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A totally Eulerian Finite Volume solver for multi-material fluid flows : Enhanced Natural Interface Positioning (ENIP)

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Abstract

This work concerns the simulation of compressible multi-material fluid flows and follows the method FVCF-NIP described in the former paper [5]. This Cell-centered Finite Volume method is totally Eulerian since the mesh is not moving and a sharp interface, separating two materials, evolves through the grid. A sliding boundary condition is enforced at the interface and mass, momentum and total energy are conserved. Although this former method performs well on 1D test cases, the interface reconstruction suffers of poor accuracy in conserving shapes for instance in linear advection. This situation leads to spurious instabilities of the interface. The method Enhanced-NIP presented in the present paper cures an inconsistency in the former NIP

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method that improves strikingly the results. It takes advantage of a more consistent description of the interface in the numerical scheme. Results for linear advection and compressible Euler equations for inviscid fluids are presented to assess the benefits of this new method.

Keywords: Multi-material fluid flow, Finite Volume, Natural Interface Positioning

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16 1. Introduction

The two-material compressible hydrodynamics equations (Euler equations) are considered in this work. The flow regime is such that molecular viscosity within materials is neglected: materials are supposed immiscible and separated by sharp interfaces, with perfect sliding between materials. Each material is characterized by its own equation of state (EOS).

The formalism of finite volume methods is close to the mechanical viewpoint, and generic for different types of physical models. Thus, it might be easier to add such models; surface tension or turbulent diffusion for instance. The discretization order is limited, but this method is accurate to simulate hydrodynamic shock waves, because of the consistency between numerical treatment and mechanics.

The extension of Eulerian schemes to multi-material fluid flows can be ob-28 tained by various techniques. One is to introduce the cell mass fraction c_{α} of 29 material α and let it evolve according to material velocity. The cell is called 30 pure if a material α satisfies $c_{\alpha} = 1$ and is called mixed if $c_{\alpha} \in]0,1[$. Pure 31 cells filled by material α are calculated in the same manner as for the single 32 material method. Mixed cell evolution is computed using a mixing equation 33 of state that takes into account material mass fractions, see e.q. [1]. One 34 drawback of this approach is the numerical diffusion of the interface that ob-35 viates sharp interface capturing. It turns out that for some applications, this 36 drawback is not acceptable since the diffusion of one material into another 37 one will correspond to a different physics. For example the two material 38 could react when a molecular mixture is formed. Hence such a diffusion 39 should occur only for physical reasons and not for numerical ones. 40

In the case of sharp interface capturing methods, the interface is approx-41 imated in a mixed cell by a segment by most authors. However more com-42 plex curves than straight line or more complex theory (see [6] for instance) 43 might be used. A famous method using sharp interface reconstruction is 44 the Lagrange+Remap Finite Volume scheme, initiated in [9] and further im-45 proved in [10]. It belongs to the family of so called Volume of Fluid (VOF) 46 methods. The first step of this method is a Lagrangian scheme, resulting 47 in a mesh displacement with material velocity. The second step is a multi-48 material remapping of Lagrangian mesh onto the original Eulerian mesh, by 49 exchanging volume fluxes between cells related to the Lagrangian motion of 50 cell edges. The new interface position in mixed cells is determined using 51 the partial volumes of the materials and the interface normal vector. The 52 later is calculated using volume fractions from neighboring cells. Thus the 53 ratio of each material in volume fluxes is deduced from the multi-material 54 remapping. Some methods with the same kind of operator splitting are used 55 for incompressible multi-material fluid flows as in [8]. These methods pro-56 vide sharp interface between materials and discontinuous quantities in mixed 57 cells, allowing large deformations and transient flows. In this context, the 58 drawback of these Lagrange+Remap methods is the limited accuracy of the 59 underlying single phase scheme due to diffusion induced by the remapping 60 step. Moreover, more complex physics at material interfaces such as sliding 61 effects, is not possible. 62

The FVCF scheme (Finite Volume with Characteristic Flux) has been introduced in [7] for simulating single phase compressible flows or multiphase models without sharp interface capturing. The method described in

[5], so called NIP method (Natural Interface Positioning), is an add-on to 66 the FVCF method in order to deal with multi-material fluid flows with sharp 67 interface capturing. It is a cell centered totally Eulerian scheme, in which ma-68 terial interfaces are represented by a discontinuous piecewise linear curve. A 69 treatment for interface evolution is proposed on Cartesian structured meshes 70 which is locally conservative in mass, momentum and total energy and allow 71 the materials to slide on each others. Discrete conservation laws are writ-72 ten on partial volumes as well as on pure cells, considering the interface in 73 the cell as a moving boundary without any diffusion between materials. A 74 specific data structure called *condensate* is introduced in order to write a 75 finite volume scheme even when the considered volume is made of moving 76 boundaries, i.e. interfaces. This treatment includes an explicit computation 77 of pressure and velocity at interfaces. 78

In [5] are shown 2D results illustrating the capability of the method to 79 deal with perfect sliding, high pressure ratios and high density ratios. This 80 former method however produces non satisfactory results in the context of 81 advection of geometrical shapes especially when dealing with low Mach num-82 bers. It is however a classical misbehavior of most of advection and recon-83 struction methods which have a tendency to destroy the shape of advected 84 objects due to numerical approximations. However, this former method gives 85 very poor results when advecting geometrical shapes especially when dealing 86 with low Mach number flows. In this work we propose a new method called 87 ENIP (Enhanced NIP) that is an improvement of the NIP method by a more 88 accurate treatment of condensates. On a very simple example: the advection 89 of a square, an inconsistency in the NIP interface reconstruction method will 90

⁹¹ be exhibited. We will then introduce ENIP that cures this situation. Nu⁹² merical examples are presented in the last Section to assess the validity and
⁹³ efficiency of this new approach.

⁹⁴ 2. FVCF-ENIP: Finite Volume Characteristics Flux with Enhanced ⁹⁵ Natural Interface Positioning technique

96 2.1. Governing equations

The model addressed in this work is the compressible Euler equations in space dimension d that can be written in a conservative form as follows:

$$\frac{\partial}{\partial t}(\rho) + \operatorname{div}(\rho u) = 0, \qquad (1)$$

$$\frac{\partial}{\partial t}(\rho u) + \operatorname{div}\left(\rho u \otimes u + pI\right) = 0, \qquad (2)$$

$$\frac{\partial}{\partial t}(\rho E) + \operatorname{div}\left((\rho E + p)u\right) = 0, \qquad (3)$$

where ρ denotes the density, $u \in \mathbb{R}^d$ the velocity field, p the pressure, $E = e + |u|^2/2$ the specific total energy and e the specific internal energy. An equation of state of the form $EOS(\rho, e, p) = 0$ or $p = p(\rho, e)$ is provided in order to close the system.

Let us consider a generic conservative form with $\mathbf{V} = (\rho, \rho u, \rho E)^t$ the unknown vector of conservative variables and flux \mathbf{F} is a matrix valued function defined as:

$$\begin{aligned} \boldsymbol{F} : & \mathbb{R}^{d+2} & \longrightarrow & \mathbb{R}^{d+2} \times \mathbb{R}^d \\ & \boldsymbol{V} & \longmapsto & \boldsymbol{F}(\boldsymbol{V}), \end{aligned}$$

$$\tag{4}$$

for all direction $n \in \mathbb{R}^d$, $F(V) \cdot n$ is given in terms of V by:

$$\boldsymbol{F}(\boldsymbol{V}) \cdot \boldsymbol{n} = \left(\rho\left(\boldsymbol{u} \cdot \boldsymbol{n}\right), \rho \boldsymbol{u}\left(\boldsymbol{u} \cdot \boldsymbol{n}\right) + p \boldsymbol{n}, \left(\rho \boldsymbol{E} + \boldsymbol{p}\right)\left(\boldsymbol{u} \cdot \boldsymbol{n}\right)\right).$$
(5)

The compressible Euler equations (1-3) can then be rewritten as:

$$\partial_t \boldsymbol{V} + \operatorname{div} \boldsymbol{F}(\boldsymbol{V}) = 0.$$
(6)

97 2.2. FVCF: Single material scheme

FVCF method uses a directional splitting on Cartesian structured meshes. The method is thus detailed for only one generic direction denoted by x. In d dimensions of space, the algorithm described for direction x has to be replicated d times, one for each direction. However, this directional splitting does not modify at all the underlying single material scheme FVCF for pure cells. In 2D:

- variables at $t^{n,x}$ are calculated from those at t^n by the x direction step, - variables at t^{n+1} are calculated from those at $t^{n,x}$ by the y direction step.

$$\operatorname{Vol}_{i} \frac{\boldsymbol{V}_{i}^{n,x} - \boldsymbol{V}_{i}^{n}}{\Delta t} + A_{x} \left(\boldsymbol{\phi}_{\ell}^{n} + \boldsymbol{\phi}_{r}^{n}\right) = 0, \qquad (7)$$

$$\operatorname{Vol}_{i} \frac{\boldsymbol{V}_{i}^{n+1} - \boldsymbol{V}_{i}^{n,x}}{\Delta t} + A_{y} \left(\boldsymbol{\phi}_{d}^{n} + \boldsymbol{\phi}_{u}^{n}\right) = 0, \qquad (8)$$

where the cell volume is Vol_i , the cell face area are A_x and A_y respectively normal to x and y directions, up, down, right and left direction fluxes ϕ_u^n , ϕ_d^n , ϕ_r^n , ϕ_ℓ^n calculated with respect of the outgoing normal direction n_d of cell face Γ_d in direction d using variables at time t^n , i.e.

$$\boldsymbol{\phi}_{d}^{n} = \frac{1}{A_{d}} \int_{\Gamma_{d}} \boldsymbol{F}(\boldsymbol{V}^{n}) \cdot n_{d} dS.$$
(9)

¹⁰⁷ This flux is further approximated using the finite volume scheme FVCF de-¹⁰⁸ scribed in [7].

109 2.3. FVCF-NIP: Multi-material scheme

One considers multi-material flows. The subcell model addressed here for the multi-material representation is a cell C of volume Vol_C containing n_m different materials, each of them filling a partial volume Vol_C^k such that

$$\sum_{k=1}^{n_m} \operatorname{Vol}_C^k = \operatorname{Vol}_C.$$
(10)

Cell C is referred to as pure if $n_m = 1$, and as mixed if $n_m > 1$. The interfaces in mixed cells are approximated by segments separating materials into two partial volumes which are pure on both sides of the interface.

A partial volume cell-centered variable vector $\mathbf{V}_k = (\rho_k, \rho_k u_k, \rho_k E_k)^t$ and an equation of state $EOS_k(\rho_k, e_k, p_k) = 0$ are also associated with each material labeled by $k \leq n_m$ in the mixed cell.

FVCF-NIP method uses a directional splitting scheme for the interface evolution without loosing the accuracy of the Eulerian scheme in the bulk of materials. Consequently this scheme is restricted to structured Cartesian mesh.

The multi-material extension proposed in [5] considers the finite volume scheme (7-8) on each partial volume in a mixed cell. The obtained scheme is conservative by construction and is constrained with the same CFL condition as the single material scheme¹. NIP method consists in removing cell edges when this cell contains an interface. Therefore each partial volume is merged with the neighbor pure cells filled with the same material, see Figure 1. Variables in these enlarged partial volumes are obtained by writing the

¹Without such a special treatment the time step would be constrained by the smallest partial volume, which is arbitrarily small.

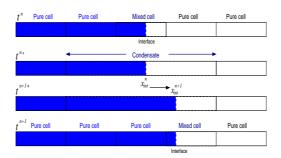


Figure 1: Sketch of a condensate. Evolution of an interface through a cell edge during one time step. Mixed and pure neighbor cells are merged to obtain the so called condensate at fictitious time t^{n*} . Interface evolution is performed within this condensate from t^{n*} to t^{n+1*} This condensate is then split back into Eulerian cells.

conservation laws on the merged volumes

$$\overline{\mathrm{Vol}_1} = \mathrm{Vol}_1 + \mathrm{Vol}_{pure 1}, \tag{11}$$

$$\overline{\text{Vol}_2} = \text{Vol}_2 + \text{Vol}_{pure 2}, \qquad (12)$$

then on the conserved variables

$$\overline{\boldsymbol{V}}_{1} = \frac{\operatorname{Vol}_{1} \boldsymbol{V}_{1} + \operatorname{Vol}_{pure 1} \boldsymbol{V}_{pure 1}}{\overline{\operatorname{Vol}_{1}}}$$
(13)

$$\overline{\boldsymbol{V}}_2 = \frac{\operatorname{Vol}_2 \boldsymbol{V}_2 + \operatorname{Vol}_{pure \ 2} \boldsymbol{V}_{pure \ 2}}{\overline{\operatorname{Vol}_2}}.$$
(14)

This set of cells is associated with its left and right single material fluxes ϕ_{ℓ} and ϕ_r . Internal cell edges are forgotten, considering only enlarged volumes $\overline{\text{Vol}_1}$ and $\overline{\text{Vol}_2}$ and averaged variables \overline{V}_1 and \overline{V}_2 , separated by an interface; this system is called a condensate.

Actually, this numerical strategy consists in condense neighboring mixed cells in one direction of the Cartesian mesh, in which interfaces are considered as mono dimensional objects, namely they are considered vertical

during x direction step and horizontal during y direction step. A condensate 127 then contains layers of successive different materials that are separated by 128 straight interfaces. The thickness of these layers is calculated through vol-129 ume conservation. The ordering of layers is given by the 2D description from 130 the previous time step. It is determined thanks to the volume fractions of 131 neighboring cells. The layer evolution is calculated in a Lagrangian fashion 132 which implies that layers can be as thin as partial volumes are small. Once 133 quantities and interface positions inside the condensate are known at time 134 t^{n+1} , they are remapped back onto the original Eulerian mesh. Finally a 2D 135 normal in each mixed cell is computed as described in [10]: the method is 136 based on an approximation of the gradient of the volume fraction function 137 in mixed cells. It provides the normal to materials interface in each cell 138 that is further used to locate materials within mixed cells. The numerical 139 scheme used in a condensate is presented in great details in [5] and we omit 140 this description in this work and rather focus on the interface reconstruction 141 method. 142

As shown in [5] this numerical method has several attractive properties as conservation and perfect sliding of materials as instance. Moreover Δt is not restricted by small partial volume thanks to a tight control of density and pressure [3]. The numerical experiments carried out in [7, 2, 5, 4] have confirmed the efficiency of such a method for compressible multi-material computation. Although very promising, the method suffers from the way interfaces are dealt with.

In order to illustrate the interface reconstruction method NIP let us consider a square like interface cutting the Eulerian cells, as in Figure 2-(A). These interfaces are indeed defined by their normals within each cell. NIP method consists of the following steps assuming the condensate is in the xdirection:

- Representation Figure 2-(B). The representation step can be seen as the way of determining on which side (left or right) of the mixed cell the material is to be put. This is done by comparing the direction of the interface normal at time t^n with the vertical direction.
- Condensate construction Figure 2-(C). The construction of the conden sate consists in discarding any cell edges in the mixed cells considered.
 Then the partial volumes of the same contiguous materials are glued
 together into so called condensate layers. As instance cell 2 and 3 dark
 materials are merged into one stand-alone layer with associated volume
 averaged values.
- Condensate evolution Figure 2-(D). The condensate layers evolution is computed from t^n to t^{n+1} thanks to the numerical scheme developed in [5]. In short, each vertical interface is assigned a velocity and, consequently, a new position of each layer within the condensate is determined in a Lagrangian way. Any conserved variable is computed accordingly.
- *Reconstruction* Figure 2-(E). This phase consists in "guessing" the shape of each layer in the condensate before remapping. The reconstruction phase was not originally considered as a true phase of the algorithm as the author used the same shapes as the ones produced in phase *Condensate construction*, i.e. only vertical interfaces.

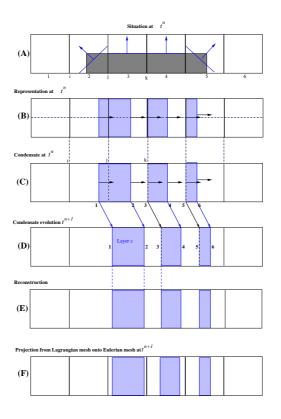


Figure 2: NIP method — (A) Situation at t^n with real materials geometry, interfaces and normals to them. (B) Representation of partial volumes at t^n . (C) Construction of a condensate at t^n by merging layers of contiguous partial volumes of the same material. (D) Evolution of condensate in a Lagrangian fashion during Δt . (E) Condensate reconstruction at t^{n+1} . (F) Condensate projection/remapping from Lagrangian mesh onto original mesh.

Projection Figure 2-(F). The projection step consists in remapping the
 shapes obtained from the reconstruction phase onto the Eulerian grid.
 This step produces updated partial volumes in mixed cells. Volume
 fractions are deduced.

When all mixed cells in the domain are treated for direction x, the interface normals are computed using the updated volume fractions. This concludes the system evolution in direction x, as we are back to a similar situation as the one described in Figure 2-(A).

In the case where the normal is almost vertical, positioning the material on 184 either side of the cell might be, at least inaccurate, or, worse, incorrect. Fur-185 thermore the reconstruction phase is here clearly inconsistent: the interfaces 186 are initially horizontal in cell 3 and 4 (Figure 2-(A)), while in the Recon-18 struction Figure 2-(E) and in the Projection Figure 2-(F) phase interfaces 188 are set vertical for any initial geometry. This situation of a horizontal inter-189 face is the worst case, but it illustrates the lack of geometrical consistency of 190 NIP. This inaccurate reconstruction step leads to a lack of accuracy of the 191 volume fractions obtained after the remapping step. Ultimately, it impacts 192 the whole numerical method in any advection process. 193

As an illustration let us consider the diagonal advection of a square back and forth as shown in Figure 3. We omit the exhaustive description of this test as it will be done in the numerical Section of this paper. On the right panel it is obvious that the shape of the square is not well approximated. More important the horizontal and vertical edges of the square do not remain so. This behaviour is less pronounced if one refines the mesh but still remains. Our goal is to improve the reconstruction step so that the new method, de-

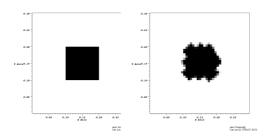


Figure 3: Diagonal advection of a square by NIP method — Left: Exact configuration — Right: Numerical configuration obtained by NIP.

noted ENIP standing for Enhanced Natural Interface Positioning, cure this
 geometrical inconsistency during the advection phase of the algorithm.

203 2.4. FVCF-ENIP

The main idea of the new interface reconstruction method ENIP emanates from the following remarks:

- 1. At time t^n any interface normal in mixed cell *i* denoted \vec{n}_i is known. It is used to locate the partial volumes within cell *i* when the condensate is constructed (phase (B) and (C) of Figure 2). However \vec{n}_i is never taken into account in the reconstruction and projection phases (E) and (F) from the same figure.
- 2. Any layer of the condensate evolves as a Lagrangian object in the original method. Consequently the cell faces could evolve in an almost
 Lagrangian manner within this condensate. This makes possible to
 conserve the initial geometry of partial volumes during this Lagrangian
 motion.

Therefore ENIP modifies several steps of NIP as depicted in Figure 4. Once a patch of neighbor mixed cells in x direction² are agglomerated, The same five steps as for NIP method are performed. The first two steps are kept unmodified. The last three are modified as described in the following.

220 2.4.1. Lagrangian Condensate evolution step

Cell interface Lagrangian velocity. After the condensate at t^n is constructed, each layer labeled c is located thanks to the left and right interface position respectively called x_c^-, x_c^+ . The numerical scheme provides the layer evolution, and as a by-product, the velocity of these interface positions, u_c^-, u_c^+ are given by

$$x_c^{-,n+1} = x_c^{-} + \Delta t \ u_c^{-}, \quad x_c^{+,n+1} = x_c^{+} + \Delta t \ u_c^{+}.$$
(15)

We make the following fundamental linear displacement assumption: The velocity linearly varies within any layer, see Figure 5 for a sketch. This assumption implies that any point $x_i \in [x_c^-; x_c^+]$ characterized by its 1D barycentric coordinates

$$\lambda_i^- = \frac{x_c^+ - x_i}{x_c^+ - x_c^-}, \qquad \lambda_i^+ = \frac{x_i - x_c^-}{x_c^+ - x_c^-},\tag{16}$$

moves to location

$$x_i^{n+1} = \lambda_i^- x_c^{-,n+1} + \lambda_i^+ x_c^{+,n+1} = x_i + \Delta t \left(\lambda_i^- u_c^- + \lambda_i^+ u_c^+ \right).$$
(17)

Then the point velocity is naturally set to $u_i = \lambda_i^- u_c^- + \lambda_i^+ u_c^+$. Using this previous formula one can associate a "Lagrangian" velocity to any cell interface. As instance in Figure 4-(C) cell interface located at x_i^n moves to the

²The y direction is treated likewise.

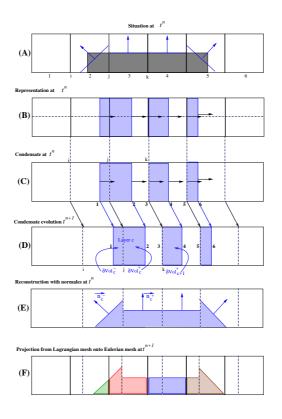


Figure 4: ENIP method — (A) Situation at t^n with real material, interfaces and normals to them. (B) Representation of material at t^n . (C) Construction of a condensate at t^n by merging of mixed cells leading to layers of contiguous pieces of the same material. (D) Evolution of condensate in a Lagrangian fashion during Δt . Determine layer compression rates $\delta \text{Vol}_c^{\pm}$ through the evolution of Lagrangian cells during Δt . (E) Condensate reconstruction at t^{n+1} using interface normals defined at t^n . (F) Condensate projection/remapping from Lagrangian mesh onto Eulerian mesh.

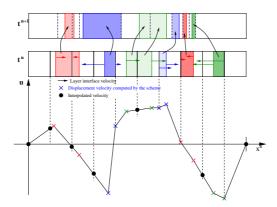


Figure 5: Sketch of linear displacement assumption — Displacement velocity varies linearly between the layer interface velocities (× in color) computed by the numerical scheme. The cell interface velocity (•) is interpolated. The two top rows represent the evolution of a condensate in the x direction from t^n to t^{n+1} .

position $x_i^{n+1} = x_i^n + \Delta t \ u_i$ with u_i being the linear combination between u_c^- and u_c^+ via the barycentric coordinates of point x_i in $[x_c^-; x_c^+]$. With the same formula one gets $x_{i+1}^{n+1} = x_{i+1}^n + \Delta u_{c+1}^-$ in the next layer as $x_{i+1}^n \equiv x_{c+1}^-$.

Compression/expansion rates. The global rate of compression/expansion in layer c during Δt is given by

$$\delta \text{Vol}_{c} = \frac{x_{c}^{+,n+1} - x_{c}^{-,n+1}}{x_{c}^{+} - x_{c}^{-}} = 1 + \Delta t \frac{u_{c}^{+} - u_{c}^{-}}{x_{c}^{+} - x_{c}^{-}}.$$
(18)

The linearity assumption provides a simple way to determine the rates of compression/expansion at left/right of a point $x_i \in [x_c^-; x_c^+]$

$$\delta \operatorname{Vol}_{c}^{-} = \frac{x_{i}^{n+1} - x_{c}^{-,n+1}}{x_{c}^{+} - x_{c}^{-}}, \quad \delta \operatorname{Vol}_{c}^{+} = \frac{x_{c}^{+,n+1} - x_{i}^{n+1}}{x_{c}^{+} - x_{c}^{-}}, \tag{19}$$

that fulfil $\delta \text{Vol}_c^- + \delta \text{Vol}_c^+ = \delta \text{Vol}_c$. Moreover the substitution of x_i^{n+1} in the previous equations yields

$$\delta \text{Vol}_{c}^{-} = \frac{x_{i} - x_{c}^{-}}{x_{c}^{+} - x_{c}^{-}} + \Delta t \frac{u_{i} - u_{c}^{-}}{x_{c}^{+} - x_{c}^{-}} = \lambda_{i}^{+} + \Delta t \frac{u_{i} - u_{c}^{-}}{x_{c}^{+} - x_{c}^{-}},$$
(20)

where $u_i - u_c^- = (\lambda_i^- u_c^- + \lambda_i^+ u_c^+) - u_c^- = \lambda_i^+ (u_c^+ - u_c^-)$, therefore the compression rates simply writes

$$\delta \operatorname{Vol}_{c}^{-} = \lambda_{i}^{+} \left(1 + \Delta t \frac{u_{c}^{+} - u_{c}^{-}}{x_{c}^{+} - x_{c}^{-}} \right) = \lambda_{i}^{+} \delta \operatorname{Vol}_{c}, \qquad (21)$$

$$\delta \operatorname{Vol}_{c}^{+} = \lambda_{i}^{-} \left(1 + \Delta t \frac{u_{c}^{+} - u_{c}^{-}}{x_{c}^{+} - x_{c}^{-}} \right) = \lambda_{i}^{-} \delta \operatorname{Vol}_{c}.$$
(22)

Each $\delta \operatorname{Vol}_c^+$ or $\delta \operatorname{Vol}_c^-$ is associated to a unique Eulerian cell; as instance in 227 Figure 4, δVol_c^- is associated to cell 2, δVol_c^+ to cell 3, $\delta \text{Vol}_{c+1}^+$ to cell 4 228 and so on. Therefore $\delta \operatorname{Vol}_c^{\pm}$ provides de facto the compression/expansion 229 of the partial volume originating from its associated Eulerian cell motion. 230 Furthermore, as any Eulerian mixed cell i possesses a unique normal denoted 231 \vec{n}_i , this last is associated to the corresponding partial volume $\delta \text{Vol}_c^{\pm}$; this 232 normal is consequently labeled \vec{n}_c^{\pm} . These rates are then used to reconstruct 233 the material topology into the Lagrangian cell. 234

235 2.4.2. Reconstruction step

The Lagrangian cell i + 1/2 at t^{n+1} the interfaces of which moved as

$$x_i^{n+1} = x_i + \Delta t \ u_i, \qquad x_{i+1}^{n+1} = x_{i+1} + \Delta t \ u_{i+1}, \tag{23}$$

changed its volume as

$$\delta \operatorname{Vol}_{i+1/2} = \frac{V_{i+1/2}^{n+1}}{V_{i+1/2}} = \frac{x_{i+1}^{n+1} - x_i^{n+1}}{x_{i+1} - x_i} = 1 + \Delta t \frac{u_{i+1} - u_i}{x_{i+1} - x_i}.$$
 (24)

The velocity u_i depends on u_{c-1}^-, u_{c-1}^+ and u_{i+1} depends on u_c^-, u_c^+ . Moreover $u_{c-1}^+ \equiv u_c^-$ by definition.

The second fundamental assumption states that the interface normals \vec{n}_c^{\pm} do not change their direction during their Lagrangian evolution. The goal is to locate the partial volume into the Lagrangian cell at t^{n+1} and construct the linear interface, knowing its normal \vec{n}_c^{\pm} . Necessarily this partial volume is either in contact with cell interface x_i (superscript +) or x_{i+1} (superscript -). Its volume at t^{n+1} is given by

$$V_{c}^{\pm,n+1} = V_{c}^{\pm} \,\,\delta \text{Vol}_{c}^{\mp} = V_{c}^{\pm} + \Delta t \,\,\lambda_{i}^{\mp} (u_{c}^{+} - u_{c}^{-}).$$
(25)

If $V_c^{\pm,n+1} \leq V_{i+1/2}^{n+1}$ then there exists a unique line oriented by the normal \vec{n}_c^{\pm} 236 and separating the cell volume into two sub-volumes $V_c^{\pm,n+1}$ and $(V_{i+1/2}^{n+1} -$ 23 $V_c^{\pm,n+1}$) respectively by the PLIC ("Piecewise Linear Interface Construction" 238 [10]) method. As the displacement velocity u(x) is supposed to be piecewise 239 linear (by the first assumption see Figure 5), then, if $x_i < x_c^- < x_{i+1}$ one 240 deduces $x_i^{n+1} < x_c^{-,n+1} < x_{i+1}^{n+1}$. Therefore the sub-volume at t^{n+1} is strictly 24 included into the Lagrangian cell volume $V_{i+1/2}^{n+1}$. This phase is depicted in 242 Figure 4-(E)243

244 2.4.3. Projection step

The projection step performs the exact intersection between the La-245 grangian condensate obtained after the reconstruction step in Figure 4-(E)246 and the Eulerian mesh (bold line squares in Figure 4-(A)). This step is de-24 picted in Figure 4-(F). The exact intersection consists in projecting each 248 partial volume that is accurately located into the condensate, onto some Eu-249 lerian fixed cell(s). As instance in Figure 4-(F) the first partial volume is 250 projected onto Eulerian cells 2 (green cell) and 3 (red cell). Contrarily the 25 last partial volume is totally projected into Eulerian cell 5 (brown cell). This 252 projection provides the quantity of material per Eulerian cell, or, equivalently 253 its volume fraction. 254

Once volume fractions in the mixed cells are updated though the evolution of condensates, 2D normals are computed using the same technique as in original NIP method.

258 3. Numerical results

In this Section we present a set of test cases to assess the efficiency of the approach described in the previous Sections. First, one validates the technique on pure advection test cases that often present excessive smearing of interfaces due to the numerical inaccuracy embedded into the scheme. A square shaped object is advected with constant velocity in a diagonal direction in a first test, then into a rotating flow. Finally an hydrodynamics test case is presented.

266 3.1. Advection context

An initial square $[0.1; 0.1] \times [0.2; 0.2]$ is located into the domain $\Omega = [0: 0.4] \times [0; 0.6]$. The density into the square is set to $\rho_0(x) = 1$ whereas it is set to $\rho_0(x) = 0$ outside. In the pure advection context this square shape should be perfectly conserved through the equation

$$\frac{\partial}{\partial t}\rho + u\frac{\partial}{\partial x}\rho + v\frac{\partial}{\partial x}\rho = 0, \qquad (26)$$

where (u, v) is a constant velocity field. The exact solution at any point xand any time t is $\rho^{ex}(x, y, t) = \rho_0(x - u t, y - v t)$. If the numerical method provides an approximated solution called ρ_i^n in cell i at time t^n then the error in L_{α} norm is evaluated by $(\alpha = 1, 2)$

$$\varepsilon_{\alpha} = \frac{\sum_{i} |\rho_{i}^{n} - \rho^{ex}(x_{i}, t^{n})|^{\alpha}}{\sum_{i} |\rho^{ex}(x_{i}, t^{n})|^{\alpha}}.$$
(27)

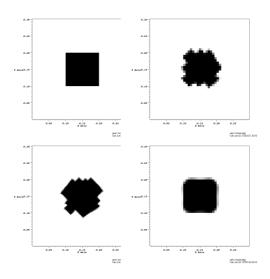


Figure 6: Advection of a square (zoom around the exact position of the initial and final square) — Top-left: exact solution — Top-right: classical NIP with a 60×60 mesh — Bottom-left: classical NIP with a 120×120 mesh — Bottom-right: ENIP with a 60×60 mesh.

The first test consists in advecting the square with the constant velocity 26 field u = 1, v = 3 up to the time t = 0.1 then reversing the advection 268 field by setting u = -1, v = -3 up to final time t = 0.2 so that the final 269 configuration perfectly fits the initial one. Any method (NIP and ENIP 270 included) introduces some error that we intend to measure with this test. 271 In Figure 6 are shown the exact solution (top-left) and the results obtained 272 with a 60×60 mesh for NIP (top-right) and ENIP (bottom-right). ENIP is 273 visibly able to preserve the shape of the square whereas NIP is not. A mesh 274 refinement of NIP computation $(120 \times 120 \text{ mesh for the bottom-left panel})$ 275 does not improve the situation. In table 1 we gather the errors for the L_1 , 276 L_2 norms for successively refined meshes for the NIP and the proposed ENIP 277

| $\Delta x = \Delta y$ | L_1 NIP | L_1 ENIP | L_2 NIP | L_2 ENIP |
|-----------------------|------------------|------------|------------------|-------------------|
| 0.02 | 3.652 | 0.196 | 2.575 | 0.079 |
| 0.0133 | 0.389 | 0.165 | 0.318 | 0.081 |
| 0.01 | 0.339 | 0.111 | 0.284 | 0.053 |
| 0.005 | 0.221 | 0.042 | 0.195 | 0.017 |
| 0.0033 | 0.155 | 0.025 | 0.138 | 0.010 |

Table 1: Error in L_1, L_2 norms for the advection problem — NIP versus ENIP methods.

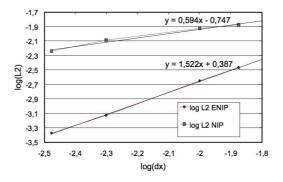


Figure 7: Convergence of ENIP vs NIP for a pure advection problem. The log of the L_2 error is displayed as a function of the log of Δx .

method on this advection problem. Systematically ENIP over-tops NIP. In Figure 7 we display the log-log scale results for the error in L_2 norm for both methods showing the improvement gained by ENIP; indeed the slope which represents a measure of the numerical order of convergence is improved by a factor 2.5 (0.6 for NIP and 1.5 for ENIP).

The next test consists in the rigid rotation of a square $[0.06; 0.46] \times [0.3; 0.7]$ (density 1) into the unit square domain, see Figure 8 top-left panel. A 100 × 100 uniform mesh is considered and the rotation is given by the Figure 8: Top-left: Sketch of the rigid rotation of a square — Top-right: After 5/8 of the full rotation — Bottom-left: After one full rotation — Bottom-right: After three full rotations.

velocity field

$$u = -100(y - 0.5), \quad v = 100(x - 0.5).$$

In Figure 8 we display the density after 5/8 of the full rotation, after one and three rotations. The square shape is almost preserved. Contrarily the classical NIP method would totally lose the shape after one rotation.

286 3.2. Hydrodynamics context

We run an idealized 2D test case that corresponds to the free drop of a liquid rectangle within a 2D rectangular tank filled with gas [4]. This

context is inspired by the problem of sloshing that may appear in the tanks 289 of Liquid-Natural-Gas (LNG) carriers. The study focuses on the ability for 290 the numerical simulations to take properly into account the physics that is 29 of major importance during the liquid impact such as the escape of the gas 292 underneath and its compression. As a strong sliding process occurs between 293 the compressed gas and the falling liquid. The ability of the method to 294 properly deal with sliding conditions at the interface has a major effect on 295 the final numerical compression and shape of the trapped air. This has 296 ultimately a strong influence on the impact pressure. 29

The test case consists in a domain $\Omega = [0.0; 0.0] \times [10m; 15m]$ filled with air. 298 The liquid is initially at rest in the rectangle $[0; 2] \times [5; 10]$ and is falling under 299 the gravity that is pointing downward with magnitude $g = 9.81m.s^{-2}$. A 300 free fall of the liquid into vacuum would impact at $t_{\text{impact}} = 0.64s$ however 30 due to the presence of the gas this theoretical value is not correct for our 302 simulation however some critical phenomena still occur in the vicinity of 303 this time. As instance around t_{impact} a pocket of gas is trapped under 304 the falling liquid and this strongly impacts the numerical impact pressure 305 by decelerating and damping the free fall of the liquid. Therefore a good 306 interface reconstruction method should qualitatively improve the numerical 307 results. One considers a mesh made of 100×150 uniform cells on the domain. 308 One shows the results for NIP and ENIP at time t = 0.6s Figure 9-(a)-(b) 309 and t = 0.64s in Figure 9-(c)-(d). The classical NIP method was already able 310 to deal with such sliding effects. However the interface reconstruction method 311 employed is not accurate and stable enough to be free of oscillation that 312 one suspects to be only a numerical artifacts (see panels (a-c)). Contrarily 313

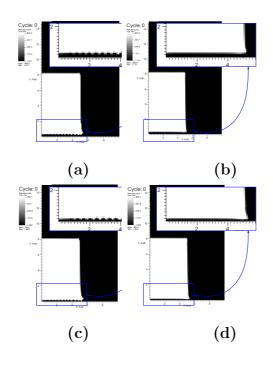


Figure 9: — (a) NIP results at t = 0.6 (full view and zoom on the impact zone) — (b) ENIP results at t = 0.6 — (c) NIP results at t = 0.64 — (d) ENIP results at t = 0.64.

the new reconstruction method ENIP on this very same test case is able to produce a smooth interface that permits to obtain a more realistic simulation. Indeed this simulation prominently displays the fact that the "bubbling" effects of NIP is of pure numerical origin and that ENIP cures this drawback.

319 4. Conclusion and perspectives

This paper deals with the improvement of the so-called NIP (Natural Interface Positioning) method. The NIP method described in [5] is an add-on to the FVCF method in order to treat multi-material fluid flows uses the

concept of condensate. A condensate is the association of contiguous mixed 323 cells in either x or y direction. They are further treated as an entity to 324 make possible the treatment of each mixed cell taken individually. NIP is 325 the method based on the following steps: Representation, Condensate con-326 struction, Condensate evolution, Reconstruction, and Projection. The present 327 paper points the weakness of the NIP method in pure advection context and, 328 consequently, in a full multi-material hydrodynamics one. An enhanced NIP 329 method is proposed (ENIP). It modifies several of the previous listed steps. 330 More precisely the condensate is assumed to evolved in an almost-Lagrangian 33 fashion. The reconstruction step assumes that the condensate keeps the same 332 form modulo some expansion/compression that the numerical scheme already 333 provides. So the displacement of the condensate is performed either with the 334 true computed velocity or with an interpolation of it. In fine the condensate 335 preserves its topology contrarily to the original NIP method for which the 336 condensate has no recollection of its shape from the beginning of the time 337 step. 338

The capability of the full numerical method is now dramatically improved 339 as seen on advection test cases (advection and rigid rotation of a square). 340 Moreover we ran ENIP on a difficult multi-material hydrodynamics tests 341 simulating the free drop of a liquid rectangle within a 2D rectangular tank 342 filled with gas in the context of sloshing that may appear in the tanks of 343 Liquid-Natural-Gas carrier (see [4]). The accuracy, stability and robustness 344 of the ENIP method is clearly seen especially at the time some air is trapped 345 under the water. In the near future we plan to investigate the evolution of 346 this method to the case of mixed cells with more than two materials. In this 34

case the only difficulty lays in the positioning of the different materials in the cell, but their evolution within the condensate follows exactly the same algorithm ENIP with no modification of the numerical scheme. We also plan to investigate the evolution of the method in 3D.

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