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Networked Control Systems

Quality of Service aware Quality of Control adaptation

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Abstract

We consider the implementation of simple process control applications through a CAN network. The goal of this paper is to study modifications on-line of controller parameters according to the global time delay in the control loop. Two methods that we use are the phase margin method and the dominant pole one. We evaluate the performances of the two methods in terms of the time response.

1. Introduction

Networked Control Systems (NCSs) are a very important research area because of their multidisciplinary aspect: Automatic control, computer science (task scheduling), communication network (message scheduling, message transfer). Here we consider two aspects: automatic control and message scheduling. A realistic design, in this framework, is to have a co-design approach between the controller law and the message scheduling, *i.e.* with a bi-directional relation between the Quality of Control (QoC) provided by the controller and the Quality of Service (QoS) provided by the scheduling of messages (QoC \rightleftharpoons QoS). The idea of the link (QoC \rightarrow QoS) is to re-allocate the implementation system resources on-line to guarantee an expected QoS level required by the control application. In [6], we have in particular shown the interest of this link (QoC \rightarrow QoS) by means of the concept of dynamic priority schemes for messages in the MAC layer of a CAN network [5].

In this paper, we want to show the interest of the link (QoS \rightarrow QoC) *i.e.* where the controller is aware on-line of the time delay in the control loop and adapts, in consequence, its parameters. We consider a simple continuous linear process control application (one variable) implemented on a CAN network with a Proportional-Derivative (PD) controller.

Two methods for controlling the consequences of

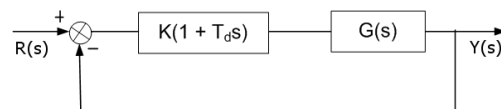


Figure 1. Continuous control system.

the time delay in the control loop will be the phase margin and the dominant poles methods.

This paper includes the following sections: the section 2 presents the study context; the section 3 concerns the proposal for the implementation on-line of the link (QoS \rightarrow QoC); the section 4 concerns an application of this proposal; the conclusion is represented in the last section 5.

2. Study context

2.1. Considered continuous control system

The model of the considered process control application is given on the figure 1: the process to control $G(s) = \frac{1000}{s(s+1)}$, the PD controller $K(1 + T_d s)$, the step input $R(s)$ and the output $Y(s)$.

The phase margin (Pm) of $G(s)$ is $Pm_0 = 1.8^\circ$ at the crossover frequency $\omega_c = 31.6 \text{rad/s}$ (*i.e.* ω_c such that $|G(j\omega_c)| = 1$). This phase margin (Pm_0) is not enough and thus initially we want to use a PD controller to compensate the phase and to have a phase margin Pm of 45° still at ω_c .

Then the controller must bring, at ω_c , a positive phase $\varphi_c = 45^\circ - Pm_0$. To do this, it must be: $tg(\varphi_c) = T_d \omega_c$ and $20|\log(K(1 + j\omega_c T_d))| = 0$.

Thus we have the formula (1) which allows to get the values $T_d = 0.0297 \text{s}$ and $K = 0.7291$.

$$\begin{cases} T_d = \frac{tg(\varphi_c)}{\omega_c} \\ K = \frac{1}{\sqrt{1 + (\omega_c T_d)^2}} \end{cases} \quad (1)$$

In such condition, the main characteristics of the continuous control system are: $Pm = 45^\circ$; poles $p_{1,2} = -11 \pm j24.5$; rise time $t_r = 37.5 \text{ms}$, steady state error $e_{ss} = \lim_{s \rightarrow 0} s \frac{1}{1 + K(1 + T_d s)G(s)} R(s) = 0$.

3.2. Computation of the parameters K and T_d

We present now the two methods which have been used: Phase margin and Dominant pole.

A/Phase margin method

The purpose of the phase margin method is to compensate the time delay of each sampling period to maintain an expected phase margin.

A time delay τ induces a reduction of the phase margin of $\Delta\varphi = \tau\omega_c$ [4]. Hence in order to have $Pm = 45^\circ$, the controller must provide a positive phase $\varphi_c = 45^\circ - Pm_0 + \Delta\varphi$. The new values of T_d and K are obtained by using the formula (1) in Section 2.1 with the new value of φ_c .

Note that the maximal positive phase that the PD controller can bring is 90° , the maximal phase φ_{cmax} that the controller can bring is $90^\circ - 45^\circ - Pm_0 = 43.2^\circ$ corresponding to $\tau = \frac{\varphi_{cmax}}{\omega_c} = 23.8ms$. This means that we can only compensate to have $Pm = 45^\circ$ if the global time delay $\tau \leq 23.8ms$.

B/Dominant pole method

The closed loop transfer function of the control system is $F(s) = \frac{K(1+T_d s)e^{-\tau s}G(s)}{1+K(1+T_d s)e^{-\tau s}G(s)}$. By using an approximation Pade of the 1st order $e^{-\tau s} \approx \frac{-s+2/\tau}{s+2/\tau}$ and call $a = \frac{2}{\tau}$, we have:

$$F(s) = \frac{1000K(1+T_d s)(-s+a)}{b_0 s^3 + b_1 s^2 + b_2 s + b_3} \quad (2)$$

where $b_0 = 1$; $b_1 = 1 + a - 1000KT_d$; $b_2 = 1000Ka + a - 1000K$ and $b_3 = 1000Ka$.

The denominator is a third order function with polynomials, thus we will have three poles. Note that there are two zeros ($-\frac{1}{T_d}, \frac{2}{\tau}$) that get closer to the origin when the time delay increases.

The objective of the method is to make to appear in the denominator the two poles of the continuous process control application $p_{1,2} = R \pm jI$ (with $R = -11$ and $I = 24.5$) found in the subsection 2.1 and to see the condition which gives a negligible role for the third pole p_3 . Poles p_1 and p_2 are called the dominant poles.

The denominator can be written:

$$(s - p_1)(s - p_2)(s - p_3) = s^3 - (2R + p_3)s^2 + (2Rp_3 + R^2 + I^2)s - (R^2 + I^2)p_3$$

By identifying with the denominator of the equation (2), we obtain the values of p_3 , K and T_d :

$$\begin{cases} p_3 = -\frac{a^3 + (2+2R)a^2 - (R^2 + I^2)a}{a^2 - 2Ra + R^2 + I^2} \\ K = -\frac{(R^2 + I^2)p_3}{1000a} \\ T_d = \frac{1000a}{1000K + a + p_3 + 2R} \end{cases} \quad (3)$$

The condition for an insignificant pole p_3 : the pole is considered "insignificant" if the magnitude of the real part of this pole is at least 5 to 10 times that

of a dominant pole (see [3], page 281). Therefore $p_3 = -\frac{a^3 + (2+2R)a^2 - (R^2 + I^2)a}{a^2 - 2Ra + R^2 + I^2} \leq 5R \Rightarrow \tau < 40ms$.

Remark:

- The compensable maximum delays of the two methods (23.8ms and 40ms) are conditions to have expected specifications and will change if we want other specifications. They depend on the used method and on the specifications we want, thus they are different.
- The two methods require to change on-line the proportional gain K (formulas (1), (3)), that will change the static gain of the controller. However the steady state error $e_{ss} = 0 \forall K$ (Sec.2.1), hence we have no problem about the static gain when the gain K is modified.

3.3. Computation of the control signal u_k

The controller computes the control signal u_k (which includes the Proportional component P_k and the Derivate component D_k) by using the formula (4):

$$\begin{cases} P_k = Ke_k \\ D_k = \frac{T_d}{Nh+T_d}D_{k-1} + \frac{NKT_d}{Nh+T_d}(e_k - e_{k-1}) \\ u_k = P_k + D_k \end{cases} \quad (4)$$

where $e_k = r_k - y_k$, N is a constant ([1], page 307).

4. Application of the proposal

4.1 Context

We consider an implementation of four identical process control applications (denoted $P1, P2, P3, P4$) implemented on the same CAN network. The processes have different priorities, so they have different time delays. The goal of the consideration of several processes instead of only one process is to well see the impact of the proposal in Sec.3 on performances of processes which have different time delays.

The sensor tasks of the 4 processes are periodic ($h = 10$ ms) and synchronous. Call P_{sci} and P_{cai} the priorities of the flows f_{sc} and f_{ca} of Pi . The static priorities associated to the message flows of 4 processes are as follows: $P_{ca1} > P_{ca2} > P_{ca3} > P_{ca4} > P_{sc1} > P_{sc2} > P_{sc3} > P_{sc4}$. That means that Pi is considered more important than Pj with $i < j$.

Two cases of controller will be considered in order to well see the importance of the link (QoS \rightarrow QoC): either the controller is not changed with time delays, we say Fixed Controller (denoted Fix-Controller) or the controller is changed and adapted according to time delays, we say Adaptative Controller (denoted Adapt-Controller); this last case shows the interest of the link (QoS \rightarrow QoC).

Remark: the global time delay of the less important process ($P4$) is $4 \times (D_{sc} + D_{ca}) + \tau_{ZOH} = 10.12ms$, it is less than the maximal compensable time delays of the two methods (23.8ms and 40ms). Thus we can have the expected phase margin and poles.

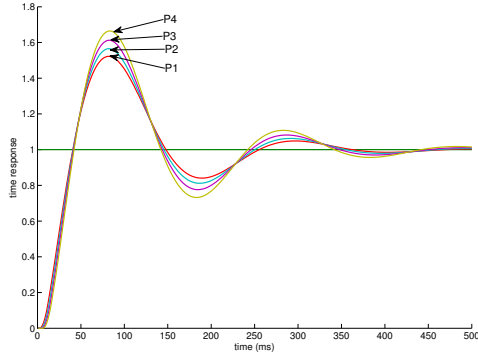


Figure 4. Fix-Controller.

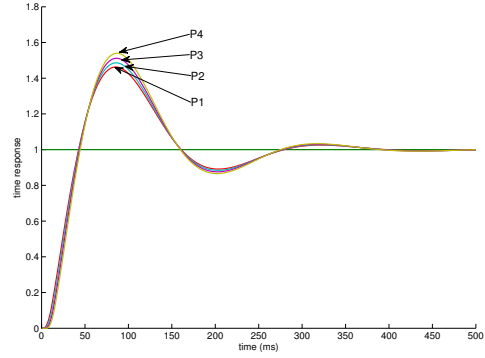


Figure 6. Adapt-Controller: dominant pole.

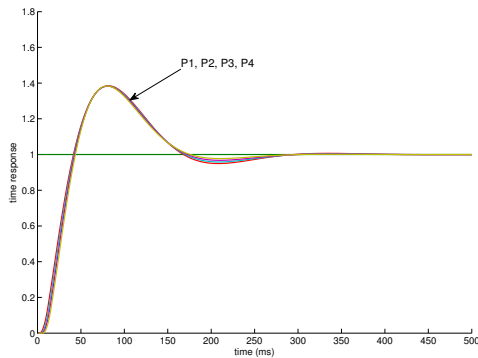


Figure 5. Adapt-Controller: phase margin.

4.2 Results

The time responses are represented on Fig.4 for the Fix-Controller and on Figs.5 and 6 for the Adapt-Controller respectively based on the phase margin method and the pole dominant method.

We see on Fig.4 the impact of the differences in the priorities which induce different time delays and then different overshoots. The process that has a higher priority has a better performance. P_4 is the less important, so it has the biggest time delay and that's why it has the highest overshoot.

We see on Fig.5 that the phase margin method compensates very well the time delays and then we have identical time responses for the 4 processes.

On Fig.6 we have not the identical time responses for the 4 processes with the dominant pole method. P_i is less good than P_j with $i > j$. That results from the effect of the zeros of the closed transfer function (Equ.2). The zeros get closer to the origin with time delays so that they induce a higher overshoot ([2], page 226). But we can see that the result in terms of overshoot is better than this of the Fix-Controller.

The phase margin method gives better results than the dominant pole design since it takes exactly into account for the phase shift of all poles and the zeros of the open loop transfer function.

5. Conclusion

This paper has shown the interest that the awareness on-line of the network QoS by the controller in a NCS can bring in terms of performances for process control applications.

Two methods for the modification on-line of the controller parameters, on the basis of the knowledge of the global time delay in the control loop, have been considered. The phase margin method gives excellent results showing its ability to compensate perfectly the time delays. The dominant pole method is less powerful than the phase margin method in this particular application because of the effect of zeros in the closed loop transfer function.

This work presents, in our opinion, an interesting and practical contribution to the link (QoS \rightarrow QoC). Future works will consider the bidirectional link (QoS \rightleftharpoons QoC) in order to achieve a more efficient NCS design.

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