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Turbulent Von Kármán flow between two counter-rotating disks

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The present work considers the turbulent Von Kármán flow generated by two coaxial counter-rotating smooth (viscous stirring) or bladed (inertial stirring) disks enclosed by a cylindrical vessel. Numerical predictions based on one-point statistical modeling using a low Reynolds number second-order full stress transport closure (RSM) are compared to velocity measurements performed at CEA. An efficient way to model the rule of straight blades is proposed. The influences of the rotational Reynolds number, the aspect ratio of the cavity, the rotating disk speed ratio and of the presence or not of impellers are investigated to get a precise knowledge of the dynamics and the turbulence properties in the Von Kármán configuration. In particular, we highlighted the transition between the Batchelor [1] and the Stewartson [25] flow structures and the one between the merged and separated boundary layer regimes in the smooth disk case. We determined also the transition between the one cell and the two cell regimes for both viscous and inertial stirrings.

Keywords: Von Kármán flow, counter-rotating disks, turbulence modeling, Reynolds Stress Model

Introduction

The flow between two finite counter-rotating disks enclosed by a cylinder, known as the Von Kármán [27] geometry, is of practical importance in many industrial devices. Counter-rotating turbines may indeed be used to drive the counter-rotating fans in gas-turbine aeroengines. Moreover, this configuration is often used for studying fundamental aspects of developed turbulence and especially of magneto-hydrodynamic turbulence.

From an academic point of view, the laminar flow between two infinite disks has indeed justified many works since the beginning of the controversy between Batchelor [1] and Stewartson [25] on the flow structure. Batchelor [1] solved the system of differential equations

relative to the steady rotationally-symmetric viscous flow between two infinite disks. In the exactly counter-rotating regime, the distribution of tangential velocity is symmetrical about the mid-plane and exhibits five zones: one boundary layer on each disk, a transition shear layer at mid-plane and two rotating cores on either side of the transition layer. As stated by Batchelor himself, "this singular solution may not be realizable experimentally, of course". In 1953, Stewartson [25] found that the flow is divided into three zones for large values of the Reynolds number based on the interdisk spacing H : $Re_H = \Omega H^2/\nu > 100$ (Ω the rotation rate of the disks and ν the kinematic viscosity of the fluid): one boundary layer on each disk separated by a zone of zero tangential velocity and uniform radial inflow. Kreiss and Parter [15]

have proved the existence and non-uniqueness of solutions at sufficiently large Reynolds numbers for the two-disk configuration. Thus, both Batchelor and Stewartson solutions are possible depending on the initial and boundary conditions but the Batchelor prediction has not been mentioned in the literature for the exact counter-rotating disk case. The reader is referred to the work of Holodniok et al. [13] and to the review of Zandbergen and Dijkstra [28] for a more extensive survey until 1987.

In the turbulent case, the Von Kármán flow is a model flow to study the turbulence characteristics on small scales. The main flow is axisymmetric and so offers an interesting intermediate situation between two-dimensional and three-dimensional flows. Maurer et al. [17] established, using low-temperature helium gas, the turbulence characteristics (structure functions, PDF of the velocity differences) and confirmed that turbulence on small scales has universal properties independent of the forcing. Mordant et al. [19] investigated the dynamical behavior of the Von Kármán flow at moderate to high Reynolds numbers using spatially averaged measurements. Data of the power input and of pressure fluctuations at the wall are sufficient to calculate the main turbulence characteristics. Cadot and Le Maître [6] considered the turbulent flow between two counter-rotating stirrers. They measured the instantaneous torques driving the flow and compared them to similarity laws having no dependence on the Reynolds number with a good agreement. Ravelet et al. [22,24] reported experimental evidence of a global bifurcation on a highly turbulent flow between two counter-rotating impellers. The transition between the symmetric and the unsymmetric solutions is subcritical and the system keeps a memory of its history. Monchaux et al. [18] investigated the properties of the mean and most probable velocity fields in the same configuration. They showed that these two fields are described by two families of functions depending on both the viscosity and the forcing. For large values of the Reynolds number, a tendency for Beltramization of the flow is obtained. Boronski [3] simulated the laminar Von Kármán flow between two counter-rotating disks equipped or not by straight blades. For a rotational Reynolds number based on the disk radius R , equal to 500, the poloidal-to-toroidal ratio is increased from 13% in the smooth disk case to 51% in the bladed disk case.

A renewal of interest for the Von Kármán flow is born from the dynamo experiments. The flow between counter-rotating impellers is indeed considered as a possible candidate for the observation of a homogeneous fluid dynamo less constrained than the Riga and Karlsruhe devices. The flow needs to be highly turbulent in order for nonlinearities to develop in the magnetic

induction. Numerous experimental [26] or numerical [4,23] studies have then been dedicated to magneto-hydrodynamics turbulence in the Von Kármán geometry.

To our knowledge, only very few numerical works have been devoted to the characterization of the mean and turbulent flow properties in the Von Kármán geometry. Kilic et al. [14] performed a combined numerical and experimental study of the transitional flow between smooth counter-rotating disks for $-1 \leq \Gamma \leq 0$, $Re = 10^5$ and $G=H/R=0.12$, where Γ is the ratio between the rotating speeds of the two disks and G is the aspect ratio of the cavity. They compared mean radial and tangential velocity measurements using a single-component laser Doppler anemometer with computed results either a classical low-Reynolds number $k-\epsilon$ turbulence model or a laminar elliptic code. For $\Gamma = -1$, the weakly turbulent flow is of Stewartson type, whereas the laminar computations and measurements produce a Batchelor type of flow. The transitions from laminar to turbulent regime and from Batchelor to Stewartson flow structure occur for $\Gamma = -0.4$. A good agreement is obtained in the rotor-stator configuration ($\Gamma = 0$) and in the exactly counter-rotating regime ($\Gamma = -1$) but at intermediate values of Γ , the agreement is less satisfactory.

In this paper, we present comparisons between numerical predictions using a Reynolds Stress Model, denoted RSM, and velocity measurements performed at CEA for the turbulent flow between two counter-rotating disks. The main objective is to acquire a precise knowledge of both the flow structure and the turbulence properties of the high turbulent Von Kármán flow between smooth disks for a large range of the flow control parameters. A second objective is to propose an easy and efficient way to model impellers and to quantify their effect on the Von Kármán flow at high Reynolds number.

Experimental Procedure

Geometrical model

We consider the Von Kármán flow generated by two counter-rotating disks enclosed by a cylindrical vessel, as illustrated in Fig. 1. The cylinder radius and height are respectively, $R_c=100$ mm and $H_c=500$ mm. The radius ratio R/R_c between the rotating disk radius R and the cylinder radius is fixed to 0.925. The distance between the inner faces of the disks H can vary between 10 and 180 mm. We use bladed disks to ensure inertial stirring or flat disks for viscous stirring. The impellers are driven by two independent 1.8 kW motors, with speed servo loop control. The motor rotation rates Ω_1 and Ω_2 can be varied independently in the range 0-900 rpm,

with $|\Omega_1| \geq |\Omega_2|$. The working fluid is water.

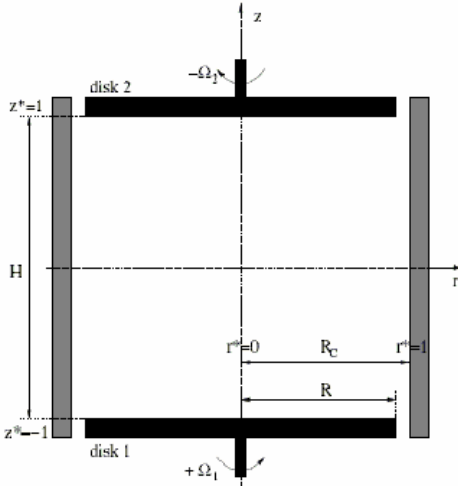


Fig. 1 Sketch of the cavity and relevant notation.

Flow control parameters

The main flow is controlled by the ratio between the two rotation rates $\Gamma = -\Omega_2/\Omega_1$, the aspect ratio of the cavity $G = H/R_c$ and the rotational Reynolds number $Re = \Omega_1 R_c^2/\nu$. In the case of inertial stirring, the number of straight blades n and their dimensionless height $h^* = h/R_c$ are also considered.

Measurement technique

Velocity measurements are done using a laser Doppler velocimetry (LDV). A basic measurement is a two minutes acquisition of 190000 randomly sampled values of one velocity component at one point of the flow. Due to geometry reasons, we have access to the axial V_z and tangential V_θ mean velocity components. From this raw data, one may compute the time-averaged flow point by point on a 11×15 grid.

Statistical modeling

The predictions of the Reynolds Stress Model (RSM) used in the present work have already been validated in the rotor-stator configuration ($\Gamma = 0$) [10,21] for a wide range of aspect ratio G and Reynolds number Re . It showed that this level of closure is adequate in such flow configurations, while the usual $k-\varepsilon$ model, which is blind to any rotation effect presents serious deficiencies. Thus, the purpose of this paper relying on a well established turbulent model is to extend its application to new flow conditions and to get a better insight into the dynamics of the highly turbulent Von Kármán flow. The reader is thus referred to [9,10,20,21] for more details about the model and the numerical method.

The differential Reynolds Stress Model (RSM)

The flow studied here presents several complexities (high rotation rate, wall effects, transitional zone, shear layer), which are severe demands for turbulence modeling methods. Our approach is based on one-point statistical modeling using a low Reynolds number second-order full stress transport closure derived from the Launder and Tselepidakis [16] model and sensitized to rotation effects [10]. This approach allows for a detailed description of near-wall turbulence and is free from any eddy viscosity hypothesis. The general equation for the Reynolds stress tensor R_{ij} can be written:

$$\frac{dR_{ij}}{dt} = P_{ij} + D_{ij} + \Phi_{ij} - \varepsilon_{ij} + T_{ij} \quad (1)$$

where P_{ij} , D_{ij} , Φ_{ij} , ε_{ij} and T_{ij} respectively denote the production, diffusion, pressure-strain correlation, dissipation and extra terms. The diffusion term D_{ij} is split into two parts: a turbulent diffusion D_{ij}^T , which is interpreted as the diffusion due to both velocity and pressure fluctuations and a viscous diffusion D_{ij}^V , which cannot be neglected in the low Reynolds number region. In a classical way, the pressure-strain correlation term Φ_{ij} can be decomposed as below:

$$\Phi_{ij} = \Phi_{ij}^{(1)} + \Phi_{ij}^{(2)} + \Phi_{ij}^{(w)} \quad (2)$$

$\Phi_{ij}^{(1)}$ is interpreted as a slow nonlinear return to isotropy and is modeled as a quadratic development in the stress anisotropy tensor, with coefficients sensitized to the invariants of anisotropy. This term is damped near the wall. The linear rapid part $\Phi_{ij}^{(2)}$ includes cubic terms. A wall correction $\Phi_{ij}^{(w)}$ is applied to the linear part which is modeled using the Gibson and Launder hypothesis [12] with a strongly reduced numerical coefficient. However the widely adopted length scale $k^{3/2}/\varepsilon$ is replaced by the length scale of the fluctuations normal to the wall. The viscous dissipation tensor has been modeled in order to conform with the wall limits obtained from Taylor series expansions of the fluctuating velocities. The extra term T_{ij} accounts for implicit effects of the rotation on the turbulence field. It contains additional contributions in the pressure-strain correlation, a spectral jamming term, inhomogeneous effects and inverse flux due to rotation, which impedes the energy cascade [7].

The dissipation rate ε equation to solve is the one proposed by Launder and Tselepidakis [16]. The turbulence kinetic energy k equation which is redundant in a

RSM model is still solved, in order to get faster numerical convergence. It is verified that after convergence the turbulence kinetic energy is exactly equal to $R_{jj}/2$.

Numerical method

The computational procedure is based on a finite volume method using staggered grids for mean velocity components with axisymmetry hypothesis in the mean. The computer code is steady elliptic and the numerical solution proceeds iteratively. We have verified that a 120^2 mesh in the (r,z) frame is sufficient in smooth rotating disk cases to get grid-independent solutions. A refined mesh 160^2 is necessary to model flows with straight blades. It is to be compared to the 140×80 mesh used by Elena and Schiestel [9,10] and Poncet et al. [20,21] in rotor-stator systems. The calculation is initialized using realistic data fields, which satisfy the boundary conditions. About 20000 iterations (several hours on the bi-Opteron 18 nodes cluster of IRPHE) are necessary to obtain the numerical convergence of the calculation. The stress component equations are solved using matrix block tridiagonal solution to enhance stability using non staggered grids.

Boundary conditions

At the wall, all the variables are set to zero except for the tangential velocity V_θ , which is set to $\Omega_1 r$ on disk 1, $-\Omega_2 r$ on disk 2 and zero on the cylinder. At the periphery of the disks ($R \leq r \leq R_c$) V_θ is supposed to vary linearly from zero on the cylinder up to $\Omega_1 R$ on disk 1 and $-\Omega_2 R$ on disk 2 and the radial V_r and axial V_z velocity components are fixed to zero.

We can not implement real straight blades in our two-dimensional code. So we limit to modeling their most important effect, which is to increase the efficiency of the disks in forcing the flow. Thus, we add a volumic drag force f in the equation of the tangential velocity component V_θ . If we consider n straight blades, the volumic drag force f can be written as:

$$f = \frac{n}{2\pi} \frac{F}{r} = \frac{n}{4\pi} \frac{\rho}{r} C_D |V_{rel}| V_{rel} \quad (3)$$

where F is the drag force of one blade, ρ the fluid density, C_D the dimensionless drag coefficient and $V_{rel} = \Omega_1 r - V_\theta$ the relative tangential velocity on disk $i=1,2$. The force is designed to make the fluid velocity closer to the local disk velocity near the disks. This form is close to the one proposed by Boronski [3] for spectral code. For curved blades, the same approach can be used: a volumic lift force can be added in the equation of the radial velocity V_r . It will be the subject of a next study.

Some calculations have been performed for $\Gamma = -1$,

$G=1.8$, $Re = 2.10^5$ and straight blades ($h^*=0.2$, $n=8$) to study the influence of the trailing coefficient C_D . The differences on the extrema of the tangential velocity component are inferior to 0.5% for C_D in the range $[0.1-2]$. Thus, we have chosen to fix the value of C_D equal to 0.5, which agrees with the values proposed by Blevins [2] in the case of a thin rectangular plate perpendicular to an uniform flow.

Smooth disk case: viscous stirring

In this section, we consider the turbulent flow between two counter-rotating flat smooth disks. Thus, we ensure a viscous stirring and we investigate the influence of the Reynolds number Re , the aspect ratio of the system G , and the ratio Γ between the two rotation rates on the mean and turbulent fields.

Flow structure in the exact counter-rotating regime

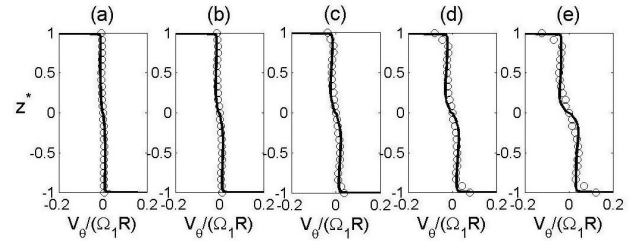


Fig. 2 Axial profiles of the tangential velocity for $\Gamma=-1$, $Re = 6.28 \times 10^5$ and $G=1.8$ at (a) $r^*=0.35$, (b) $r^*=0.48$, (c) $r^*=0.61$, (d) $r^*=0.74$, (e) $r^*=0.87$. Comparisons between the numerical results (lines) and the experimental data (symbols) in the smooth disk case.

The structure of the mean flow in the exact counter-rotating regime is henceforth globally well known: it can be decomposed into two toroidal cells in the tangential direction (not modelled here because of the axisymmetry hypothesis) and into two poloidal recirculations in the (r,z) plane. We focus here on the poloidal cells (Fig.6a): the fluid at the top and the bottom of the cavity is forced into two opposite rotation speeds, and is then entrained by the disks. Consequently, a shear layer develops in the equatorial plane. This is perceptible in Fig.2, which presents axial variations of the tangential velocity component for $\Gamma = -1$, $Re = 6.28 \times 10^5$, $G=1.8$ at five radial locations in the range $r^*=0.35-0.87$. The radial and axial velocity components are not presented here because they are almost zero in the whole cavity both in the experiments and in the calculations. The tangential component is quite weak too except in the two very thin boundary layers, which develop on each disk and whose size is shown in Fig.3 and close to the periphery, where the shear layer is observed.

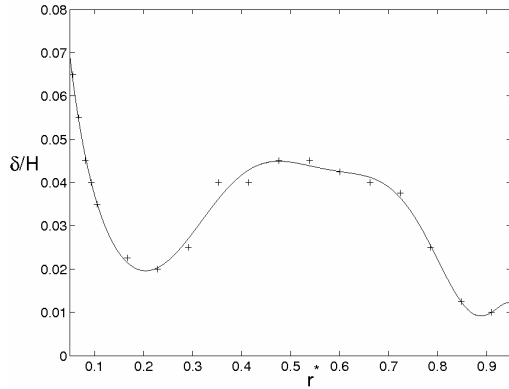


Fig. 3 Radial distribution of the boundary layer thickness δ/H (symbols: RSM, lines: polynomial interpolation). See legend Fig.2.

For $r^* < 0.48$ (Fig.2a), the profile exhibits a Stewartson flow structure: a quasi zero tangential velocity zone enclosed by two boundary layers on each disk. The flow in the boundary layers is characterized by a strong tangential velocity component (positive on disk 1 and negative on disk 2) and by a radial outward component not shown here. Towards the periphery (Fig.2b-e), the flow gets of Batchelor type with five distinct zones: two boundary layers on the disks, a shear layer at mid-plane and two zones enclosed between the two. These last two zones are characterized by a weak but non zero tangential velocity component. The shear layer thickens when the local radius r^* increases. Contrary to the laminar case reported by Kilic et al. [14], there is practically no radial inflow around $z^*=0$. A good agreement between the numerical results and the experimental data is obtained even the values are quite weak. The RSM model catches the appearance and the thickening of the shear layer. The agreement between the numerical predictions and the measurements is less satisfactory in the boundary layers as it can be seen Fig.2. These zones are in fact hardly attainable by LDV measurements.

The transition between the Stewartson and Batchelor flow structures can also be seen in Fig.3 from the radial evolution of the boundary layer thickness δ for the same set of parameters. Very close to the rotation axis, the axial flow impinges the disks and creates very large boundary layers on both disks, whose size decreases with the local radius. The flow is then of Stewartson type. During the transition, δ increases as already observed by Poncet [20] for rotor-stator flows ($\Gamma = 0$). For $r^* \approx 0.47$, the flow is clearly of Batchelor type and then, δ decreases towards the periphery of the cavity.

We investigate the influence of the Reynolds number on the mean flow. Fig.4 presents radial profiles of the tangential velocity component for $\Gamma = -1$, $G=1.8$ and four Reynolds numbers at different axial locations. The nu-

merical predictions of the RSM model are compared to present LDV measurements and to the velocity measurements of Ravelet [22] for $Re \geq 10^5$. These data are also compared to the local disk 1 and disk 2 velocities.

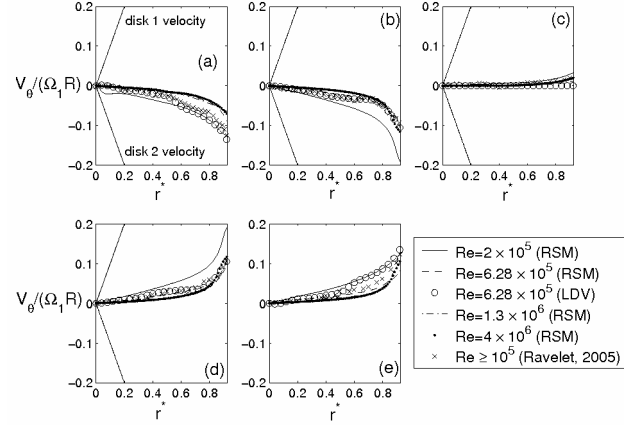


Fig. 4 Radial profiles of the tangential velocity for $\Gamma=-1$ and $G=1.8$ at (a) $z^*=0.91$, (b) $z^*=0.59$, (c) $z^*=0.02$, (d) $z^*=-0.59$, (e) $z^*=-0.92$.

The numerical data for $Re \geq 6.28 \times 10^5$ merge almost into a single fitting curve. It means that there is practically no effect of the Reynolds number on the mean field ever since the flow is turbulent. For $Re = 2 \times 10^5$, a significant increase of the magnitude of V_θ is observed whatever the axial position, which is characteristic of the laminar regime. The critical Reynolds number for the transition from the laminar to the turbulent state is thus overestimated compared to the one obtained by Ravelet [22]: $Re = 10^5$. Nevertheless, the present velocity measurements performed on the same experimental set-up as [22] confirm the numerical results. Compared to the previous measurements, an effect of Re is observed on the radial profiles of V_θ at the periphery of the cavity. In fact, the critical Reynolds number for the laminar to turbulent state transition depends strongly on the boundary conditions and especially on the conditions imposed in the radial gap. We recall that a linear profile is imposed in the numerical code for V_θ , that does not take into account any recirculation zone and that could explain this difference. This tendency for relaminarization of the RSM model has already been noticed by Poncet et al. [20,21] in the rotor-stator configuration. As a conclusion, there is no significant effect of the Reynolds number on the mean flow for $Re \geq 10^5$, which confirms the results of Cadot et al. [5] and Ravelet [22].

Fig.6a presents the corresponding streamline patterns. The mean flow is divided into two symmetric poloidal cells, whose size is equal here to $0.5 H$ along the axial

direction and independent of the Reynolds number. In the radial direction, the diameter of the largest eddies observed is of the order of the disk radius R , showing this scale is the order of the energy scale injection.

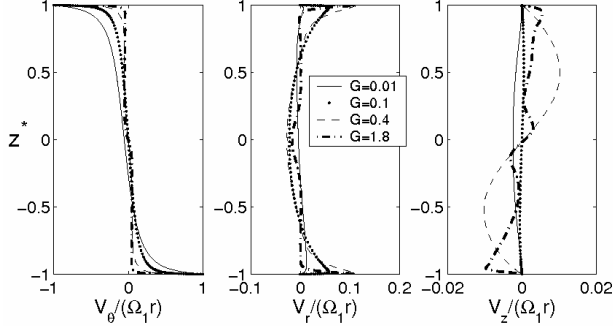


Fig. 5 Axial profiles of the mean velocity components for $r^*=0.81$, $\Gamma=-1$, $Re = 1.3 \times 10^6$ and viscous stirring (RSM).

The influence of the aspect ratio of the cavity G on the mean field has also been investigated for $G=[0.01;1.8]$ (Fig.5) and a given Reynolds number $Re = 1.3 \times 10^6$. For $G=1.8$, the boundary layers are separated as already mentioned and the mean tangential velocity component is constant in the core of the flow. When one decreases the aspect ratio, the flow gets of torsional Couette type with merged boundary layers. For $G=0.01$, V_θ (Fig.5a) varies indeed linearly in the median region of the flow. The transition between the merged and the separated boundary layer regime occurs for $G=0.4$. This is to be compared to the value $G=0.012$ obtained in the rotor-stator configuration [21]. The transition is continuous and not clear from the V_θ -profile. Nevertheless, if we consider the V_z -profile (Fig.5c), we can clearly see that the axial velocity component is almost zero whatever the value of G , expect for $G=0.4$, where the fluid moves towards the upper and lower disks. The transition can also be characterized by considering the V_r -profiles (Fig.5b), which exhibit the thinning of the boundary layers for increasing values of the aspect ratio.

Flow structure for $-1 \leq \Gamma \leq 0$

Another interesting feature in counter-rotating disk flows is the influence of the ratio Γ between the two rotating disk speeds (Fig.6). The Reynolds number and the aspect ratio of the cavity are respectively fixed to $Re = 1.3 \times 10^6$ and $G=1.8$. We focus on the counter-rotating disk case for which $\Gamma = [-1; 0]$. In the exact counter-rotating regime (Fig.6a), the flow is symmetric and two cells with the same size $0.5 H$ coexist. For small rotating speed differences, the structure of the

mean flow is strongly dominated by the faster disk (Fig.6b-e). Varying the ratio Γ displaces the shear layer towards the slower disk. The cell close to the lower disk invades almost the whole interdisk spacing for $\Gamma=-0.7$ (Fig.6d). For $\Gamma=-0.2$ (Fig.6e), the flow structure resembles the one observed in the rotor-stator configuration [20] with streamline patterns parallel to the rotating axis.

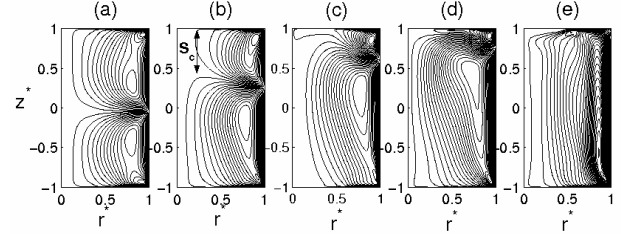


Fig. 6 Computed streamlines patterns between smooth disks for $G=1.8$, $Re = 1.3 \times 10^6$ and (a) $\Gamma=-1$, (b) $\Gamma=-0.9$, (c) $\Gamma=-0.8$, (d) $\Gamma=-0.7$, (e) $\Gamma=-0.2$.

This transition between the two cell and the one cell regimes can be seen also from Fig.7. It presents the evolution with Γ of the dimensionless size S_c/H of the smallest cell (along the upper disk) in the axial direction defined in Fig.6b. In the smooth disk case, we notice that S_c decreases rapidly for decreasing values of $|\Gamma|$ in the range $[-1; -0.8]$ following $S_c/H \propto -2.2\Gamma$. For smallest values of $|\Gamma|$, the cell is reduced to a very thin region attached to the upper disk (Fig.6d-e), which disappears progressively along the external cylinder and so S_c tends to zero.

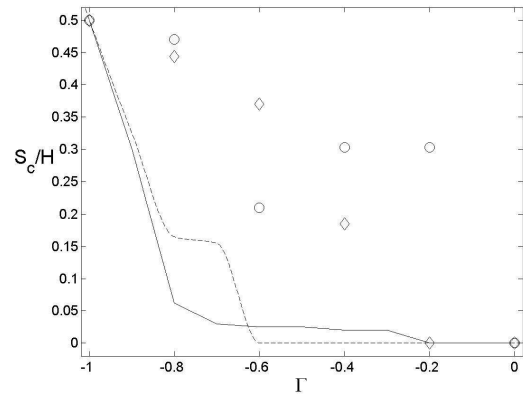


Fig. 7 S_c/H against Γ for $G=1.8$ (RSM). Comparisons between the (—) smooth disk case ($Re = 1.3 \times 10^6$), the (---) bladed disk case and previous results of (o) Kilic et al. [14] and (◇) Gan et al. [11].

In Fig.7, our results are compared to the ones obtained by Kilic et al. [14] and Gan et al. [11], who performed calculations for $\Gamma = [-1; 0]$ and $G=0.12$ using a classical

k - ϵ turbulence model. For $Re = 10^5$, Kilic et al. [14] found that the evolution of S_c against Γ is non monotonous. It decreases more slowly from $\Gamma=-1$ to $\Gamma=-0.2$ than in our case. It is a combined effect of both the Reynolds number and the aspect ratio of the cavity. For $\Gamma=-0.4$, they observed a double transition: from laminar to turbulent flow and from Batchelor to Stewartson type of flow. The decrease of S_c is much faster with Γ in the laminar case [14]. For $Re = 1.25 \times 10^6$, Gan et al. [11] obtained streamline patterns different from the ones shown in Fig.6 for $\Gamma = [-0.8; -0.2]$ essentially because of the small value of G . A large cell along the slower disk is still observed for $\Gamma=-0.4$. This cell is trapped by the main flow due to the faster disk in the zone $r^*=0.3-0.45$.

Turbulence field in the exact counter-rotating regime

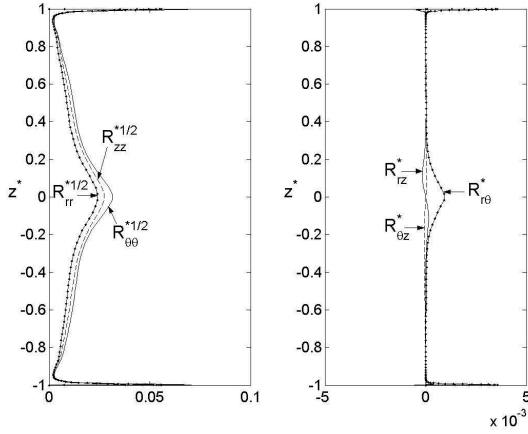


Fig. 8 Axial profiles of the Reynolds stress tensor at $r^*=0.81$ for $\Gamma=-1$, $G=1.8$ and $Re = 6.28 \times 10^5$ in the smooth disk case (RSM).

As already mentioned below, there is practically no effect of both the Reynolds number and the aspect ratio on the mean flow. In the following, we focus on the exact counter-rotating regime $\Gamma=-1$ and Re and G are fixed respectively to $Re = 6.28 \times 10^5$ and $G=1.8$. Fig.8 presents the axial profiles of the six components of the Reynolds stress tensor. These components are normalized by the local disk 1 velocity. For example, R_{rr}^* is defined as: $R_{rr}^* = \overline{v_r^2} / (\Omega_1 r)^2$. As in all rotating disk problems [21], turbulence is mainly concentrated in the boundary layers with the same turbulence levels in the upper and lower disk boundary layers. The main difference with the rotor-stator configuration is that turbulence is also generated in the median region of the interdisk spacing and is due to the shear, stretched by the recirculations. The Von Kármán arrangement is indeed known to

produce an intense turbulence in a compact region of space [17]. The magnitudes of the three normal components (in principal axes) are almost the same in the equatorial plane. It means that turbulence is quasi isotropic in that region. The cross components are quite weak except for the $R_{r\theta}^*$ component, which behaves like the normal components with a bump at mid-plane.

Bladed disk case: inertial stirring

To increase the efficiency of the disks in forcing the flow, we used n blades of height h^* mounted on both disks. The stirring is called inertial because the fluid is set into motion thanks to areas of forcing perpendicular to the motion itself. In that case, Ravelet [22] showed that all mean and turbulent quantities are independent of the Reynolds number in the range $Re = [10^5, 2 \times 10^6]$.

Thus, we have chosen to fix the values of $Re = 2 \times 10^5$ and $G=1.8$. In that case, the boundary layers are separated and the flow is found to be highly turbulent. Moreover, direct comparisons with the experiments of Ravelet [22] can be performed. The purpose of this section is to propose an efficient way to model the effect of straight blades on both the mean and turbulent fields.

Flow structure in the exact counter-rotating regime

In the bladed disk case, the flow structure is completely different from the smooth disk case, where the velocity gradient are located in the boundary layers along the disks and decrease when the Reynolds number increases. For an inertially driven flow, the mean flow does not present any appreciable velocity gradient in the vicinity of the blades (Fig.9) and the gradients are distributed in the median region of the flow. The mean flow is divided into three main regions: a shear layer at mid-plane and two fluid regions close to each bladed disk. The intensity of the shear at mid-plane is increased compared to the viscous stirring case. This shear is due to the two recirculation cells. It induces a strong radial inflow ($V_r < 0$) around $z^*=0$ and two opposite axial flows towards the disks. The magnitude of the mean axial and radial velocity components increase from the periphery (Fig.9c) to the rotation axis (Fig.9a). From the disk to the top of the blades, the tangential fluid velocity is fairly close to the local disk velocity. Moreover, a strong radial outflow is created along the bladed disks and goes with the impellers. At the top of the blades, there is a strong decrease of $|V_\theta|$ interpreted as the wake of the blades.

There is a very good agreement between the numerical predictions and the velocity measurements concerning the V_θ -profiles. A small difference is observed in the shear layer, where the RSM model predicts a thinner

layer than the one measured by Ravelet [22]. This last author observed, for the same set of parameters, high energy levels for frequencies inferior to the injection frequency. This contribution is attributed to the appearance of strong coherent structures in the shear layer not observed in the smooth disk case and which may explain the weak discrepancies obtained.

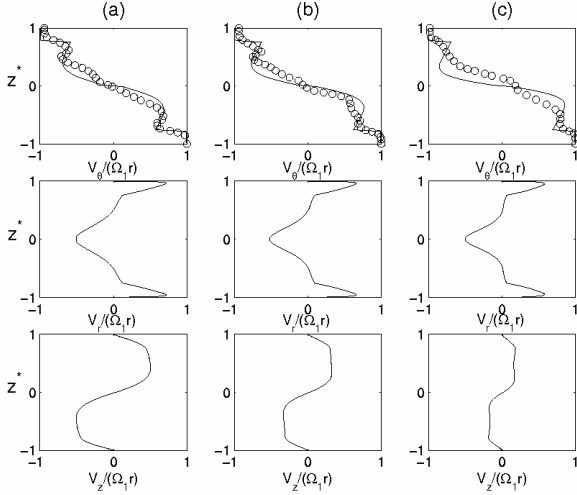


Fig. 9 Axial profiles of the mean velocity components for $\Gamma=-1$, $G=1.8$ and $Re = 2 \times 10^5$ and bladed disks ($n=8$, $h^*=0.2$) at (a) $r^*=0.4$, (b) $r^*=0.5$, (c) $r^*=0.6$. Comparisons between the numerical predictions (lines) and the LDV data of Ravelet [22] (symbols).

Flow structure for $-1 \leq \Gamma \leq 0$

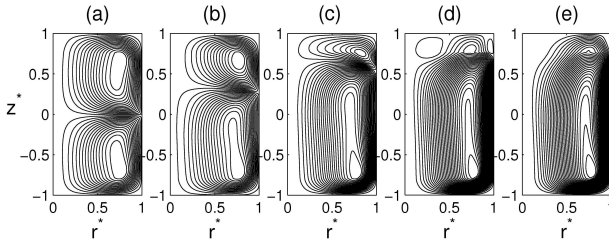


Fig. 10 Computed streamlines patterns between bladed disks ($n=8$, $h^*=0.2$) for $G=1.8$, $Re = 2 \times 10^5$ and (a) $\Gamma=-1$, (b) $\Gamma=-0.9$, (c) $\Gamma=-0.8$, (d) $\Gamma=-0.7$, (e) $\Gamma=-0.6$.

We perform the same analysis as in the smooth disk case by varying the ratio Γ between the two rotating disk speeds. Fig.10 presents comparisons between the smooth and bladed disk cases concerning the size S_c of the cell along the slowest disk for $\Gamma = [-1; 0]$. The same behavior is obtained but the transition between the two cell and the one cell structures ($S_c \rightarrow 0$) is slightly delayed. It occurs in the inertial stirring case for $\Gamma = -0.65$, which is close to the experimental value obtained by Cadot and Le Maître [6] in the same configuration $\Gamma=-0.69$ and the analytical

one obtained by Dijkstra and Van Heijst [8] for $Re \rightarrow 0$ in the smooth disk case $\Gamma = -2/3$. The measurements of Ravelet [22] reveal a transition for $\Gamma = -0.78$. It confirms the similitude observed by [6] between the smooth disk flow with a large viscosity and the mean flow in the inertial stirring case.

The transition from the two cell to the one cell structures can be seen also from Fig.7 Compared to the smooth disk case, the cell along the slowest disk is larger for $\Gamma=-0.8$ (Fig.10c). For $\Gamma=-0.7$, only a small recirculation subsists along the upper disk and completely disappears for $\Gamma=-0.6$. For $\Gamma \geq -0.6$, the same pattern is observed with streamlines parallel to the rotation axis.

Turbulence field in the exact counter-rotating regime

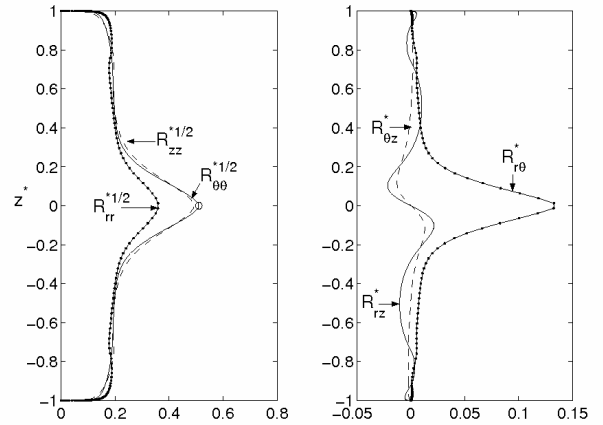


Fig. 11 Axial profiles of the Reynolds stress tensor at $r^*=0.81$ for $\Gamma=-1$, $G=1.8$ and $Re = 2 \times 10^5$ and bladed disks ($n=8$, $h^*=0.2$). (lines) RSM and (o) LDV data [22].

To enable direct comparisons with the viscous stirring case, Fig.11 presents the axial profiles of the six components of the Reynolds stress tensor at the same radius $r^*=0.81$ and for the same values of G and Γ . The main difference between the smooth and the bladed disk configurations is that, in the latter case, the turbulence intensities vanish towards the disks. Apart from that, turbulence is also mostly generated at mid-plane because of the shear stretched by the recirculations. The blades induce a much stronger shear zone in the equatorial plane compared to the smooth disk case as already seen from the mean velocity profiles (Fig.9). Thus, the turbulence levels, regarding the normal Reynolds stress components (Fig.11), are almost 20 times larger than for viscous stirring and quite comparable to the mean fluid velocity. It confirms the previous measurements of Cadot et al. [5] in steady regimes of turbulence in the Von Kármán geometry. They found that the fluid velocity fluctuations are close to the fluid mean velocity and 6 times larger in the

bladed disk case than in the smooth disk case. In the present study, the R_{rr}^* component is much weaker than the two other normal components, which indicates the turbulence anisotropy in the core of the flow. The cross components are also stronger than in the smooth disk case. The level of the $R_{r\theta}^*$ component (Fig.11) is of the order of R_{rr}^* . Note that the maximum of the $R_{\theta\theta}^*$ component obtained at mid-plane ($z^*=0$) using the RSM model is in excellent agreement with the asymptotic value measured by Ravelet [22] for Re larger than 10000 (relative error inferior to 0.1%).

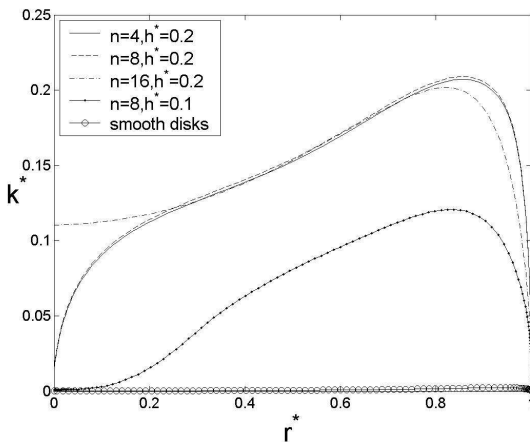


Fig. 12 Radial profiles of the turbulence kinetic energy k^* at $z^*=0$ for $\Gamma=-1$, $G=1.8$ and $Re = 2 \times 10^5$ (RSM).

To study the influence of the number n of blades and their height h^* on the turbulent field, Fig.12 shows radial profiles of the turbulence kinetic energy k^* normalized by $(\Omega_1 R_c)^2$ for various impeller configurations. These profiles are plotted at mid-plane where the maximum of k^* prevails. As expected, k^* increases towards the periphery of the cavity, it means for increasing local Reynolds number. Then, k^* decreases for radial locations in the gap between the disks and the external cylinder. We can first notice the very weak level of turbulence kinetic energy in the smooth disk case compared to the bladed disk cases. Secondly, the influence of the blade number n is quite weak for $n=4, 8$ or 16 . Only very close to the rotation axis, we can notice a different behavior in the configuration with 16 blades. Nevertheless, in the whole flow, four blades seem to be sufficient to force the flow. On the other hand, the blade height h^* plays a more important role. The k^* level is twice higher when the blades are twice higher too. Ravelet [22] showed that all mean and turbulent quantities are independent of the Reynolds number in the range $Re = [10^5, 2 \times 10^6]$. The turbulent dissipation is indeed much stronger than the dissipation

due to the boundary layers and hides the dependence on Re . All these results can thus be extended to higher Reynolds numbers.

Conclusion

We have performed some comparisons between numerical predictions using a RSM model and velocity measurements considering the turbulent flow between two flat or bladed counter-rotating disks. This configuration known as the Von Kármán geometry is used to produce an intense turbulence in a compact region of space.

For viscous stirring, the flow is of Stewartson type close to the rotation axis and so exhibits three distinct regions: two boundary layers and one shear layer at mid-plane. When one approaches the periphery of the cavity, for $r^* \approx 0.48$, the flow gets of Batchelor type. Turbulence is mainly concentrated in the boundary layers and in the transitional shear layer, where turbulence is almost isotropic. Turbulence intensities increase towards the outer cylinder. While the aspect ratio of the cavity G is lower than 0.4, the boundary layers are mixed and the flow is then of torsional Couette type. In the case of inertial stirring, the impellers are more efficient to force the flow. Thus, the transitional shear layer intensifies. Turbulence is so mainly concentrated around $z^*=0$ and vanish towards the disks. The turbulence intensities are almost 20 times larger than in the flat disk case. The height of the blades is found to be the preponderant parameter to increase the turbulence intensities more than the number of blades. In the flat and bladed disk cases, we have numerically verified the statement of Cadot et al. [5]: "smooth or rough, the efficiency of a given type of stirrer to set the bulk of the fluid in motion is independent of the Reynolds number". Moreover, we have characterized the transition between the two cell and the one cell regimes. For inertial stirring, it occurs for $\Gamma \approx -0.65$ close to the values obtained by [6,8].

The agreement between the numerical predictions and the LDV measurements is very satisfactory in both cases. For the first time, an easy and efficient way to model the main effect of straight blades has been proposed. Further experimental works are now required to provide more comparisons for the turbulent fields but also some calculations for curved blades.

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