

Fig. 1



**Fig. 2** 



Fig. 3



Fig. 4



**Fig. 5** 



Fig. 6



Fig. 7



Fig. 8

B/AI*	BET Specific Surface Area (SSA; m <sup>2</sup> .g <sup>-1</sup> )	Water Pore Volume (PV; cm <sup>3</sup> .g <sup>-1</sup> )	BJH Pore Volume (PV; cm <sup>3</sup> .g <sup>-1</sup> )	Average Pore Diameter** (APD; nm)	Total Acidity*** (mmol.g <sup>-1</sup> )	Proportion of strong acid sites**** (%)
0	363	1.9	0.84	9.3	1.58	85.9
0.02	474	1.95	0.78	6.4	2.26	69.5
0.04	532	1.9	0.82	6.1	2.51	64.2
0.08	554	1.75	0.8	5.6	1.85	58.2
0.20	485	1.55	0.59	4.6	2.07	65.8
0.32	510	1.55	0.66	4.9	2.65	67.7
0.49	616	1.35	0.87	5.2	2.42	56.7
0.61	606	2.6	1.22	6.8	4.09	65.2

Table 1 Textural and acidic properties of the sol-gel prepared B-Al<sub>2</sub>O<sub>3</sub> supports

\* Corrected for nominal B/AI ratios larger than 0.15 (see Ref. [36] and section 2.1 in the text).

\*\* Calculated using the BET SSA and BJH PV.

\*\*\* Total amount of adsorbed NH<sub>3</sub> on each catalyst.

\*\*\*\* Ratio of strong acidity relative to the total acidity. Strong acidity was defined as the area of the high temperature peak at about 523 K.

	BET Specific Surface Area		BJH Pore Volume (PV)		Average Pore Diameter	
Corrected	(SSA)				(APD**)	
B/AI*	(m <sup>2</sup> .g <sup>-1</sup> )	Ratio*** (-)	(cm <sup>3</sup> .g <sup>-1</sup> )	Ratio*** (-)	(nm)	Ratio*** (-)
0	387	1.1	0.63	0.71	6.5	0.70
0.02	368	0.78	0.59	0.76	6.4	1.00
0.04	391	0.47	0.54	0.41	5.5	0.90
0.08	358	0.65	0.46	0.58	5.1	0.91
0.20	345	0.71	0.44	0.75	5.1	1.11
0.32	365	0.72	0.49	0.74	5.4	1.10
0.49	341	0.56	0.51	0.60	6.0	1.15
0.61	342	0.56	0.77	0.63	9.0	1.32
IRC****	271	-	-	-	7.6	-

**Table 2** Physical properties of the CoMo/B-Al<sub>2</sub>O<sub>3</sub> oxidic precursors

\* See the first footnote of Table 1.

\*\* Calculated using the BET SSA and BJH PV.

\*\*\* Ratio relative to that of the corresponding  $B-AI_2O_3$  support.

\*\*\*\* Industrial reference catalyst.

Corrected	HDS Rate	Product Distribution					
B/AI* (x	$(x \pm 10^8 \text{ mol goot o}^{-1})$	Cia but $2 \text{ and } (9/)$	But-1-ene +	$Butana\left( 0/\right)$			
	(x to mongeans )	CIS-Dut-2-ene (%)	Trans-but-2-ene (%)	Butarie (%)			
0	120	40.3	18	41.7			
0.02	186	29.9	27.6	42.5			
0.04	191	34.7	31.7	33.6			
0.08	176	31.9	29.6	38.5			
0.20	167	34.7	31.7	33.6			
0.32	137	39.2	33.5	27.3			
0.49	128	44.8	34.9	20.3			
0.61	108	41.4	37.5	21.1			
IRC	135	39.7	21.8	38.5			

## Table 3 Catalytic activities in HDS of thiophene

\* See the first footnote of Table 1.

Corrected	HDS Pate	Product Distribution						
B/AI*	$(x \ 10^6 \ \text{mol.gcat}^{-1}.\text{s}^{-1})$	Biphenyl (%)	Cyclohexylbenzene (%)	4H-DBT** (%)	6H-DBT***(%)			
0	4.30	90.6	7.4	1.8	0.2			
0.02	5.79	92.9	6.1	1	< 0.2			
0.04	6.05	93.1	5.8	1.1	< 0.2			
0.08	4.22	94.1	4.5	1.4	< 0.2			
0.20	3.37	94.1	4	1.9	< 0.2			
0.32	2.94	92.4	4.8	2.8	< 0.2			
0.49	2.85	90.2	6.1	3.7	< 0.2			
0.61	1.66	89.7	6.2	4.1	< 0.2			
IRC	3.57	76.2	22.5	1.1	0.2			

## Table 4 Catalytic activities in HDS reactions of DBT

\* See the first footnote of Table 1.

\*\* 4H-DBT: tetrahydrodibenzothiophene.

\*\*\* 6H-DBT: hexahydrodibenzothiophene.

Corrected	HDS Rate Product Distribution					
	(x 10 <sup>6</sup> mol.gcat⁻	3,3'-DMCHB**	3,3'-DMBP***	4H-4,6-	Cracking	Ratio
D/AI	<sup>1</sup> .s <sup>-1</sup> )	(%)	(%)	DMDBT**** (%)	Products (%)	Toluene / MCH
0	0.628	86.3	5.8	0.7	7.2	1.08
0.02	0.483	84	9.4	1.3	5.3	1.11
0.04	0.288	82.3	8.9	1.9	6.9	1.16
0.08	0.108	50.1	2.4	2.9	44.5	1.21
0.20	0.174	58.2	8.4	3.9	29.6	1.34
0.32	0.269	56.8	7.0	4.7	31.5	1.46
0.49	0.133	51.8	5.8	3.9	38.6	1.53
0.61	0.204	57.9	7.3	1.9	32.9	1.47
IRC	0.831	88.4	11.3	0.3	0	-

Table 5 Catalytic activities in HDS reactions of 4,6-DMDBT

\* See the first footnote of Table 1.

\*\* 3,3'-Dimethylcyclohexylbenzene. Including trace amounts of 3,3'-Dimethylbicyclohexyl (3,3'-DMBCH).

\*\*\* 3,3'-Dimethylbiphenyl.

\*\*\*\* Tetrahydro-4,6-dimethyldibenzothiophene. Including trace amounts of hexahydro-4,6-dimethyldibenzothiophene (6H-4,6-DMDBT) (less than an absolute value of ~ 0.2 %).