# WWW-YES World Wide Workshop for Young Environmental Scientists



**Optimization of NaOH thermo-chemical** pretreatment process for enhancing solubilization of rice straw by Response Surface Methodology in order to prevention of water resource pollution

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# INTRODUCTION

Organic fraction of municipal solid wastes (OFMSW)

Readily biodegradable

Non- readily biodegradable

Readily biodegradable

Non- readily biodegradable 5-25% of the total waste mass)

such as starch and sucrose that can be easily bio degradation into the monosaccharide

such as lignocellulosic materials in a bioconversion process, pretreatment is necessary

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## **Thermo chemical pretreatment**

Alkaline thermochemical pretreatment process is a well know method that can be used to dissolving complex substrates before biological treatment by remove lignin and a part of the hemicelluloses, and efficiently increase the accessibility of enzyme to the cellulose

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#### **Main objectives**

Identification the optimum conditions for enhancing of rice straw dissolving by response surface methodology (RSM).

Determination of physicochemical property of rice straw

Simulation the cellulose solublization reaction by Equation

ability to produce maximum methane gas in anaerobic process

Maximum SCOD

minimum residual of un-compostable materials in compost process

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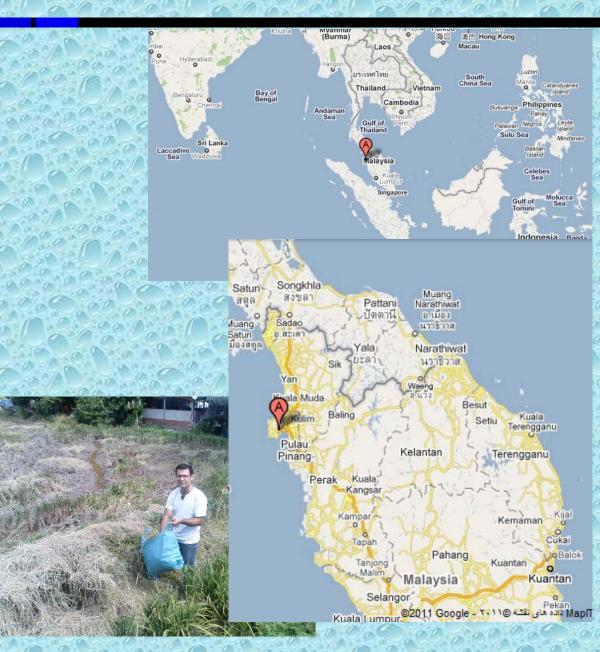
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Means

#### **Collection of sample**

Around 10 kg of rice straw was collected from local farm of Sungai Dua in Pulau Penanag

Firstly, rice straw was cut to 5-10cm length, washed thoroughly with tap water and then air-dried. It was then grinded to 2-3mm size and used for further treatment.



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### **Response surface methodology**

		Coded levels of variables				
Factor	variable	-1	-0.5	0	0.5	1
Temperature, °C	A	30	72.5	115	157	200
time, min.	В	10	52.5	95	137	180
NaOH Concentration, g/L	С	0	7.5	15	22.5	30

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# Rice Straw: before and after Hydrolysis process





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### **ANOVA** analysis for the quadratic model

Source	Sum of Squares	Degree of freedom (DF)	Mean Square	F Value	Prob > F	
Model	2.782E+008	9	1.513E+008	19.09	< 0.0001	significant
А	1.302E+008	1	2.782E+008	35.11	0.0001	
В	4.718E+008	1	1.302E+008	16.43	0.0023	
С	2.799E+007	1	4.718E+008	59.55	< 0.0001	
A2	8.495E+006	1	2.799E+007	3.53	0.0896	
B2	7.961E+007	1	8.495E+006	1.07	0.3248	
C2	5.787E+007	1	7.961E+007	10.05	0.0100	
AB	2.350E+008	1	5.787E+007	7.30	0.0222	
AC	9.853E+007	1	2.350E+008	29.66	0.0003	
BC	2.782E+008	1	9.853E+007	12.44	0.0055	
Residual	7.922E+007	1	7.922E+006			
Lack of Fit	7.904E+007	10	1.581E+007	429.82	< 0.0001	No significant
Pure Error	1.839E+005	5	36777.29			
Cor Total	1.441E+009	5	<b>R-Squared</b>	0.9450		
Std. Dev.	2814.65	19	Adj. R-Squared	0.8955		
Mean	8923.33		Pred. R- Squared	-0.6740		
Critical Value (C.V)	31.54		Adeq. Precision	19.568		
PRESS	2.412E+009		R-Squared	0.9450		

# **ANOVA** analysis

The value of "PNF" for the models is less than 0.05 to indicate that it is significant and desirable as it indicates that the terms in the model that have a significant effect on the response.

P-values lower than 0.01 indicates that the model is considered to be statistically significant at the 99% confidence level .

Values greater than 0.1000 indicate the model terms are not significant. Therefore, A, B, C, AB, AC and BC are significant model terms to affect the SCOD value

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## **Model fitting**

 $Y = 8217.91 + 5720.59 A + 3913.72 B + 7450.00 C -12246.72 A^{2} -6746.72 B^{2} + 20653.26 C^{2} + 2689.58 AB + 5419.79 AC + 3509.38 BC$ 

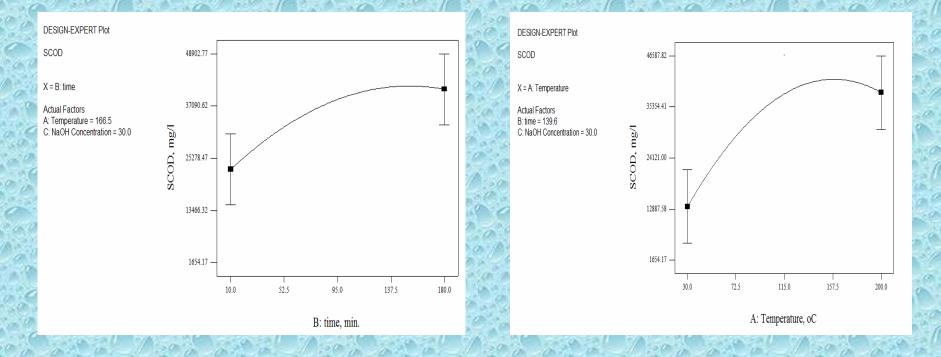
• The response functions are representing as the response for SCOD value, A as the coded value of variable temperature, B as the coded value of stirring time and C as the coded value of alkaline concentration

# **Effect of process** conditions

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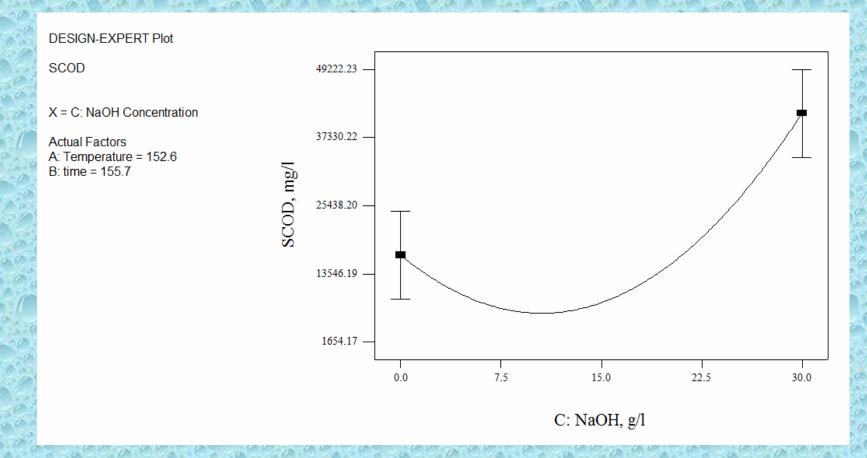
# Influence of stirring time on SCOD

### Influence of temperature and stirring time on SCOD



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# Influence of alkaline concentration on SCOD



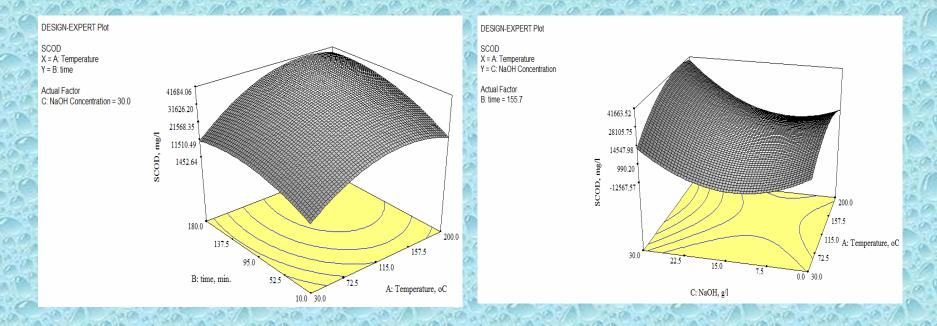
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### **Interactions between the** variables

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### Influence of temperature and stirring time on SCOD

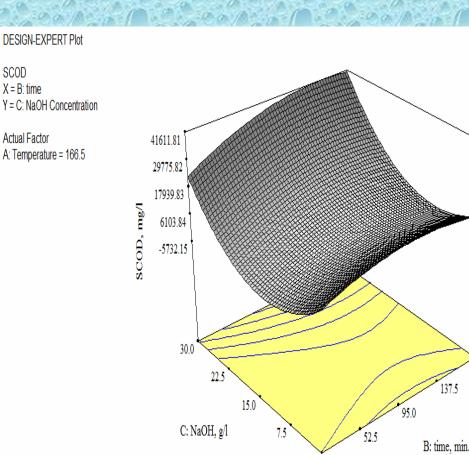
### Influence of NaOH concentration and stirring time on SCOD



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# Influence of stirring time and NaOH concentration on SCOD

By analyzing the Figure, it can be easily seen that at high NaOH concentration at fixed temperature 166.5 °C, the SCOD rises proportionally with stirring time. For example, at 30 g/l of NaOH, when the sample was subject to an alkaline thermochemical process stirring time increment of 180 min from 10 min., it consequently led to a proportional increase of SCOD to 41611.81 mg/l by approximately 17939.83 mg/l.



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### **Optimum conditions for maximum SCOD production**

No.	Temperature,	Time, min	NaOH, g/l	SCOD,	Desirability
	°C			mg/l	
1	157.6	133.1	29.9	41211	1.000
2	142.9	145.7	30.0	41204	1.000
3	166.6	164.2	30.0	41387	1.000
4	163.4	136.1	30.0	41422	1.000
5	173.8	142.8	30.0	41243	1.000
6	122.8	115.8	30.0	38712	0.937
7	116.4	97.8	0.0	21430	0.500
8	116.8	98.6	0.0	21429	0.500
9	122.8	108.9	0.0	21273	0.496

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# CONCLUSION

•A well dissolving of cellulosic compounds in rice straw is achieved by alkaline thermochemical hydrolysis.

•Alkaline thermochemical hydrolysis process leads to the increasing of transformation of non-solution complex cellulosic compounds to soluble simple compounds.

•The mathematical model developed could predict the SCOD yield at any point in the experimental domain as well as the determination of the optimal solubilization conditions with sufficient degree of accuracy

•The effect of alkaline and the thermochemical hydrolysis conditions to achieve an optimal response with 41211 mg/l of SCOD value were found to be 157.6 °C for the reaction temperature, 133.1 min for the stirring time and 29.9 g/l for the NaOH concentration.

•These results proved that alkaline thermochemical pretreatment was highly potential for increasing the SCOD value of rice straw and the use of RSM based on CCD was practical for the simultaneous study of effects by process variables on the SCOD value and the possible interaction between them

•Also from the results, a process for the production of biogas or compost from organic solid waste shall have two main stages. The two-stage design must involve alkaline pretreatment, followed by anaerobic digestion or composting process unit. In this situation the rejected and risk of water and soil resource waste will be decreased to minimum

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