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Stéphane Abanades, Stéphane Grief

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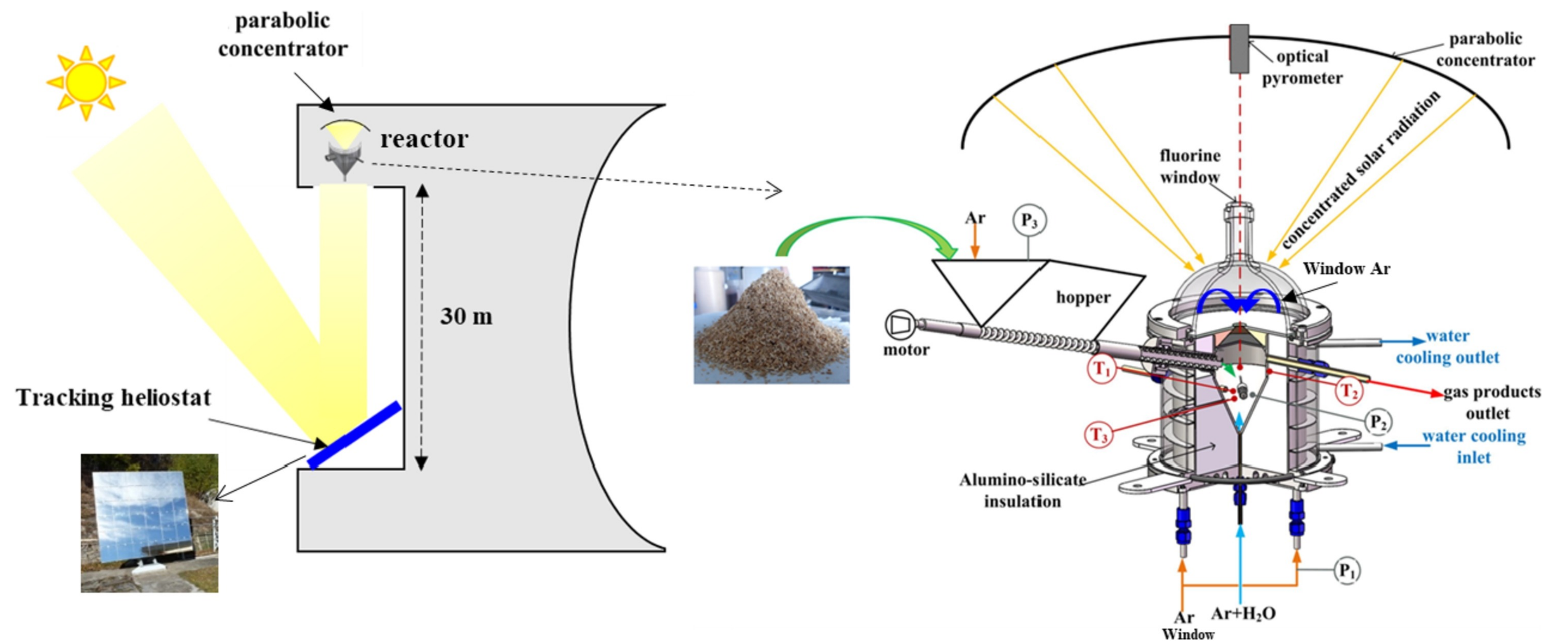
Model-based predictive control of a solar reactor dedicated to syngas production

Youssef Karout, Axel Curcio, Julien Eynard, Stéphane Thil, Sylvain Rodat, Stéphane Abanades, and **Stéphane Grieu**
PROMES-CNRS laboratory (UPR 8521), University of Perpignan Via Domitia



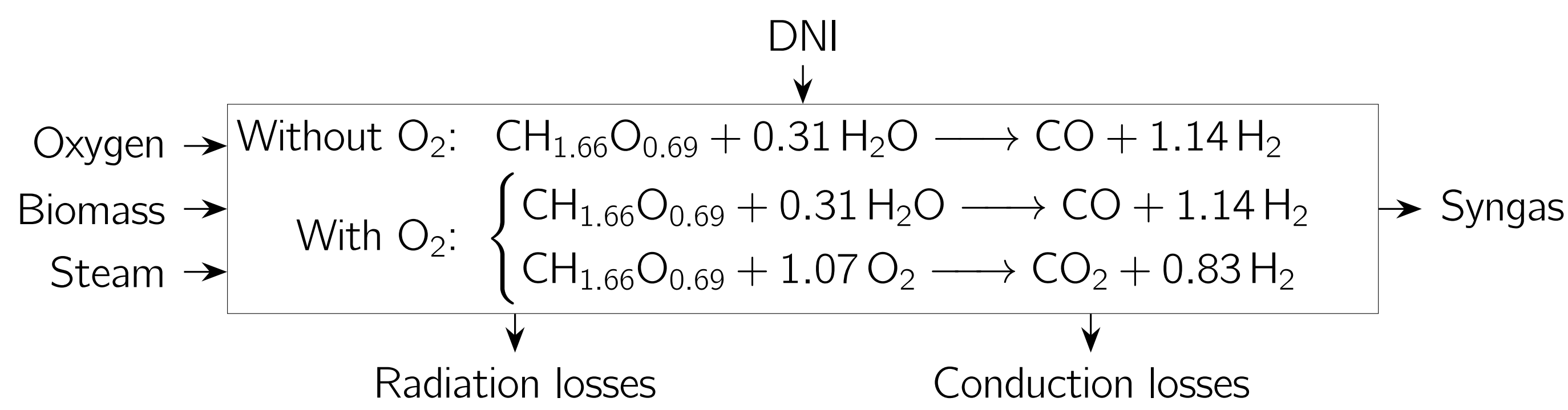
Solar reactor for syngas production

- ▶ A solar spouted-bed gasifier has been conceived by Bellouard et al. [1], and its hybrid solar-autothermal operation has been investigated by Boujjat et al. [2] and Curcio et al. [3].
- ▶ This work aims at conciliating the solar-autothermal hybrid control strategy of a gasifier with the efficient implementation of a model-based predictive control (MPC) algorithm.
- ▶ Goal: maintain reactor's temperature to ensure its stability and optimal chemical reactions.



- [1] Q. Bellouard et al. "Biomass Gasification in an Innovative Spouted-Bed Solar Reactor: Experimental Proof of Concept and Parametric Study". In: Energy Fuels 31.10 (Sept. 2017).
[2] H. Boujjat et al. "Experimental and numerical study of a directly irradiated hybrid solar/combustion spouted bed reactor for continuous steam gasification of biomass". In: Energy 189 (Dec. 2019).
[3] A. Curcio et al. "Experimental assessment of woody biomass gasification in a hybridized solar powered reactor featuring direct and indirect heating modes". In: International Journal of Hydrogen Energy 46.75 (Oct. 2021).

Solar reactor modeling



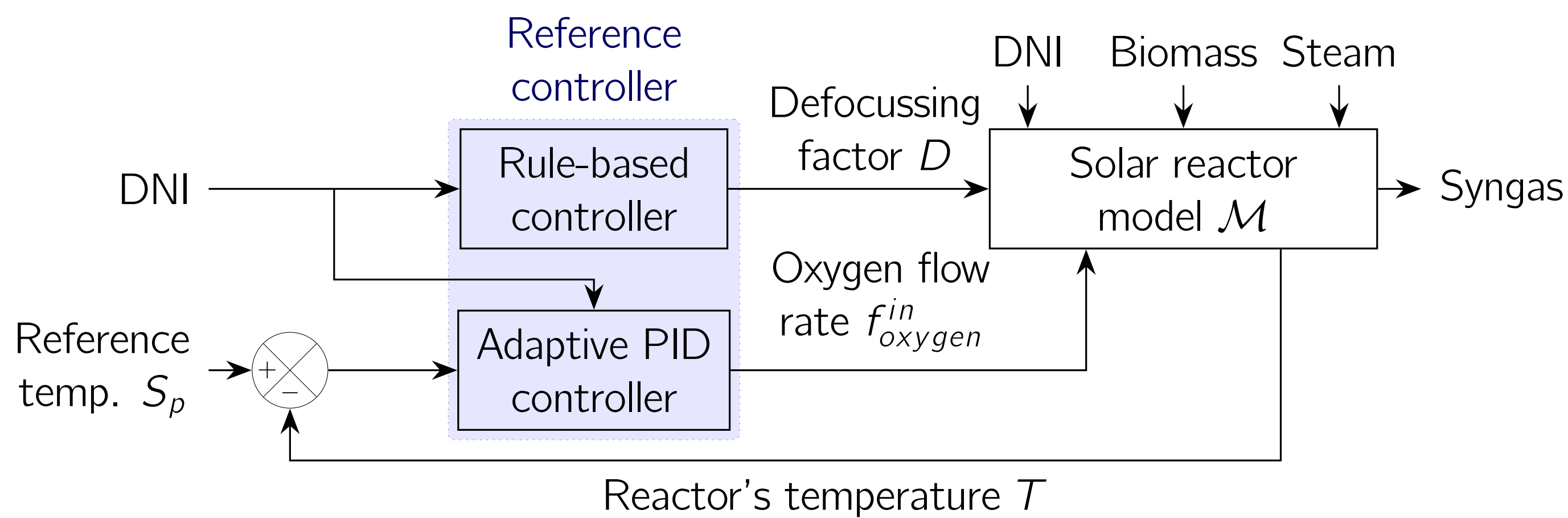
The model also includes the thermal balance of the reactor walls, and a thermodynamic calculation using the open-source library Cantera [4].

[4] D. G. Goodwin et al. "Cantera: An object-oriented software toolkit for chemical kinetics, thermodynamics, and transport processes". <https://www.cantera.org> (2022).

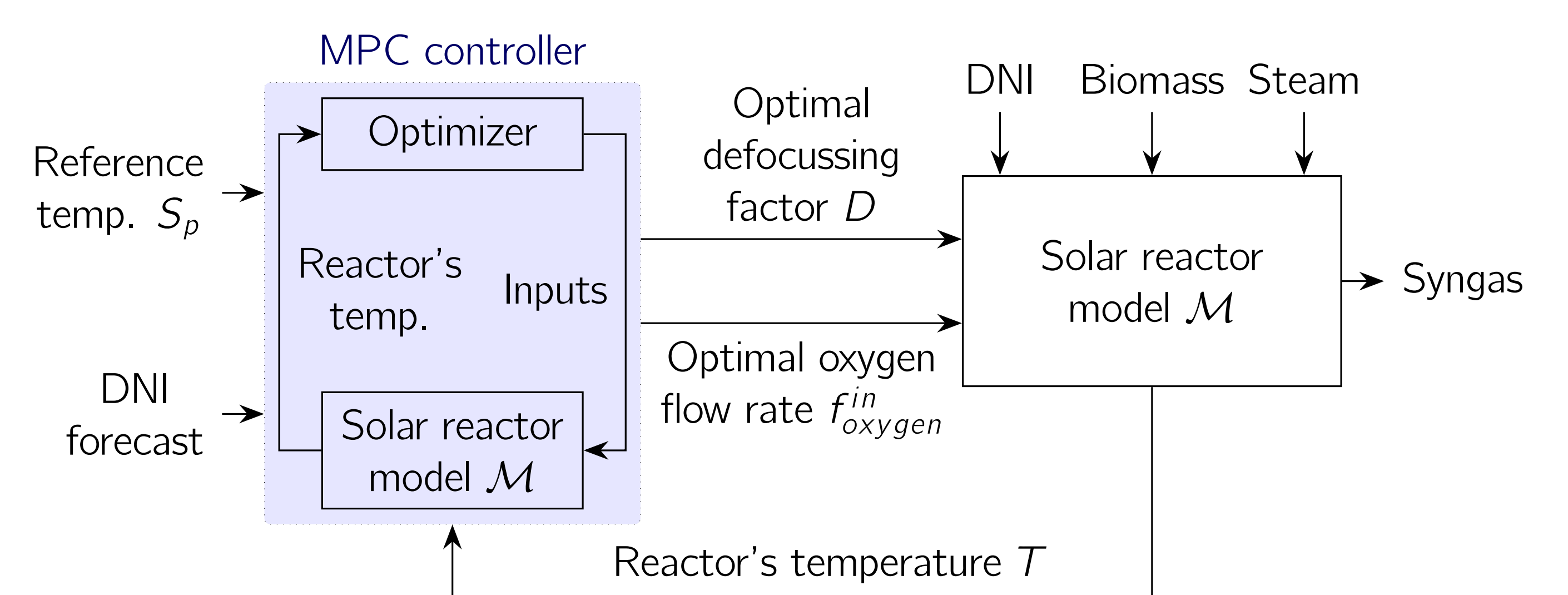
Reference controller

- ▶ Oxygen flow rate is controlled by an adaptive proportional integral derivative (PID) controller with optimized gains.
- ▶ Defocussing factor is controlled by a rule-based controller as follows:

$$D(t) = \begin{cases} 1, & \text{if } \text{DNI}(t) \leq 800 \text{ W m}^{-2} \text{ and } T(t) < 1473 \text{ K} \\ \frac{800}{\text{DNI}(t)}, & \text{if } \text{DNI}(t) > 800 \text{ W m}^{-2} \text{ and } T(t) > 1473 \text{ K} \end{cases}$$



Model-based predictive controller



- ▶ MPC strategy 1: maintain the reactor's temperature at any cost.

$$\begin{aligned} &\text{minimize}_{D, f_{oxygen}^{in}} \sum_{k=1}^n (T(t+k) - S_p)^2 \\ &\text{where } T(t+1) = \mathcal{M}(D(t), f_{oxygen}^{in}(t), T(t)) \\ &\text{subject to } 0 \leq D(t+k) \leq 1 \text{ and } 0 \leq f_{oxygen}^{in}(t+k) \leq 2 \end{aligned}$$

- ▶ MPC strategy 2: maintain the reactor's temperature, while minimizing O₂ consumption and maximizing solar energy use.

$$\begin{aligned} &\text{minimize}_{D, f_{oxygen}^{in}} \sum_{k=1}^n (\alpha(T(t+k) - S_p)^2 + \beta f_{oxygen}^{in}(t+k)^2 - \gamma D(t+k)^2) \\ &\text{where } T(t+1) = \mathcal{M}(T(t), D(t), f_{oxygen}^{in}(t)) \\ &\text{subject to } 0 \leq D(t+k) \leq 1 \text{ and } 0 \leq f_{oxygen}^{in}(t+k) \leq 2 \end{aligned}$$

- ▶ DNI forecasts: perfect forecasts, smart persistence forecasts, and proposed image-based forecasts.

Simulation results over one week and case studies

Strategies	Performance metrics	Perfect forecasts	Image-based forecasts	Smart persistence forecasts
MPC strategy 1	RMSE [K]	$\ll 0.01$	1.34	1.45
	O ₂ cons. [kg]	41 920.00	36 365.80	38 509.00
	ATV [K]	$\ll 0.01$	1.32	1.32
MPC strategy 2	RMSE [K]	0.07	1.60	1.71
	O ₂ cons. [kg]	31 968.33	32 091.00	32 089.23
	ATV [K]	0.03	1.54	1.54
Reference strategy	RMSE [K]		4.88	
	O ₂ cons. [kg]		31 933.00	
	ATV [K]		2.27	

- ▶ Performance metrics: root mean squared error (RMSE), O₂ consumption, and average temperature variation (ATV).
- ▶ The MPC controller, with all forecast models, outperforms the reference controller at the cost of an O₂ consumption increase.
- ▶ Integration of image-based forecasts results in better performance for both strategies.
- ▶ MPC strategy 1 is recommended if low RMSE and ATV values are required, while MPC strategy 2 is preferable if O₂ consumption should be minimized.

