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Water-in-ionic liquid microemulsion-based organogels as novel matrices for enzyme immobilization

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List of abbreviations

[bmim]BF₄: 1-butyl-3-methyl imidazolium tetrafluoroborate

[bmim]PF₆; 1-butyl-3-methyl imidazolium hexafluorophosphate

ATR: attenuated total reflectance

AOT: bis-(2-ethylhexyl) sulfosuccinate sodium salt

CalB: Candida antarctica lipase B

- Cvl: Chromobacterium viscosum lipase
- FT-IR: Fourier-transform infrared spectroscopy
- HPMC: (hydroxypropyl)methyl cellulose

IL: ionic liquid

MBGs: microemulsion-based organogels

Tween 20: Polyethylene glycol sorbitan monolaurate

- w/IL: water-in-ionic liquid
- w/o: water-in-oil

Abstract

The use of water-in-ionic liquid microemulsion-based organogels (w/IL MBGs) as novel supports for the immobilization of lipase B from Candida antarctica and lipase from Chromobacterium viscosum was investigated. These novel lipase-containing w/IL MBGs can be effectively used as solid phase biocatalysts in various polar and non-polar organic solvents or ionic liquids, exhibiting up to 4.4-fold higher esterification activity compared to water-in-oil microemulsion-based organogels. The immobilized lipases retain their activity for several hours at 70°C, while their half life time is up to 25-fold higher compared to that observed in w/IL microemulsions. Fourier transform infrared spectroscopy data indicate that immobilized lipases adopt a more rigid structure, referring to the structure in aqueous solution, which is in correlation with their enhanced catalytic behaviour observed.

1. INTRODUCTION

Water-in-oil (w/o) microemulsions, also known as reverse micelles, have been widely reviewed as tool for achieving various enzymatic reactions in hydrophobic solvents [1-3]. These microheterogeneous media consist of aqueous nanodroplets dispersed in a non-polar organic phase stabilized by surfactants. Enzymes maintain their catalytic activity when hosted in these aqueous nanodroplets, catalyzing both synthetic and hydrolytic reactions [3, 4]. Reverse micelles have been associated with the idea of micro-reactors for enzymatic reactions, when substrates and/or products are lipophilic and low water content is desired [1, 2].

Interestingly, w/o microemulsions can be "gelled" by the addition of biopolymers, such as gelatin or cellulose derivatives, yielding a matrix suitable for enzyme immobilization [5-8]. The immobilization procedure can affect the catalytic behaviour of the entrapped enzymes, in terms of reaction rate, selectivity and stability, improving the catalytic performance of the immobilized enzymes [9]. The enzymes immobilized into microemulsion-based organogels (MBGs) retain their catalytic activity in several organic media, and therefore can be used for various biotransformations involving synthetic or natural substrates [5, 8, 10, 11]. Moreover, these enzyme-containing organogels overcome to a great extent the major problems which must be solved for the employment of a microemulsion system in industrial processes; most notably, the recovery of the products and the regeneration of the biocatalyst.

Nowadays, environmental demands necessitate the development of new type of green solvents and innovations towards more sustainable enzymatic processes. Room temperature ionic liquids (ILs), because of their specific physicochemical characteristics and their ability to dissolve compounds of different polarities, have

Biotechnology Journal

shown great potential as an attractive alternative to conventional organic solvents, in catalytic processes on both a laboratory and industrial scale. Recently the formation of nano/micrometer-sized water droplets in ionic liquid continuous phase stabilized by suitable surfactant (noted as w/IL microemulsions) was reported [12, 13]. These new IL-based microemulsion systems combine the advantages of the ILs and those of the organized nano-structure media and could be used as a novel "green" media for biocatalytic reactions [14-16]. In a previous work we showed that w/IL microemulsions formulated with Tween 20 and the hydrophobic ionic liquid [bmim]PF₆ can be used for efficient entrapment of lipases [15]. Lipases entrapped in these microheterogeneous systems exhibit high synthetic activity and significantly high thermal and operational stability [15].

In the present study we report the formation of MBGs formulated with w/IL microemulsions and a biocompatible polymer such as (hydroxypropyl)methyl cellulose (HPMC) and we investigate the application of these novel organogels as solid supports for enzyme immobilization. The biocatalytic behaviour and the stability of two commercial lipases, namely lipase B from *Candida antarctica* (CalB) and lipase from *Chromobacterium viscosum* (Cvl), was investigated and compared to that observed either in w/o MBGs, or in w/IL microemulsions. Lipases used in the present work are widely employed in various biocatalytic processes [8, 20-22]. Their catalytic behavior has been reported to differ, resulting from structural differences; Cvl has a well-formed lid and presents interfacial activation, acting as a typical lipase, while CalB has a very small lid and doesn't exhibit interfacial activation [23-27]. Particular attention has been focused on the factors that affect the immobilized enzyme's stability, as this is a critical factor when considering practical applications of the immobilized enzymes in biocatalytic processes. Moreover, Fourier transform-infrared

(FT-IR) spectroscopy was employed to investigate possible changes in enzyme structure upon immobilization and correlate with the biocatalytic behaviour of the immobilized enzymes.

2. MATERIALS AND METHODS

2.1. Materials

Lipases from *Candida antarctica* (lipase B, CalB), *Chromobacterium viscosum* (Cvl), *Candida rugosa* and *Rhizomucor miehei* were purchased from Fluka. Novozyme TL 100 L (*Thermomyces lanuginosa* lipase) was a generous gift from Novozymes. The ionic liquid 1-butyl-3-methylimidazolium hexafluorophosphate ([bmim]PF₆) was purchased from Alfa Aesar. Tween 20 (Polyethylene glycol sorbitan monolaurate) and 1-butyl-3-methylimidazolium tetrafluoroborate ([bmim]BF₄) were purchased from Fluka. (Hydroxypropyl)methyl cellulose (HPMC, 80-120 cP) and bis-(2-ethylhexyl) sulfosuccinate sodium salt (AOT) were purchased from Sigma. All other reagents were of analytical grade. The aqueous lipase solutions were prepared by dissolving lipase in 25 mM Tris-HCl buffer (pH 7.5).

2.2. Preparation of microemulsions and MBGs

In all cases a 25 mM Tris/HCl pH 7.5 buffer solution was used as aqueous phase. All microemulsion systems were prepared as described elsewhere [13]. The water-in-oil (w/o) microemulsions were prepared by adding appropriate amount of lipase in a 0.1 M AOT solution in isooctane with final molar hydration ratio w_0 ($w_0 = [H_2O]/[surfactant])$ equal to 10. Preliminary results showed that at $w_0 = 10$ immobilized lipases exhibit high activity and stability (data not shown). The w/IL

Biotechnology Journal

microemulsions were prepared by mixing buffer solution, Tween 20 and [bmim] PF_6 (35:50:15 weight ratio, except otherwise described).

The MBGs were prepared by introducing appropriate amount of w/o or w/IL microemulsion containing lipase to a second solution of HPMC in water. In a typical immobilization procedure, 1 ml of microemulsion containing 190 μ g of CalB or 200 μ g of Cvl was gelled with 1 g of HPMC and 2 ml of water at 30°C. Mixtures were vigorously shaken and stirred until homogeneous. Then, the organogel was overlaid on a glass surface and incubated for 3 hours at 30 °C to yield the MBG. The preparations were cut in small pieces of diameter from 0.2 to 0.5mm, washed twice with *n*-hexane, air-dried and stored at 4 °C until used.

2.3. Lipase-catalyzed esterification reactions

The lipase-containing MBGs were used in various organic solvents and in ionic liquids to catalyze a model reaction such as the esterification of lauric acid (0.1 M) with 1-butanol (0.2 M). Lipase-catalyzed reactions took place in capped vials placed in an orbital shaker at 30 °C at 200 rpm, with 100 mg of MBG per 1 ml of organic solvent or ionic liquid. At fixed time intervals aliquots were withdrawn (extracted with equal volume of *n*-hexane when ionic liquid was used as reaction medium) and were analyzed for ester content by gas chromatography (GC), using *n*-decane as internal standard. All experiments were carried out in triplicate.

Gas chromatography analysis was performed by a Shimatzu GC 17A device (Tokyo, Japan), which was equipped with a β -DEXTM 120, fused silica capillary column (30m x 0.25mm x 0.25µm film thickness, Supelco) and a Flame Ionization Detector with helium as the carrier gas in a similar manner as described elsewhere [15].

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2.4. Stability of free and immobilized lipases

The thermal and operational stability of CalB and Cvl immobilized in w/IL MBGs was investigated and compared to that observed in water and in w/IL microemulsions. The stability of the immobilized lipases was determined in isooctane over a 7 day period at temperatures up to 70 °C in the absence of substrates. After incubation, samples were withdrawn at regular time intervals in order to measure the remaining enzyme activity by monitoring the butyl laurate synthesis at 30 °C by GC, as described in Section 2.3. The stability of lipases in aqueous solution and w/IL microemulsions was monitored as described elsewhere [15].

The experimental results were elaborated with the series type deactivation model introduced by Henley and Sadana [28] ($E^{-\frac{k_1}{1}} \rightarrow E_1^{a_1} \xrightarrow{k_2} E_2^{a_2}$), where E, E₁ and E₂ are the three enzyme states having different specific activities, the parameters α_l and α_2 are the ratio of specific activities E₁/E and E₂/E respectively, and k_1 and k_2 are firstorder deactivation rate coefficients, respectively for E \rightarrow E₁ and E₁ \rightarrow E₂ steps.

The non-linear Levenberg-Marquadt regression method was applied to fit the residual activity data. In all cases, a good correlation between the experimental and the predicted values was found (correlation coefficient r > 0.950). The Newton-Raphson method was used to calculate the half-life times ($t_{1/2}$) from the two-step deactivation equation [28], using the parameter values calculated from the experimental data.

2.5. Structural Studies

IR spectra were measured using a Shimadzu FT-IR 8400 spectrometer (Tokyo, Japan) equipped with a deuterated triglycine sulfate detector, in the region of 4000-700 cm⁻¹. The spectrum acquisition (liquid samples were overlaid on a zinc selenide

attenuated total reflectance accessory, immobilized enzymes were measured as 2 % wt. KBr pellets), the data analysis of the amide I region and the band assignment were performed as described in previous work [15]. The data were manipulated using WinSpec software (LISE-Faculte's Universitaires Notre-Dame de la Paix, Namur, Belgium).

3. RESULTS AND DISCUSSION

3.1. Formation of w/IL MBGs containing lipase

In the present work we studied the formation of w/IL microemulsions-based organogels (MBGs) formulated with a biocompatible polymer such as (hydroxypropyl)methyl cellulose (HPMC) and we investigated the suitability of these novel MBGs as matrices for enzymes immobilization. It was found that MBGs can be formed with various w/IL microemulsions composed of [bmim]PF₆, Tween 20 and water, as described in our previous work [15]. HPMC forms w/IL MBGs with mass fraction of HPMC in the gels from 0.137 to 0.322 (prior to the drying step). It must be noted that MBGs formed at the above concentration range of HPMC were stable and maintained their structural integrity for several months at room temperature. Figure 1 shows the effect of the mass fraction of HPMC in the gels on the reaction rate and conversion yield of the esterification of 1-butanol with lauric acid catalyzed by w/IL MBGs containing lipase B from Candida antarctica (CalB) in n-hexane. As can be seen, the higher synthetic activity of the immobilized enzyme was observed in MBGs with mass fraction of HPMC in the gels 0.240. Similar catalytic behaviour was observed from Cvl immobilized in w/IL MBGs (data not shown). This mass fraction was used in all cases studied in this work.

As it can be seen from Table 1, various microbial lipases immobilized in w/IL MBGs exhibited up to 4.4-fold higher activity for the synthesis of butyl laurate compared to that observed in w/o MBGs at the same reaction conditions. Similar catalytic behaviour was observed for the esterification of fatty acids of different carbon chain length (C_8 - C_{18}) with various primary alcohols (C_1 - C_8) (data not shown). It is interesting to note that the esterification activity of CalB and Cvl immobilized in these novel w/IL MBGs was found to be up to 7 times higher than this observed when enzymes are immobilized in HPMC hydrogels, indicating that the presence of w/IL microemulsions is crucial for the preservation of the enzyme activity during the immobilization procedure. The hydrophobic ionic liquid used in the immobilization procedure could increase the accessibility of the hydrophobic reactants in the enzyme's microenvironment, resulting in higher esterification activity [29, 30].

The highest enzyme concentration that can be achieved in w/IL MBGs is about 2.5mg/g, significantly higher than that reported for MBGs formulated with w/o microemulsions [5, 6]. This difference can be attributed to the larger aqueous phase of w/IL microemulsions compared to these of w/o microemulsions, in which higher amount of enzyme can be solubilized [5, 15]. Moreover, the esterification rate linearly increases as the amount of lipase in the w/IL MBGs increases up to 0.8 mg/g. However, at higher enzyme concentration, the dependence of the reaction rate on the enzyme concentration is not linear, probably due to mass transfer limitations, as described for other MBGs [11].

3.2. Effect of system composition on lipase activity

The effect of the composition of the microemulsion used for the formation of w/IL MBGs on the esterification activity of the immobilized CalB is presented in Table 2. When the water content is constant (5% w/w), the activity of the immobilized

Biotechnology Journal

lipase increases as the surfactant concentration increases. Similar catalytic behaviour was observed in w/o MBGs [6]. An increase in surfactant concentration at constant water content leads to increase of the number of microdroplets formed, which probably facilitates the dispersion of enzyme in the gel matrix. On the other hand, at constant surfactant concentration (50% w/w), the enzyme activity strongly depends on the water content of the w/IL microemulsion system. In this case, the highest lipase activity was observed at a molar ratio of water to surfactant (w_o) around 14. This value is significantly lower than this reported for other w/o MBGs [6, 31-33]. This difference could be attributed to the fact that lipases entrapped in w/IL microemulsions exhibit their maximum catalytic activity in significantly lower w_o values than those observed in other w/o microemulsions [15].

3.3. Effect of the reaction medium on lipase activity

It is well established that the nature of the reaction medium significantly affects the catalytic behaviour of the immobilized enzymes and, in some extent, the structure of the matrix. In previous studies it was reported that polar solvents (such as acetone) affect the rigidity of w/o MBGs, leading to loss of incorporated surfactant and to deactivation of immobilized enzyme [5]. In the present study the influence of the reaction medium on the esterification activity of lipases immobilized in w/o and in w/IL MBGs was studied using various polar and non-polar organic solvents and ionic liquids as reaction medium. As it was found, w/IL and w/o MBGs maintained their structural integrity in all solvents tested after incubation for several days at 30 °C. As it can be seen in Table 3, the catalytic behaviour of both lipases immobilized in w/IL MBGs depends significantly on the reaction medium. High esterification activity was observed in non-polar organic solvents such as *n*-hexane and isooctane which is in accordance to that reported previously for MBGs formulated with AOT or lecithin

microemulsions [5]. Moreover, lipases immobilized in these novel w/IL MBGs keep their activity in solvent free systems (1-butanol was used as substrate and reaction medium) as well as in polar organic solvents (acetone, acetonitrile). Interestingly, both lipases immobilized in w/IL MBGs exhibited their highest esterification activity in [bmim]PF₆. On the other hand, the activity of CalB immobilized in w/o MBGs was very low in both ionic liquids used, indicating that the entrapment of the lipase in w/IL microemulsions prior the immobilization process significantly improves its activity in such media.

3.4. Effect of incubation temperature on lipase activity

The effect of the temperature on the esterification activity of lipases immobilized in w/IL MBGs as well as of enzyme entrapped in w/IL microemulsion was studied using the esterification of lauric acid with 1-butanol. The reaction was initiated by addition of the lipase-containing w/IL MBGs in the reaction solution (isooctane for the immobilized enzymes, w/IL microemulsion for the free enzyme) which had been pre-equilibrated to the desired temperature. For esterification reactions in w/IL microemulsions, the substrates were dissolved in the pre-incubated microemulsion system and then the enzyme was added as aqueous solution. Figure 2 shows the effect of the temperature on the esterification activity for the two enzyme forms of CalB (entrapped in w/IL microemulsions and immobilized in w/IL MBGs). As it can be seen, the optimum temperature for the esterification activity of the CalB entrapped in w/IL microemulsions was 50 °C, while at higher temperatures a decrease of the esterification rate was observed. Significant modifications in the temperature profile were observed after immobilization of CalB on w/IL MBGs since an increase on the incubation temperature from 30 to 80 °C resulted in an increase in esterification activity. Similar catalytic behavior was observed when a commercially available

immobilized CalB, Novozyme $435^{\text{®}}$, was used for the polymerization of ε caprolactone [34]. In the case of Cvl, although the optimum temperature value was practically the same for the two enzyme forms (about 60 °C), the immobilized enzyme retained higher fraction of its activity at temperatures up to the optimum value (data not shown). The beneficial effect of immobilization on the catalytic behaviour observed for both lipases could be attributed to increased thermal stability of the immobilized enzymes, as discussed in the next paragraph.

3.5. Lipase stability

Figure 3 depicts the deactivation curves of Cvl at 50 °C obtained in w/IL MBG, in w/IL microemulsion system and in water. As it can be seen, the stability of the lipase entrapped in w/IL microemulsions increases compared to that observed in water, which is in accordance to that reported previously [15]. Moreover, the lipase immobilization in w/IL MBGs further increases the lipase stability. The immobilized Cvl retained about 60 % of its initial activity after 5 days incubation in isooctane at 50 °C, while the non-immobilized lipase in aqueous solution or in w/IL microemulsion systems retained less than 5 %.

Table 4 shows the two-step deactivation kinetic constants and the half-life times for CalB and Cvl immobilized in MBGs formulated with w/IL microemulsions. As it can be seen, both immobilized enzymes are extremely stable. It must be noted that the half-life time of both immobilized lipases at 50 °C increases at least 150-fold compared to that observed in aqueous solution and 25-fold compared to that observed in w/IL microemulsions. These observations indicate that w/IL MBG matrix provides a protective environment for the lipases, especially at high incubation temperatures.

It is worth mentioning that at 30 °C an activation of both immobilized lipases was observed, as indicated from the α_1 values (α_1 >1 in these cases). It was proposed

that the first unfolding step exposes to the protein's surface some unstable amino acid residues and this probably provides flexibility to the lipase's structure (E₁) and therefore higher activity [35]. This phenomenon is not observed at higher incubation temperatures, where the inactivation of the enzyme is faster and the activity of the intermediate (E₁) is lower than that of the native enzyme (α_1 <1).

Both lipases immobilized in w/IL MBGs were recycled for the esterification of 1-butanol with caprylic acid in isooctane. The reaction was performed for 3 h at 50 °C after which MBGs containing enzyme was removed from the reaction medium, washed 5 times with isooctane and added to the fresh substrate solution. When ten reaction cycles were completed (30 h of total operation), the residual activity of the lipase was more than 50 %, as presented in Figure 4. Moreover, both lipases immobilized at w/IL MBGs retained more that 80 % of their initial activity after 100 hours of total operational time at 30 °C, which was significantly enhanced compared to that reported in previous studies [3, 6, 36], indicating that the immobilization of both lipases onto these novel organogels significantly increases their operational stability.

3.6. Structural studies

It is well established that the enzymes may undergo structural changes upon immobilization [37, 38]. In the present study, FT-IR spectroscopy was applied in order to monitor possible conformational changes of lipases during the immobilization procedure. The secondary structure elements of lipases in aqueous solution, entrapped in w/IL microemulsion system or immobilized in w/IL MBGs are presented in Table 5. A difference between the structure of lipase in aqueous solution and the crystallographic data was observed [26, 27]. This difference can be attributed to the high enzyme concentration used in ATR FT-IR experiments (1.5mg/ml), which

Biotechnology Journal

can lead to protein aggregation [39]. As it can be seen in Table 5, lipases entrapped in w/IL microemulsions and immobilized in w/IL MBGs undergo some alterations in their structure. More specifically, an increase in the β -sheet content is observed when enzymes are entrapped in w/IL microemulsions compared to that observed in aqueous solution, while no significant changes in the α -helix content were observed. The same trend was observed when enzymes were immobilized in w/IL MBGs. In order to further investigate the origin of the β -sheet content increase, we monitored the content of the lipases in antiparallel β -sheets. The content of antiparallel β -sheets is an index for intermolecular interactions, which lead to the formation of protein aggregates [40]. The increase in the β -sheet content observed upon immobilization is not proportional to this of antiparallel β -sheets, so the increase is not due to intermolecular interactions; on the contrary, in the case of Cvl the antiparallel β -sheet content significantly decreases, indicating that less protein-protein interactions are present in the immobilized preparation.

These structural data presented in this work leads us to the assumption that the lipase may adapt a more rigid structure, referring to the structure in aqueous solution, which is in accordance to previous works [15, 41, 42]. This more rigid structure adopted from the immobilized enzymes results in enhanced thermal and operational stability as described before.

4. CONCLUDING REMARKS

In the present work we have shown that w/IL microemulsion-based organogels can be efficiently used as solid matrices for enzyme immobilization. These novel lipase-containing w/IL MBGs are more biocompatible, compared to well known w/o MBGs used so far for enzyme immobilization. The operational and storage stability of immobilized lipases was significantly enhanced when immobilized in these MBGs, indicating that the w/IL microemulsion systems provide a protecting environment for the enzymes. This observation was confirmed by conformational studies, which indicate that the lipases immobilized in w/IL MBGs tend to adopt a more rigid structure compared to that observed in water or in w/IL microemulsions. The high enzyme loading which can be attained in these MBGs, among with the enhanced stability, the reusability even at relatively high incubation temperatures suggest that these novel lipase-containing w/IL MBGs can be effectively used for biocatalytic processes in various polar and non-polar organic solvents or ionic liquid-based media.

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Conflict of interest

The authors have declared no conflict of interest.

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Biotechnology Journal

Figure legends

Figure 1: Effect of mass fraction of HPMC (prior to the drying step) in the w/IL MBGs on the esterification activity of immobilized CalB in *n*-hexane.

Figure 2: Effect of the reaction temperature on the esterification activity of CalB entrapped in w/IL microemulsions (●) and immobilized in w/IL MBGs (■).

Figure 3: Thermal deactivation curves of Cvl in aqueous system (\blacksquare), entrapped in w/IL microemulsions (\blacktriangle), and immobilized in w/IL MBGs (\blacktriangledown) at 50°C. Symbols correspond to the experimental results and lines correspond to the predicted deactivation curve.

Figure 4: Reusability of CalB and Cvl immobilized in w/IL MBGs at 50°C in isooctane.

Table 1: Effect of microemulsion type on the esterification activity of immobilized

 lipases onto MBGs at 30°C in isooctane.

Linase	Reaction rate (mM/h)			
Lipuse	w/o MBG	w/IL MBG		
Candida antarctica lipase B	7.5 ± 0.3	8.1 ± 0.3		
Candida rugosa lipase	not determined	0.4 ± 0.0		
Chromobacterium viscosum lipase	3.7 ± 0.2	16.4 ± 0.8		
Rhizomucor miehei lipase	1.1 ± 0.1	1.9 ± 0.1		
Thermomyces lanuginosa lipase	13.1 ± 0.7	13.7 ± 0.6		

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Table 2: Effect of w/IL microemulsion composition on the esterification activity of immobilized CalB onto MBGs. Standard deviation in all cases was less than 5%.

Weight Ratio (%)					Reaction Rate (mM/h)	
	[bmim]PF ₆	PF ₆ Tween 20 Aqu		Wo	(% Conversion after 24 h	
					of incubation)	
	47.5	50.0	2.5	3.4	4.6 (78.2)	
	45.0	50.0	5.0	6.8	5.1 (80.8)	
	40.0	50.0	10.0	13.7	10.8 (100.0)	
	35.0	50.0	15.0	20.5	8.1 (100.0)	
	30.0	50.0	20.0	27.3	7.9 (77.8)	
	20.0	50.0	30.0	40.9	5.8 (88.6)	
	10.0	85.0	5.0	4.0	9.3 (89.0)	
	20.0	75.0	5.0	4.6	6.0 (75.0)	
	40.0	55.0	5.0	6.2	5.2 (81.9)	
	60.0	35.0	5.0	9.7	4.1 (79.8)	
	80.0	15.0	5.0	22.8	0.5 (17.4)	



Table 3: Effect of the reaction medium on the esterification activity (mM/h) and the 24 hour-conversion (in the brackets, %) of lipases immobilized in MBGs. Standard deviation in all cases was less than 7%.

Reaction	Log P	w/IL MBG		w/o MBG	
medium	Lug I	Cvl	CalB	CalB	
Isooctane	4.0	16.4 (100.0)	8.1 (100.0)	7.5 (80.5)	
<i>n</i> -Hexane	3.4	7.9 (84.2)	6.7 (81.7)	6.9 (80.6)	
Isopropyl ether	1.9	4.7 (64.7)	4.8 (66.4)	5.8 (68.4)	
tert-Butanol	1.45	7.7 (33.6)	3.8 (41.6)	1.4 (19.3)	
1-Butanol	0.80	8.6 (47.4)	2.5 (18.7)	0.6 (16.0)	
Acetone	-0.23	1.7 (16.9)	0.8 (10.3)	0.5 (19.1)	
Acetonitrile	-0.33	7.9 (87.2)	14.7 (90.3)	10.1 (79.9)	
[bmim]PF ₆	-2.38	25.7 (100.0)	23.0 (100.0)	0.9 (61.9)	
[bmim]BF ₄	-2.44	1.1 (13.3)	1.3 (49.2)	0.1 (3.0)	

Table 4: Deactivation kinetic constants and half-life time as predicted from the twostep deactivation model described in Section 2.4. In all cases $\alpha_2 = 0$. The correlation coefficient *r* was higher than 0.950 in all cases.

Lipase	Temperature (°C)	α1	$k_1 (h^{-1})$	$k_2(h^{-1})$	t _{1/2} (h)
CalB	30	1.612	1.085	0.003	391
	50	0.748	2.056	0.002	202
	70	0.510	1.830	0.030	2
Cvl	30	1.263	0.006	0.006	319
	50	0.670	0.451	0.002	149
	70	0.431	0.662	0.026	3

Table 5: Quantitative estimation (%) of the secondary structure elements of lipases in water, entrapped in w/IL microemulsions and immobilized in w/IL MBGs calculated by FT-IR analysis in amide I region.

	System	α-helix	β-sheet	Other	Antiparallel		
Lipase					β-sheet		
CalB	Aqueous	24.0	29.0	47.0	8.5		
	w/IL microemulsion	25.7	33.4	40.9	8.7		
	w/IL MBGs	21.0	42.0	37.0	11.7		
Cvl	Aqueous	22.0	37.5	40.5	25.9		
	w/IL microemulsion	25.1	39.6	35.2	11.5		
	w/IL MBGs	21.8	53.1	25.2	5.1		





Effect of mass fraction of HPMC (prior to the drying step) in the w/IL MBGs on the esterification activity of immobilized CalB in n-hexane. 1155x808mm (150 x 150 DPI)



Effect of the reaction temperature on the esterification activity of CalB entrapped in w/IL microemulsions (●) and immobilized in w/IL MBGs (■). 1187x839mm (150 x 150 DPI)







Figure 3: Thermal deactivation curves of Cvl in aqueous system (■), entrapped in w/IL microemulsions (▲), and immobilized in w/IL MBGs (▼) at 50°C. Symbols correspond to the experimental results and lines correspond to the predicted deactivation curve. 1147x806mm (150 x 150 DPI)





Reusability of CalB and CvI immobilized in w/IL MBGs at 50oC in isooctane. 1147x806mm (150 x 150 DPI)

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