in Figure 6. There does not appear to be a not clear dependency of conversion on silica content.

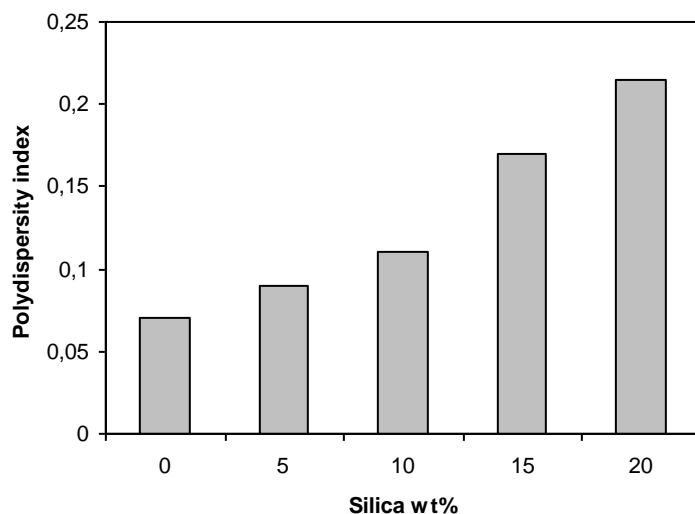


Figure 5. Evolution of polydispersity index as a function of silica content.

Figure 7 shows the evolution of particle diameter as a function of polymerization time. As can be seen from this figure, particle size decreases at the beginning of the polymerization and then slightly increases and reaches to a plateau. As stated previously this could be attributed to the homogeneous nucleation¹⁵ at the beginning of reaction and the coagulation of newly created particles (There might not be enough surfactant in the system). When the silica content reaches 15 wt % the final average particle size is smaller than in cases with less than 15 wt% silica content. This suggests that a significant number of new particles created by secondary nucleation appear to be stabilized. Because the droplets are larger when silica content reaches to 15 wt%, there is more free surfactant in aqueous phase. Creation of new particles during polymerization can be clearly seen from Figure 8 where we see the PI of miniemulsions as a function of time for different silica content. As can be seen, the PI decreases during polymerization and at the end of polymerization it is slightly higher than 0.1 for silica content higher than 10% and lower than this value for silica content less than 10%.

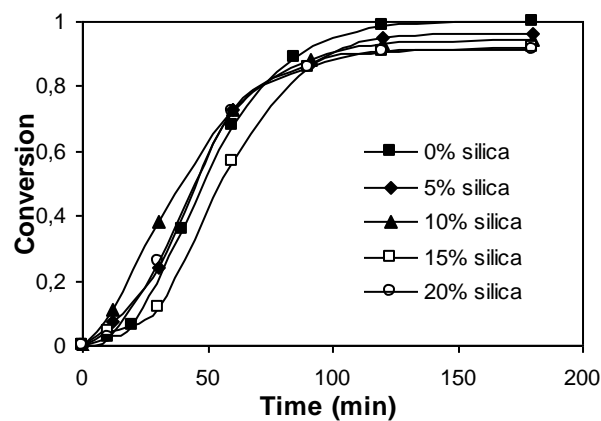


Figure 6. Conversion of polymerization for miniemulsion with different silica content

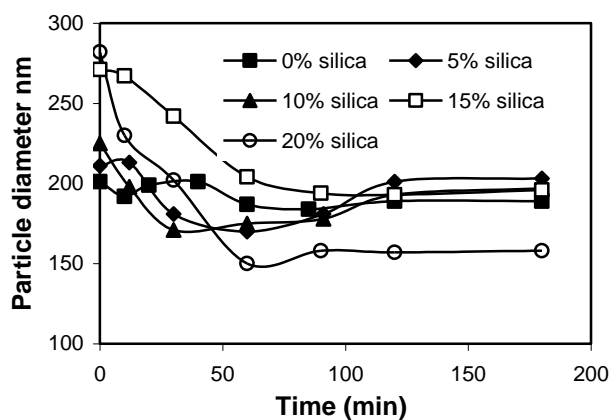


Figure 7. Evolution of particle diameter during polymerization

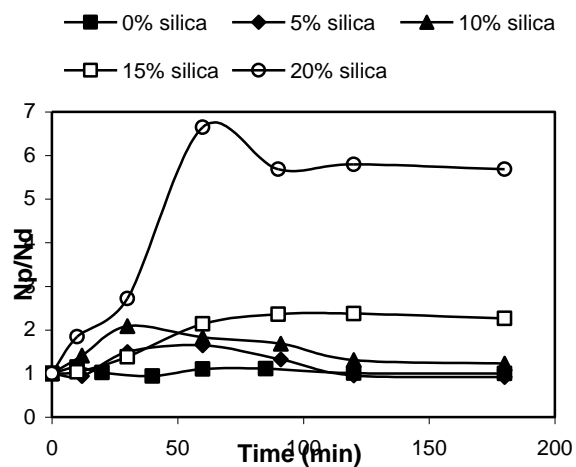


Figure 8. Monitoring of Np/Nd during polymerization

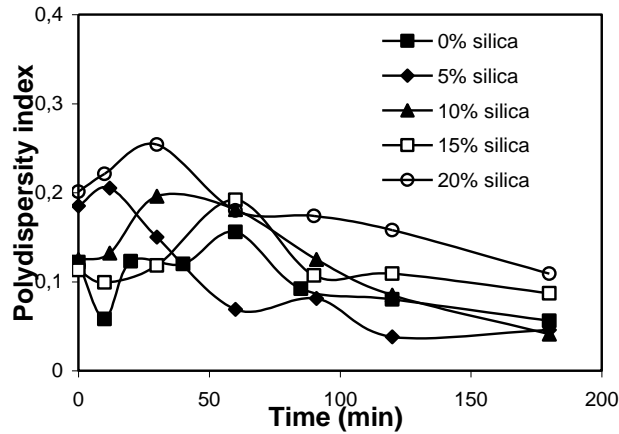


Figure 9. Variation of polydispersity during the polymerization

The variation of N_p/N_d as function of PI is shown in Figure 10. It should be noted that when PI is close to 0.1 and the DSD of a miniemulsion is relatively narrow, N_p/N_d remains closer to unity during and at the end of polymerization. This suggests that PI has an important effect on the nucleation step and a good droplet nucleation can be occurred if droplet size is small enough and DSD is narrow enough.

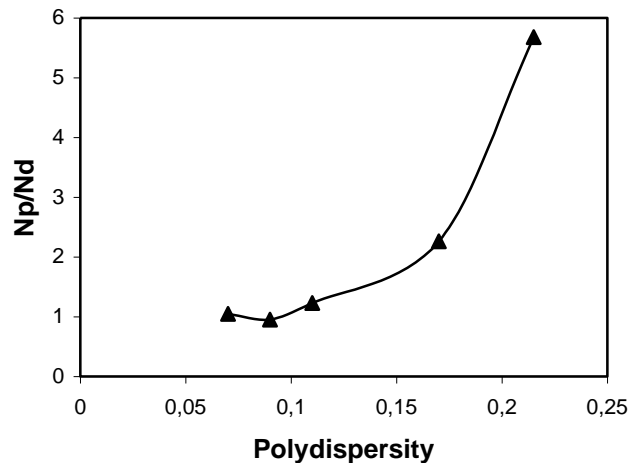


Figure 10. Effect of the polydispersity of miniemulsion on N_p/N_d

Conclusion

A Sulzer SMX mixer set-up was successfully used as homogenization device for the miniemulsification of a mixture of monomers (MMA/BA 50/50 wt%). Then the same homogenization system was used to disperse silica-loaded monomer. The resulting

miniemulsions had narrow enough DSD to be successfully polymerized to prepare silica/polyacrylate composite nanoparticles. It was found that the droplet size depends on the silica content and increases with increasing the silica concentration. It was also shown that there is a relationship between the droplet size and the viscosity of the dispersed phase. The majority of droplets were nucleated upon polymerization when less than 15% silica was used. However, when the silica content exceeded 15%, N_p/N_d increased to value much higher than 1 indicating the occurrence of homogeneous nucleation.

References

1. Ugelstad; El-Aasser, M. S.; Vanderhoff, J. W. *Journal of Polymer Science* 1973, 11, (8), 503-513.
2. Schork, F. J.; Luo, Y.; Smulders, W.; Russum, J. P.; Butte, A.; Fontenot, K. *Advances in Polymer Science* 2005, 175, (Polymer Particles), 129-255.
3. Landfester, K. *Macromol. Rapid. Commun.* 2001, 22, P896-936.
4. Antonietti, M.; Landfester, K. *Progress in Polymer Science* 2002, 27, (4), 689-757.
5. Asua, J. M. *Progress in Polymer Science* 2002, 27, (7), 1283-1346.
6. Ouzineb, K. Emulsion and miniemulsion polymerization: Stabilization, Turbular reactor and paractical application. Université de Lyon1, Lyon, 2003.
7. Ouzineb, K.; Lord, C.; Lesauze, N.; Graillat, C.; Tanguy, P. A.; McKenna, T. *Chemical Engineering Science* 2006, 61, (9), 2994-3000.
8. Farzi, G. A., Bourgeat-Lami, E., McKenna, T.F.L., . *Journal of Applied Polymer Science* 2009, in press.
9. Hansen, F. K.; Ugelstad, J. *Journal of Polymer Science, Polymer Chemistry Edition* 1978, 16, (8), 1953-79.
10. Landfester, K.; Bechthold, N.; Förster, S.; Antonietti, M. *Macromolecular rapid communications* 1999, 20, (2), 81-84.
11. Qi, D.-m.; Bao, Y.-z.; Weng, Z.-x.; Huang, Z.-m. *Polymer* 2006, 47, (13), 4622-4629.
12. Erdem, B.; Sudol, E. D.; Dimonie, V. L.; El-Aasser, M. S. *Journal of Polymer Science Part A: Polymer Chemistry* 2000, 38, (24), 4419-4430.
13. Erdem, B.; Sudol, E. D.; Dimonie, V. L.; El-Aasser, M. S. *Journal of Polymer Science Part A: Polymer Chemistry* 2000, 38, (24), 4431-4440.
14. Erdem, B.; Sudol, E. D.; Dimonie, V. L.; El-Aasser, M. S. *Journal of Polymer Science Part A: Polymer Chemistry* 2000, 38, (24), 4441-4450.
15. Fitch, R. M. *British polymer journal* 1973, 5, (6), 467-483.