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► To cite this version:

E. Frappé, A. de Bernardinis, O. Bethoux, D. Candusso, F. Harel, et al.. PEM fuel cell fault detection and identification using differential method: simulation and experimental validation. European Physical Journal: Applied Physics, 2011, 54 (2), 10.1051/epjap/2011100277 . hal-00698838

HAL Id: hal-00698838

<https://hal.science/hal-00698838v1>

Submitted on 18 May 2012

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PEM fuel cell fault detection and identification using differential method: simulation and experimental validation

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Keywords: PEMFC, Fault detection, Cell on-line monitoring, Non-intrusive techniques, Flooding.

Abstract

PEM fuel cell performance and lifetime strongly depend on the polymer membrane and MEA hydration. As the internal moisture is very sensitive to the operating conditions (temperature, stoichiometry, load current, water management...), keeping the optimal working point is complex and requires real time monitoring. This article is centered in the PEM fuel cell stack health diagnosis and more precisely on stack fault detection monitoring. This paper intends to define new, simple and effective methods to get relevant information on usual faults or malfunctions occurring in the fuel cell stack. For this purpose, the authors present a fault detection method using simple and non-intrusive on-line technique based on the space signature of the cell voltages. The authors have the objective to minimize the number of embedded sensors and instrumentation in order to get a precise, reliable and economic solution in a mass market application. A very low number of sensors are indeed needed for this monitoring and the associated algorithm can be implemented on-line. This technique is validated on a 20-cell PEMFC stack. It demonstrates that the developed method is particularly efficient in flooding case. As a matter of fact, it uses directly the stack as a sensor which enables to get a quick feedback on its state of health.

1 Introduction

Environmental issues have increased the demand for less polluting energy generation technologies. A hydrogen fuel cell (FC) directly converts the electrochemical energy of hydrogen into electricity and only produces heat and water. Proton

Exchange Membrane Fuel Cell (PEMFC) is an attractive technology because of its high power density, its solid membrane and its low operating temperature allowing fast startups and immediate response to changes in the demand of power [1]. However, the membrane has to be fully water saturated in order to enhance its ionic conductivity. As present cells operate at a rated temperature range between 60°C to 80°C, stack water management is a PEMFC key issue. Flooding, due to an excess of water in the cells, inhibits gas transport to the reaction sites and reduces the active surface area of the catalysts. The adverse effect is a significant rise of the activation and concentration losses leading sometimes to a catastrophic decrease of the cell efficiency [2]. On the contrary, a drying situation results in an increase of the membrane resistivity also reducing cell efficiency [3-5]. A long operation with low water content reduces the FC lifetime [6].

Any fault induces a voltage drop [5]. Hence, cell voltage is a good failure indicator, easy to implement. Moreover a voltage sensor is a high bandwidth and accurate device. Nevertheless voltage monitoring makes fault identification difficult to achieve. A first approach is to use the frequency signature of each failure: dehydration adversely affects the ionic conductivity which is a low time response phenomenon, whereas flooding negatively diminishes gas diffusion performance which is a very low time response observable fact. Hence, electrochemical impedance spectroscopy (EIS) provides more complete information about the FC state of health thanks to fuel cell impedance measure [12-14]. However, EIS is a relatively slow method since it needs time to perform a full frequency spectrum [7]. EIS also requires a stabilized working point which is difficult to obtain in real operation. Furthermore, it involves expensive and sometimes voluminous devices to perform the identification. Nevertheless, partial frequency impedance may be fast

executed and gives interesting but limited information. Hinaje et al. [8] use the HF current ripple generated by the power converter, which is commonly used for FC system electric power conditioning. Using this principle, they perform a membrane resistance measure. Subsequently drying is easily detected by resistance increase but flooding cannot be identified. Even though EIS remains a promising “perturb and observe” technique, it becomes difficult to implement in stack with large number of cells. As a matter of fact, individual cell voltages must be monitored within a stack since a failure (flooding, drying, poisoning,...) can only occur in a few cells. Although some methods exist [9,10], the use of a huge number of sensors is subject to failure. This makes voltage monitoring a challenge for high voltage stacks (long stacks).

Power fuel cells (FCs) are currently developed for applications like traction for electrical vehicle, auxiliary power units (APU) or even battery charger in some high power vehicles or fuel cell hybrid electric vehicles (FCHEVs). For example, the French research project SPACT-80 designed, manufactured and tested in real conditions a robust and durable air/H₂ 80 kW PEM fuel cell-based system, specifically developed for railway and road applications [11-13]. The GENEPAC project was run in order to design and build a fuel cell for automotive applications. It focuses on the development of a compact 80 kW fuel cell stack with high output dynamic performances [14]. Recently, Toyota revealed its new FCHV powered by an 80 kW fuel cell [15]. All these high power PEM stacks are made of large specific areas and composed of about a hundred cells. They are sometimes used as a twin-stack or a multi-stack fuel cell generator [16] because PEMFC power increase is limited by technical and mechanical constraints [17]. As a matter of fact, stacks with large membrane electrode assembly (MEA) and an important cell number are difficult to operate because of heterogeneous fluidic distribution between cells. This discrepancy affects FC performances [18] and makes water management difficult to operate efficiently. Consequently online monitoring is particularly important for safe operating. In order to get a precise, reliable and economic solution in a mass market application, the objective is to minimize the number of embedded sensors, the price of instrumentation and the complexity of the related algorithm.

In this perspective, a new fault detection method is proposed and studied in this article. It still relies on voltage measurement but is no longer based on frequency signature. It intends to make use of the small disparity of temperature and the non-uniform distribution of reactants along the stack. The fact is that many authors pointed out the cell discrepancies throughout the stack which depend on the operating conditions [19]. Some authors show that cell voltage is lower in the cells furthest from the fuel inlet of the stack (nearest to the air inlet) due to uneven gas distribution or water flooding [20]. Different experiments also point out that the central interior of the stack is hotter to its exterior, and subsequently drying mostly occurs in center cells [21,22]. In fact, Ramousse et al. [23] highlights that water in the cells is highly dependent on the temperature; as a result flooding occurs in cooler cells and drying in hotter cells. Based on these

remarks, we suggest measuring the voltage of group of cells in the inlet, the center and the outlet of the stack. It will allow the detection of a fault when a voltage difference occurs and also permit identification using the shape of this voltage non-uniformity.

In this paper, we propose a differential voltage method, which only needs a few voltage sensors located judiciously along the FC stack and supervising only some particular cells or groups of cells. It can be performed on-line without disturbing the FC electric load neither with a small signal (EIS) nor with current interrupt (CI). Moreover, the measurements are associated with a simple algorithm which permits to get rid of many signal disturbances; for instance, load changes and slow dynamic phenomena (ageing effects...) don't affect the accuracy of the detection.

The paper is organized as follow. First a dynamic modeling of a cell is presented which allows performing the simulations and studying the behavior of the PEM fuel cell when a fault occurs. Then, the paper focuses on the fault detection and identification method applied to the multi-cell stack. The originally developed approach is first simulated in drying and flooding cases. In a second step, the method is experimented and validated on a 20-cell PEMFC test bench in the particular case of stack flooding. Finally the advantage of the method is discussed and compared to EIS and CI techniques.

2 Fuel cell modeling and polarization signature

2.1 Fuel cell modeling: application to a 20-cell PEMFC

Some work has already been reported in the literature, static and dynamic modeling based on empirical equations was given by [1,24-27]. The voltage drop across the fuel cell (FC) can be written as a function of the activation, ohmic and concentration overvoltages given by (1) for one cell:

$$V_{cell} = E - \eta_{act} - \eta_{ohm} - \eta_{conc} \quad (1)$$

With E the electromotive force given using the Nernst equation:

$$E = 1.229 - 8.5 \times 10^{-4} (T_{fc} - 298.15) + 4.3085 \times 10^{-5} \times T_{fc} (\ln(P_{H_2}) + 0.5 \ln(P_{O_2})) \quad (2)$$

T_{fc} is the fuel cell stack temperature; P_{H_2} and P_{O_2} are the partial pressures of hydrogen and oxygen respectively (in bar).

The activation voltage losses represent the fact that some energy is needed to generate a reaction product. They are obtained by the Tafel equation [1]:

$$\eta_{act} = A \cdot \ln((J + J_n)/J_0) \quad (3)$$

with

$$A = (R T_{fc}) / (2 \alpha F) \quad (4)$$

J is the fuel cell current density, J_n the leakage current density, J_0 the exchange current density, R the perfect gas constant, α the charge transfer coefficient and F the Faraday's constant.

The ohmic voltage losses are due to the resistance for both electronic and ionic currents. They result in a slow and linear voltage drop with an increasing current. The main parameter of this voltage drop is the membrane resistance R_{mem} :

$$\eta_{ohm} = R_{mem} \cdot J \quad (5)$$

The concentration voltage losses are due to the reduction of the reactant concentration at the electrode surface induced by reactants consumption. This irreversibility becomes significant at high current density and the related overvoltage is obtained empirically:

$$\eta_{conc} = m \cdot \exp(nJ) \quad (6)$$

m and n are constants depending on the construction of the cell. It is useful to formulate the real voltage of the cell when there is no current; this voltage is named the open circuit voltage (OCV). Using (2) and (3), the open circuit voltage E_{ocv} can be computed as follows:

$$E_{ocv} = 1.229 - 8.5 \times 10^{-4} (T_{fc} - 298.15) + 4.3085 \times 10^{-5} \times T_{fc} (\ln(P_{H_2}) + 0.5 \ln(P_{O_2})) + A \ln(J_0) \quad (7)$$

$$\eta_{act2} = A \cdot \ln(J + J_n) \quad (8)$$

More precisely the cell voltage becomes:

$$V_{cell} = E_{ocv} - \eta_{act2} - \eta_{ohm} - \eta_{conc} \quad (9)$$

Concentration of charges (electrons and H^+ ions) on the active surface (electrode and electrolyte surface) greatly influences the probability of reaction. This build-up of charges takes time to establish, drives non-faradic current and depends on the load current. Consequently during current transient, overvoltage does not change instantaneously. This phenomenon is complex and known as charge double layer; it can be modeled by a capacitor [25,28].

In the dynamic model, the double layer capacitor is placed in parallel to the sources representing electrochemical voltage losses (η_{act2} and η_{conc}). That is the reason why we have to modify the model elements. As a matter of fact, the fuel cell current density J is shared between the double layer capacitor and η_{act2} , η_{conc} . Then the current in the voltage loss branch (J_f) needs to be calculated. For that purpose, we proceed as follows:

η_{act2} is replaced by a current source, called J_f , controlled by the voltage η_{act2} , which is calculated with the Kirchhoff's voltage law:

$$\eta_{act2} + \eta_{conc} = V_{cdl} \quad (10)$$

$$\eta_{act2} = V_{cdl} - \eta_{conc} \quad (11)$$

J_f is calculated thanks to (8)

$$J_f = \exp(\eta_{act2}/A) - J_n \quad (12)$$

η_{conc} is a voltage source controlled by J_f . The ohmic loss is modeled by a resistor. The model representation with the

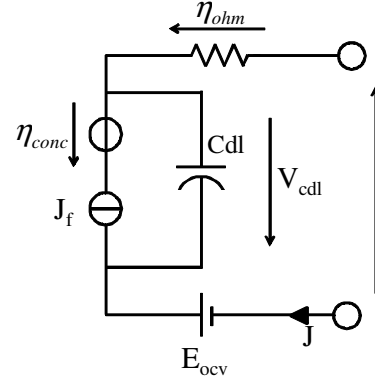


Fig. 1. Dynamic FC model: Representation of the double layer phenomenon.

The cell model is tuned with parameters given in Tab 1. In order to have the fuel cell voltage, V_{cell} is multiplied by the number of cells. Figure 2 shows the polarization curve of the simulated model compared with a polarization curve obtained by experimental measurement on a 20-cell stack. The experimental polarization curve is obtained as follow: first fuel cell is set to nominal point (stack temperature = 60°C, H_2/O_2 stoichiometry = 2/4, H_2/O_2 hygrometry = 14/22%). Then current is reduce from 60 to 0A in ten minutes (ramp current = -0.1A/s). As shown, the simulated curve fits in accordance with the experimental curve.

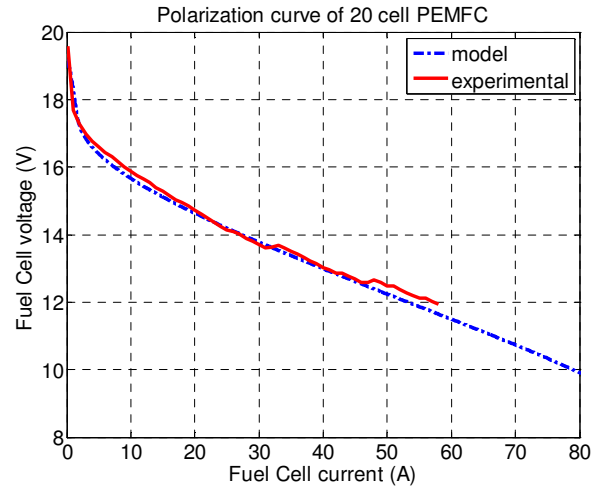


Fig. 2. Polarization curves of the experimented PEMFC stack and its related model.

Tab 1 : Parameters used in the FC analytical electrical model

α	Charge transfer coefficient	0.44	C_{dl}	Double layer capacity	50 mF/cm ² [7]
m	Concentration coefficient	2.11×10^{-5}	F	Faraday's constant	9.65×10^4 C/mol
n	Concentration coefficient	8×10^{-3}	R	Perfect gas constant	8.314472 J/mol/K
S_{cell}	Cell surface	100 cm ²			
R_{mem}	Membrane resistance	300×10^{-6} k Ω .cm ²	T_{fc}	Fuel cell temperature	333.15 K
J_n	Leakage current density	3 mA/cm ²	P_{H_2}	Hydrogen partial pressure	0.93 bar
J_0	Exchange current density	4×10^{-4} mA/cm ²	P_{O_2}	Oxygen partial pressure	0.17 bar

2.2 Polarization signature

The work described in this article focuses on two kinds of fault: membrane drying and cell flooding. A drying, due to insufficient water content in the membrane, increases its resistance [22,29]. In case of a flooding, del Real et al. [24] explain that the water forms a thin film blocking part of the active fuel cell area. This phenomenon results in a lower apparent active area [30,31] and thus a higher current density which increases over voltages.

In general faults don't occur in the entire stack but only affect a few cells [18]. The impact on a single cell voltage is shown in Fig. 3. Plot (A) shows the cell polarization curve in rated conditions. (B) displays the polarization curve of the same cell when membrane drying occurs: the dried membrane resistance is increased by 1.5 compared to the rated value [8]. (C) illustrates the polarization curve of this cell when membrane flooding happens: the active area was reduced to 80%, [this will act on the cell current density according to this relation \$J = I_{fc} / \(S_{cell} * k\)\$ with \$k = 0.8\$ the degree of reduced active area](#) [24]. As already described in [32], the voltage drop is similar either in the drying case or in flooding circumstances. The V-I characteristics become different only when the cell voltage is lower than its minimum voltage (0.4 V). The fuel cell should not be used under this voltage [33].

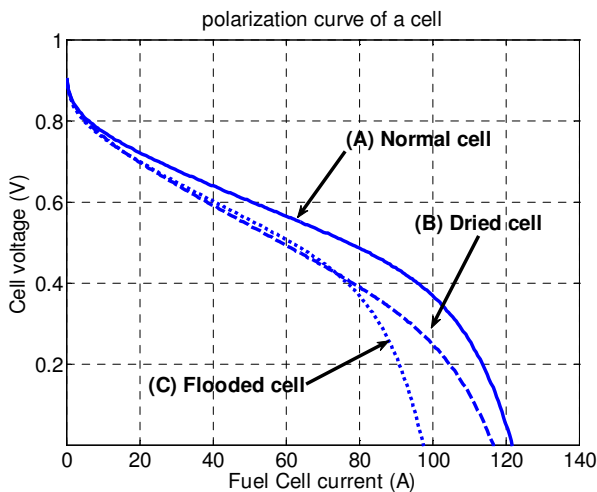


Fig. 3. Different polarization curves of a cell obtained by simulation.

3 Fault detection for a power stack

3.1 Monitoring for a power stack

Stack-level investigations offer more opportunities than single cell level analysis. In particular, [19,23,34] show that flooding or drying only affects some localized cells or groups of cells. In case of a high dew point temperature, humidified air quickly condenses at the inlet of the stack. Furthermore water produced by the electrochemical reaction can easily accumulate at the outlet of the stack. Eckl et al. [22] demonstrates that, during flooding experiments on a 20-cell stack, the most perturbed cells were the cells 3 and 5. Hernandez's experiments [34] pointed out, with a 20-cell stack, voltage degradation due to flooding in cells 4, 5, 6 and 18, 20. In Corbo's experiments on a 34-cell stack [35], flooding has a great effect on the 6th and 28th cells. Conversely the center of the stack is hotter than its extreme parts; the

presence of liquid water is lower. In Park's drying experiments on an 8-cell stack, the most affected cells were the 4th, 5th and 6th [29]. Eckl gives the same observation with a 20-cell stack [22], where cell voltages V_9 , V_{11} and V_{13} were deeply disturbed by a drying.

Hence a flooding may occur in the inlet and outlet of the stack while a drying may occur in the center of the stack. That is the reason why, instead of monitoring all the cells, it could be judicious to monitor only a group of representative cells: cells located at the inlet and the outlet in order to detect a flooding, and cells in the center of the stack for detecting a drying.

3.2 Fault detection and identification (FDI) strategy using the differential method: approach by simulation

Referring to the previous studies mentioned in the article, it appears relevant to instrument with voltage sensors three main areas of the stack: the inlet, the outlet and the center (Fig. 4). In this case, the detection principle is based on the monitoring of a differential between the voltage in the center of the stack (V_{center}) and the inlet/outlet voltages (resp. V_{inlet} , V_{outlet}). This principle allows to generate a new state-of-health indicator of the fuel cell stack. In the case of no fault, all voltages are constant or drop similarly due to load variation: the differential voltages equal zero. If a drying appears, only V_{center} drops and the two differential voltages become positive. However, if a flooding occurs, the inlet and/or the outlet voltage drops leading to a decrease of one or two differential voltages.

Using the differential method, the FC stack can be assimilated to a voltage sensor. Its characteristic is to provide two key signals representative of the state of health. The feedback information is simple, fast and based on the real-time operating conditions without adding any external disturbance. Moreover the method can be applied also when the operating conditions are slightly modified.

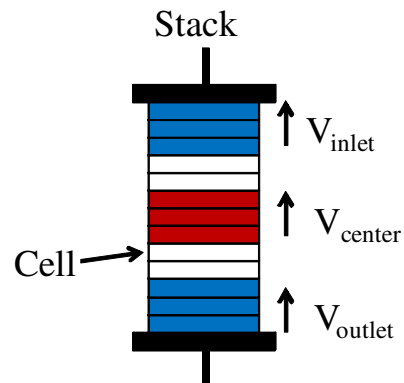


Fig. 4. Principle of monitored cells for a fuel cell stack.

As a first approach, the proposed detection method is validated by numerical simulations.

3.2.1 Fuel cell model enhancement

In order to study the differential method, the FC stack is modeled in the following way: firstly, FC is segmented into 5 segments of 3, 6, 3, 5, 3 cells distributed from the inlet to the outlet of the stack. Previous cell model is used to calculate

each segment voltage $V_{st,i}$. Then electrical model of segment i is coupled with thermal one as represented in Fig. 5.

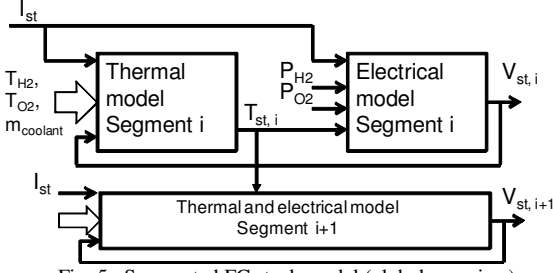


Fig. 5. Segmented FC stack model (global overview)

The temperature of one stack segment is calculated as follow [24,36]:

$$m_{st} C_{st} \frac{\partial T_{st}}{\partial t} = \dot{H}_{react} - Q_{cool} - Q_{conv} - Q_{rad} - P_{El} + Q_{cond} \quad (13)$$

$m_{st} C_{st}$ is the thermal capacity of the system, T_{st} is the stack segment temperature.

With \dot{H}_{react} the energy of the electrochemical reaction:

$$\dot{H}_{react} = \dot{m}_{H2} \Delta h_{H2} + \dot{m}_{O2} \Delta h_{O2} - \dot{m}_{H2O} (h_f^0 \Delta h)_{H2O} \quad (14)$$

H_f^0 is the mass specific enthalpy of formation and \dot{m} denotes the mass flow of the substance:

$$\dot{m}_{H2} = M_{H2} N_{cell} \frac{I_{st}}{2F} \quad (15)$$

$$\dot{m}_{O2} = M_{O2} N_{cell} \frac{I_{st}}{4F} \quad (16)$$

$$\dot{m}_{H2O} = M_{H2O} N_{cell} \frac{I_{st}}{2F} \quad (17)$$

M is the molecular mass in kg/mol, N_{cell} is the stack segment number of cell, F the Faraday constant and I_{st} the current stack.

Δh is the mass specific enthalpy difference from the present state to the reference state:

$$\Delta h_{H2} = C_{pH2} (T_{H2in} - T_0) \quad (18)$$

$$\Delta h_{O2} = C_{pO2} (T_{airin} - T_0) \quad (19)$$

$$\Delta h_{H2O} = C_{pH2O} (T_{airout} - T_0) \quad (20)$$

C_p are the specific heat energies, T_{h2in} , T_{airin} and T_{airout} are the inlet H2 gas temperatures, the inlet air gas temperature and the outlet air gas temperature.

Outlet gas temperature is calculated thanks to:

$$T_{airout} = 2T_{air}^{stack} - T_{airin} \quad (21)$$

Where:

$$T_{air}^{stack} = T_{st} - \frac{\dot{H}_{react} - P_{El}}{k_T} \quad (22)$$

Here it is assumed that the temperature difference between the FC and the cathode air is proportional to the total waste heat of the reaction. The constant proportionality k_T can be determined experimentally.

Q_{conv} and Q_{rad} are the heat transfer to the surrounding area by a convective and a radiative heat flow.

$$Q_{conv} = h_{amb} A_{amb} (T_{st} - T_{amb}) \quad (23)$$

$$Q_{rad} = \epsilon \sigma A_{amb} (T_{st}^4 - T_{amb}^4) \quad (24)$$

h_{amb} is the heat transfer coefficient of the FC, A_{amb} denotes the outer surface of the body, ϵ is the emissivity of the body, σ is the Stefan-Boltzmann constant and T_{amb} represents the temperature of the environment.

The electric power of the system equals the product of the stack segment voltage with the current:

$$P_{El} = V_{st} I_{st} \quad (25)$$

Q_{cool} represent the heat transfer rate from the body to the coolant:

$$Q_{cool} = h_{cool} A_{cool} (T_{st} - T_{cool}) \quad (26)$$

with A_{cool} the heat transfer area, T_{cool} the temperature of the coolant inside the FC and h_{cool} the heat transfer coefficient given by :

$$h_{cool} = K_h \left(\dot{m}_{coolant} \right) \quad (27)$$

This heat transfer coefficient is a function of the coolant mass flow $\dot{m}_{coolant}$, the coefficient K_h has to be determined experimentally.

The temperature of the coolant inside the FC is calculated as follow:

$$m_{cool} C_{cool} \frac{\partial T_{cool}}{\partial t} = \Delta \dot{H}_{cool} + Q_{cool} \quad (28)$$

$m_{cool} C_{cool}$ is the thermal capacity of the coolant system in the FC segment

$\Delta \dot{H}_{cool}$ is the enthalpy difference of the coolant flow :

$$\Delta \dot{H}_{cool} = \dot{m}_{coolant} C_{pH2O} (T_{coolin} - T_{cool}) \quad (29)$$

with T_{coolin} the inlet coolant temperature.

Lastly conductive effects between one segment to its neighbor is given by:

$$Q_{conv} = \begin{cases} \frac{D}{\delta}(T_2 - T_{st}) & \text{for segment 1} \\ \frac{D}{\delta}(T_{n+1} + T_{n-1} - 2T_{st}) & \text{for segment } n = 2, 3, 4 \\ \frac{D}{\delta}(T_4 - T_{st}) & \text{for segment 5} \end{cases} \quad (30)$$

D is the transfer coefficient and δ the thickness between two segments. All parameters required for the thermal model are summarized in Tab.2.

Temperature along the stack is plotted in Fig. 6. H₂ and Air gas temperature is set to 40°C, ambient temperature is 25°C. Coolant inlet temperature is 50°C. FC current is set to 30A.

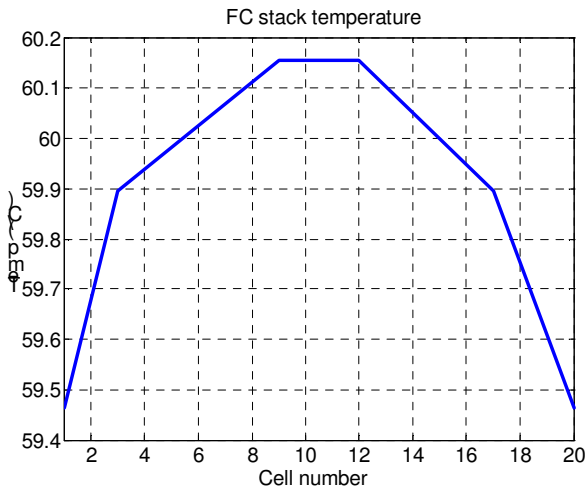


Fig. 6. Fuel cell stack temperature profile versus cell number.

As expected the center of the FC is hotter than extremity.

A temperature raise of 0.7°C in the center of the stack increases the vapor partial pressure by 2.4%. Then less liquid water should be present in the center of the fuel cell.

3.2.2 Simulation results

Fig. 7 shows the detection method in the case of a flooding. Flooding occurs at 3 seconds in the inlet and outlet of the stack, and water is slowly accumulated in the cells until the active area is reduced to 80%, while inlet and outlet monitored voltage drop slowly. The global stack voltage does not drop significantly. On the contrary, monitoring the three groups of cells makes it possible to detect the early fault. The differential voltages ($V_{inlet} - V_{center}$) and ($V_{outlet} - V_{center}$) are negative and are falling slowly as the water content increases.

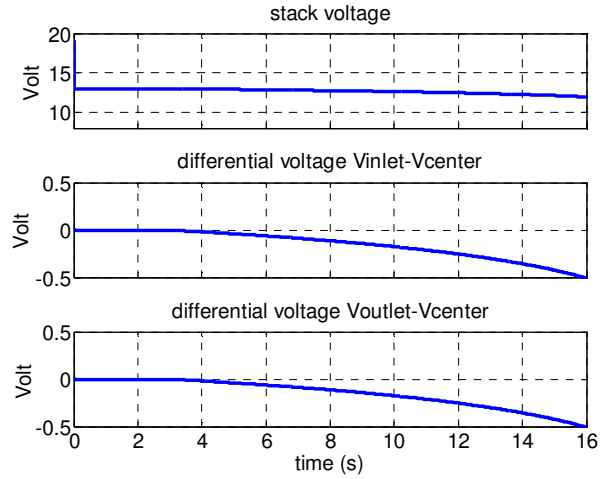


Fig. 7. Principle of monitored cells: flooding case.

Fig. 8 shows the case of a drying affecting the center cells. In this case, because the center cells are drying, their resistances increase gradually up to a 1.5 factor resulting in a voltage drop of center cells only. In that case the two differential voltages are positive and increase. In this case too, the global stack voltage does not drop significantly, but thanks to the differential voltages, the fault can be detected in a sensitive way.

Tab 2 : Parameters used in the FC thermal model

m_{st}	Mass of the stack segment	1.4 kg	h_{amb}	Heat transfer coefficient of FC	$3.9 \text{ W m}^{-2} \text{ K}^{-1}$
C_{st}	Stack specific heat	$1300 \text{ J kg}^{-1} \text{ K}^{-1}$	A_{amb}	Convection exchange surface	0.023 m^2
M_{H_2, O_2, H_2O}	Molecular mass of H ₂ , O ₂ and H ₂ O	Kg/mol	ϵ	Emissivity of the body	0.9
N_{cell}	Number of cell in the segment		σ	Stefan-Boltzmann constant	$5.678 \cdot 10^{-8} \text{ W m}^{-2} \text{ K}^{-4}$
$C_{p_{H_2, O_2, H_2O}}$	Specific heat energy of H ₂ , O ₂ and H ₂ O	$\text{J kg}^{-1} \text{ K}^{-1}$	A_{cool}	Heat transfer area of coolant	0.011 m^2
T_0	Reference temperature	298.15 K	K_h	Heat transfer coefficient	$2.16 \cdot 10^5 \text{ W kg}^{-2} \text{ k}^{-1}$
K_T	Constant proportionality	340 W K^{-1}	$m_{cool} C_{cool}$	Thermal capacity of the coolant system	110 J k^{-1}
D	Heat transfer coefficient between 2 FC segments	0.35 W m k^{-1}	$\dot{m}_{coolant}$	Coolant mass flow	0.08 kg s^{-1}
δ	Thickness between 2 FC segments	$5 \cdot 10^{-3} \text{ m}$	H_f^0	Mass specific enthalpy of formation	$-1.58 \cdot 10^7 \text{ J k}^{-1}$

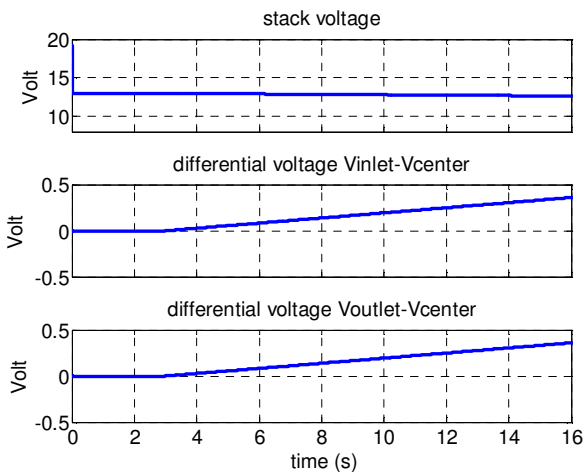


Fig. 8. Principle of monitored cells: drying case.

Simulation results demonstrate the validity of the technique on well known faults. However, it should distinguish between a real fault and a disturbance in order to prevent false alarm.

Fig. 9 shows the case of a load variation of a healthy stack in order to validate the detection principle during transient. In this occurrence, all cells are perturbed in the same way and thus their voltage drops are equal leading to a constant differential voltage.

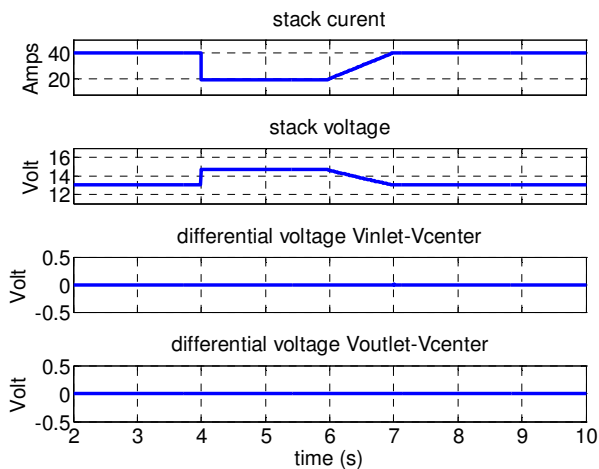


Fig. 9. Principle of monitored cells: healthy stack with current variation.

Thanks to the measurement of the three voltages representing the three key parts of a stack, this fault detection method reveals very sensitive. It allows detecting early fuel cell failure, before it completely affects the entire stack behavior. It requires a very low number of sensors, is a non intrusive technique and also does not perturb the stack functioning. Moreover, it could be easily implanted in embedded applications.

4 Experimental validation

Experimentations have been performed on a real FC stack in the FC LAB in Belfort. The PEMFC is a 500 W, 20-cell, 100 cm² stack from ZSW - UBZM manufacturer (Fig. 10). The objectives of these experiments are:

- To control that inlet and outlet voltage cells are negatively influenced during flooding.

- To visualize which cells are flooded in each case.
- To choose cells representative of FC state of health and instrument them.
- To apply the differential method.

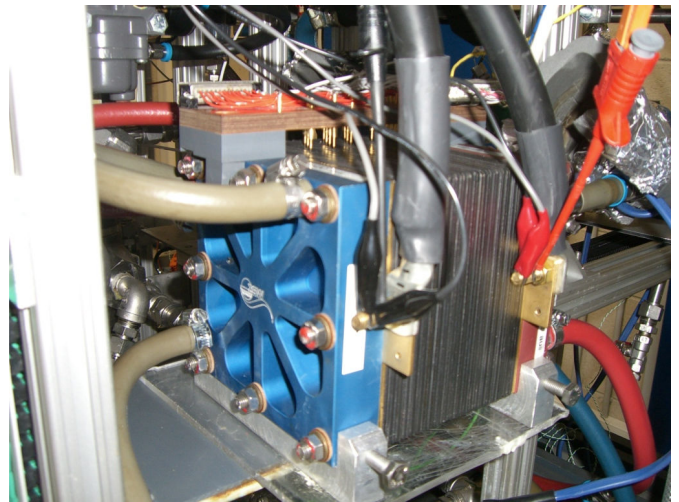


Fig. 10: Picture of the instrumented 20-cell PEMFC stack under test.

Many flooding experiments are performed at different operating conditions: different stack temperatures and hygrometry rates. Some experimental results are summarized in Tab. 3. It presents the cells with the greater voltage degradation due to flooding during all the experiments. White table cell correspond to cell voltage above 0.6V, blue colored table cell means that cell voltage drops between 0.5 and 0.6V. Finally, red table cell with a cross signify cell voltage drops under 0.5V.

This table points out that cells 4, 5, 6 and 18, 20 are always influenced by flooding. These results are in good agreement with previous observations. Ramousse et al. [23] experiment multiple floodings on a 65-cell stack: they observe that the worst voltage degradation always affects the same cells. They show that this performance mismatch is due to a non uniform thermal distribution. The gas flow distribution plays also an important role in the flooding process [37]. In theory, all cells have the same air flow distribution but in reality bipolar plates are slightly different [38]. Moreover, the clamping pressure, due to stack assembly, modifies the air flow and plays an important role in FC performance and flooding phenomenon [18,39]. Thus, because of these material differences, some cells are more prone to flooding than others. Then we can consider that these cells are representative of FC state of health.

During the tests, in many occurrences, cell voltage 13 presents voltage degradation. This is not in agreement with previous observations, but an explanation could be the FC ageing. The stack has been previously tested for about 500 hours under different operating conditions. In normal conditions, this cell voltage was already lower than others; we suspect a possible degradation of its material. For example an increase of its channel friction would imply a lower gas flow in this cell and then an important flow disparity [38]. But we can't exclude possible flooding space cyclicality where, in long cell assembly, some cells could be affected by flooding in a cyclic location along the stack. Tests on others stacks should be performed in particular on large stack to validate this hypothesis.

As explained in the previous section, it is judicious to monitor only 3 groups of cell voltage in order to detect a flooding or a drying. The choice of the number of measured cells is in fact a trade-off between easy sensor implementation by measuring sufficient voltage amplitude and the need of a good signal/noise ratio. In our case, 3 cells are monitored in the inlet (V4+V5+V6 named Vinlet), 3 cells in the center (V11+V12+V13 named Vcenter) and 3 cells in the outlet of the stack (V18+V19+V20 named Voutlet).

For the next step of this study, figures 11, 12 and 13 focus on the particular experiment number 5, performed under a flooding fault with the following conditions:

- Temperature of the stack: 40°C
- FC current: 40A
- Air inlet hygrometry rate: 45%

Each cell voltages are depicted in figure 11. Firstly flooded cell voltages drop smoothly because of water accumulation in the gas diffusion layer (GDL), and then the voltages behave regarding the characteristic of the flooding signature. Indeed, water droplet formation blocks the gas channel and causes the voltage drop owing to local gas starvation. Meanwhile, the inlet pressure increases. Finally gas pressure evacuates the droplet; as a result the voltage increases until the next droplet is generated. Water droplet formation and extraction, associated with local gas starvation [40] cause cell voltage oscillations.

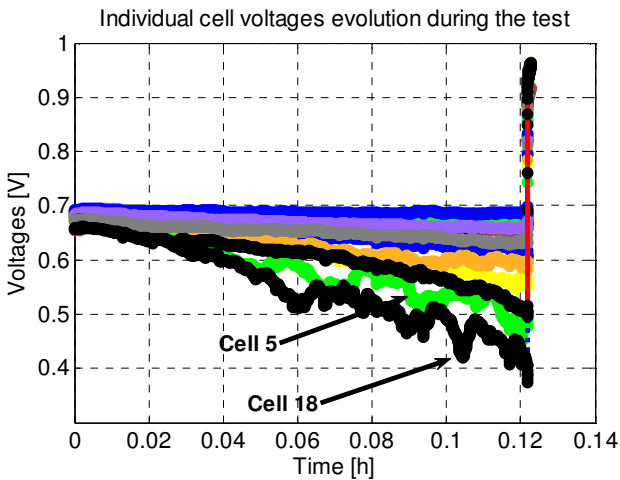


Fig. 11. Evolution of individual cell voltages.

At $t = 0.12$ h, the cell voltage 18 drops under the safety level set to 380 mV. Thus, so as not to degrade irreversibly the catalysts of FC materials [41,42], the stack is disconnected.

The cell voltage discrepancy is shown in Fig. 12. This figure illustrates the voltage drop during all the experiment. Thus 2 areas can be identified:

- When FC is delivering current: cell voltages are under 0.7 Volt.
- When FC is disconnected: cell voltages are on OCV (i.e. above 0.9V).

The voltage drop of the cells number 4, 5, 13, 18, 20 is clearly observed.

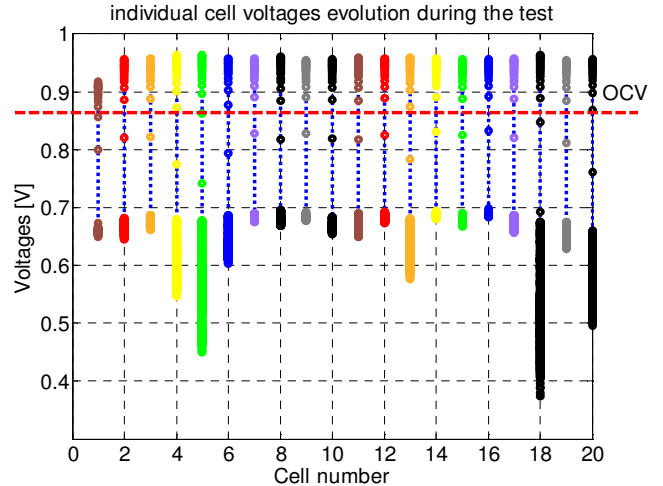


Fig. 12. Dispersion of individual cell voltages.

The two differential voltages are plotted figure 13 in the two upper subplots. Because the flooding takes place in the inlet and outlet cells, the differential measures are negative and slightly drop according to the flooding degree. This figure points out that the differential measures could detect the fault with a threshold set to -0.2 V, before the stack is disconnected because of a low cell voltage. This behavior is in agreement with the simulation study. It should be noted, that a fuel cell stack is affected by many degradation processes that are not yet well understood. Nevertheless the ageing phenomenon leads to a slow voltage decrease [11,43] and an inhomogeneous voltage distribution along the stack even in nominal conditions. Consequently an aged fuel cell will present a mismatch difference voltage in normal operation mode. Hence, the ability to discriminate between ageing and malfunction leads to define a high level threshold. However this tuning has two drawbacks: on the one hand it may delay the detection alarm, on the other hand it may be not enough accurate to perform the detection.

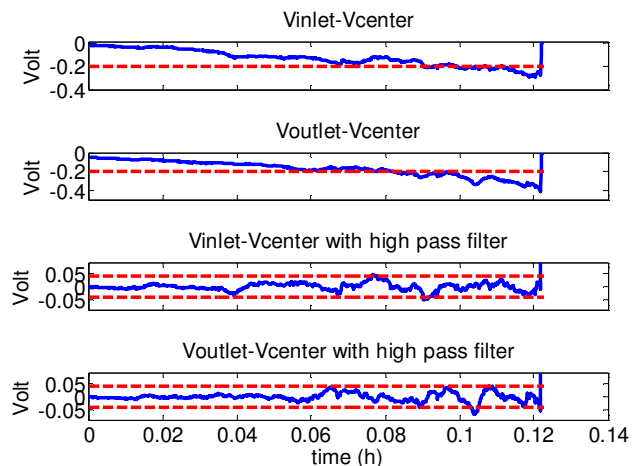


Fig. 13. Differential and filtered differential measures for cell voltages with their thresholds.

Figure 11 also points out the erratic voltage behavior owing to the water droplet. That is the reason why we suggest to filter differential measures with a high pass filter in order to get rid of the slow voltage derivation and only visualize the voltage oscillation due to water propagation. As droplet formation and extraction are slow phenomena, high pass cut-off frequency is

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