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## Sucrose phosphorylase as cross-linked enzyme aggregate: Improved thermal stability for industrial applications

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### Keywords

CLEA, sucrose phosphorylase, thermostability, enzyme immobilization, biocatalysis

### Abbreviations

SPase: sucrose phosphorylase; G1P:  $\alpha$ -glucose-1-phosphate; GA: glutaraldehyde;

CLEA: cross-linked enzyme aggregate

## Abstract

Sucrose phosphorylase is an interesting biocatalyst that can glycosylate a variety of small molecules using sucrose as a cheap but efficient donor substrate. The low thermostability of the enzyme, however, limits its industrial applications, as these are preferably performed at 60 °C to avoid microbial contamination. Cross-linked enzyme aggregates (CLEAs) of the sucrose phosphorylase from *Bifidobacterium adolescentis* were found to have a temperature optimum that is 17 °C higher than that of the soluble enzyme. Furthermore, the immobilized enzyme displays an exceptional thermostability, retaining all of its activity after one week incubation at 60 °C. Recycling of the biocatalyst allows its use in at least ten consecutive reactions, which should dramatically increase the commercial potential of its glycosylating activity.

## 1. Introduction

Enzymes are powerful biocatalysts that find increasing applications in various industrial processes. The major advantages of the use of enzymes for chemical transformations are their high chemo-, regio- and stereospecificity, as well as their environmentally friendly properties. Unfortunately, natural enzymes are often not optimally suited for industrial applications, which can be hampered by their lack of long-term stability under process conditions and by their difficult recovery and recycling. These drawbacks can, however, be overcome by immobilization of the enzymes [1-4].

Cross-linked enzyme aggregates (CLEAs) have emerged as a novel class of immobilized biocatalysts for use in both aqueous and non-aqueous environments [5]. Such preparations are obtained by the physical aggregation of the enzymes followed by chemical cross-linking (Fig. 1). This procedure allows enzymes to be immobilized without the use of a carrier, which not only decreases the cost but also avoids “dilution” of the enzymes’ activity [6]. CLEAs share their beneficial properties with cross-linked enzyme crystals (CLECs) but do not require tedious crystallization procedures [7, 8].

Sucrose phosphorylase (SPase) catalyses the reversible phosphorolysis of sucrose into  $\alpha$ -D-glucose-1-phosphate (G1P) and fructose. This enzyme is mainly found in lactic acid bacteria and bifidobacteria, where it contributes to an efficient energy metabolism [9]. SPase is formally classified as a glycosyl transferase (EC 2.4.1.7),

although it belongs to glycoside hydrolase family 13 [10] and follows the typical double displacement mechanism of retaining glycosidases [11]. The crystal structure of the enzyme from *Bifidobacterium adolescentis* has been determined and consists of a  $(\beta/\alpha)_8$  barrel containing two carboxylic amino acids as catalytic residues [12].

A number of practical applications have been developed for SPase [13, 14]. The enzyme has long been used for the production of G1P, an efficient donor for chemical and enzymatic glycosylation reactions [15]. Furthermore, SPase can also transfer a glucosyl group to different carbohydrate and non-carbohydrate acceptors thanks to its broad substrate specificity [16, 17]. Goedl *et al.*, for example, have developed an exceptionally efficient and selective process for the production of glyceryl  $\alpha$ -D-glucoside, a moisturizing agent for cosmetics that is marketed under the tradename Glycoin® [18, 19].

Unfortunately, no SPases have so far been reported that can resist the extreme process conditions that are preferred by the industry. Indeed, carbohydrate conversions are typically performed at elevated temperatures (60 °C or higher), mainly to avoid microbial contamination [20-22]. Here, we describe the production of CLEAs of the SPase from *B. adolescentis* that display exceptional thermal and operational stability.

→ Fig. 1

## 2. Materials and methods

### 2.1. Materials

*Tert*-butyl alcohol, glutaraldehyde, and sodium borohydride were purchased from Aldrich-Chemie, Fisher and Acros, respectively. All other reagents were purchased from Sigma-Aldrich.

### 2.2. Enzyme production

The SPase gene from *B. adolescentis* LMG 10502 was recombinantly expressed in *E. coli* XL10-Gold, under control of the constitutive promotor P34 [23]. The construction of the corresponding expression vector pCXhP34\_SPBa will be described elsewhere. Transformed cells were cultivated in 1 l shake flasks at 37 °C using LB medium supplemented with 100 mg l<sup>-1</sup> ampicillin. After 8 h of expression, the cells were harvested by centrifugation (7000 rpm, 4 °C, 20 min). Crude enzyme preparations were prepared by enzymatic lysis of frozen pellets using the EasyLyse Bacterial Protein Extraction Solution (Epicentre). Cell debris was removed by centrifugation (12000 rpm, 4 °C, 30 min). The crude enzyme preparation was heat purified by incubation at 60 °C for 60 min. Denaturated proteins were removed by centrifugation (12000 rpm, 4 °C, 15 min).

### 2.3. CLEAs production

Aggregates of SPase were prepared by adding 6 ml of *tert*-butyl alcohol under agitation to 4 ml of heat-purified SP enzyme (1.2 mg ml<sup>-1</sup>) at pH 7. After 30 min, varying amounts of a 25 % (v/v) glutaraldehyde solution were added to cross-link

the enzyme aggregate, and the mixture was kept under stirring for 15, 30, 60 or 120 min. Reduction of the formed imine bond was achieved by adding 10 ml of a solution containing 1 mg ml<sup>-1</sup> sodium borohydride in 0.1 M sodium bicarbonate buffer at pH 10. After 15 min, another 10 ml was added and allowed to react for 15 min. Finally, the CLEAs were separated by centrifugation (15 min at 12000 rpm) and washed five times with 0.1 M phosphate buffer at pH 7. All the steps were performed in a thermoshaker (Eppendorf) at 750 rpm and 4 °C. The immobilization yield is defined as the ratio of the activity detected in the CLEA preparation and that present in the original enzyme solution.

#### 2.4. Activity assays

The phosphorolytic activity of SPase was determined by measuring the release of the reducing sugar fructose from the non-reducing substrate sucrose with the bicinchonic acid (BCA) method [24]. The reactions were analysed in a discontinuous way, by inactivation samples (5 min at 95 °C) at regular intervals. One unit (U) of SPase activity corresponds to the release of 1 µmole fructose from 100 mM sucrose in 100 mM phosphate buffer at pH 7 and 37 °C. To determine phosphatase activity, the samples were also analysed for the release of glucose (from the α-glucose-1-phosphate generated by SPase) with the glucose oxidase / peroxidase assay [25]. One unit (U) of phosphatase activity corresponds to the release of 1 µmole of glucose from 100 mM sucrose in 100 mM phosphate buffer at pH 7 and 37 °C. When phosphatase activity was detected, this was subtracted from the values obtained by the BCA-method to calculate the net SPase activity.



The protein concentration was measured with the Protein Assay kit from Pierce, using bovine serum albumin as standard.

### 2.5. Stability assays

To determine the thermostability of SPase, soluble or immobilized enzyme was incubated in 100 mM phosphate buffer pH 7 in a water bath at 60 °C. At regular intervals, samples were inactivated and the residual activity was analysed using the BCA method. To evaluate the reusability of SPase CLEAs, the biocatalyst was used for several reaction cycles of 1 h at 60 °C. The enzyme was recuperated by centrifugation (15 min at 12000 rpm) and washed five times with 0.1 M phosphate buffer at pH 7.

## 3. Results and discussion

### 3.1. Production and purification of SPase

The SPase gene from *B. adolescentis* LMG 10502 was recombinantly expressed in *E. coli* XL10-Gold. After chemo-enzymatic cell lysis, a crude enzyme preparation was obtained with a specific SPase activity of approximately 13 U mg<sup>-1</sup> at 37 °C. As the SPase is more stable than most endogenous *E. coli* proteins, the enzyme could be partially purified by means of heat treatment (Table 1). In this way, all phosphatase activity was removed, which would otherwise degrade the  $\alpha$ -glucose-1-phosphate (G1P) produced by SPase.

After 1 hour incubation at 60 °C, the specific activity increases to 29 U mg<sup>-1</sup> and the concentration of soluble protein drops from 2.6 to 1.2 mg ml<sup>-1</sup>. The latter is completely due to the loss of contaminating proteins, as no decrease in SPase activity is observed under these conditions. Longer incubation times do not result in a further increase in specific activity. Although the final enzyme preparation is estimated to be only 20 % pure, as judged by SDS-PAGE (not shown), a higher level of purity is not required for most applications and would probably not be economical at an industrial scale.

→ table 1

### 3.2. Production of SPase CLEAs

The first step in the preparation of CLEAs consists of the aggregation of the enzymes, which can be achieved by the addition of salts, organic solvents or non-ionic polymers [5]. The choice of the additive is important, because it can result in enzymes with slightly different three-dimensional structures. Ammonium sulfate is the most widely used precipitant for protein purification, but gave unsatisfactory results with SPase. High concentrations of the salt are required (~70 % w/v) to aggregate this enzyme and generate a gelatinous suspension that is difficult to centrifuge. Precipitation was, therefore, performed with *tert*-butanol instead. A solvent concentration of 60 % (v/v) resulted in complete removal of SPase activity from the supernatant after centrifugation. The precipitate could be redissolved in phosphate buffer without loss of activity, indicating that the aggregation procedure does not damage the structural integrity of the protein.

In the second step, the aggregated enzyme molecules are chemically cross-linked to obtain an immobilised biocatalyst. Glutaraldehyde (GA) is generally used for that purpose, as it contains two aldehyde groups that can form imine bonds with lysine residues from two enzyme molecules (Fig. 1). It is well known that the immobilization yield strongly depends on the incubation time of the cross-linking step as well as on the GA / protein ratio [26]. These parameters have, therefore, been optimized for the production of CLEAs of SPase (Fig. 2). A maximal immobilization yield of 31 % could be achieved at a GA / protein ratio of 0.17 mg mg<sup>-1</sup> and an incubation time of 1 hour. Higher ratios and longer incubation times result in a considerable reduction in catalytic activity, most likely because glutaraldehyde then starts to react with residues in the active site. Indeed, this problem can sometimes be avoided by the use of polymeric cross-linkers that are too large to access the active site [27], but these have not been tested in this work. Even under optimal conditions, the activity recovered in the CLEA preparation is lower than that of the free SPase, which means that diffusion limitations are operative and/or that the catalytic site has undergone some kind of distortion.

→ Fig 2

### 3.3. Characterization of SPase CLEAs

Many studies have shown that the activity and stability of an immobilized enzyme can differ considerably from that of its soluble counterpart [28, 29]. Therefore, the properties of the CLEAs were compared with those of the native SPase. The

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6 optimal pH and temperature for phosphorolytic activity of the immobilized  
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8 enzyme were found to be 6.0 and 75 °C, compared to 6.5 and 58 °C, respectively,  
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10 for the soluble enzyme (Fig. 3 and Fig. 4). Cross-linking thus results in an enzyme  
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12 whose temperature optimum has increased with an impressive 17 °C.  
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14 Furthermore, the immobilized enzyme is active in a broader pH-range, indicating  
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16 a higher operational stability.  
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20 → Fig 3 & 4  
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24 To determine the thermostability of the SPase preparation, the enzyme was  
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26 incubated at 60 °C and its residual activity was measured at several points in time.  
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28 The CLEAs were found to retain full activity after 1 week incubation, whereas the  
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30 free enzyme loses 20 % of its activity after only 16 h incubation. The stability of  
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32 the biocatalyst is, therefore, dramatically improved by the cross-linking process.  
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34 As industrial carbohydrate conversions are preferably performed at 60 °C, the  
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36 properties of these CLEAs will undoubtedly allow the development of novel  
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38 processes of high economic value.  
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45 One of the major advantages of immobilization is that it leads to an enzyme  
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47 preparation that can be recycled, which often is a key determinant of its industrial  
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49 potential. CLEAs can be easily recycled by either filtration or centrifugation [6],  
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51 and the latter strategy has been used in our experiments. Centrifugation at high  
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53 speeds (12000 rpm) was found to be required for the precipitation of CLEAs and  
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55 the complete removal of phosphorolytic activity from the supernatant. To evaluate  
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the mechanical stability of the biocatalyst under these conditions, several reaction cycles of 1h at 60 °C were performed with thorough washing in between. After ten cycles, no loss of activity could be detected, revealing the excellent operational stability of the new enzyme preparation.

### 3.4. Production of G1P with SPase CLEAs

To evaluate the efficiency of the SPase CLEAs in a production process, the phosphorolysis of sucrose into G1P was monitored at 60 °C and pH 7 until maximal conversion. The reaction was performed with 500 U of CLEAs in a solution containing 1 M of sucrose and inorganic phosphate. After about 20 h, the conversion was finished and 0.7 M G1P was produced. This corresponds to an equilibrium constant ( $K_{eq}$ ) of 5.63, which is lower than the value previously determined at 30°C [15].

In view of the exceptional mechanical and thermal stability of the CLEAs, it should be possible to repeat this reaction at least seven times in one week time. In that way, more than 1 kg of G1P would be produced with only about 50 mg of protein, which still would be fully active. This is the first report on a production process with SPase at elevated temperatures.

## 4. Concluding remarks

In this work, the preparation of cross-linked enzyme aggregates was found to be a simple but efficient strategy to increase the thermostability of the sucrose

phosphorylase from *Bifidobacterium adolescentis*. These CLEAs remain fully active after one week incubation at 60 °C and can be recycled at least ten times for the repeated conversion of sucrose into  $\alpha$ -glucose-1-phosphate. This low-cost and easy procedure should allow the development of industrial processes to exploit the different glycosylation reactions catalyzed by sucrose phosphorylase.

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The authors have declared no conflict of interest.

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**Table 1 Heat purification of SPase from *B. adolescentis***

Incubation at 60 °C	SPase activity	Phosphatase activity	Protein concentration	Specific activity
(min)	(U/ml)	(U/ml)	(mg/ml)	(U/mg)
0	35.1	2.7	2.6	13.5
20	35.2	0.7	1.6	22.0
40	35.0	0.0	1.5	23.3
60	35.1	0.0	1.2	29.3
90	35.0	0.0	1.2	29.2

Assays were performed at 37 °C using 100 mM sucrose in 100 mM phosphate buffer pH 7 as substrate. SPase activity corresponds to the release of fructose, while phosphatase activity corresponds to the release of glucose (from the  $\alpha$ -glucose-1-phosphate formed by SPase).

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**Figure legends**

Fig. 1 General scheme for the production of cross-linked enzyme aggregates (CLEAs).

Fig. 2 The effect of the cross-linking ratio (●) and reaction time (○) on the immobilization yield of SPase from *B. adolescentis*. The immobilization yield is defined as the ratio of the activity detected in the CLEA preparation and that present in the original enzyme solution.

Fig. 3 The effect of pH on the activity of soluble (○) and immobilized (●) SPase from *B. adolescentis*. Reactions were performed with 0.1 M sucrose in a 0.1 M phosphate buffer at 37 °C.

Fig. 4 The effect of temperature on the activity of soluble (○) and immobilized (●) SPase from *B. adolescentis*. Reactions were performed with 0.1 M sucrose in a 0.1 M phosphate buffer at pH 7.

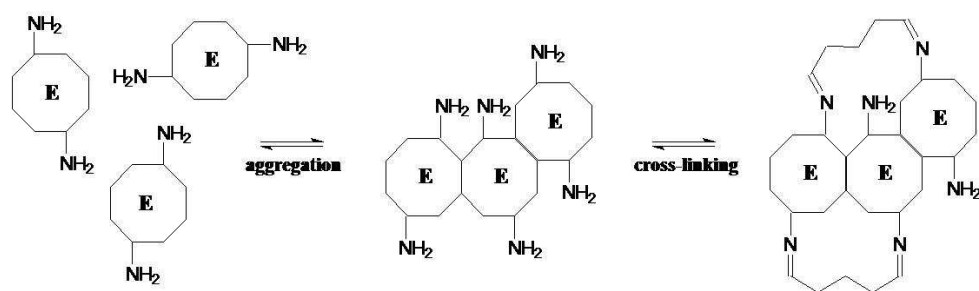


Fig. 1 General scheme for the production of cross-linked enzyme aggregates (CLEAs).  
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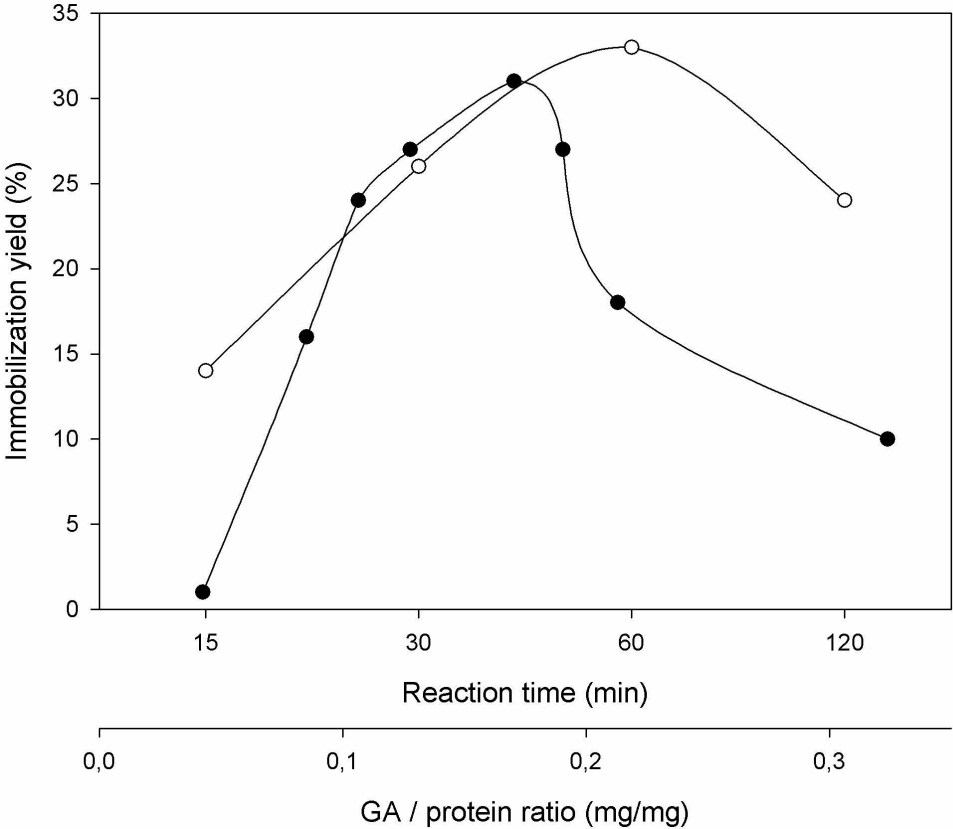


Fig. 2 The effect of the cross-linking ratio (●) and reaction time (○) on the immobilization yield of SPase from *B. adolescentis*. The immobilization yield is defined as the ratio of the activity detected in the CLEA preparation and that present in the original enzyme solution.  
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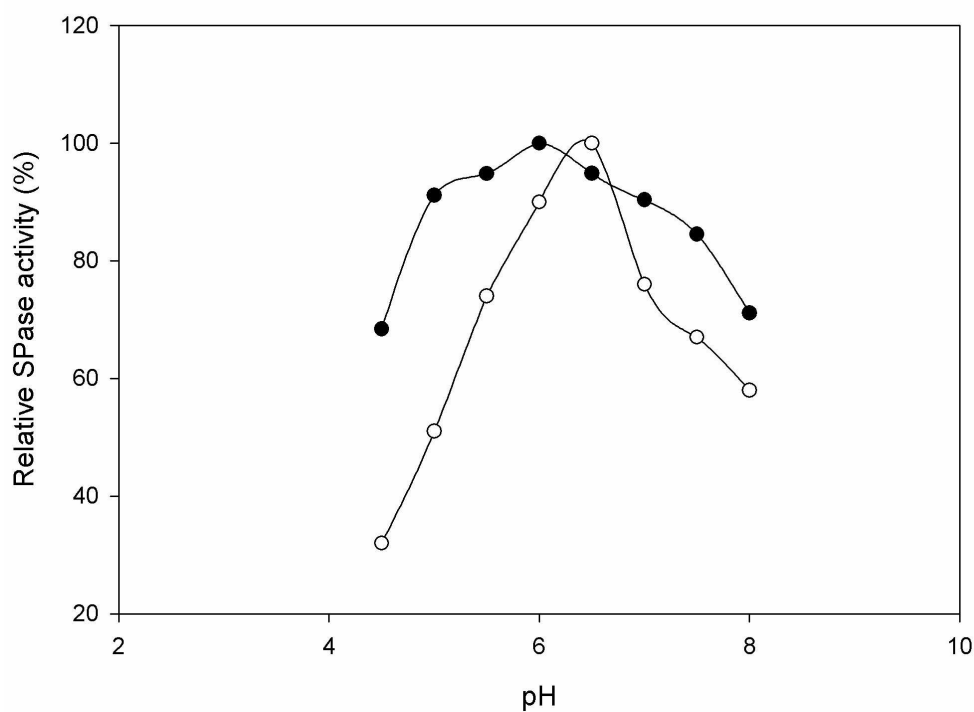


Fig. 3 The effect of pH on the activity of soluble (○) and immobilized (●) SPase from *B. adolescentis*. Reactions were performed with 0.1 M sucrose in a 0.1 M phosphate buffer at 37 °C.

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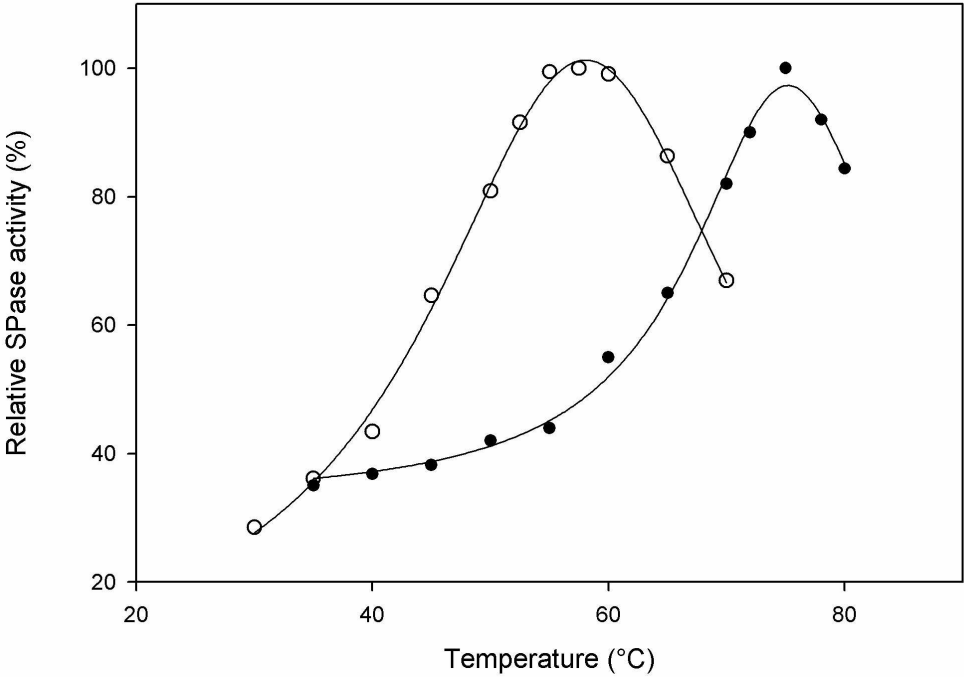


Fig. 4 The effect of temperature on the activity of soluble (○) and immobilized (●) SPase from *B. adolescentis*. Reactions were performed with 0.1 M sucrose in a 0.1 M phosphate buffer at pH 7.